

**SIMULATION OF LITHIUM-ION CONCENTRATION PROFILES  
IN SEPARATOR AND CATHODE OF LITHIUM-ION BATTERY  
USING THETA FORMULATION UNDER FINITE DIFFERENCE  
METHOD**

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*Md Jauharul Haqaiq Bin Harun*

## ABSTRACT

This research focuses on the material balance equation governing the lithium-ion concentration in an electrolyte/solution phase of a lithium-ion battery. The main objective of this research is to obtain the solution for this governing equation in order to simulate the concentration profile of a lithium-ion battery during discharge process. The second objective of this research is to study the behavior of these lithium-ion concentrations in the electrolyte/solution phase of a lithium-ion battery under various conditions. In order to achieve the second objective of this study, various simulations of lithium-ion concentrations in the electrolyte/solution phase of a lithium-ion battery were performed. Several difference parameter values of discharge current ( $I$ ), electrode porosity ( $\varepsilon$ ), discharge time ( $\tau$ ) and combination of separator/cathode thicknesses ( $L_s/L_c$ ) were used to simulate the behavior of lithium-ion in the battery system.

The material balance equation governing the lithium-ion concentration in the electrolyte/solution phase of a lithium-ion battery for separator is defined as

$$\frac{\partial(c)}{\partial t} = \nabla \cdot (D\nabla c) - \frac{i_2 \cdot \nabla t_+^0}{z_+ v_+ F}$$

and for cathode is defined as

$$\varepsilon \frac{\partial(c)}{\partial t} = \nabla \cdot (\varepsilon D_{eff} \nabla c) - \frac{i_2 \cdot \nabla t_+^0}{z_+ v_+ F} + \frac{aj_n (1 - t_+^0)}{v_+}$$

These equations are solved using the Theta formulation from Finite Difference Method (FDM) based on the relevant initial and boundary conditions. Three schemes are considered from this Theta formulation, which are explicit scheme ( $\alpha = 0$ ), implicit scheme ( $\alpha = 1$ ) and Crank Nicolson scheme ( $\alpha = 0.5$ ). The coding for all three schemes are done using Wolfram MATHEMATICA 8 software and were solved.

The significant *t*-test is used to prove that the profiles of lithium-ion concentration calculated from this work are in good agreement with the published analytical results within 95% confidence interval. The Root Mean Square Error (RMSE) and Mean Absolute Error (MAE) are used to evaluate the effectiveness and accuracy of the profiles of lithium-ion concentration calculated from this work compared to the published work. Computational time needed by Wolfram Mathematica 8 software to solve the equation is also recorded to identify the fastest scheme based on the same style of computer coding from Theta formulation.

## ABSTRAK

Kajian ini memberi tumpuan pada persamaan imbangan bahan yang mempengaruhi kepekatan ion litium di dalam elektrolit/fasa larutan bateri ion litium. Tujuan utama dari kajian ini adalah untuk mendapatkan penyelesaian bagi persamaan imbangan bahan ini bagi membolehkan dilakukan simulasi profil kepekatan bateri litium-ion semasa proses nyahcas. Tujuan kedua dari kajian ini adalah untuk mempelajari perilaku kepekatan ion litium dalam elektrolit/fasa larutan bateri litium-ion di bawah pelbagai keadaan. Bagi mencapai tujuan kedua kajian ini, pelbagai simulasi kepekatan ion litium dalam elektrolit/fasa larutan bateri litium-ion telah dijalankan. Beberapa nilai parameter yang berbeza seperti arus nyahcas ( $I$ ), keporosan elektrod ( $\varepsilon$ ), masa nyahcas ( $\tau$ ) dan kombinasi ketebalan pemisah/katod ( $L_s/L_c$ ) telah digunakan untuk mensimulasi perilaku ion litium di dalam sistem bateri.

Persamaan imbangan bahan yang mempengaruhi kepekatan ion litium di dalam fasa elektrolit/larutan bateri litium-ion untuk pemisah ditakrifkan sebagai

$$\frac{\partial(c)}{\partial t} = \nabla \cdot (D\nabla c) - \frac{i_2 \cdot \nabla t_+^0}{z_+ v_+ F}$$

dan untuk katod sebagai

$$\varepsilon \frac{\partial(c)}{\partial t} = \nabla \cdot (\varepsilon D_{eff} \nabla c) - \frac{i_2 \cdot \nabla t_+^0}{z_+ v_+ F} + \frac{aj_n (1 - t_+^0)}{v_+}$$

Persamaanimbangan bahan ini diselesaikan dengan formulasi Theta dari Kaedah Beza Terhingga berdasarkan nilai awal dan nilai sempadan yang relevan. Tiga skim dipertimbangkan dalam formulasi Theta iaitu skim eksplisit ( $\alpha = 0$ ), skim implisit ( $\alpha = 1$ ) dan skim Crank Nicolson ( $\alpha = 0.5$ ). Pengaturcaraan komputer untuk ketiga-tiga skim ini dibuat menggunakan perisian Wolfram MATHEMATICA 8 dan diselesaikan.

Ujian signifikan-t digunakan untuk membuktikan bahawa profil kepekatan ion litium yang dikira dari kajian ini adalah menepati keputusan analitik yang pernah diterbitkan bagi 95% julat kesahihan. Ralat Bagi Punca Kuasa Dua Min dan Ralat Mutlak Min digunakan untuk menilai keberkesanan dan ketepatan profil kepekatan ion litium yang didapati dari kajian ini dibandingkan dengan hasil kerja analitik yang pernah diterbitkan. Masa pengkomputeran yang diperlukan oleh perisian Wolfram Mathematica 8 untuk menyelesaikan persamaanimbangan bahan ini juga direkodkan untuk mengenalpasti skim penyelesaian terpantas berdasarkan gaya pengaturcaraan yang sama dari formulasi Theta.

## TABLE OF CONTENTS

	<b>pages</b>
<b>Declaration</b>	<b>ii</b>
<b>Acknowledgement</b>	<b>iii</b>
<b>Abstract</b>	<b>iv</b>
<b>Abstrak</b>	<b>vi</b>
<b>Table of Contents</b>	<b>viii</b>
<b>List of Paper Published &amp; Presented</b>	<b>x</b>
<b>List of Symbols</b>	<b>xi</b>
<b>List of Tables</b>	<b>xiii</b>
<b>List of Figures</b>	<b>xv</b>
<b>CHAPTER 1        INTRODUCTION</b>	<b>1</b>
1.1    Research Background	1
1.2    Objective	6
1.3    Thesis Organization	7
<b>CHAPTER 2        LITERATURE REVIEW</b>	<b>9</b>



<b>CHAPTER 3</b>	<b>MODEL DEVELOPMENT</b>	<b>50</b>
3.1	Mathematical Modeling	50
3.2	Governing Equations	54
<b>CHAPTER 4</b>	<b>METHODOLOGY</b>	<b>75</b>
4.1	Analytical and Numerical	75
4.2	Finite Difference Method (FDM)	78
4.3	Wolfram Mathematica 8 Software	87
4.4	Wolfram Mathematica 8 Software Algorithm	96
<b>CHAPTER 5</b>	<b>RESULTS AND DISCUSSION</b>	<b>106</b>
5.1	Concentration Profiles	106
5.2	Effectiveness and Accuracy	114
5.3	Simulation of Lithium-ion Cell	127
<b>CHAPTER 6</b>	<b>CONCLUSIONS</b>	<b>147</b>
6.1	Conclusion	147
6.2	Future Work	150
<b>References</b>		<b>151</b>

## LIST OF PAPERS

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**LIST OF SYMBOLS**

$a$	specific interfacial area ( $\text{cm}^{-1}$ )
$c_i$	concentration of species $i$ ( $\text{mol}/\text{dm}^3$ )
$c_T$	total concentration
$D$	diffusion coefficient ( $\text{cm}^2/\text{s}$ )
$f_{+-}$	mean molar activity coefficient of the electrolyte
$F$	Faraday's constant (96487 C/cq)
$I$	superficial current density ( $\text{mA}/\text{cm}^2$ )
$j_n$	pore wall flux of lithium-ion across interface ( $\text{mol}/\text{m}^2/\text{s}$ )
$K_{ij}$	friction coefficients (or interaction coefficients)
$m$	molality
$n$	number of electrons transferred in electrode reaction
$N_i$	diffusive flux of species $i$ ( $\text{mol}/\text{cm}^2/\text{s}$ )
$R$	universal gas constant (8.3143 J/mol/K)
$t$	time (seconds)
$t_+^0$	transference number of lithium-ion
$T$	temperature (K)
$v_i$	<i>velocity of species <math>i</math></i>
$x$	distance along x-axis ( $\mu\text{m}$ )
$y$	dimensionless distance
$z_i$	ionic valence of the charged species $i$ .

**Greek letters**

$\varepsilon$	porosity
$\delta$	thickness
$\wp$	diffusion coefficient of the electrolyte based on a thermodynamic driving force
$\vartheta$	dimensionless concentration
$\tau$	dimensionless time
$\mu_i$	electrochemical potential of species $i$
$\gamma_{+-}$	mean molal activity coefficient

**Subscripts/Superscripts**

A	anode
C	cathode
S	separator
0	initial condition
2	electrolyte/solution phase

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## LIST OF TABLES

Table 1.1: History of Battery Development.....	2
Table 1.2: Comparison among three common commercialize batteries.....	5
Table 2.1: Comparison between several materials of cathode.....	12
Table 2.2: Partial list of macroscopic full-cell sandwich battery models, with year of publication.....	13
Table 2.3: Comparison of lithium-ion technologies being developed by various companies.....	14
Table 3.1: Summary of model equations in dimensionless form.....	74
Table 4.1: Comparison of mathematical programs for data analysis in aspect of (a) installation, learnability and usability, (b) mathematical functionality, (c) graphical functionality, (d) data handling, (e) Available operating systems, (f) speed comparison, (g) Functionality of the programming environment and (h) overall result.....	88-94
Table 5.1: Parameters and values used by (Doyle and Newman 1997).....	106
Table 5.2: $p$ value from t-test (significant test) compared to Doyle & Newman (1997) for 5 minutes of discharge with 0.5, 1.0 and 1.39 mA/cm <sup>2</sup> discharge current for three techniques in Theta formulation.....	115
Table 5.3: RMSE compared to Doyle & Newman (1997) for 5 minutes of discharge with 0.5, 1.0 and 1.39 mA/cm <sup>2</sup> discharge current for three techniques in Theta formulation.....	118

Table 5.4: MAE compared to Doyle & Newman (1997) for 5 minutes of discharge with 0.5, 1.0 and 1.39 mA/cm<sup>2</sup> discharge current for three techniques in Theta formulation.....121

Table 5.5: Computational time needed by Wolfram Mathematica 8 to perform the result of concentration profile during 5 minutes of discharge with 0.5, 1.0 and 1.39 mA/cm<sup>2</sup> discharge current for three techniques in Theta formulation.....124

Table 5.6: Parameters and values for Li//LiMn<sub>2</sub>O<sub>4</sub> as reported by various worker.....127

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## LIST OF FIGURES

Figure 1.1: Four variations of Volta's electric battery.....	3
Figure 1.2: Example of lithium-ion battery that was used in some devices nowadays.....	5
Figure 2.1: Example of the structure of Lithium-ion Battery.....	9
Figure 2.2: The mechanism of (a) discharging and (b) charging process. ( <a href="http://electronics.howstuffworks.com/lithium-ion-battery1.htm">http://electronics.howstuffworks.com/lithium-ion-battery1.htm</a> ).....	10
Figure 2.3: Concentration Profile at (a) long time and (b) short time: $I = 10 A/m^2$ discharge. Dashed line divides the separator and composite cathode. Initial concentration is $1000 mol/m^3$ . (Doyle et al. 1993).....	17
Figure 2.4: Concentration profiles across the cell during galvanostatic discharge at $I = 4 mA/cm^2$ . Carbon negative electrode is 21.5% thicker than the manganese dioxide positive electrode. The separator region is set off by the dashed lines. (Fuller et al. 1994).....	18
Figure 2.5: Salt concentration profiles across (a) cell 1 during galvanostatic discharge at $I = 1.75 mA/cm^2$ , (b) cell 2 during galvanostatic discharge at $I = 10.416 mA/cm^2$ and (c) cell 2 during galvanostatic discharge at $I = 6.25 mA/cm^2$ The separator region is set off by dashed lines. Time since the beginning of discharge is given in minutes. (Doyle and Newman 1996).....	20
Figure 2.6: Simulated salt concentration profiles across the thin cell during galvanostatic discharge at the (a) $C/6$ rate ( $0.387 mA/cm^2$ ) and (b) $3C$ rate ( $6.936 mA/cm^2$ ). The separator region is set off by dashed lines. Times since the beginning of discharge are given in minutes. (Arora et al. 2000).....	24
Figure 2.7: (a) and (b) Comparison dimensionless transient profile in a time in a lithium-ion cell sandwich with previous Doyle and Newman work. (c) Concentration profiles in a lithium-ion cell sandwich as a function on applied current $J$ at particular time $\tau = I$ . (Subramanian and White 2001).....	25

---

Figure 2.8: Electrolyte concentration profile for a galvanostatic theoretical discharge rate of 2C at short ( $t=15s$ ) and long times ( $t =390s$ ). (Botte and White 2001).....	26
Figure 2.9: Dimensionless concentration at the (a) electrode/separator interface, (b) current collector for different (b) rate of discharge and (c) values of $r$ (ratio of electrode length to separator length) is plotted against dimensionless time at the $IC$ rate of discharge ( $60 A/m^2$ ). The solid lines represent the exact model and the dotted lines represent the approximate solution. (Subramanian et al. 2004).....	29
Figure 2.10: $LiPF_6$ concentration profile across the electrode after 2.0 Ah had been discharged from the cells. (Valøena and Reimers 2005).....	31
Figure 2.11: (a) Classified about micro-scale and macro-scale diffusion model and (b) Electrolyte concentration inside the cell sandwich predicted using an approximate model for the solid phase concentration is compared with electrolyte concentration obtained using 20 nodes in the particles. Solid line represents the node model (rigorous solution) and solid dots represent the approximate model. (Subramanian et al. 2005).....	32
Figure 2.12: Change in the solution phase concentration at various rates of discharge as predicted by the PP model. (Santhanagopalan et al. 2006).....	33
Figure 2.13: Simulations of lithium concentration in the electrolyte phase. (Ning et al. 2006).....	35
Figure 2.14: Concentration profile in solid-phase across the cathode for (a) short-time interval and (b) long-time interval during galvanostatic discharge $I=1.39 mA/cm^2$ . (Hashim Ali et al. 2002).....	36
Figure 2.15: Concentration profile in solution phase across the cathode for (a) short-time interval during galvanostatic discharge ( $I=1.0 mA/cm^2$ and $I=1.39 mA/cm^2$ ), (b) long-time interval during galvanostatic discharge ( $I=1.39 mA/cm^2$ ) and (c) various discharge current rate, $I$ . (Hashim Ali et al. 2002).....	37

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Figure 2.16: Profiles of lithium ion concentration for various (a) times ( $t = 0, 300, 600, 900, 1500$ and $14400$ seconds) with the initial concentration $1000 \text{ mol/m}^3$ and (b) discharge current ( $I = 0.5, 1.0, 1.39$ and $1.92 \text{ mA/cm}^2$ ). (Hashim Ali et al. 2003).....	38
Figure 2.17: Profile of lithium-ion concentration in (a) solution phase and (b) solid phase under various time, $t$ . (Hashim Ali et al. 2004).....	39
Figure 2.18: Concentration profile across (a) separator and cathode during galvanostatic discharge at $60 \text{ min}$ for $I = 0.5, 1.0, 1.39$ and $1.92 \text{ mA/cm}^2$ , (b) separator and cathode during galvanostatic discharge at $240 \text{ min}$ for $I = 0.5, 1.0, 1.39$ and $1.92 \text{ mA/cm}^2$ and (b) cathode during galvanostatic discharge of $I = 1.92 \text{ mA/cm}^2$ for time $t=5, 15, 20$ and $60 \text{ minutes}$ . (Ali and Mohamed 2006).....	40
Figure 2.19: Concentration profiles in solution phase across cathode (a) compared with previous published results and (b) during galvanostatic discharge at a particular time ( $\tau = 1$ ). (Johan and Arof 2007).....	41
Figure 2.20: Flowchart of Subramanian et al. work regarding to their model simplification (Subramanian et al. 2007).....	42
Figure 2.21: Comparison of the predictive capability of the simplified model solution by Subramanian et al. for predicting the electrolyte concentration with rigorous numerical solution. (Subramanian et al. 2007).....	43
Figure 2.22: (a) Electrolyte concentration distributions during $5 \text{ C}$ discharge from $50\%$ SOC initial condition: CFD model (o) and 5th order negative electrode/5th order positive electrode/3rd order electrolyte linear submodels (–) and (b) Distribution of electrolyte surface concentration at various times during $30 \text{ C}$ discharge from $100\%$ SOC initial condition with sluggish electrolyte diffusion, $D_e = 2.6 \times 10^{-7} \text{ cm}^2/\text{s}$ . (Smith et al. 2007).....	44
Figure 2.23: Interdependency of macro- and micro-scales. (Golmon et al. 2009).....	46
Figure 2.24: (a) Evolution of $\text{Li}^+$ concentration in electrolyte over time and (b) Normalized $\text{Li}$ concentration in cathode for different porosities at average utilization of the cathode material of $0.35$ . (Golmon et al. 2009).....	46

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Figure 2.25: Evolution of $\text{Li}^+$ concentration in electrolyte for $t \leq 20\text{ s}$ ; left: results of (Doyle et al. 1993) right: results predicted by numerical framework presented in their paper (Golmon et al. 2009).....	46
Figure 2.26: Lithium-ion concentration distribution in electrolyte. (Abe et al. 2009).....	47
Figure 2.27: Concentration profile of the lithium-ion across distance (a) at $t = 30\text{ minutes}$ with $I = 0.5, 1.0$ and $0.5\text{ mA/cm}^2$ and (b) with $t = 10, 30$ and $60\text{ minutes}$ for $I = 1.39\text{ mA/cm}^2$ . (Norzihani et al. 2010).....	48
Figure 3.1: Schematic diagram for (a) the “rocking-chair” type battery with an insertion-type cathode and (b) the lithium ion battery with a lithium foil as anode.....	53
Figure 4.1: Grid Lines commonly used in Finite Difference Method (FDM).....	81
Figure 4.2: WM8 notebook sheet.....	97
Figure 5.1: Concentration profile using three schemes of Theta Formulation under FDM compared with Doyle and Newman (1997) at different discharge currents. (a) explicit scheme, (b) implicit scheme, (c) Crank Nicolson scheme and (d) Doyle and Newman (1997) with three schemes together.....	107-108
Figure 5.2: Concentration profile using three schemes of Theta Formulation under FDM compared with Subramanian and White (2001) at applied current, $J = -1$ . (a) explicit scheme, (b) implicit scheme, (c) Crank Nicolson scheme and (d) Subramanian and White (2001) with three schemes together.....	111-112
Figure 5.3: Profile for lithium-ion concentration in the solution phase during $1.75\text{ mA/cm}^2$ discharge current at various values of dimensionless time, $\tau$ .....	128
Figure 5.4: Profile for lithium-ion concentration in the solution phase during $1.75\text{ mA/cm}^2$ discharge current at various values of dimensionless distance, $y$ .....	129

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Figure 5.5: Profile for lithium-ion concentration in the solution phase during 1.75 mA/cm <sup>2</sup> discharge current in 3D Simulation.....	130
Figure 5.6: Profile for lithium-ion concentration across the cathode for different discharge times at (a) 1.0 mA/cm <sup>2</sup> and (b) 1.39 mA/cm <sup>2</sup> discharge current.....	131
Figure 5.7: Profile for lithium-ion concentration across the cathode during (a) $\tau = 5$ and (b) $\tau = 30$ for different discharge current.....	133-134
Figure 5.8: Profile for lithium-ion concentration across the cathode at different distance, $r$ using (a) 1.0 mA/cm <sup>2</sup> and (b) 1.93 mA/cm <sup>2</sup> discharge current.....	135-136
Figure 5.9: Profile for lithium-ion concentration across the cathode at certain discharge current for different discharge times with electrode porosity (a) $\varepsilon = 0.8$ and (b) $\varepsilon = 0.2$ .....	138
Figure 5.10: Profile for lithium-ion concentration across the cathode during certain discharge time for different discharge current with electrode porosity (a) $\varepsilon = 0.8$ and (b) $\varepsilon = 0.2$ .....	140-141
Figure 5.11: Profile for lithium-ion concentration across the cathode for different distance, $r$ using electrode porosity (a) $\varepsilon = 0.8$ and (b) $\varepsilon = 0.2$ at certain discharge current.....	143
Figure 5.12: Profile for lithium-ion concentration for 5 different thicknesses combination of separator and cathode. The thicknesses of separator and cathode are measured in $\mu\text{m}$ during certain discharge current and time.....	145