

**STUDY ON THERMOPHYSICAL PROPERTIES OF FLUIDS
CONTAINING CARBON NANOTUBES**

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ABSTRAK

Di kala permintaan yang akut terhadap tenaga, cecair pemindah haba adalah diperlukan untuk mengubahsuai dan membangunkan cecair berprestasi tinggi dikenali sebagai cacair-nano. Ciri-ciri cecair ini masih lagi belum di perolehi sepenuhnya. Karbon nanotub(CNT) didapati mampu untuk meningkatkan dayaupaya termal bagi cecair pemindah haba konvensional. Walaupun begitu kebanyakan penyelidikan terdahulu telah memfokuskan kesan konsentrasi bahan ini terhadap ciri-ciri termal-fizikal cecair-nano. Tiada penyelidikan yang mendalam dilakukan untuk menentukan secara terus kesan keadaah penyediaan terhadap kestabilan, konduktiviti termal dan kelikatan CNT terampai. Ciri –ciri termal cacair mengandungi CNT berbeza bergantung kepada teknik penyediaan yang berbeza dan pengukuran jitu telah dilakukan pada eksperimen ini untuk menentukan kesan keadaah-kaedah ini. Kesan variasi masa ultrasonikasi dan surfaktan yang berlainan terhadap ciri-ciri termal-fizikal multi dinding karbon nanotub (MWCNTs) telah dikaji. Ciri-ciri termal-fizikal yang diukur adalah konduktiviti termal dan kelikatan pada suhu yang berlainan. Gam Arabic (GA), Sodium dodecylbenzene sulfonate (SDBS) and Sodium dodecyl sulfate (SDS) telah digunakan sebagai surfaktan. Penggunaan GA menunjukkan konduktiviti termal yang lebih tinggi berbanding SDBS and SDS. Sampel yang mengandungi 0.5 wt% MWCNT, 0.25% GA mengikut peratusan berat dan air tersuling sebagai cacair asas telah di sediakan pada masa ultrasonikasi yang berbeza dalam kajian ini. Pengimejan telah dilakukan menggunakan teknik TEM untuk melihat ciri-ciri penyebaran sampel dan melihat pengurangan penggumpalan CNT serta panjang. Pengurangan penggumpalan didapati lebih penting dari panjang. Hasil kajian menunjukkan ultrasonikasi memberi kesan terhadap konduktiviti termal, kelikatan dan penyebaran. Peningkatan maksimum konduktiviti termal adalah sebanyak 22.31% (nisbah sebanyak 1.22) pada suhu 45 darjah celsius bagi sampel yang mengalami sonikasi selama 200minit. Konduktiviti

termal meningkat dengan peningkatan suhu dan masa sonikasi. Pertimbangan terhadap kelikatan mendapati cacair-nano diklasifikasikan sebagai penipisan ricih dan cacair bukan Newtonian. Kelikatan meningkat kepada maksimum untuk sampel yang mengalami sonikasi selama 50minit dan kemudiannya berkurangan dengan pertambahan masa sonikasi. Oleh yang demikian kelikatan yang terendah dan konduktiviti termal yang tertinggi dicapai dengan memanjangkan tempoh sonikasi dimana ianya amat berguna untuk aplikasi pemindahan haba.

ABSTRACT

In the verge of acute energy demand the heat transfer fluids were required to modify and develop a high performance liquid as nanofluid. The properties of the fluids are not yet fully obtained. The carbon nanotubes (CNT`s) are able to enhance the thermal performance of the conventional heat transfer liquids, nonetheless the majority of past works have been focused on the impacts of concentrations of carbon nanotubes on the thermo-physical properties of the nanofluids. No considerable researches have been performed to straightly indicate the influence of preparation methods on stability, thermal conductivity and viscosity of carbon nanotubes suspensions. The thermo-physical properties of CNT` nanofluids differ under different preparation techniques and the precise measurements were performed in this current experiment to figure out the impacts of these methods. The effect of variation of ultrasonication time and different surfactants on the thermal properties of Multi-walled carbon nanotubes(MWCNT`s) were studied. The thermo-physical properties measured were thermal conductivity and viscosity under different temperatures. Gum Arabic (GA), Sodium dodecylbenzenesulfonate (SDBS) and Sodium dodecyl sulfate (SDS) were used as surfactants. Addition of GA showed superior thermal conductivity of nanofluids than that of SDBS and SDS dispersants in it. Samples of 0.5 wt% MWCNT, 0.25% GA and distilled water as the base liquid were prepared at different ultrasonication times in this study. Imaging was carried out by TEM technique to view the dispersing characteristics of samples and observed both the reduction of CNT agglomerations and length. The reduction in agglomerations was found to be more important than that of CNT length. The results exhibited that the ultrasonication affects thermal conductivity, viscosity and dispersion. The maximum thermal conductivity enhancement was found to be 22.31% (the ratio of 1.22) at 45 °C temperature of the sample sonication bath for 200 minutes. The thermal conductivity enhanced with the increase of both temperature and sonication time.

In the consideration of viscosity, the nanofluids treated as shear thinning and non-Newtonian fluids. The viscosity was raised to the maximum for the sample sonication of 50 minutes and the subsequently decreased with the further increase of sonication time. Thus the lowest viscosity and the highest thermal conductivity ratios were achieved by utilizing prolonged sonication time, which could be useful in heat transfer applications.

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LIST OF ABBREVIATIONS

ANL	Argon National Lab
ASHRAE	American Society of Heating, Refrigerating and Air- Conditioning
BET	Brunauer Emmett Teller
CNT	Carbon Nano-tube
Co.	Company
Conc.	Concentration
CTAB	Cetyltrimethylammoniumbromide
DI	Deionised
GA	Gum Arabic
EG	Ethylene Glycol
JCPDS	Joint Committee on Powder Diffraction Standard
H-C	Hamilton-Crosser
HVAC	Heating, Ventilation and Air conditioning
MWCNT	Multi-walled Carbon Nano-tube
PG	Propylene Glycol
SWCNT	Single-walled carbon nanotube
SDS	Sodium dodecyl sulfate
SDBS	Sodium dodecyl benzene sulfonate
TEM	Transmission electron microscopy
THW	Transient Hot Wire
UDD	Ultra Dispersed Diaamond
VOL.	Volume
XRD	X-ray Diffraction
ZP	Zeta Potential

CHAPTER ONE: INTRODUCTION

1.1 Background

Due to rapid growth in power consumption, also rapid development in all sectors, such as Industrial, Infrastructure, Transportation, Defense, Space, etc, call for saving energy is a daily campaign; in addition, managing high thermal loads has become critical. For these reasons, energy efficiency should be enhanced in heating and cooling systems for all of the sectors mentioned above, at which the conventional technique of heat transfer employed by means of a flow system, including fluids, such as: water, ethylene glycol and mineral oils, are used as the heat transfer fluid. A fluid used to cool or heat a system, or to transfer heat from one part to another call heat transfer fluid.

In spite of the low heat transfer properties of such fluids which obstruct the performance of the heat transfer equipments they had always been desired and would always remain in demand, because of their simple characteristics.

The systems working by Conventional heat transfer fluids, used in applications same as power generation, refining and petrochemical, are very large and include considerable amount of heat transfer fluids, however in specific usages like electronics, cooling in laptops and microprocessors, cooling in space applications and many other areas, the small heat transfer systems are needed, these applications have a critical relationship between the mechanical system size, and the cost related to operation and manufacturing. If developments may be done in the existing systems of heat transfer such as increasing the heat transfer fluid performance, smaller heat exchanger and hence, a lesser space would be required to handle a specified amount of cooling load, the situation would lead to smaller

heat transfer systems with lower capital costs and higher energy efficiencies [3] .Micro-channel heat exchanger could be developed in HVAC and automotive industries with the space saving and lighter weight features. These advantages could also come out as an attractive approach to companies in saving more material.

Low heat transfer performance reduced the efficiency of lower thermal conductivity of the base liquids (i.e. water, ethylene glycol and oil). In this pursuit numerous researchers have been investigating better methods to increase the thermal conductivity of heat transfer liquids. For the first time, long ago the basic concept of dispersing solid particles in fluid (millimeter or micrometer sized) to enhance the thermal conductivity was introduced by James clerk Maxwell (W Yu & Choi, 2003)

In over the years the incorporation into base liquid high thermal conductive particulate solid such as metals and metal oxide had been used for enhancement (Ahuja, 1975a, 1975b; Hetsroni & Rozenblit, 1994; Lee, Choi, Li, & Eastman, 1999; Sohn & Chen, 1981; Xuan & Li, 2000)

Because solid particles have a higher thermal conductivity compared to conventional heat transfer based liquid for example at room temperature, copper has 700 and 3000 times greater thermal conductivity than that of water and engine oil respectively as shown in Figure 1.1(S. Choi, Zhang, & Koblinski, 2004; Komarneni, Parker, & Wollenberger, 1997)

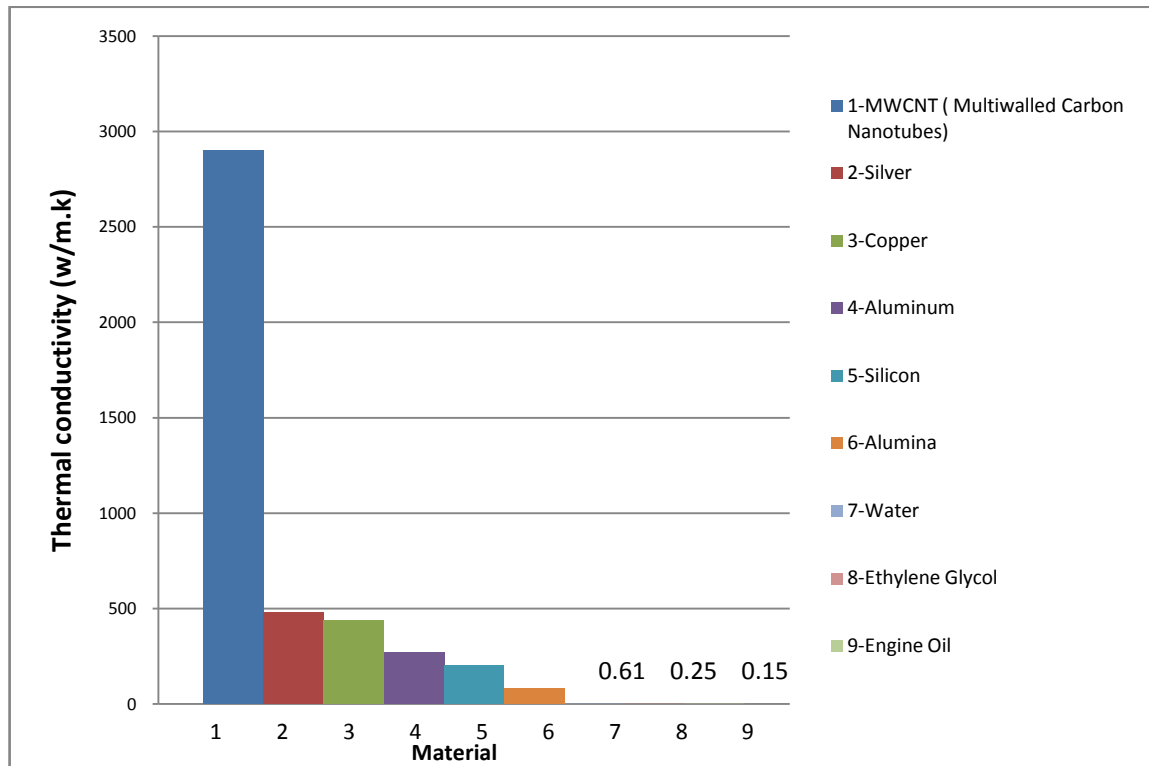


Figure 1.1 Thermal conductivity of some materials(solids and liquids) at 300 K

Metallic solid particles have higher thermal conductivity than non-metallic particles except some substance like Carbon Nanotubes(CNT) and diamond(Marquis & Chibante, 2005).

Despite the improved thermal conductivity by dispersing solid particles (mm or μm sized) in based fluids, it couldn't be used in practical application because of problems such as sedimentation, erosion, fouling and increased pressure drop of the flow channel and also channel clogging which caused by poor suspension stability particularly in the case of mini and micro channels(Ding, Alias, Wen, & Williams, 2006; Trisaksri & Wongwises, 2007; Wang & Wei, 2009)

Over the last several decades, scientists and engineers have attempted to develop fluids, which offer better cooling or heating performance for a variety of thermal systems compared to conventional heat transfer fluids.

Until for the first time Choi at the Argonne National Laboratory employed the particles of nanometer dimension (nanoparticle) suspended in solution as nanofluid and showed considerable increase in the nanofluid thermal conductivity (S. U. Choi & Eastman, 1995).

This new class of heat transfer fluids (nanofluids) is engineered by dispersing nanometer sized (one billionth of a meter) solid particles, rods or tubes (nanotube) in traditional heat transfer fluids. From the investigations in the past decade, nanofluids were found to exhibit significantly higher thermal properties, in particular, thermal conductivity and convective heat transfer than those of base fluids, Liu et al. (M. S. Liu, Lin, Huang, & Wang, 2006), Eastman et al. (Eastman, Choi, Li, Thompson, & Lee, 1997), Yu et al. (Wei Yu, Xie, Chen, & Li, 2009), and Mintsu et al. (Mintsu, Roy, Nguyen, & Doucet, 2009), Hwang et al. (Hwang, Park, Lee, & Jung, 2006), Eastman et al. (Eastman, Choi, Li, Yu, & Thompson, 2001), Xuan, Y. and Q. Li (Xuan & Li, 2000), Putranandi (Putra, Thiesen, & Roetzel, 2003), P. Garg et al. (Garg et al., 2009), Murshed (Murshed, Leong, & Yang, 2005), Hong et al. (Hong, Yang, & Choi, 2005) and, Li and Peterson (C. H. Li & Peterson, 2006), observed great enhancement of nanofluids' thermal conductivity. Enhancement of convective heat transfer was reported by Zeinali Heris et al. (Zeinali Heris, Nasr Esfahany, & Etemad, 2007), Kim et al. (D. Kim et al., 2009), Jung et al. (Jung, Oh, & Kwak, 2009) and Sharma et al. (Sharma, Sundar, & Sarma, 2009)

Thus, nanofluids have attracted great interest from the research community due to their potential benefits and applications in numerous important fields such as microelectronics, transportation, manufacturing, medical, and HVAC

The better stability of nanofluids will prevent rapid settling and reduce clogging in the walls of heat transfer devices. The high thermal conductivity of nanofluids translates into higher energy efficiency, better performance, and lower operating costs. They can reduce energy consumption for pumping heat transfer fluids. Miniaturized systems require smaller inventories of fluids where nanofluids can be used. Thermal systems can be smaller and lighter. In vehicles, smaller components result in better gasoline mileage, fuel savings, lower emissions, and a cleaner environment.

Dispersion of Nano-particles like metal (copper), metal oxide (alumina) and carbon component (Carbon Nanotubes) augment heat transfer of the fluid by transferring more energy, resulting to fuel, energy and money saving. For example dispersion of copper Nanoparticles and alternatively carbon Nanotubes provided the most promising result so far with observed thermal conductivity enhancement of 40% and 160% respectively in relation to the base fluid (Assael, Chen, Metaxa, & Wakeham, 2004; S. Choi, Zhang, Yu, Lockwood, & Grulke, 2001; Eastman et al., 2001)

Actually it is the goal of Nanofluids to achieve the highest thermal properties with lower concentration and good stability.

Thermal conductivity enhancement of nanofluids offers plenty of benefits and applications like higher heat transfer, decreased pumping power needs, smaller and lighter cooling systems, reduced inventory of heat transfer fluids, reduced friction coefficients and improved wear resistance, those kind of benefits prepared nanofluids for various application such as coolants, lubricants, hydraulic fluids and metal cutting fluids (Saidur, Leong, & Mohammad, 2011)

Compared with millimeter or micrometer sized particle suspensions, Nanofluids have higher stability due to the ultra small particle size, and can have dramatically higher thermal conductivities (Ding et al., 2006; M.-S. Liu, Ching-Cheng Lin, Huang, & Wang, 2005; Saidur et al., 2011)

Nanofluids do not carry too big a momentum as in case of micro fluids, which reduced erosion and wear in tube and channel, figure 1.2 compares the effect of micro particles and nanoparticles with the same volume concentration in a cooling system.

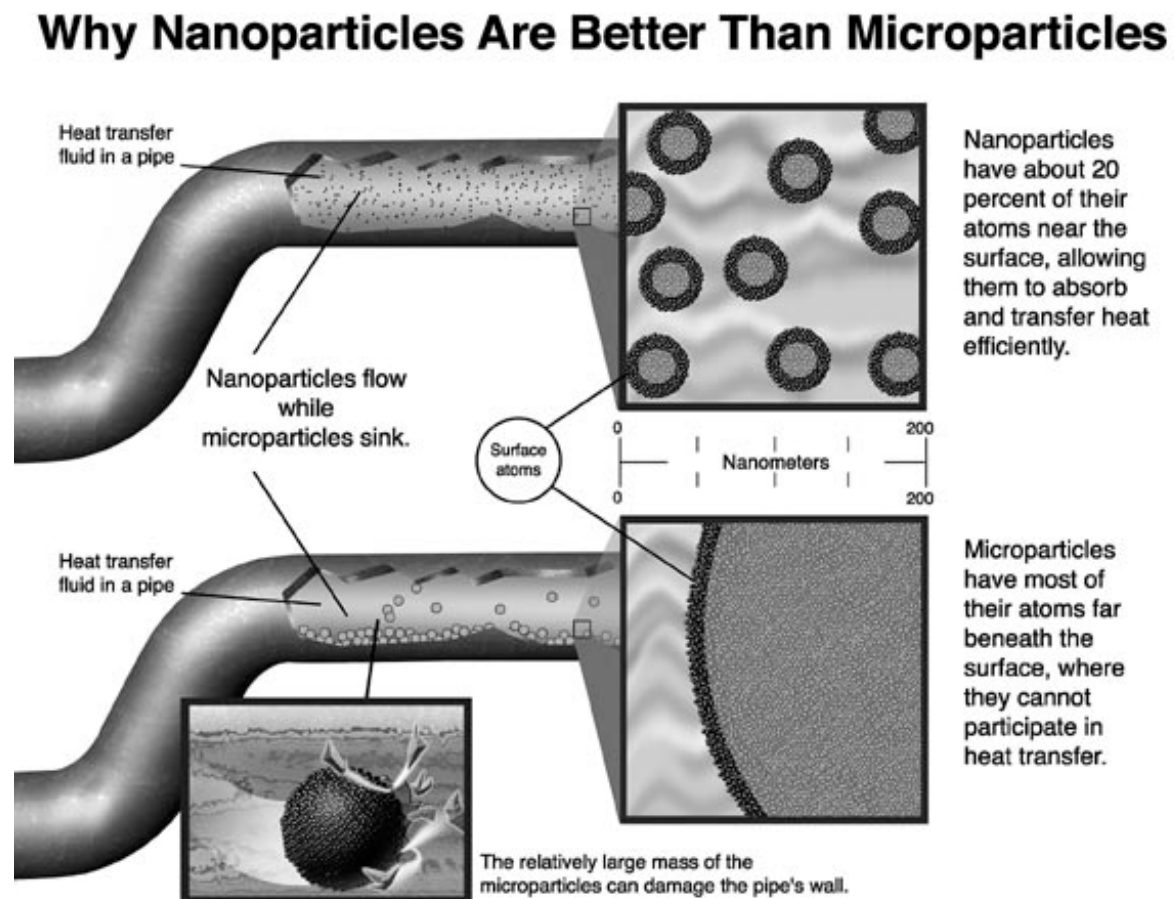


Figure 1-2 effects of micro particles and nanoparticles in a cooling system [34]

These liquid suspensions containing particles significantly smaller than 100 nm in at least one dimension (Ding et al., 2006)

Serrano et al.(Serrano, Rus, & Garcia-Martinez, 2009) provided an excellent example of nanometer in comparison with millimeter and micrometer to understand clearly as can be seen in Figure1-3 nano-sized particles could be either spherical or cylindrical. The metal and metal oxidenanoparticles are generally synthesized in spherical form, however, carbon nanoparticles could be synthesized both in spherical and cylindrical form. Of the two forms of carbonnanoparticles, the cylindrical form is more common and is called as (CNT) carbon nanotubes. A kind of these nanotubes is called multi-walled carbon nanotubes (MWCNT)which are more popular in heat transfer based applications.

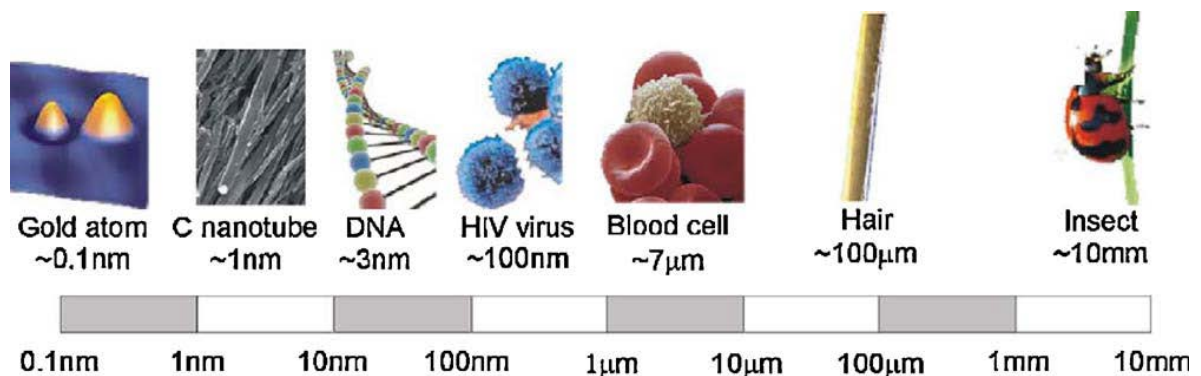


Figure1-3 Length scale and some examples related

The main focus of this work is concerned with the preparation of Nanofluids by dispersingMWCNTs in Distilled water (DW) and its use in heat transfer fluids. It has been proven, when CNT`s are dispersed in common heat transfer liquids, increase in thermal conductivity is observed (Assael et al., 2004; Assael, Metaxa, Arvanitidis, Christofilos, & Lioutas, 2005; S. Choi et al., 2001; Ding et al., 2006; Nasiri, Shariaty-Niasar, Rashidi,

Amrollahi, & Khodafarin, 2011) The enhancement can be significant even when CNTs are added in small concentrations, the motivations in present work are as follows.

No considerable researches have been performed to straightly indicate the influence of preparation methods on stability, thermal conductivity and viscosity of carbon nanotubes suspensions since The thermo-physical properties of CNT` nanofluids differ under different preparation techniques, In this study in order to prevent aspect ratio (L/D) reduction a combination of a mechanical method through ultrasonication and a chemical method through surfactants were used for dispersing.

The thesis comprises of five chapters. The current chapter gives the introduction and the importance of the research. The chapter 2 is the literature review done in relevance to the past work done in nanofluid research and how it is connected to this work. Experimental set-ups experimental procedures and measurements technique are provided in chapter 3. Chapter 4 presented the outcome of experiments, discussion about results and comparison with other studies. Finally, conclusion and suggestions for future works are provided in chapter 5.

1.2 Objectives

The overall goal of this study was to investigate the impact of sonication time on viscosity and thermal conductivity of aqueous suspensions of multi-walled carbon nanotubes. To satisfy the overall objective of this research, the following tasks are were undertaken:

1. Prepared multi-walled carbon nanotubes aqueous suspensions with concentration of 0.5wt%, by using threedifferent kinds of surfactants of SDS, SDBS and GA
2. Measured the thermal conductivity for all MWCNT samples employing KD 2 Pro Thermal Properties Analyzer, under temperature range of 20 to 45°C

3. The microscopic pictures of the samples were taken by utilizing Transmission Electron Microscopy (TEM) imaging technique. And compared the pictures together.
4. Measured the viscosity under different shear rates and temperatures of 30 and 15 °C for each of the samples using a rotating DG spindle Brookfield Rheometer.

CHAPTER TWO: LITERATURE REVIEW

2.1 History of nanofluids

Historical evidence has shown that nanoparticles and nanofluids were and initially exploited by the artisans for color and shine effect, apparently no one was aware of their particles size and abnormal properties. Medieval artisans used the gold nanoparticles suspension for coloring the windows glass of cathedral. Also in 15th century, Italian's potters applied metal nanoparticle in liquid host to make shiny pottery (S. U. Choi, 2009).

Study to develop advanced energy transmission fluids began in 1985 at Argon National Laboratory (ANL). Masuda et al. (Masuda, Ebata, Teramae, & Hishinuma, 1993) firstly, studied thermal conductivity and viscosity influence of ultra fine alumina, titanium dioxide and silicon dioxide in Japan. Following Masuda, Choi (S. U. Choi & Eastman, 1995) came

up with the result of enhanced thermal conductivity of colloidal dispersion with nanoparticles which coined them nanofluids. Indeed ANL's research was the first coherent research in nanofluids and thermal conductivity enhancement; although some parts were in common with Masuda's work but there were several distinctions between them. Dramatic enhancement of thermal conductivity of nanofluids, reported by previous researchers, attracted the present scientists and commercial investigators to launch an expansion effort on exploration of properties and utilization of nanofluids. The importance and attraction of this area is apparent from compilation report on publication about nanofluids, figure 2-1.

Many scientists and engineer studied nanoparticle production and preparation of nanofluids for experimental and application. Also they investigated effective function on thermal conductivity and viscosity of nanofluids like particle size and volume concentration, temperature, etc. however, researches on viscosity behavior are much less compare to thermal conductivity.

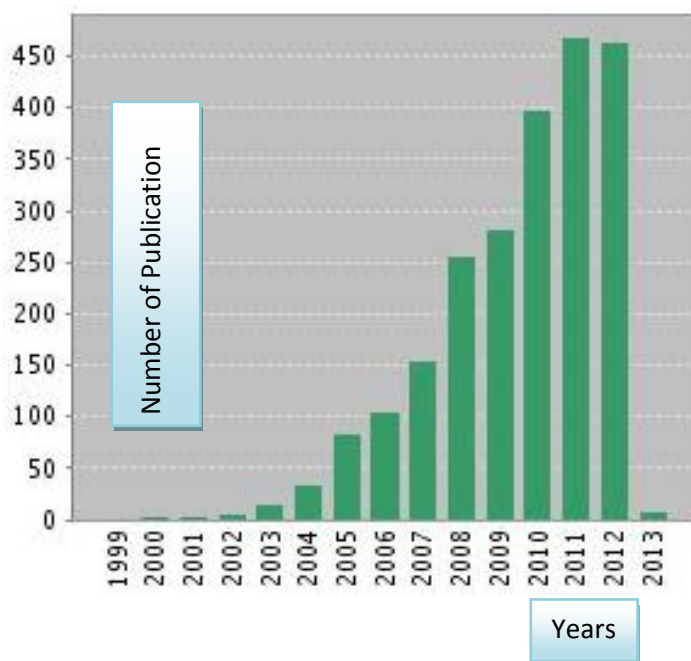


Figure 2-1 Publications in nanofluids (Web of science on Dec 2012)

In this chapter, review and discussion on experimental and basic theoretical activity in synthesis and thermal conductivity are presented.

2.2 Carbon Nanotubes (CNTs)

Carbon nanotubes are allotropes of carbon, structured as long, thin hollow cylinders of carbon. A typical nanotube has the diameter of the order of a nanometer and the length of the order of a few micrometers. They can be thought of as a sheet of graphite (a hexagonal lattice of carbon) rolled into a cylinder. They were discovered in 1991 by S.Iijima(Iijima, 1991). He reported the first observation of multi-walled carbon nanotubes (MWCNT) in carbon-soot made by arc-discharge. About two years later, he made the observation of single-walled nanotubes (SWCNT)(Iijima & Ichihashi, 1993). The basic structural difference between MWCNT and SWCNT is that the former has concentrically nested multiple layers of graphene structures whereas the later has only a single layer of grapheme structure. These intriguing structures have given a very broad range of electronic, thermal, and mechanical properties which have sparked excitement amongst the researchers in recent years. SWCNTs exhibit certain important electric properties which are not shared by

the MWCNTs and thus are more likely candidates for miniaturizing electronics. One useful application of SWCNTs is in the development of the first intramolecular field effect transistors (FETs) (Martel et al., 2001). On the other hand, MWCNTs have certain distinguished mechanical and thermal transport properties which make them suitable for applications related to structural composites, energy storage and heat transfer. Basic research over the past decade has shown that CNTs could have a thermal conductivity an order of magnitude higher than copper, ~ 3000 W/m-K for MWCNTs (P. Kim, Shi, Majumdar, & McEuen, 2001) and ~ 6000 W/m-K for SWCNTs (Berber, Kwon, & Tomanek, 2000). This suggests that CNTs have the potential to improve thermal conductivity of base fluids like water, ethylene glycol, mineral oils, etc., even when added in small quantities. Though based on the figures, SWCNTs have more potential to improve thermal conductivity; however, due to cost advantage and comparatively easy deagglomeration of MWCNTs, they have been studied more in heat transfer applications. The peculiar property of MWCNTs has made researchers interested all together in an area directed towards heat transfer-based nanotechnology applications.

2.3. Preparation of nanofluids

A dominant influence on behavior of nanofluids is governed by the preparation procedure of them. Proper dispersion of nanoparticles in base liquid, stability of suspension, stability of thermal conductivity of nanofluids and durability of nanofluids are crucial roles for production of nanofluids. Nanoparticles can be produced in two ways, the physical processes that include mechanical grinding method and the inert-gas-condensation technique, and chemical processes that include chemical precipitation, micro-emulsions, chemical vapour deposition, spray pyrolysis, and thermal spraying. Sonochemical synthesis

is also able to make suspensions of iron nanoparticles with oleic acid as a dispersant (Q. Yu, Kim, & Ma, 2008).

Generally nanofluids are the suspension of nanoparticles such as metals (Cu, Ag, Au), ceramics (Al₂O₃, CuO, TiO₂, SiC) and also carbon components (Diamond, MWCNT) in proper liquid like water, ethylene glycol and oil, the procedure of mixing nanoparticles with basic liquid are divided in two main techniques: two-step method and one –step method.

2.3.1 Two-step method

The first and classic method of preparing the nanofluids was the two-step method, which was also the most common way for nanofluids synthesis in the last decade. In this method the prepared nanoparticle by physical or chemical methods are dispersed in base liquid. The size of nanoparticles is maintained to prepare different nanofluids with different particle size and having different properties. One of the disadvantages of this method is agglomeration and settlement of nanoparticles in host liquid due to van der Waals bonding effect. Ultrasonication or advanced mechanical mixing devices are used for well dispersion of nanoparticles and reduction of agglomeration effect. Sonication and mixing time should be optimized for obtaining suspension of smaller nanoparticle size, higher stability leading to higher thermal conductivity and also lower viscosity of nanofluids (Tavman & Turgut, 2010) This method has shown a fairly good result for oxide nanoparticles (S. U. Choi, 2009).

2.3.2 One step method

This method is preferable for nanofluids containing metal nanoparticles like copper to prevent nanoparticles from oxidation. With this technique, nanoparticles are formed and dispersed in a fluid in a single process. One step method involving direct evaporation has been used to prevent nanofluid from agglomeration and produce nanoparticles that remain uniformly dispersed and stably suspended in base fluids. This technique as shown in figure 2-2 involves condensing nanophase powders from the vapor phase directly into flowing low-vapor-pressure liquid in a vacuum chamber (Chopkar, Das, & Manna, 2006; Eastman et al., 2001). The well-dispersed nanofluids of Cu in ethylene glycol enhance the thermal conductivity of the base fluid by up to 40% at the particle volume concentration of 0.3 vol. %, significantly larger than the prediction of effective medium theory (Wenhua Yu, France, Routbort, & Choi, 2008).

Although the one-step method has produced nanofluids in small quantities for research purposes, it is unlikely to become the mainstay of commercial nanofluid production. It would be difficult to scale up for two reasons. Processes that require a vacuum significantly slow the production of nanoparticles and nanofluids, thus limiting the rate of production. Furthermore, producing nanofluids by one-step physical processes is expensive.

These two methods are the most regular ways to produce nanofluids but there is still other way for nanofluids production like shape and size control synthesis of ZnO that has shown a good potential for controlling nanoparticles (Cao, Cai, & Zeng, 2006).

Recently W. Yu et al. proposed a phase transfer method for kerosene based Fe₃O₄ nanofluids, which compared to two step technique needs less sonication time. There is no clear relation between particle size and sonication time (W.-Y. Chen & Chen, 2010)

In this work, we would be concentrating on carbon nanotubes dispersed in de-ionized (DI) water based on their optimal thermal properties as reported by others.

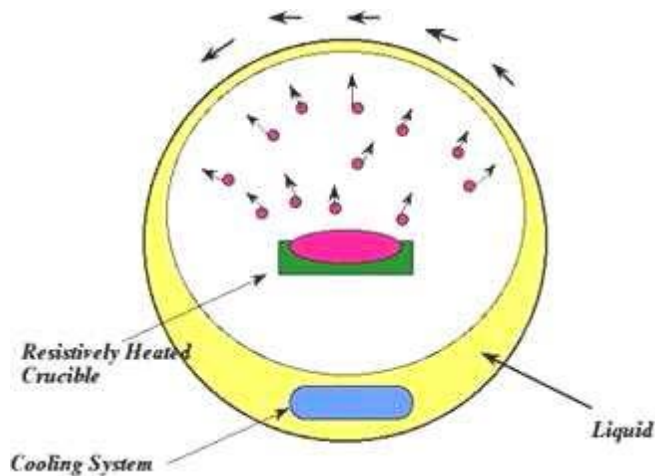


Figure 2-2 Schematic diagram of nanofluid production system designed for direct evaporation of materials into low-vapor-pressure liquids (Eastman et al., 2001)

2.4 preparation of Carbon nanotubes nanofluids(CNTsnanofluids)

Dispersing MWCNT is one of the critical steps in preparing CNTnanofluids in the base liquids. Due to having aspect ratio and strong Van DerWaal's forces between carbon surfaces, dispersion of MWCNT's in base fluids can be challenging.

The carbon nanotube cannot be dispersed in water under normal conditions, because they are hydrophobic in nature. Even when they are being dispersed, they have a tendency

to entangle and form clusters or agglomerates. There are regularly two procedures to disperse CNT's in base liquids : chemical and mechanical (Hilding, Grulke, George Zhang, & Lockwood, 2003).

Mechanical methods such as ultrasonication can separate the nanotubes but if it is not done in a controlled way, it may physically damage the nanotubes by decreasing the corresponding aspect ratio. Chemical methods include using surfactants or hydrophilic functional groups (functionalization) to attach onto CNT's to stabilize them. For this approach, hydrophilic functional groups such as nitric/sulfuric acid mixture, potassium hydroxide group (L. Chen, Xie, Li, & Yu, 2008; Ko et al., 2007). The method changes the wetting or adhesion treatment which helps in decreasing their trend to agglomerate. Chemical functionalization generally includes treating the CNTs with acids at high temperature. This results in addition of polar groups like $-COOH$ or $-OH$ at defect sites on nanotube surface, thus making CNTs hydrophilic in nature. However, aggressive chemical functionalization, can damage the CNT's. For the chemical methods to be effective either aggressive chemical functionalization or high concentrations of surfactant need to be used, for example, Jiang et al. (Jiang, Gao, & Sun, 2003) reported that the optimum amounts of SDS used to obtain a stable homogeneous suspension of 0.5 wt% CNTs was 2wt%. On the other hand aggressive chemical functionalization can cause defects on CNTs altering their thermal and physical properties. High surfactant concentrations can significantly increase the base fluid viscosity and the interface thermal resistance between the carbon nanotubes, thus, limiting the thermal transport in the nanotubes matrix (L. Chen & Xie, 2010b)

Both chemical and mechanical methods can alter the CNT aspect ratio. It has been reported that thermal conductivity enhancement in CNT nanofluids increases with aspect ratio (Amrollahi, Hamidi, & Rashidi, 2008; Garg et al., 2009; Nasiri et al., 2011), however, proper care still has to be taken during processing to minimize adverse effects. In this work, a combination of chemical method with surfactants and mechanical method through sonication, is used. Ultrasonication disperses particles by a series of bubble nucleation and collapse events. Ultrasonication can be done either by using an ultrasonic bath or by ultrasonic probe. Ultrasonication of fluids leads to three physical mechanisms: cavitations of the fluid, localized heating, and the formation of free radicals (Hilding et al., 2003). In the case of CNTs, this phenomenon reduces the nanotube length and reduces their tendency to entangle, which helps them disperse in a base fluid. However, even the mechanical method is not good enough to form stable suspensions. Through our experimental work, it has been found that nanotubes dispersed by just ultrasonication re-agglomerate and settle down after few days. This phenomenon results in sedimentation. This is why a chemical method involving surfactants is used as it provides milder conditions than functionalization using acids. The surfactant gets adsorbed on the carbon nanotube surface which induces electrostatic repulsions to counterbalance Van der Waals attractions (Hunter, 1986) between CNTs. This prevents the agglomeration of nanotubes under Van der Waal's attractions and thus provides stable suspensions. Surfactants have been used to disperse carbon nanotubes in several cases. Wide range of surfactants such as sodium dodecyl benzene sulfonate (SDBS) (Wen & Ding, 2004), sodium dodecyl sulfate (SDS) (Assael et al., 2004), Nanospense AQ (Assael et al., 2005), Hexadecyltrimethylammonium bromide (CTAB) (Assael et al., 2005), Chitosan (Phuoc, Massoudi, & Chen, 2011) and Gum Arabic (GA) (Ding et al., 2006; Garg et al., 2009) have

been used. Through past works Cationic surfactants such as hexadecyltrimethylammonium bromide (CTAB), Gemini surfactant (L. Chen & Xie, 2010b), and cationic-onionic mixed surfactant (Madni, Hwang, Park, Choa, & Kim, 2010) have been found to be effective in stabilizing CNTs and various metal particles (G.-y. Li, Jiang, Huang, Ding, & Chen, 2008) with low surfactant concentrations. Because higher concentration of Cationic Gemini give rise to the sediment of MWNTs in the nanofluids, resulting in decrease of thermal conductivity enhancement of MWNTs nanofluids. (L. Chen & Xie, 2010a). another kind of Cationic surfactant called Chitosan, found as an effective stabilizer for dispersing CNTs in water by T.X. Phuoc et al (Phuoc et al., 2011), it is biocompatible and is a natural polymer isolable from crustacean cell. (Hwang et al., 2006) displayed addition of sodium dodecyl sulfate (SDS) can improve the stability of CNT nanoparticles in aqueous suspensions. k. Wusiman et al (Wusiman, Jeong, Tulugan, & Chung, 2012) exhibited that CNT nanofluid with SDBS shows better thermal conductivity than that with SDS dispersant. M. Bystrzejewski et al (Bystrzejewski et al., 2010) studied the suspensions of MWCNT in aqueous solutions of SDS and SDBS AS two anionic surfactants It was found that both dispersing agents form stable suspensions of CNTs. The SDBS surfactant has 26–45% higher dispersing power in comparison to SDS. Also they shown the surfactant structure has also an effect on the diameter distribution of dispersed nanotubes. SDBS have increased affinity to the narrower CNTs, whilst nanotubes suspended in SDS solution has the same diameter distribution as pristine CNTs. However Experiments on SDBS at a temperature above 60-70°C showed that the dispersant failed, which led to destabilization of nanofluids (Wen & Ding, 2004). Moreover Rajdip Bandyopadhyaya et al. used a novel method for achieving the dispersion of nanotubes (Bandyopadhyaya, Nativ-Roth, Regev, & Yerushalmi-Rozen, 2002) The method makes use of physical adsorption of a water soluble

polymer called Gum Arabic, which is a natural polysaccharide and produced by Acacia Senegal trees. It has already been described to be helpful for CNT dispersion (Ding et al., 2006). This method can be used for both SWCNTs and MWCNTs, according to the current and past research, GA was found to be suitable surfactant. However, GA has a tendency to increase viscosity when added in small quantities to a base fluid like DI water. The high viscosity in nanofluids could result in sticking of nanotubes to the walls of the sample bottles and also to the surfaces of measuring instruments. Thus, a highly viscous nanofluid would also result in increase in pumping power for commercial applications. Therefore, it becomes important that the amount added is optimum (Ding et al., 2006). Through previous work and also by repeated experiments in laboratory, it was found that 0.25 wt % of GA would be suitable, the method of preparation would be discussed in detail in next chapter.

2.5 Thermal conductivity of nanofluids

Heat transfer process can be increased by altering variety of parameters like temperature difference, heat transfer surface area and heat transfer coefficient in flowing fluid. Heat transfer coefficient is mainly represented by function of Nusselt number, and thermal conductivity of fluid. Hence thermal conductivity enhancement of nanofluids became significant in heat transfer development of nanofluids. As previously noted, Argon National Laboratory (ANL) was the pioneer in nanofluids arena. Since then, numerous researches have been launched about thermal conductivity enhancement of metal oxide nanofluids but less works have been done on CNT nanofluids. Regarding CNT's, reports on thermal conductivity of nanofluids containing CNT's have not been consistent, this might be due to the differences in the experimental conditions such as carbon nanotube aspect ratios, dispersants used and the approaches used for preparing the experimental nanofluids.

2.5.1 Past research on thermal conductivity of carbon nanotubes nanofluids

As the sequence of experiments and exploration of various nanofluids in Argon National Lab (ANL) continued, for the first time a dramatic enhancement of thermal conductivity observed by Choi et al. (S. Choi et al., 2001) for multiwalled carbon nanotubes (MWCNT) dispersed in synthetic poly(α -olefin) oil as a base fluids. They reports nonlinear enhancement of thermal conductivity up to 160% at only 1% volume concentration of Carbon nanotubes in oil. They have also explained the cause of this anomalous enhancement of strangely higher magnitude than theoretical prediction for nanofluids with particle high thermal conductivity (3000 w/mk), size and shape of nanotubes. Subsequently, data was published by Xie et al. (Xie, Lee, Youn, & Choi, 2003) where, enhancements were reported for water, ethylene glycol and decene as base fluids. Assael et al. (Assael et al., 2004; Assael et al., 2005) data focused on aqueous MWCNT nanofluids with SDS, CTAB and Nanospense AQ as dispersants. However, both these works reported much less enhancements as compared to those reported by Choi et al. (S. Choi et al., 2001). The maximum thermal conductivity enhancement observed by Xie et al. (Xie et al., 2003) was only 20% for 1% nanotubes in decene by volume, and Assael et al. (Assael et al., 2004) observed enhancement of 38%, for 0.6 vol% MWCNT's-water nanofluids, using 0.1 wt% SDS (sodium dodecyl sulfate). In 2004, Wen and Ding (Wen & Ding, 2004) observed 23% and 28% enhancements for 0.84 vol% MWCNT-water nanofluids using SDBS as the dispersant at 20 c and 40 c respectively. Their results were comparable to Xie et al. (Xie et al., 2003) and Assael et al. (Assael et al., 2004) and proposed differences in the interfacial resistances and thermal conductivities of carbon nanotubes used in these studies as the main reasons for the observed discrepancies with respect to Choi et al. (S. Choi et al., 2001). Additionally, the base fluid used by Choi et al. was poly- α olefin (a lower thermal

conductivity than water), though percentage enhancement reported was high, the absolute enhancement was not as high as expected. As SDBS was also found to fail at elevated temperatures (Wen & Ding, 2004), in 2006, another set of data was published using Gum Arabic (GA) as dispersant by Ding et al. (Ding et al., 2006). In this work, thermal conductivity enhancement of 28% and 79% was reported at 25 °C and 30 °C respectively with 1 wt % MWCNT in water. Thermal conductivity measurements revealed that the effective thermal conductivity increased with increasing temperature and CNT concentration, with the dependence of the conductivity on temperature much more significant. The enhancement of the thermal conductivity was slightly higher than that reported by Assael et al. (Assael et al., 2004), Xie et al. (Xie et al., 2003) and Wen and Ding (Wen & Ding, 2004). They suggested that this discrepancy be associated with the thermal properties of CNTs used, liquid-CNT interfacial resistance, and the aspect ratio of CNTs used. Furthermore, the base liquid used also played a role.

Lately L. Chen and H. Xie (L. Chen & Xie, 2010a) by using Cationic Gemini as a surfactant reported thermal conductivity enhancements of 34.3% and 5.6% at a volume fraction of 0.6% with temperatures of 65 °C and 5 °C respectively, and shown the temperatures strongly affects on enhancement of thermal conductivity of WMCNT-water nanofluids stabilized by cationic Gemini surfactants, The enhancement is a bit lower than that published by Ding et al. (Ding et al., 2006). Moreover A. Indhuja et al. (Indhuja, KS, Manikandan, & KS, 2013) reported the thermal conductivity enhancements of 8% and 33% at a concentration of 5 wt% with temperatures of 28°C and 60°C respectively.

To date, most of the published data in MWCNT based nanofluids is focused on the thermal conductivity enhancement with parametric effects of particle volume concentration, base

fluid, and temperature. Though parametric effects of particle size(Length and diameter)(Amrollahi et al., 2008; Ruan & Jacobi, 2012), dispersant (surfactant)(Assael et al., 2004; Assael et al., 2005; Wen & Ding, 2004)and acidity (Ding et al., 2006) have been considered, only a few papers have been published in this area. As nanotubes are cylindrical in nature and exist as agglomerates, direct particle size characterization using techniques like Dynamic Light Scattering (DLS) is difficult for nanotubes. The reason behind thermal conductivity enhancement in carbon nanotube dispersions is still not completely understood. There are many phenomena postulated for the enhancement. Studies have indicated that nanotubes conduct current and heat ballistically or in fast diffusive manner (Berber et al., 2000). The ballistic conduction is associated with the large phonon mean-free path in nanotubes. Hence, nanotubes change the cause of heat conduction from diffusion in liquids to both fast diffusion and ballistic heat conduction in nanofluids. Furthermore, there is evidence that an organized solid-like structure of a liquid at the interface is a governing factor in heat conduction from a solid wall to an adjacent liquid (Suzuki, 2000). Therefore, it has been postulated that this organized solid/liquid interface structure causes the energy transport across the interface. Additionally, in 2004, Jang and Choi (Jang & Choi, 2004) postulated another theory using Brownian motion of nanoparticles as a potential factor for increased thermal conductivity of nanofluids at elevated temperatures. It suggested that as temperature is increased, the viscosity of base fluids is decreased and the Brownian motion of nanoparticles is consequently increased. It has been postulated that convection like effects are induced by Brownian motion which result in increased conductivities. However, previously Keblinski et al. (Keblinski, Phillpot, Choi, & Eastman, 2002) showed that Brownian motion is unlikely to have direct role in the enhancement of thermal conductivity. Several years later Amrollahi et al (Amrollahi et al., 2008) explored the effects

of ultrasonication time on thermal conductivity and sediment of carbon nanotubes-ethylene glycol nanofluids and found strong dependence of the effective thermal conductivity on temperature and volume fraction of CNT nanofluids. The Thermal conductivity increased with passed ultrasonication time. Brownian motion and the inter-particle potential, which influences the particle motion, were proposed to account for the phenomenon. Yang et al. (Yang, Grulke, Zhang, & Wu, 2006) explored the sonication energy/time impact on thermal conductivity of nanotube-oil suspensions and observed a decreased thermal conductivity with an increasing sonication energy/time. In the following Garg et al. (Garg et al., 2009) published the effect of ultrasonication energy on the thermal conductivity and viscosity of MWCNT-water nanofluids dispersed using gum arabic. An optimum ultrasonication energy (or sonication time) was found to exist that would be sufficient to achieve nanotubes' dispersion, without causing breakage of nanotubes. A thermal conductivity enhancement of 20% was observed for 1 wt% MWCNT-water nanofluids at the optimum ultrasonication energy of 113 J/g (40 min sonication time)

newly Ruan and Jacobi (Ruan & Jacobi, 2012) proved the thermal conductivity of MWCNT-ethylene glycol nanofluids increases nonlinearly when sonication time/energy increases, and achieved the maximum thermal conductivity enhancement of 23% at a concentration of 0.5 wt% with elapsed 1355 minutes sonication time. In addition they observed that the processes of sonication reduced both the agglomerate sizes and the length of carbon nanotubes. But the agglomerate size reduction is more important than the Length reduction. In spite of these researches and experiments it can be found that stabilization by Ultrasonication is a usual way to break up the agglomerates and promote dispersion of

nanoparticles into base fluids. However there are limited research reports about sonication effects on Carbon nanotubes nanofluid properties in the open literature.

Table 3-1 presents a summary of data for thermal conductivity comparison of CNT`s nanofluids. Particle volume concentration, particle size, thermal conductivity results, base liquid difference, and the surfactant used have been presented.

Researcher/year/reference	particle	Base fluid	Average Particle size	concentration (vol% or Wt%)	thermal conductivity enhancement	Note
choi et al. (S. Choi et al., 2001)	MWCNT	Oil	25nm*50μm	1 Vol%	150%	-
Xie et al.(Xie et al., 2003)	MWCNT	Decene/ethylene glycole/water	D=15nm L=30μm	1 Vol%	20%/13%/7%	-
Assael et al.(Assael et al., 2004)	MWCNT	(+SDS)-Water	100nm*70μm	0.6 Vol%	38%	-
Xie et al.(Xie et al., 2003)	MWCNT	Water	15*30000	0.4-1 Vol%	1.03-1.07 (Ratio)	Two-step Method
Xie et al.(Xie et al., 2003)	MWCNT	ethylene glycole	15*30000	0.23-1 Vol%	1.02-1.13 (Ratio)	Nitric acid treatment
Xie et al.(Xie et al., 2003)	MWCNT	(+Oleylamine)-decene	15*30000	0.25-1 vol%	1.04-1.20 (Ratio)	-
Wen and Ding (2004)(Wen & Ding, 2004)	MWCNT	(+ sodium dodecyl benzene)-water (20°C)	20–60 (diameter)	0.04–0.84 Vol%	1.04–1.24	Two-step method
Wen and Ding (2004)(Wen & Ding, 2004)	MWCNT	(+ sodium dodecyl benzene)-water (45°C)	20–60 (diameter)	0.04–0.84 Vol%	1.05–1.31	Temperature effect
Assael et al. (2005)(Assael et al., 2005)	MWCNT	(+ Nanospense AQ)-water (40-60) min	L 10μm OD 100-250	0.6 Vol%	1.28-1.27	Sonication time effect
Assael et al. (2005) (Assael et al., 2005)	MWCNT	(+ hexadecyltrimethyl ammonium bromide(CTAB))-water 10 min	L 10μm OD 100-250	0.6 Vol%	1.34 34%	Sonication time effect

Assael et al.(2005)(Assael et al., 2005)	DWCNT	(+ hexadecyltrimethylammonium bromide(CTAB))-water	5 nm (diameter)	1.00 Vol%	1.08	Dispersant effect
Assael et al. (2005) (Assael et al., 2005)	DWCNT	(+ hexadecyltrimethyl ammonium bromide(CTAB))-water	5 nm (diameter)	0.75 Vol%	1.03	Two-step method
Liu et al. (2005)(M.-S. Liu et al., 2005)	MWCNT	ethylene glycol	20–50 (diameter)	0.20–1.00 (1 vol.%)	1.02–1.12 (12.4%)	Two-step method
Liu et al. (2005)(M.-S. Liu et al., 2005)	MWCNT	(+ N-hydroxysuccinimide)-engine oil	20–50 (diameter)	1.00–2.00 (2 vol.%)	1.09–1.30 (30%)	Two-step Method
Marquis and Chibante(2005)(Marquis & Chibante, 2005)	SWCNT	(+ dispersant)-diesel oil (Shell Rotella 15W-40)	(10–50) × (0.3–10 μm)	0.25–1.00	1.10–1.46	Two-step Method
Ding et al. (2006)(Ding et al., 2006)	MWCNT	(+ gum arabic)-water (20°C)		0.05–0.49	1.00–1.10	Two-step method
Ding et al. (2006)(Ding et al., 2006)	MWCNT	(+ gum arabic)-water (25°C)		0.05–0.49	1.07–1.27	Temperature effect
Ding et al. (2006)(Ding et al., 2006)	MWCNT	(+ gum arabic)-water (30°C)		0.05–0.49	1.18–1.8	Temperature effect
Hwang et al. (2006)(Hwang et al., 2006)	MWCNT	mineral oil		0.5	1.09	-

Yang et al. (2006)(Yang et al., 2006)	MWCNT	(+ polyisobutene succinimide)-polyalphaolefin		0.04–0.34	1.06–3.00	Two-step method
P.Garg et al. (2009)(Garg et al., 2009)	MWCNT	(+ gum arabic)-water 40 min Ultrasonication (35°C)	OD 10-20 nm L 0.5-40 µm	1 wt%	20%	Ultrasonication effect
L.Chen, H. Xie 2010 (L. Chen & Xie, 2010a)	MWCNT	(+Cationic gemini)-water (5°C-65°C)	OD 30-50 nm L ~ 20 µm	0.6 Vol%	5.6%-34%	Temperature effect
T.X.Phuoc et al. (2011)(Phuoc et al., 2011)	MWCNT	(+ Chitosan)-water (35°C)	OD 20-30nm ID 5-10nm L 10-30 µm	(0.5-3) wt% (0.24-1.43) Vol%	2.3%-13%	Two-step Method
N.Singh et al. (2012)(Singh, Chand, & Kanagaraj, 2012)	MWCNT	ethylene glycol+water	D 60-30 nm L 5-15µm	0.4 wt%	72%	Nitric and sulfuric acid treatment
V.Kumaresan,R.Velraj (2012) (Kumaresan & Velraj, 2012)	MWCNT	(+SDBS)-ethylene glycol+water (40°C)	D 30-50 nm L 10-20 µm	0.45 Vol%	19.75%	effect of different temprature
W.Rashmi et al. (2010)(Rashmi et al., 2011)	MWCNT	(+ gum arabic)-water (25, 40, 60) °C	OD 20 nm L 30µm	0.01-0.1 wt%	1.5-2 1.4-1.75 1.25-1.6	surfactant concentration and temprature effect

A. Indhuja et al.(2013)(Indhuja et al., 2013)	MWCNT	(+ gum arabic)-water	ID 10 nm L 5-15 μ m	(0.14-0.24) Vol%	0.61-0.67 (3.2%-10%)	effect of different mwcnt concentration
A. Indhuja et al.(2013)(Indhuja et al., 2013)	MWCNT	(+ gum arabic)- water(28-60 °C)	ID 10 nm L 5-15 μ m	0.5 wt%	0.66-0.93 (8%-33%)	effect of different temprature
A. Indhuja et al.(2013)(Indhuja et al., 2013)	MWCNT	(+ gum arabic)- water(28-60 °C)	ID 10 nm L 5-15 μ m	0.3 wt%	0.63-0.88 (5%-26%)	effect of different temprature
A.Amrollahi et al.2008(Amrollahi et al., 2008)	MWCNT	Ethylene Glycol (25-50 °C)	OD 1-4 ID 0.8-1.1	2.5 vol%	20 %	Temperature Effect
A.Amrollahi et al.2008(Amrollahi et al., 2008)	MWCNT	Ethylene Glycol 1-24 hrsUltrasonication	OD 1-4 ID 0.8-1.1	0.5vol% 2.5 vol%	1.05-1.2 1.1-1.32	Ultrasonication effect
Ruan and Jacobi.2012(Ruan & Jacobi, 2012)	MWCNT	Ethylene Glycol 1355 mins	OD 10-30 L 10-30 ID 5-10	0.5 wt%	23%	Ultrasonication effect

Table 3-1 summary of data for thermal conductivity comparison of CNT` s nanofluids

2.6 viscosity of carbon nanotubes nanofluids

Viscosity, dynamic property of fluids is used for calculation of pumping power in heat transfer system and plays a significant role in application of fluids. In industry, an optimization is required between heat transfer capability and the viscosity as it has a direct bearing on the sizing of the flow and heat transfer equipment required. As nanofluids are involved, to enhance the efficiency of system by increasing the thermal conductivity and in fact heat transfer of flowing fluid. Effect of any negative parameter on efficiency must be retarded; therefore, viscosity of nanofluids is taken under investigation to assess the efficiency of nanofluids. Experimental data for the effective viscosity of aqueous nanofluids are much limited than that of thermal conductivity. Also current studies in viscosity of CNT's Nanofluids (Ding et al., 2006; Garg et al., 2009; Phuoc et al., 2011) are much less than metal oxide nanoparticles nanofluids. The parameters against which viscosity was studied were particle volume concentration, temperature and shear rate. These studies reveal that aqueous CNT Nanofluids behave as non-Newtonian shear-thinning fluids. Additionally understanding flow behavior of carbon nanotube (CNT) nanofluids by developing Mathematical viscosity models is an important area for taking the research into the next phase. However, a few empirical and accurate analytical models for prediction of the viscosity of high aspect ratio nanofluids (Ding et al., 2006) are available. The works are mainly focused on spherical nanoparticles of metal oxides, and have their basis from Einstein theory. In case of CNT nanofluids, such models cannot correlate the experimental data well because the shape of CNTs does not satisfy previous assumptions. It is difficult to do particle size characterizations for CNTs and subsequently incorporate those characterizations in the Einstein viscosity model (Equation 2-1).

$$\mu_e = (1 + 2.5v_p)\mu_m \quad (2-1)$$

Where, μ_m , v_p , μ_e , and are viscosity of the base fluid, particle volume fraction in the dispersion, and effective viscosity of the dispersion respectively. Aqueous CNT nanofluids have shown to exhibit shear thinning or pseudoplastic type of non-Newtonian behavior (Ding et al., 2006). However, there is a few works has been done in correlating this behavior to theoretical non-Newtonian viscosity models (Ding et al., 2006). The theoretical models provide equations to correlate shear stress of a flowing fluid to shear rate. This could help in classifying the flow behavior of a new nanofluid under the already studied behavior of fluids, and thus help in directing future rheological studies. The widely used models for non-Newtonian flow are Power Law (Eq 2.2) and Herschel Bulkley (Equation 2-3).

$$\tau = K \cdot \dot{\gamma}^n \quad (2-2)$$

$$\tau = \tau' + K \cdot \dot{\gamma}^n \quad (2-3)$$

Where τ , K , $\dot{\gamma}$, τ' and n are shear stress, flow consistency index, shear rate, yield shear stress and flow behavior index, respectively. The value of parameters 'K' and 'n' signify the flow behavior in quantitative and qualitative terms respectively. A high value of 'K' is attributed to high viscous behavior and a low value of 'n' is attributed to high degree of non-Newtonian behavior of the fluid. Additionally, a few work has been done in studying the effect of processing or ultrasonication time and Temperature (Garg et al., 2009) on the viscosity of MWCNT aqueous suspensions or nanofluids. Experimental work in this area could provide impetus to theoretical model development for CNT nanofluids. In this work,

an effort has been made to study this effect and subsequently fitting the experimental data in the form of a shear stress- shear rate mathematical equation.

CHAPTER THREE: METHODOLOGY

This section explains the objectives, the description of the experimental set-ups used to measure viscosity and thermal conductivity of the samples, and the steps involved in the preparation of aqueous suspensions of MWCNT.

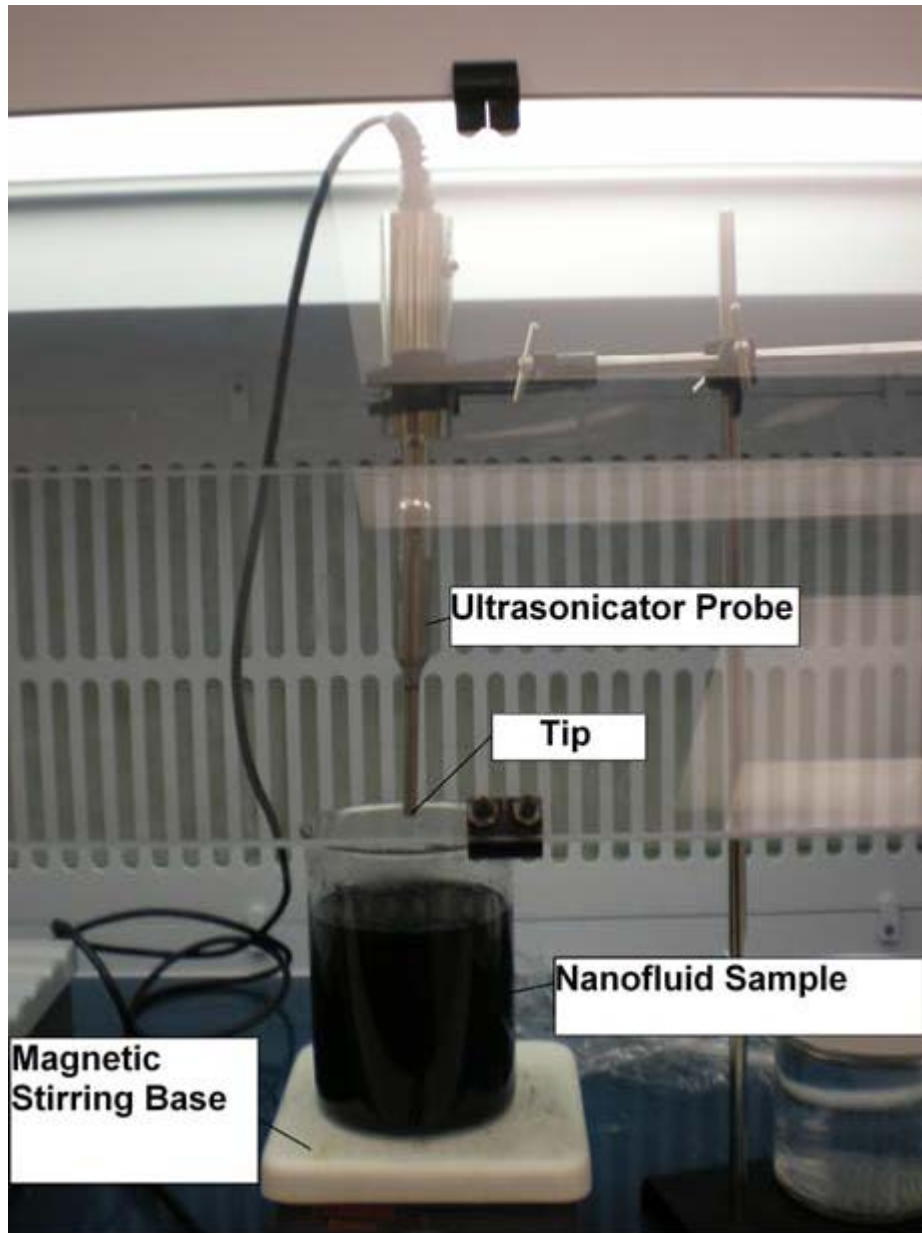
3.1 Set-up description

This section describes the working principle involved behind each of the experimental set-ups used for preparing sample and measuring viscosity, thermal conductivity

3.1.1 Ultrasonication probe

The ultrasonic processor used for sample preparation was 130 watts, 20 kHz ultrasonication probe from Sonics & Materials, Inc. According to the operator's manual of the instrument, the processor's power supply converts 60 Hz line voltage to a high frequency electrical energy. The high frequency electrical energy is changed into mechanical vibrations through a piezoelectric transducer. The vibrations when being transmitted through the probe are further intensified and create pressure waves in the liquid sample. The induction of pressure waves forms several microscopic bubbles inside the sample, which expand during negative pressure excursion and implode violently during the positive excursion. As the bubbles implode, they cause several shock waves and eddies that radiate outwardly from the site of collapse, and also generate extremes in pressures and temperatures at the implosion sites.

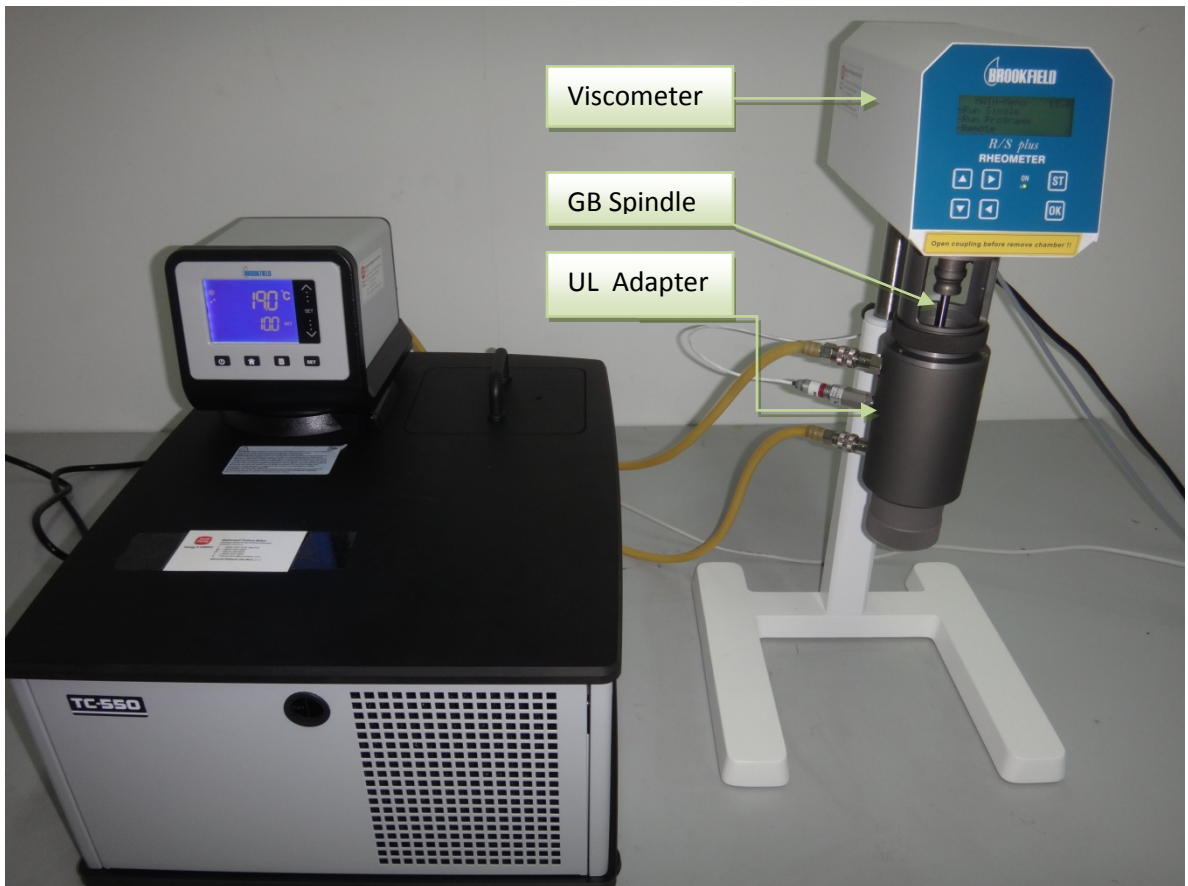
Although this phenomenon, known as cavitation, lasts few microseconds, and the amount of energy released by each individual bubble is minimal, however, the cumulative amount of energy generated is extremely high. See Figure 3-1 for the set-up picture.



**Figure 3-1 Ultrasonication processor
(Powder Lab.)**

3.1.2 Viscometer

The viscometer used was from Brookfield Engineering Laboratories, Inc. It was of the rotational variety. According to the operator's manual of the instrument, the instrument measures the torque required to rotate an immersed element (the spindle) in a fluid. The spindle is driven by a motor through a calibrated spring; deflection of the spring is converted internally through a set of formulae to display the dynamic viscosity in centipoises (cP). By utilizing a multiple speeds and different spindles, a variety of viscosity ranges can be measured. For a given viscosity, the viscous drag (indicated by the degree to which the spring winds up), is proportional to the spindle's speed of rotation and is related to the spindle's size and shape. The drag will increase as the spindle size and/or rotational speed increase. It follows that for a given spindle geometry and speed, an increase in viscosity will be indicated by an increase in deflection of the spring. Measurements made using the same spindle at different speeds are used to detect and evaluate rheological properties of the test samples. The model used in the laboratory was meant for low viscosity fluids and had a maximum torque rating of 0.06737 milliNewton-m. The instrument had a specified accuracy of $\pm 1\%$, which was verified using a Brookfield's standard viscosity test fluid. A combination of cylindrical sample container and spindle called as UL Adapter was used for the measurements. The UL Adapter is an attachment provided with the instrument for taking measurements on low viscosity test samples. See Figure 3-2 for the set-up picture.



**Figure 3-2 viscosity measurements set up
(Heat Transfer Lab.)**

3.1.4. Thermal conductivity analyzer

Thermal conductivity is defined as the ability to conduct the heat in materials. Different experimental methods have been developed for the thermal conductivity measurement which may be divided in two main categories: steady state and unsteady state (transient) techniques.

Steady state techniques are directly based on the integrated form of Fourier's law that utilize steady conduction in a fluid sample of a specified geometry. The steady state methods have certain merits, which is to ease the equipment design and make use of simple and reliable equations. Unsteady or transient techniques are a time dependent method that performs a measurement during the process of heating up, so the measurement can be conducted relatively quickly, for example transient hot wire method. Transient hot wire (THW) method is well established as the most accurate, reliable and robust technique. In this method a thin metallic wire is used as both a line heat source and a temperature sensor.

It is called transient because heat is supplied suddenly, so that eventually the wire gets heated. It replaces the steady state methods, because of the difficulty to determine the steady state conditions and for fluids the difficulty in preventing the incident of natural convection and consequently the difficulty in eliminating the natural convection effects on the heat flux. The working equation is based on a specific solution of Fourier's Law for radial transient heat conduction with a line heat source at the axis of the cylindrical domain. Where, q (W/m) is the heat released per unit time per unit length of the line source and k (W/m.K) is the thermal conductivity of sample. If temperatures T_1 and T_2 of the heat source at time t_1 and t_2 , then thermal conductivity of liquid is:

$$K = \frac{q}{4\pi(T_2 - T_1)} \ln \frac{t_2}{t_1}$$

In this study thermal conductivity of nanofluids has been measured by KD2 Pro (Decagon, USA), the instrument was based on the working principle of a transient hot wire method used in past works (Alloush, Gosney, & Wakeham, 1982; Assael et al., 2004; Assael et al., 2005; Ding et al., 2006). KD2 Pro Instrument (figure 3-3) used for thermal conductivity measurement has the instrument accuracy of about 5%. Single needle sensor are also (1.3

mm diameter \times 60 mm long) used for thermal conductivity measurement. The needle installed in the package of water jacket connected to the water bath for temperature stability and precise measurement. Thermal conductivity is estimated from temperature responses of thermocouple caused by electrical signals. The total time for measurement of thermal conductivity is about 90 seconds. The first 30 seconds is to ensure the temperature stability. The second and third 30 seconds intervals all are for heating and cooling the probe respectively. In the present study, initial checking of the KD2 Pro is done by measuring the thermal conductivity of base liquids and then checks with reference for comparison and finding the accuracy of the system. It is also necessary to measure thermal conductivity of base liquid for thermal conductivity ratio calculation. After measuring thermal conductivity of base liquid at selected temperature, thermal conductivity of nanofluids up to 0.5wt% was measured.

Temperature effect on thermal conductivity of nanofluids was investigated for all samples, for exploring both higher and lower room temperature effects on nanofluids thermal conductivity. Water bath (made by WiseCircu, Refrigerated circulators) with 0.1 °C accuracy was used for stabilizing temperature at 20, 25, 30, 35, 40, 45°C for measuring the thermal conductivity of nanofluids in various concentrations. In this case nanofluids are poured into water jacket as a container and temperatures are maintained to obtain stabilized nanofluids, Figure 3-3 presented the set-up including the KD2 Pro and jacketed beaker connected to the Circulating Water Bath water bath with an inlet and an outlet attachments for flowing and circulating water at specific temperature to stabilize the temperature of the nanofluids.

See Figure 3-3 for the set-up picture.

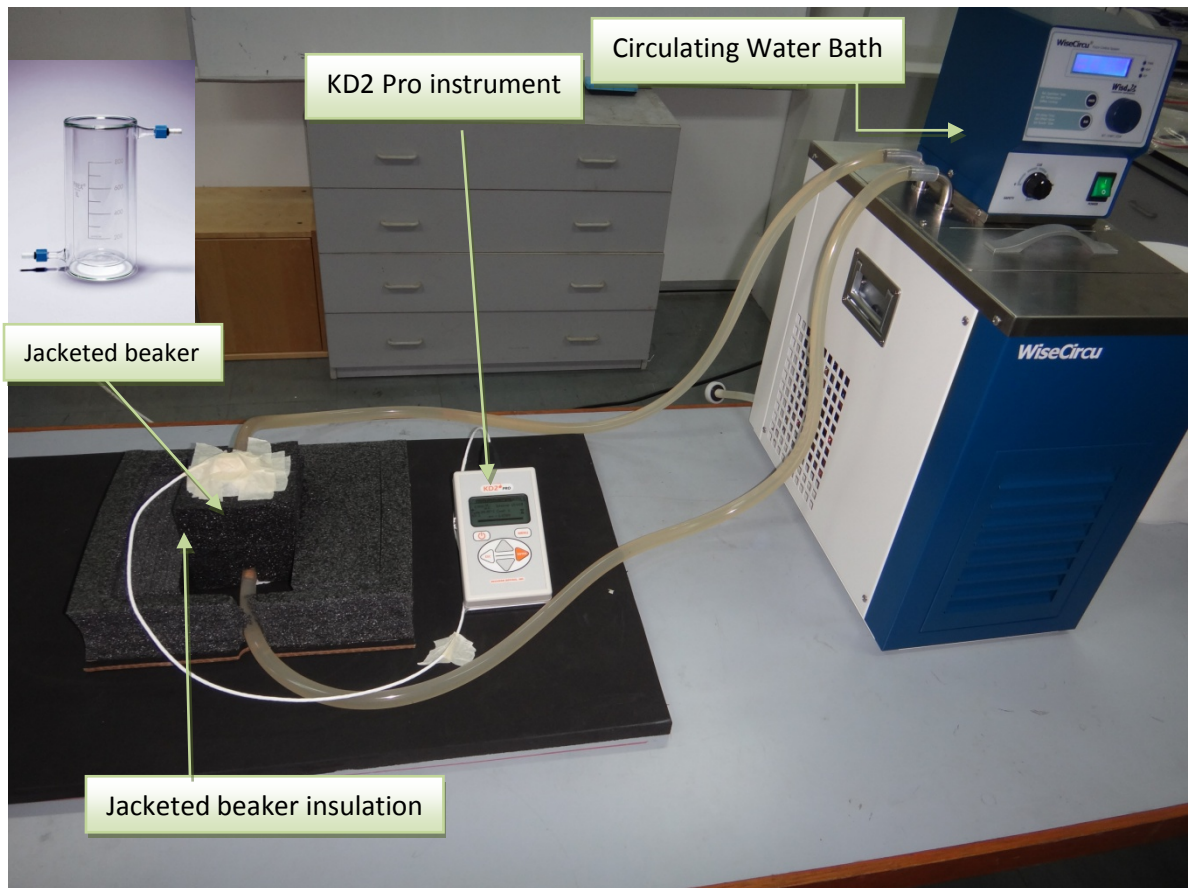


Figure 3-3 Set-up for thermal conductivity measurements set up.

(HeatTaransfer Lab)

3.2 Sample preparation

De-ionized (DI) water, Gum Arabic (GA) and multi-walled carbon nanotubes(MWCNT) were used to produce the aqueous suspensions. The nanotubes were provided from

Nanostructured& Amorphous Materials, Inc, USA. Properties of Multi-walled carbon nanotubes employed in this study are showed in Table 3-1.

	Outside Diameter,OD (nm)	Length, L (um)	Density, μ (g/cm ³)	Purity(%)	Thermal conductivity, k (w/m ² .k) at 300 K	Specific surface area, SSA (m ² /g)
sample (MWCNT)	20-30	10-30	~2.1	> 95	2800	110-130

Table 3-1 Properties of Multi-walled carbon nanotubes

The nanotubes produced by chemical vapor deposition (CVD) process. Figure 3-4 showed TEM images of MWCNT as received. It can be seen that the nanotubes without treatment are not only entangled but also some are in format of agglomerates.

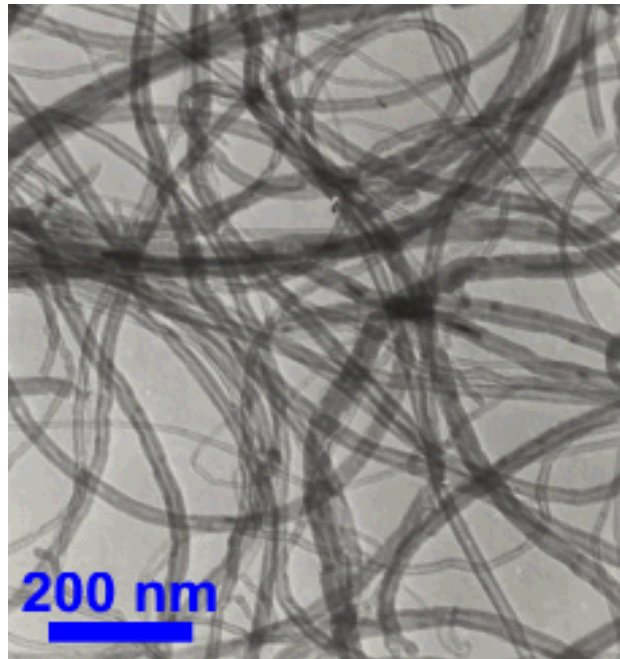


Figure 3-4 TEM Multi-walled Carbon nanotubes (MWCNT) images as received

Gum Arabic was purchased from Sigma-Aldrich Co. Malaysia. The properties of Distilled water have been presented in table 3-2.

Medium	Density (g/ml)	Thermal conductivity (w/m2.k) at 25 oC	Viscosity (mPa.s) at 20 Oc	Boiling point (oC)	Melting Point (Oc)	Specific heat (J/Kg.K)
Water	0.997	0.58	1	100	0	4179

Table 3-2 properties of Distilled-water

Since the surface of the Multi-walled carbon nanotubes is hydrophobic and Water is a polar liquid, Gum Arabic (GA), Sodium dodecylbenzenesulfonate (SDBS) and Sodium dodecyl sulfate (SDS) were used as a dispersants in order to disperse the CNT`s in the Distilled water. The required amount of base fluid was purred in a 100 ml glass beaker,by adding 0.25 and 0.5 wt% SDBS and SDS, and just 0.25 wt% GA respectively into the base fluid (distilled water), dispersed by using magnetic stirring, (Since the GA concentration of 25 wt% used in the literature proven to be optimum amount for preparing stable and high thermal performance water-MWCNT`s nanofluids(Ding et al., 2006), same concentration is considered in this study) after the surfactants were fully dissolved and a homogenous solutions were achieved, 0.5 wt% MWCNT`s was added to the fluids, using an ultrasonication probe, each solution ultrasonicated for five minutes at 100% amplitude, till a homogeneous suspensions was achieved, it was pursued of magnetic stirring by 5 minutes. The magnetic stirring and sonication processes were substituting every 5 minutes until the desired time had been obtained for sonicating samples. Consequently by studying on thermal performance of all nanofluids dispersed by different dispersant, the superior surfactant will be considered for experiments to obtain best results. The sample preparation set-up is shown in Figure 3-5

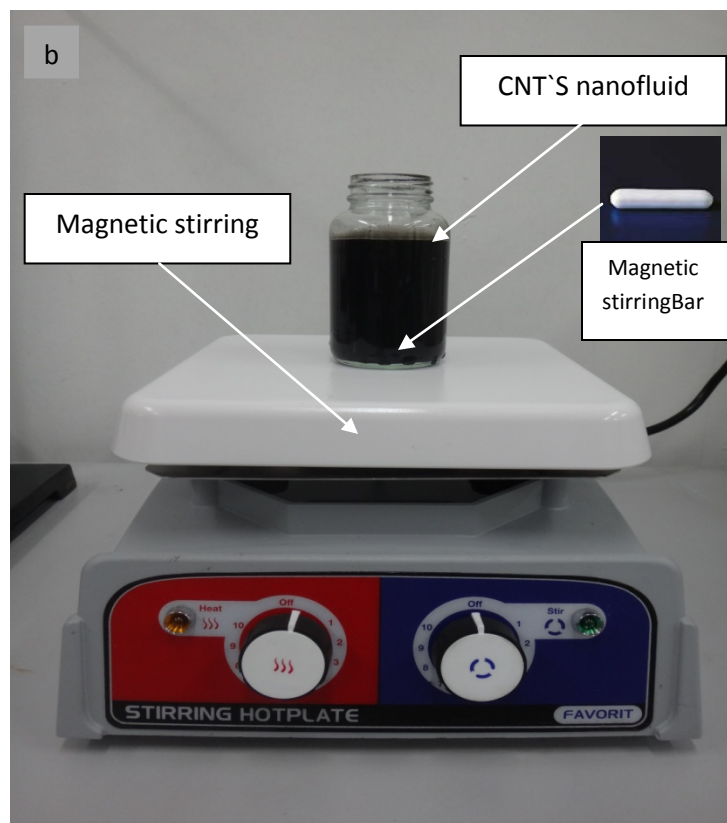
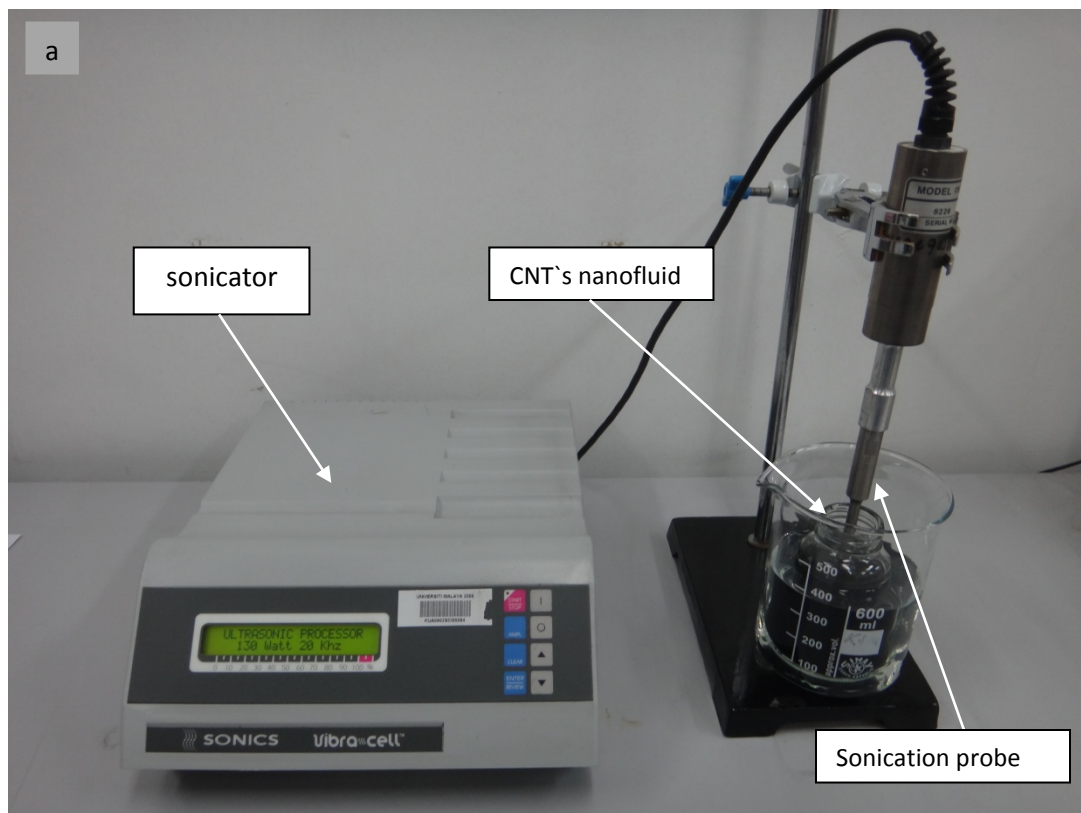


Figure 3-5 nanofluids preparation set-up: (a) Ultrasonication; (b) magnetic stirring

By using this technique the prepared samples were observed to be stable with no settling or sedimentation over 10 days, Figure 3-6 shown a homogeneous dispersion for the samples which dispersed by GA as a surfactant.



Figure 3.6 Vials including 0.5 wt % of MWCNT` s disspered in distilled water after 2 weeks and different ultrasonication times: (a) 50 minutes; (b) 100 minutes; (c) 150 minutes; (d) 200 minutes.

3.3 Brief of experiments

Table 3-3 presented the brief of experimental research carried out on the samples

Imaging	viscosity measurements	Thermal Conductivity measurements
Imaging of samples by using TEM technique	Temperatures of 30 °C and 15 °C at variable shear rates	Temperature range of 20 to 45 °C with step size of 5 °C

Table 3.3 Experiments list

CHAPTER FOUR: RESULTS AND DISCUSSION

This chapter presents the data obtained from thermal conductivity and viscosity measurements, and discusses these results in context of fundamental theory and past research.

4.1. Imaging data

Figures 4-1 to 4-4 show the pictures of Samples 1,2,3, and 4 which ultrasonicated for 50,100,150 and 200 minutes respectively as described in chapter 3 at a scale of 500 nm, using TEM technique.

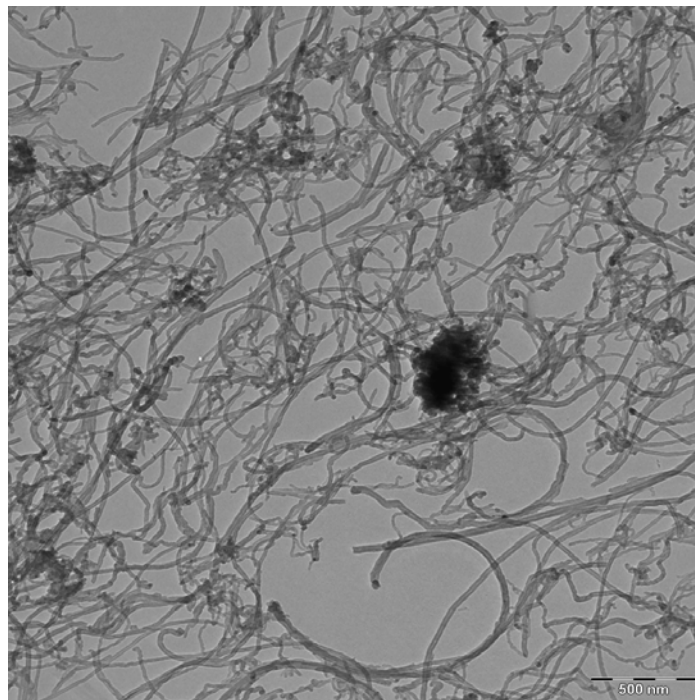


Figure 4-1 TEM image of Sample 1 at 500 nm scale. (50 min sonication, 0.5 wt % MWCNT, 0.25 wt % GA)

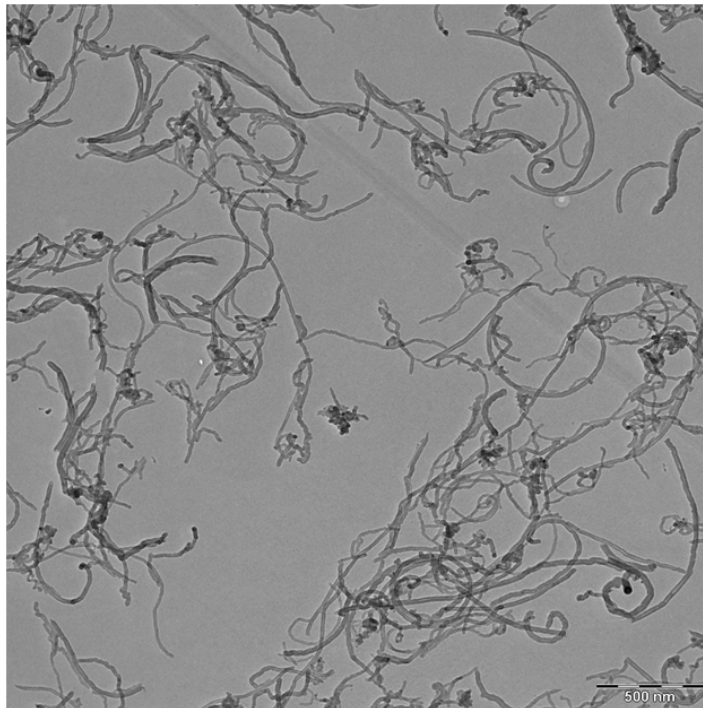


Figure 4.2 TEM image of Sample 2 at 500 nm scale. (100 min sonication, 0.5 wt % MWCNT, 0.25 wt % GA)

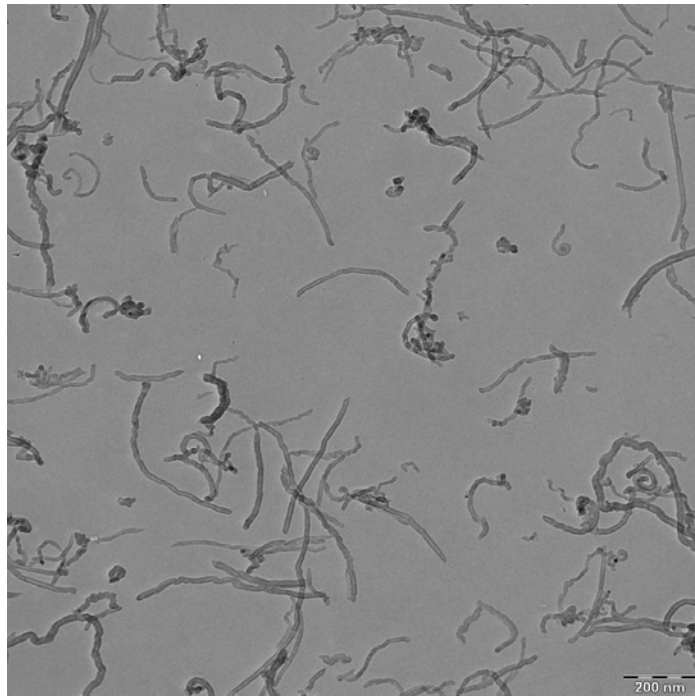


Figure 4.3 TEM image of Sample 3 at 500 nm scale. (150 min sonication, 0.5 wt % MWCNT, 0.25 wt % GA)

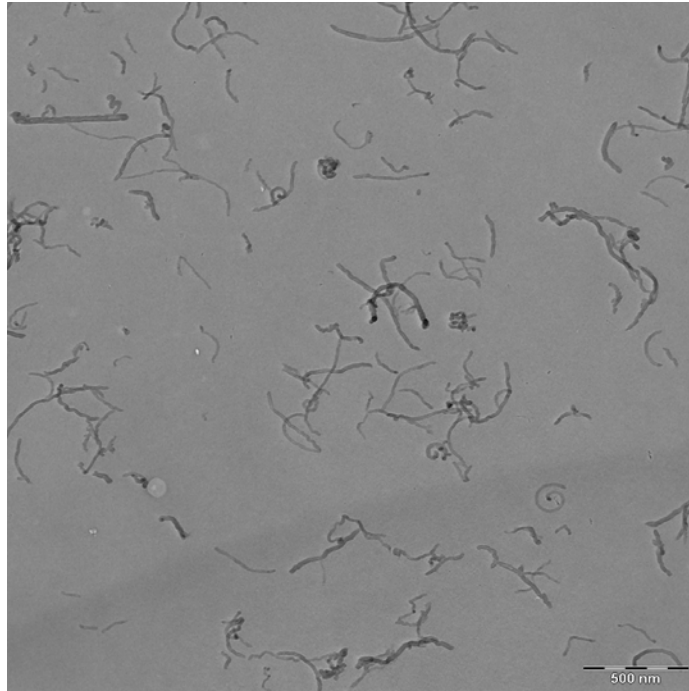


Figure 4.4 TEM image of Sample 4 at 500 nm scale. (200 min sonication, 0.5 wt % MWCNT, 0.25 wt % GA)

From Figure 4-1, it can be seen that Sample 1 exhibits a united cluster of carbon nanotubes. In contrast, from Figures 4-2, 4-3 and 4-4 , the nanotubes are freely placed without a uniform clusters structure which broken into pieces, this observation can be attributed to more ultrasonic processing in case of Samples 2, 3 and 4.

This can be further explained in more detail by comparing Samples 1 to 4. The figures show the formation of aggregates in the nanofluid since the nanofluid prepared, and by increasing the sonication time the aggregates size decreases, so it causes the length of the carbon nanotubes is also reduced. Comparing sample 4 & 1 observed also from the figures that the length of the nanotubes has been reduced in Sample 4 as compared to Sample 1, therefore a decline in length lead to reduction in aspect ratio of carbon nanotube. This phenomenon is generally consistent with Pohl et al. (Jang & Choi, 2004), the length of the

carbon nanotubes can be expressed as a function of the sonication specific energy E_v (sonication energy per unit volume):

$$L = AE_v^m$$

Where L is the length of the carbon nanotube, and A and m are constant. Yang et al. (Yang et al., 2006) recommended an alternate form of (equation 1), when the specific energy input is stable and the volume of dispersion is constant:

$$L = Bt^n$$

Where B and n are constants and t is sonication time. The value of n was measured -0.2742 by Yang et al. (Yang et al., 2006).

The imaging result would be correlated to the thermo-physical properties of each sample in following parts of this chapter.

4.2 Thermal conductivity Results

4.2.1 Base liquid

In order to establish the reliability and accuracy of our Thermal conductivity measurement set-up, thermal conductivity of base liquid (water) depending on temperature is measured and compared with the ASHRAE data (Wessel, 2001). Figure 4-1 shows the deviation of water thermal conductivity measurements in comparison with ASHRAE data (Wessel, 2001). Experimental results are showing a good agreement with reference data. All the measurements for DW Water were found to be within 1.9 % of the ASHRAE values. The specified accuracy of the Instrument was 5 %. This graph significantly verified the reliability of our subsequent waterbase nanofluid results. Based on Figure 4-1, thermal conductivity increases with rise of temperature in water base liquid.

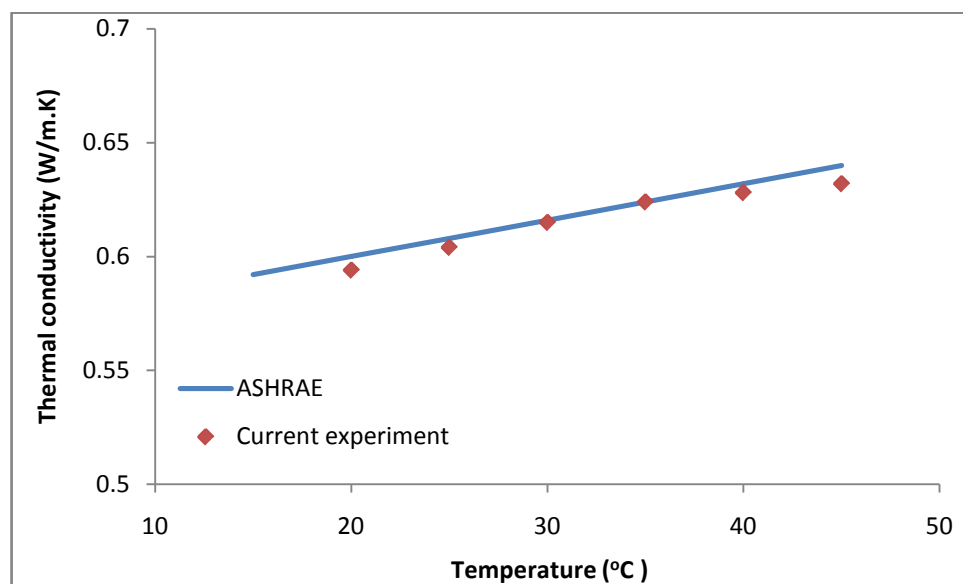


Figure 4.1 Benchmark test for water thermal conductivity

4.2.2 Base fluid Data reproducibility

Thermal conductivity measurement has shown a very well data reproducibility, which shows high reliability of KD2 Pro device and environmental stability at working temperature range (20 to 45°C). Figure 4-2 depicts thermal conductivity reproducibility for water. Comparison between first and second measurements shows maximum 1.4% error at 40 and 45°C. It can be obtained that thermal conductivity measurement accuracy reduces with rising temperature. Average value of first and second data has been used for further experiments.

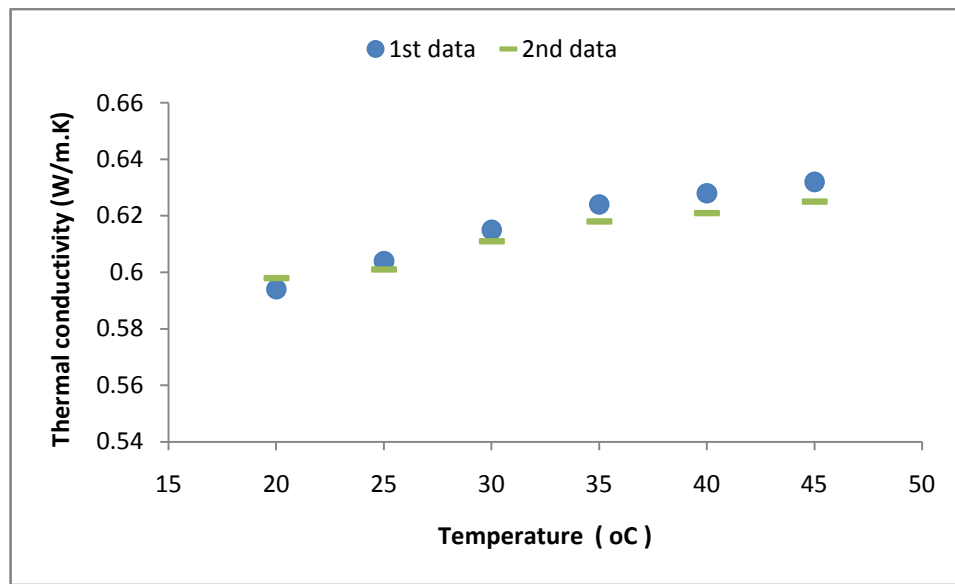


Figure 4.2 Data reproducibility for water as a function of temperature

4.2.3 SDBS, SDS and Gum Arabic dispersed in base fluid

In order to further understand how the surfactants influence nanofluid and distinguish which of the three is superior to the other in aqueous CNT suspensions, it is very necessary to investigate how the surfactants affect on thermal conductivity in their base fluid DW. Thus 0.25 wt% of each Gum Arabic, SDBS and SDS in addition 0.5 wt% of SDBS and SDS are

dispersed in DW and thermal conductivities of these solutions are measured respectively and the values are graphically compared with those of DW as shown in Figure 4-3. Since the 0.25wt% amount of GA is proven to achieve optimum stability and thermal conductivity, it is refused to using 0.5wt% amount of it. The results demonstrate that both surfactants in solutions suppress the thermal conductivity of DW. Furthermore, the thermal conductivity of DW decreases with increasing loading of all surfactants. Comparing the three surfactants in DW with the same loading, obviously GA is superior to SDS and SDBS because GA influences much less than SDS and SDBS on weakening thermal conductivity of base fluid in this figure, as shown in the figure, the thermal conductivity variation is steady over the temperature. Moreover, it seems that the thermal conductivity of DW with SDS is decreased more at higher temperature compared with that of SDBS and GA solution.

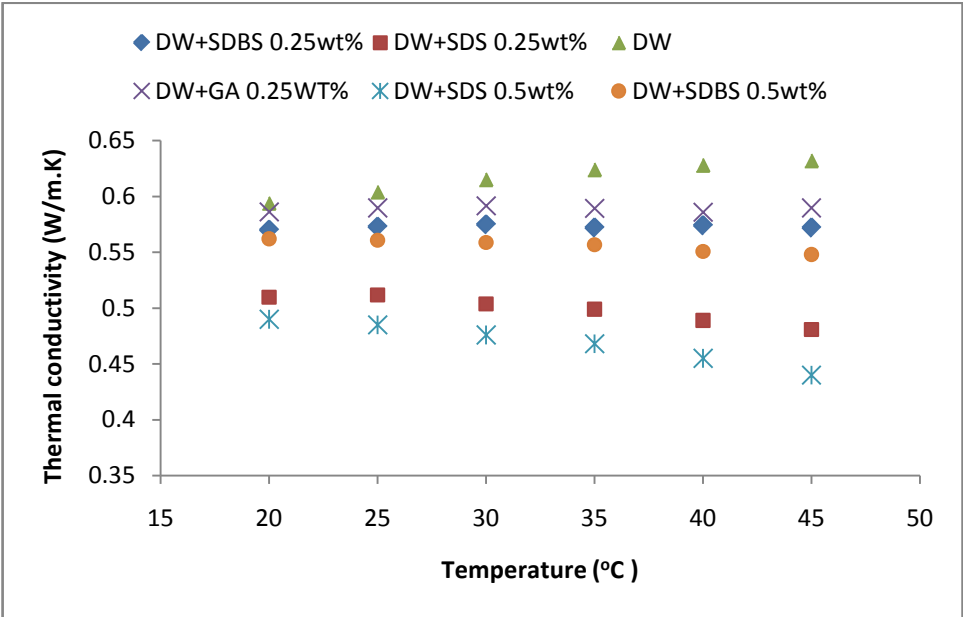


Figure 4.3 Comparison between GA, SDBS and SDS surfactant thermal conductivities

4.2.4. Effects of dispersed GA, SDBS and SDS on thermal conductivity of MWCNT Nanofluids

According to the Figure 4-4 it has been studied the effect of Three kinds of surfactants (GA, SDBS, SDS) with same concentrations (0.25wt%) on thermal conductivity of CNT`s nanofluids, Under this prescription, Fig. 4-4 graphically shows the thermal conductivity variation of CNT nanofluid at 0.5 wt.% as temperature increased. It indicates that the thermal conductivity of CNT nanofluid with SDS tendsto decrease along with the increasing temperature; probably the key reason is that SDS surfactant suppressed thermal conductivity more in base fluid which is illustrated in Figure 4-3, whereas the thermal conductivity ofnanofluids with GA and SDBS disposed to augment with increase in temperature. also it can be observed CNT`s nanofluidcontaining GA show greater thermal conductivity range than that with SDS and SDBS suspensions. According to the Figures 4-3 and 4-4 it can be proven that the GA is superior to both SDS and SDBS in thermal performance of CNT`s suspensions. Consequently GA is a excellent choice as a surfactant for MWCNT`s nanofluids in this experimental study. (All samples include in both Figures 4-3 & 4-4 sonicated for 100 minutes)

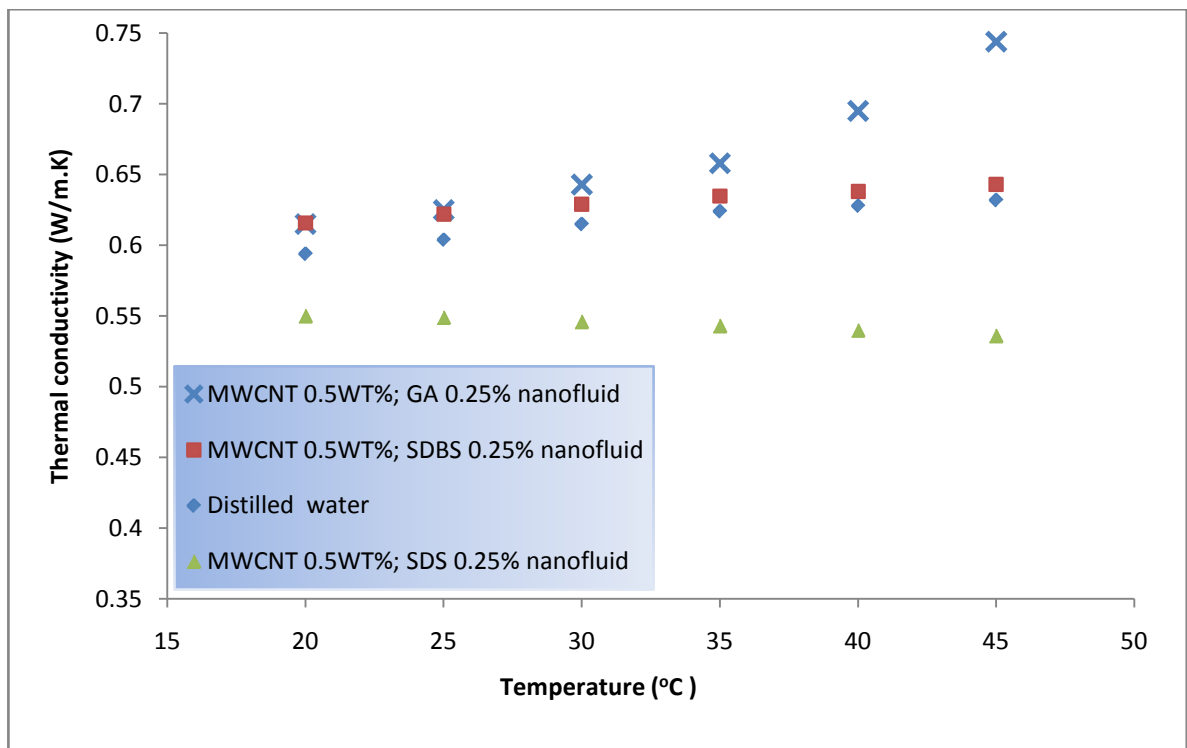


Figure 4.4 Comparison between the thermal conductivities of CNT's Nanofluids contain GA, SDBS and SDS surfactants

4.2.5 Effects of various ultrasonication time and Temperature on thermal conductivity of MWCNT's Nanofluids

Figures 4-5 presents the absolute thermal conductivity values of MWCNT's-water nanofluids with 0.5 wt% of MWCNT nanoparticles, temperature range contained in Figure 4-5 is from 20 to 45 °C. the data obtained using KD 2 Pro thermal properties analyzer. Measurements are taken for different sonication times as a function of Temperature, during sonication at 20 KHz and 100% amplitude, bubbles are created and collapsed, and the resulting shock from this cavitation process breaks up nanotubes agglomerates. However, the process also generates heat and the nanofluid temperature rises, in order to mitigate evaporation of the base fluid during sonication, a cooling system was employed during the

sonication, maintaining a sample temperature at about 25 c.each reported measurement is the average of six reading and the specified accuracy of the instruments was 3 %.

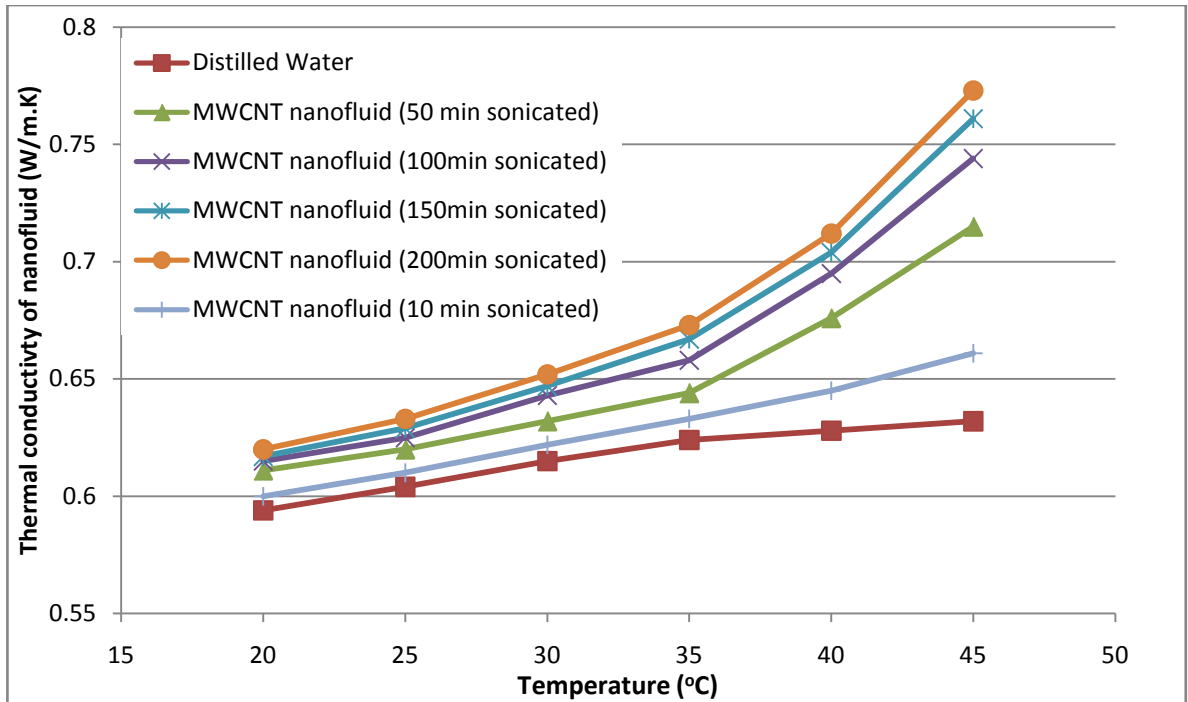


Figure 4.5 Thermal conductivity variations as a function of temperature at different ultrasonication times

As presented in figures 4.5 the temperature affects the thermal conductivity of the nanofluids. It has been observed an increase in thermal conductivity of MWCNT-water nanofluids with increase in temperature. The thermal conductivity data for water at this temperature range have also been included for comparison. The thermal conductivity increase of nanofluids with temperature is greater than the thermal conductivity increase of DI water.

Unlike water, the thermal conductivity of the nanofluid first increased slightly with temperature and after 30°C it increases nonlinearly with temperature. Figure 4-5 Indicated that the increased thermal conductivity at higher temperatures is not attributed to the corresponding increase in the thermal conductivity of base fluid alone. One of the

suggested reasons behind this phenomenon is the increased Brownian motion effect. A Amrollahi et al. (Amrollahi et al., 2008) suggested that, since random Brownian motion of the suspended nanoparticles shows a strong dependence on temperature, it is expected that the thermal conductivity of a nanofluid will vary remarkably with the suspension temperature. The frequency of the ambient fluid molecules increases as the nanofluid temperature increases so that the frequency of random motion and the averaged velocity of the nanoparticles increase, therefore the energy transport contribution is enhanced by increasing the temperature. On the other hand Jang and Choi. (Jang & Choi, 2004) suggested that, as the temperature is increased, the viscosity of the nanofluid decreases, which results in increase in Brownian motion of nanoparticles, which sets convection-like effects resulting in enhanced thermal conductivity. A strong effect of temperature on thermal conductivity of MWCNT dispersed in water also observed by Ding et al. (Ding et al., 2006).

The ratio and enhancement of nanofluid thermal conductivity to that of base fluid (DI water), are plotted in Figures 4-6 and 4-7 respectively. The influence of temperature on the thermal conductivity ratio of CNT nanofluids is obvious in Figures, the both thermal conductivity enhancement and ratio augmented from 2.02% to 22.31% and 1.2 to 1.22 respectively for all MWCNT suspensions included 0.5 wt% MWCNT and sonicated from 20 to 200 minutes. A highest augment of 22.31% was achieved for sample 4 (0.5 wt% MWCNT, 0.25 wt% GA, sonicated for 200 minutes) at a temperature of 45°C.

Since The MWCNT provided by the supplier contained the average density of 2.1 gm/cm³, the volume fraction of the nanopowder used in current experiment would be approximately 0.24 vol%. By comparing presented data with the work done by A. Indhuja et al. (Indhuja et al., 2013), it can be shown that the thermal conductivity ratio data in the current study is almost 5% higher than that reported by A. Indhuja et al. (Indhuja et al., 2013) for 0.5 wt%

MWCNT suspensions which was dispersed by GA. the higher thermal conductivity may be caused by the different ultrasonication processor and dispersing method of CNT used in current experiment. The thermal conductivity enhancement reported by T.X Phuoc et al.(Phuoc et al., 2011) were 2.4% and 4.3% with 0.5 and 1 wt% MWCNT (aspect ratio ~ 500-1000) respectively at 25 °C, and that by L. Chen, H. Xie.(L. Chen & Xie, 2010a) was almost 15% with 0.3 vol % (~0.63 wt %) MWCNT (aspect ratio ~400-670)at 45 °C.Hence, it can be said that both T.X Phuoc et al.(Phuoc et al., 2011)and L. Chen, H. Xie.(L. Chen & Xie, 2010a)used higher CNTs concentrationthan in this experiment. Nonetheless, thethermal conductivity enhancement values achieved in this study are much higher than both studies.This increase may be dependent on the type of dispersant (GA) used in current experiment.The thermal conductivity ratio shown in Figure 4-6 is much lower than that reported by Ding et al.(Ding et al., 2006)(i.e. 1.1 at 0.5 wt% MWCNT at 20 °C),in spite of the fact that the CNT`s concentration used in both studies is same. The exact reason for this difference is uncertain but it may be associated with thermal and physical properties of the MWNTs used and different dispersion method employed in both works. Moreover Ding et al (Ding et al., 2006) didn`t mention the aspect ratio (L/D) of MWCNT utilized, and it may be different from that (~ 500-1000) in current study.

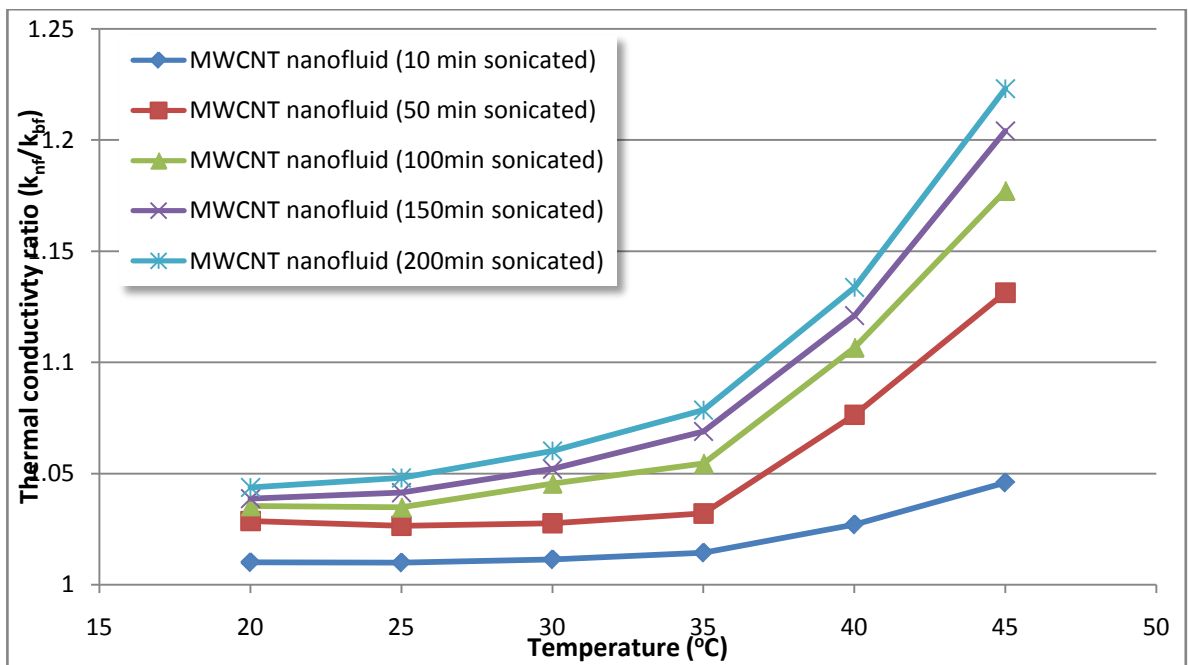


Figure 4-6 variation of Thermal conductivity ratio as a function of temperature at different ultrasonication times

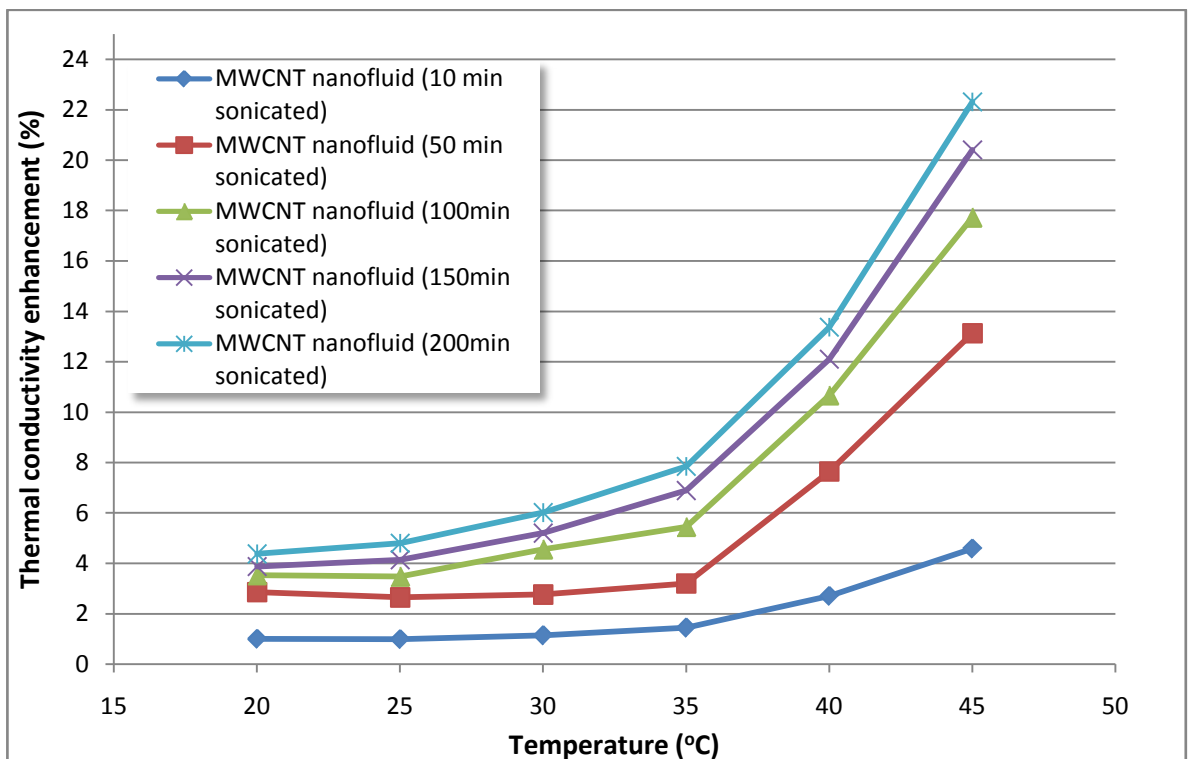


Figure 4-7 variation of Thermal conductivity enhancement as a function of temperature at different ultrasonication times

Figures 4-8 and 4-9 showed the thermal conductivity enhancement and thermal conductivity ratio of MWCNT suspensions, with 0.5 wt% of MWCNT nanoparticles as a function of ultrasonication processing at different temperatures. It is apparent from following figures that the thermal conductivity of the nanofluid initially enhances rapidly when ultrasonication time increases and it gradually reaches a peak at around 200 hours sonication.

The reason for this phenomenon may be associated with the breaking nanoparticles aggregation into smaller dimensions. A Amrollahi et al (Amrollahi et al., 2008) observed that shorter clusters move faster and include a stronger energy transport inside the nanofluid. It proposed a more steady dispersion of multi-walled CNT nanoparticles which most likely contributes to the enhancement in thermal conductivity with ultrasonication time presented in figures 4-8 and 4-9 by observing the figures 4-1 to 4-4 this impact is verified microscopically.

But on the other hand, Assael et al. (Assael et al., 2004) showed that a decline in aspect ratio reduces the enhancement of thermal conductivity. However Ruan and Jacobi (Ruan & Jacobi, 2012) proven that the effect of decline in aspect ratio on thermal conductivity is not very much compared to the enhancement of thermal conductivity resulted in reduction of clusters size.

Additionally A Amrollahi et al (Amrollahi et al., 2008) concluded that when the particles get agglomerated, The effective surface area to volume ratio decreases therefore reducing the effective area of thermal interaction of particles, result in decline in the nanofluid thermal conductivity.

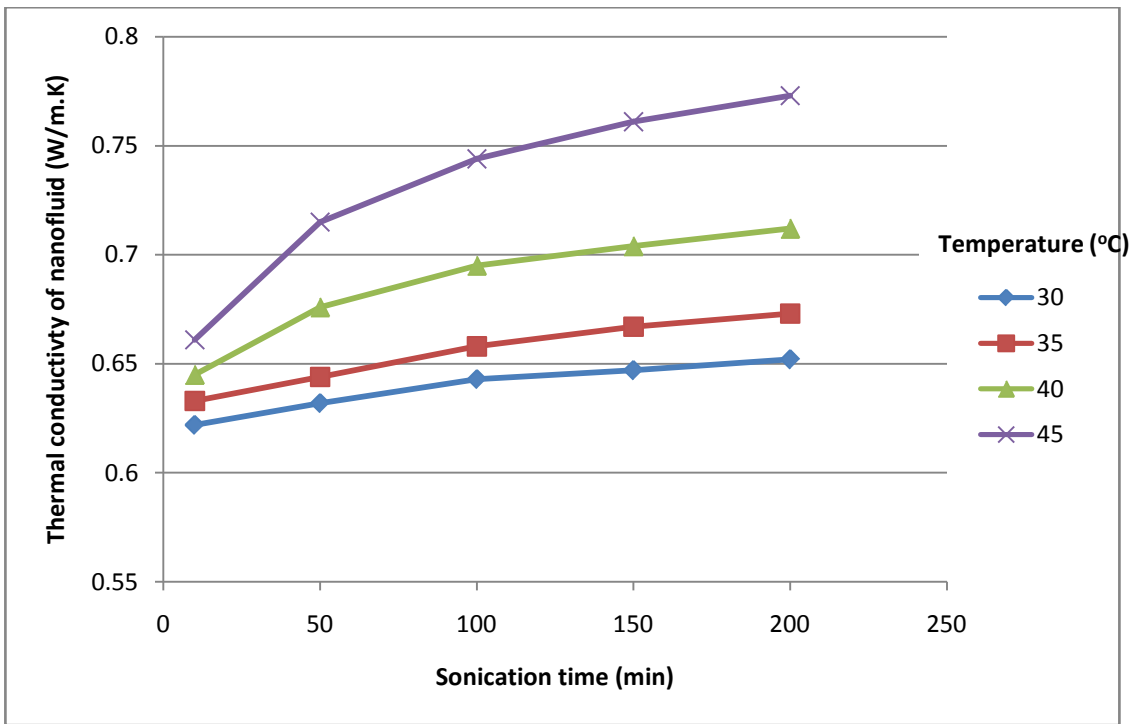


Figure 4-8 Thermal conductivity variations as a function of ultrasonication time at different temperatures

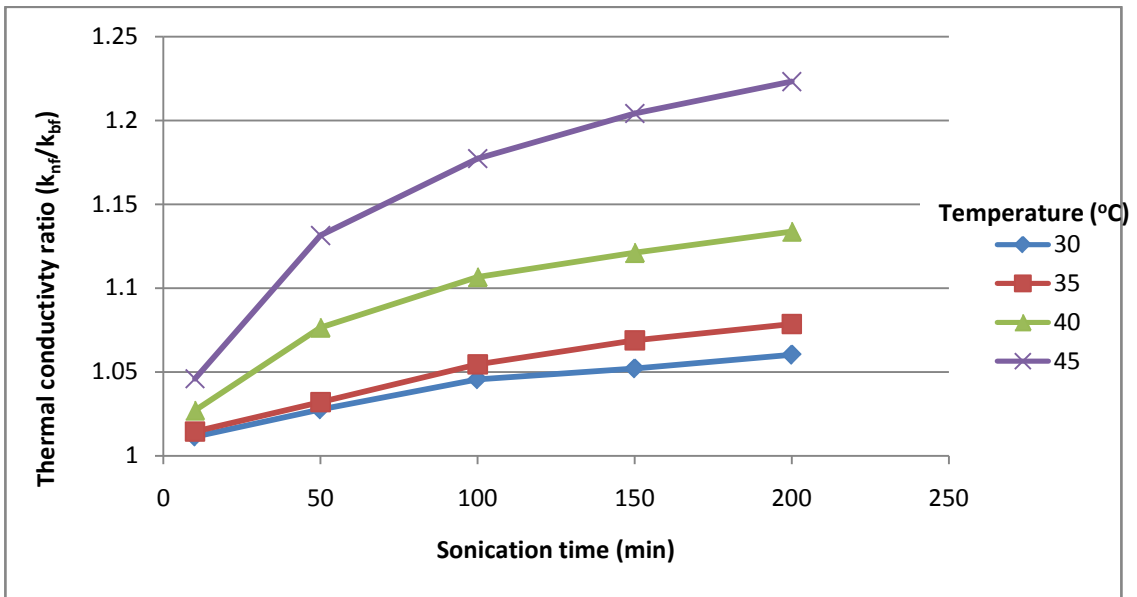


Figure 4-9 the variation of thermal conductivity ratio as a function of ultrasonication time at different temperatures

4.2.6 Study of stability of MWCNT nanofluid by reproducing the Thermal conductivity

One procedure to examine the stability of nanofluids and for any possible sign of visible sedimentation is to experiment the colloidal suspensions properties over a period of time. The stability of the MWCNT-water nanofluidsonicated for 200 minutes is repeated for 10 days. As shown in Figure 4-10, it can be observed that there is very small deviation in the measured thermal conductivity ofnanofluids. Thus the nanofluid stability is verified by monitoring the thermal conductivity of the suspensions at 40 °C for 10 days periodically.

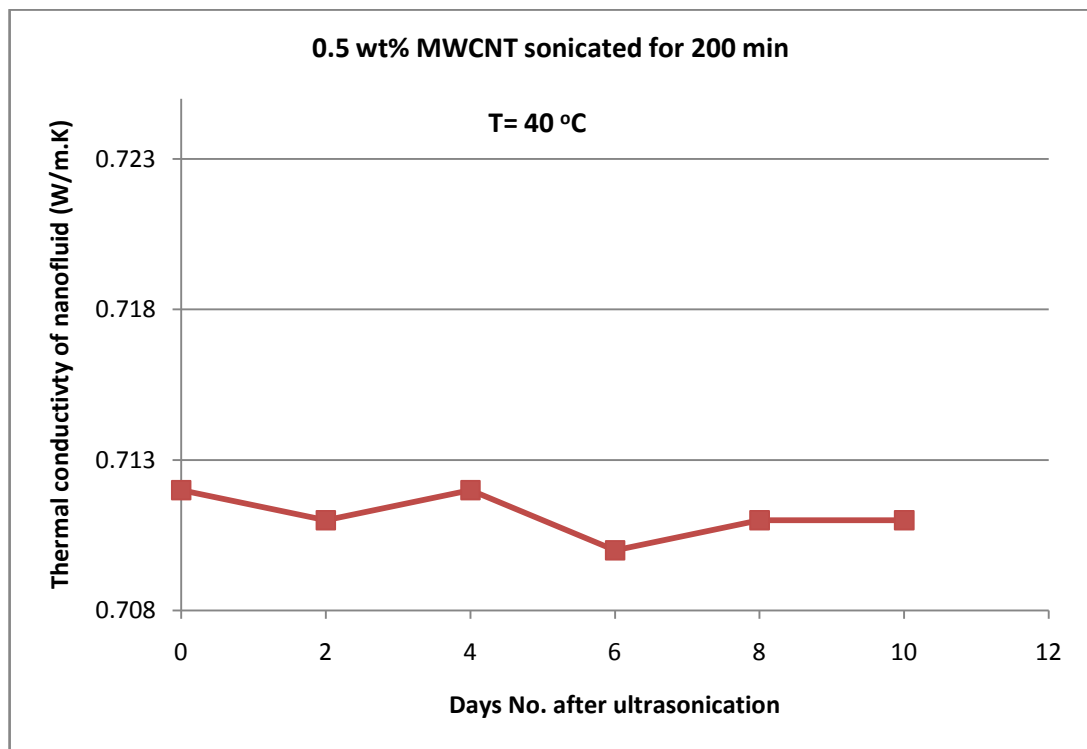


Figure 4.10 Reproducibility of thermal conductivity data within 10 days

4.3 Viscosity result

The viscosity of MWCNT-Water nanofluids stabilized by GA was measured as a function of shear rate under different ultrasonication times. Figures 4-10 and 4-11 are presented these results for 0.5 wt% MWCNT and 0.25 wt% GA at Temperatures 30 and 15°C respectively. The pure distilled water viscosity was measured prior to measure the nanofluid viscosity and compared to the result from literature to confirm the accuracy of system. The data displayed no dynamic viscosity variation with an increase in shear rate for pure distilled water. Unlike water, it can be obviously observed from both figures 4-10 and 4-11 that the MWCNT- water nanofluids behave as a non-Newtonian fluid, it is because the dynamic viscosity changes while the shear rate increases.

A shear thinning behavior was observed, which was also observed by Yang et al (Yang et al., 2006) , (Garg et al., 2009), N. Singhet al (Singh et al., 2012), T.X. Phuoc et al (Phuoc et al., 2011) and Ruan and Jacobi (Ruan & Jacobi, 2012) for CNT nanofluids, causing a decline in dynamic viscosity with increase in shear rate. It can be seen that, the viscosity dramatically reduces in lower shear rates and consequently it becomes constant gradually in the higher range of shear rate. The reason could be that since the nanofluid at the parallel plates is in under pressure at high shear force, which leads to break the carbon nanotubes bundled clusters and agglomerations or realignment in the shearing force direction, resulting in a decrease in viscosity and resistance to flow. Also it can be observed that dynamic viscosity of MWCNT which sonicated for 200 minutes indicates more plane viscosity deviation when the shear rate increases in both temperatures 15 and 30 ° C. by comparing figures 4-10 and 4-11, it is obvious that the viscosity of MWCNT suspensions was found to be reduced by elevating the temperature

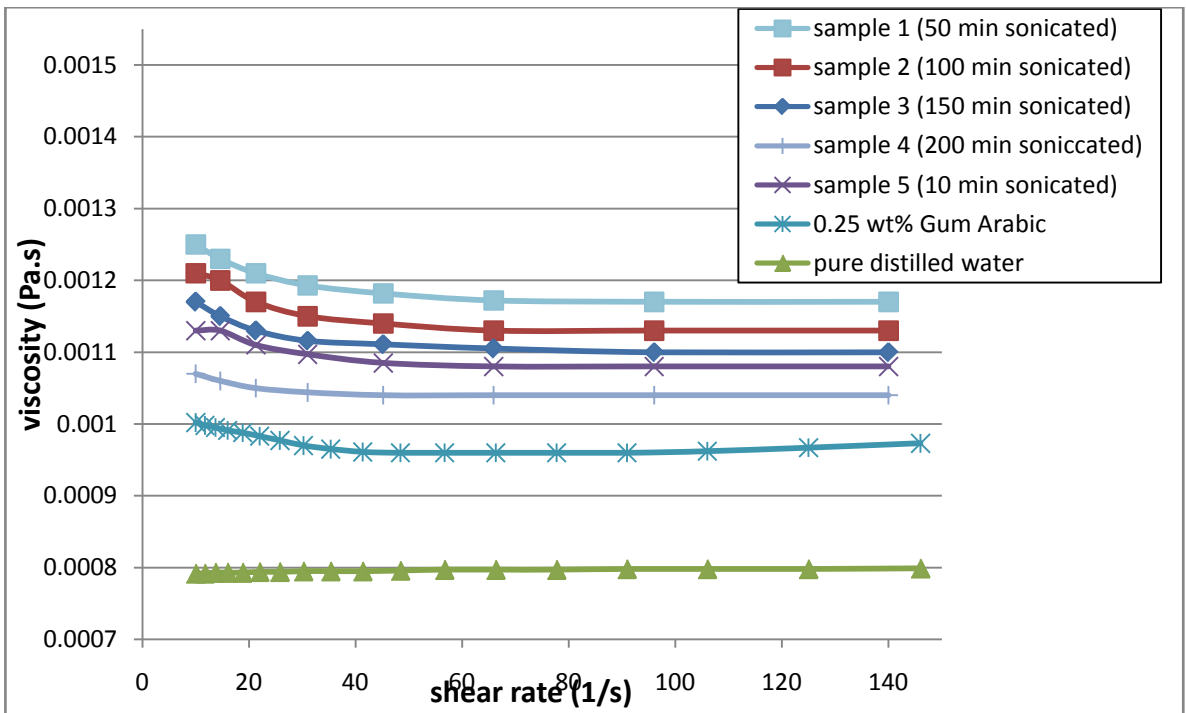


Figure 4-10 The fluctuation of Dynamic viscosity as a function of shear rate at 30 o C

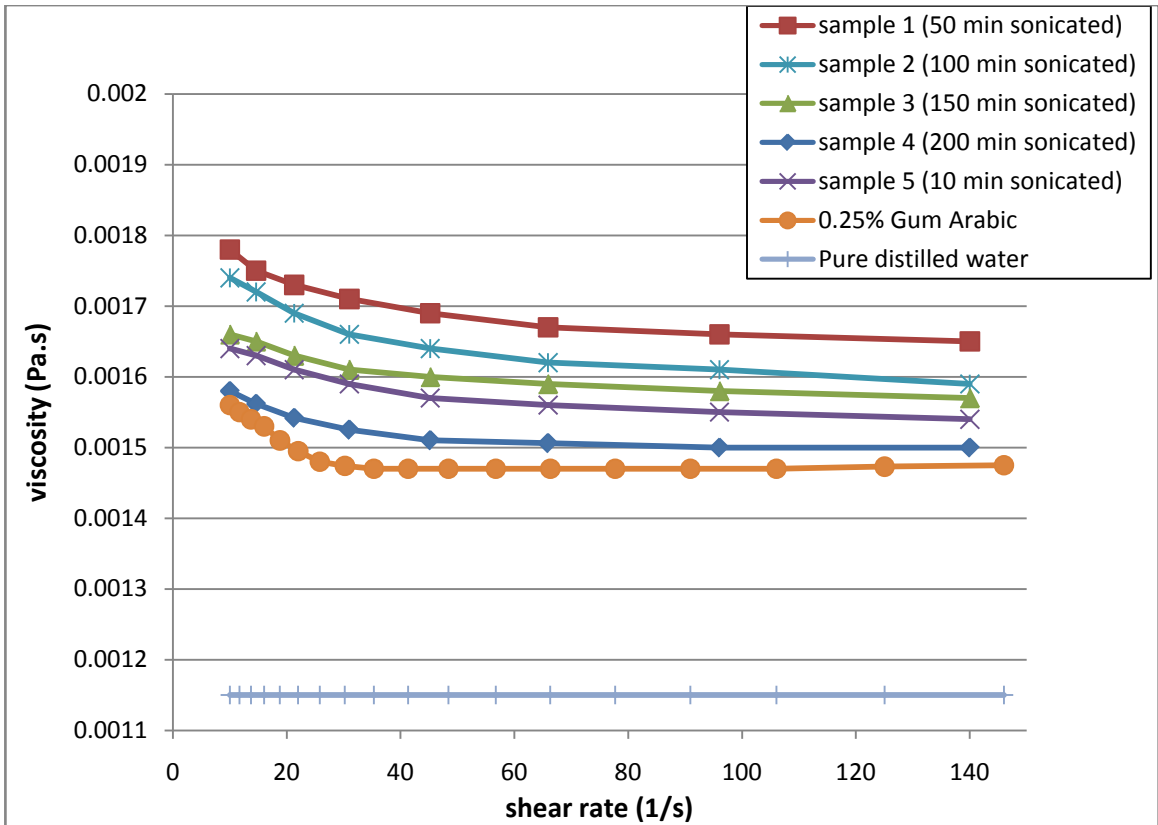


Figure 4-11 The fluctuation of Dynamic viscosity as a function of shear rate at different sonication time (15o C)

Furthermore, figures 4-12 and 4-13 present the dynamic viscosity of MWCNT`s suspensions against ultrasonication time at four different shear rates. It can be observed from both figures that at the same shear rate, the viscosity of MWCNT nanofluids first enhanced from sample 1 (sonicated for 10 min) to sample 2 (sonicated for 50 min), then declined dramatically with an increment in ultrasonication time. In addition, it is obvious that the viscosity of carbon nanotube nanofluid at low shear rates is higher compared to the larger shear rates at a same shear rate. the reason can be described that a agglomerated and non-dispersed nanofluids having lower viscosity than a dispersed nanofluids, because of increased interactions of attractive surface causing a larger surface to volume ratio in dispersed nanotubes suspensions(Starr, Douglas, & Glotzer, 2003)

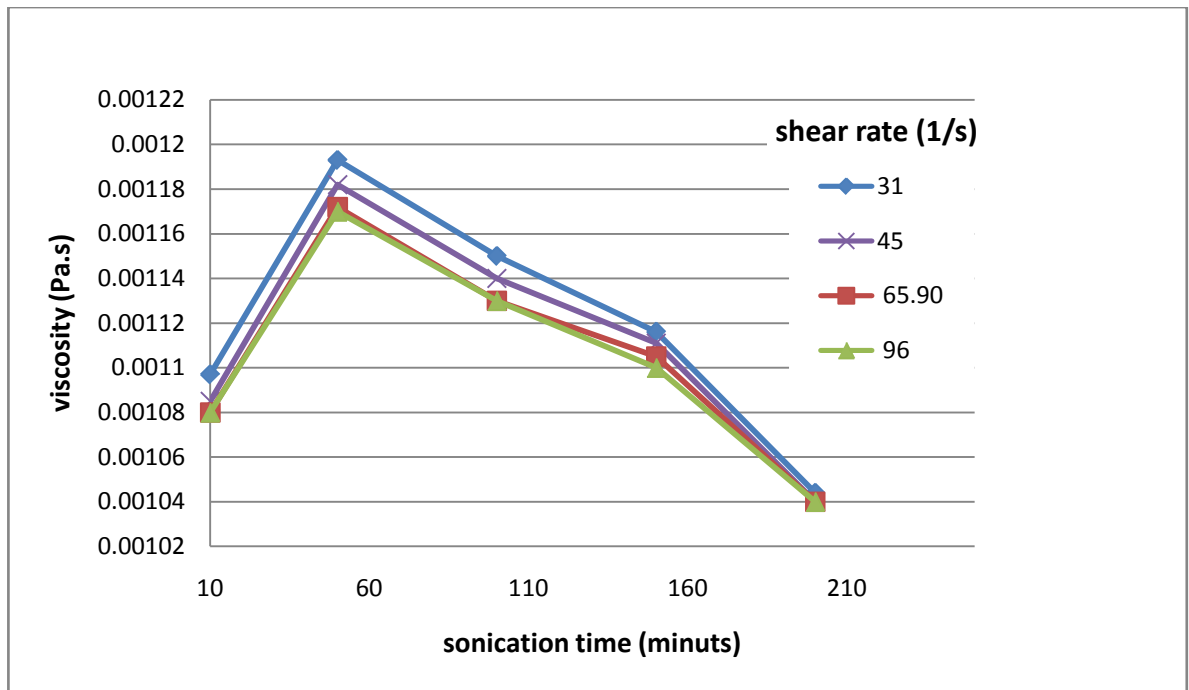


Figure 4.12 The fluctuation of Dynamic viscosity as a function of sonication time at different shear rates (30 oC)

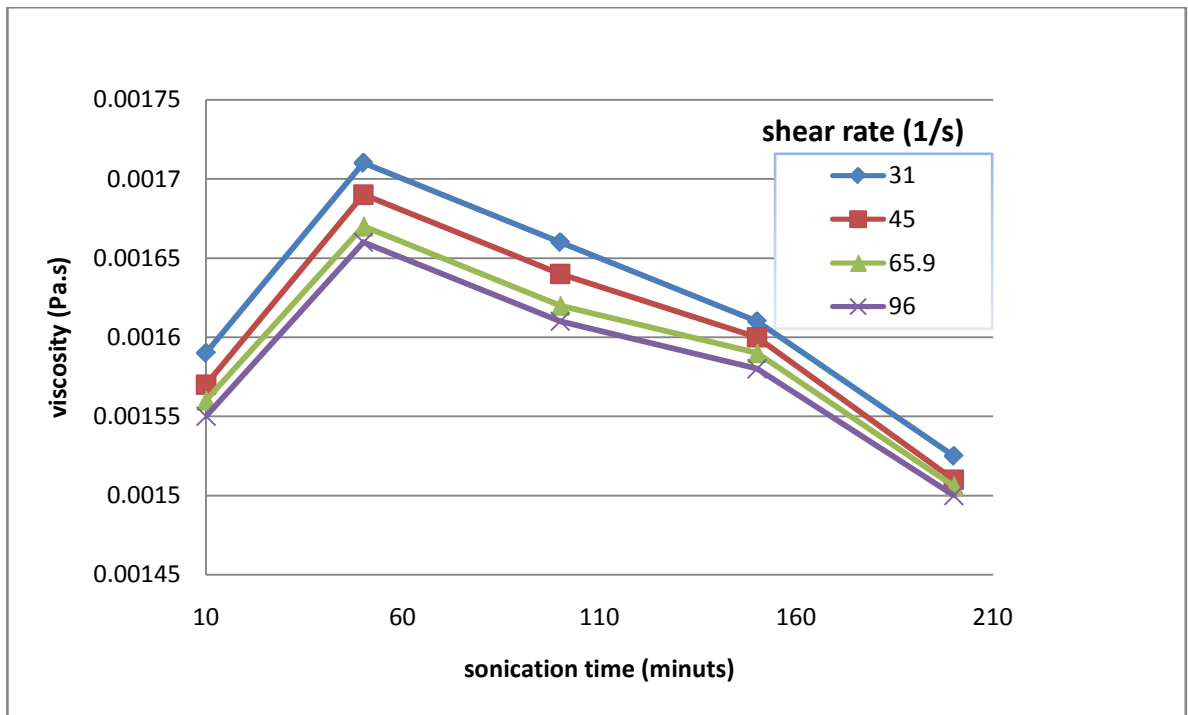


Figure 4-13 The fluctuation of Dynamic viscosity as a function of sonication time at different shear rates (15 oC)

Well-dispersed nanofluids display higher dynamic viscosity due to increase in surfaces of enclosed nanoparticles was much higher than that in the agglomerated and clustered nanofluids. In this research, it can be proposed that less sonication in sample 1 (10 min sonication) resulted in high agglomeration, but on the otherhand, sample 2 (50 min sonication) shown a steady dispersion causing higher viscosity than sample 1 (10 min sonication). For further ultrasonication (after 40 min) the dynamic viscosity dramatically declined by increase in sonication time. Breaking the carbon nanotubes bundled clusters and agglomerations may be the exact reason for this phenomena (Amrollahi et al., 2008; Garg et al., 2009; Ruan & Jacobi, 2012). Consequently it could be approved by TEM images in Figures 4-1 to 4-4.

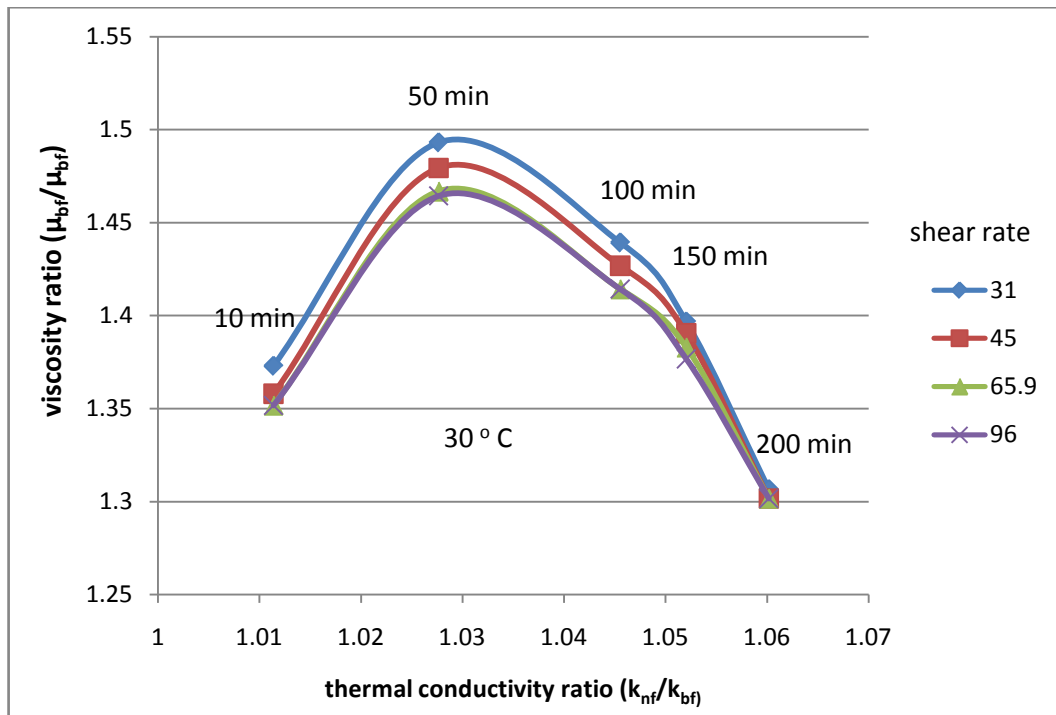


Figure 4-14 The variation of viscosity ratio of MWCNT suspensions against thermal conductivity ratio under different shear rates at 30° C

Figure 4-14 showed the viscosity ratio of MWCNT–water nanofluids as a function of thermal conductivity, under different shear rates at 30° C. It can be seen that the viscosity ratio increases in lower sonicated samples and consequently decreases dramatically with an increase in thermal conductivity and sonication time. Conclusively, the smallest viscosity and the greatest thermal conductivity could be achieved by a long ultrasonication time for MWCNT- water nanofluids, this detection could be very significant for the nanofluids applications of heat transfer.

CHAPTER FIVE: CONCLUSION

5.1 Imaging conclusion:

- The figures indicate that the aggregates are formed in the nanofluid during preparation but with the increase of sonication time, aggregates size decreases, and it also causes the length reduction of the carbon nanotubes which resulted decrease of the aspect ratio.

5.2 Thermal conductivity conclusion:

- Thermal conductivity measurement of water showed well data reproducibility by KD2 Pro device at the working temperature range of (20 to 45 °C).
- CNT nanofluids containing GA shows greater thermal conductivity range than those with SDS and SDBS suspensions thus GA is an excellent choice of surfactant for preparation of MWCNT nanofluids.
- Unlike water, the thermal conductivity of the nanofluids first increased slightly with temperature and after 30 °C, it elevated nonlinearly with temperature due to increased Brownian motion effect. The Greatest enhancement of thermal

conductivity 22.31% could be obtained at sonication 200 minutes at a temperature of 45°C for the sample number 4.

- The thermal conductivity of the nanofluid enhances rapidly at the beginning with the increase of ultrasonication time and it gradually reaches a peak at around 200 hours sonication due to breaking of nanoparticles aggregation into smaller dimensions as the shorter clusters move faster with the stronger energy transport inside the nanofluid.
- The lowest viscosity and the highest thermal conductivity could be achieved by a long ultrasonication time for MWCNT- water nanofluids, this indication could be very significant for the application of nanofluids in heat transfer.

5.3 Viscosity conclusion:

- MWCNT aqueous solution showed a non-Newtonian and shear-thinning behavior due to breaking of the carbon nanotubes bundle clusters and agglomerations with the increment in shear rate.
- The dynamic viscosity of the nanofluid enhances with the increase of ultrasonication time up to the highest value and then declines thereafter. The viscosity of MWCNT suspensions reduces with the rise of temperature.

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