

CHALCONE BASED DITHIOCARBAMATE  
DERIVATIVE INCORPORATED SOL-GEL FOR THE  
REMOVAL AND PRE-CONCENTRATION OF  
AQUEOUS MERCURY(II) ION

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FACULTY OF SCIENCE  
UNIVERSITY OF MALAYA  
KUALA LUMPUR

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AQUEOUS MERCURY(II) ION**

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**ORIGINAL LITERARY WORK DECLARATION**

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Name of Degree : Master of Science (Except Mathematics & Science Philosophy)

Title of Dissertation (“this Work”):

Chalcone based dithiocarbamate derivative incorporated sol-gel for the removal and pre-concentration of aqueous mercury(II) ion

Field of Study : Environmental Chemistry

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**CHALCONE BASED DITHIOCARBAMATE DERIVATIVE INCORPORATED  
SOL-GEL FOR THE REMOVAL AND PRE-CONCENTRATION OF  
AQUEOUS MERCURY(II) ION**

**ABSTRACT**

This study demonstrated the application of chalcone based dithiocarbamate derivative as metal capturing ligands for the removal and pre-concentration of mercury ion ( $\text{Hg}^{2+}$ ). Chalcones are a group of naturally occurring compounds, which can be extracted from fruits, vegetables, plants, and spice. In the first part of this work, chalcone was first chemically modified to produce dithiocarbamate derivative, 3-oxo-1,3-diphenylpropyl-2-(naphthalen-2-ylamino) ethylcarbamodithioate (ODPPNE). After that, chalcone incorporated sol-gel (SG-C) and ODPPNE incorporated sol-gel (SG-ODPPNE) were prepared and used as adsorbents to remove  $\text{Hg}^{2+}$ . The result showed that with the presence of dithiocarbamate functional group, SG-ODPPNE exhibited the high selectivity toward  $\text{Hg}^{2+}$  adsorption as compared to other metal ions. The effect of operating conditions (such as the size of adsorbent, adsorbent dosage, contact time, the initial concentration of  $\text{Hg}^{2+}$  and pH of solution) were examined for the adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE. The adsorption data were fitted well to Langmuir isotherm, and the monolayer adsorption capacity was found to be 13.5 mg/g. In the adsorption kinetic study, the obtained data were well fitted to pseudo-second order model. According to intraparticle diffusion model, the adsorption process of  $\text{Hg}^{2+}$  by SG-ODPPNE involves film diffusion, intraparticle diffusion, and equilibrium stages. For the second part of this study, ODPPNE incorporated silica was coated onto magnetic nanoparticle (ODPPNE@MNP). This ODPPNE@MNP was used as the solid phase in magnetic dispersive micro-solid phase extraction method (D- $\mu$ SPE) for the pre-concentration and determination of trace amount of  $\text{Hg}^{2+}$  ion in water samples. Under optimized condition, this method achieved low

method detection limit (4.0 ng/L), wide linearity (50.0-5000.0 ng/L), high pre-concentration factor (100), a good coefficient of regression (0.9985) and good repeatability (4.5-6.5%). This proposed method was also successfully utilized for determination of  $\text{Hg}^{2+}$  in drinking water, tap water and surface water with good extraction efficiency (90.1-99.0%) as well as the relative standard deviation value for intra-day and inter-day study of 0.7-8.8% and 1.1-7.7%, respectively. In conclusion, the natural product based ODPPNE is an effective and selective ligand, which can be used to determine  $\text{Hg}^{2+}$  in aqueous samples and to remove  $\text{Hg}^{2+}$  from the water.

**Keywords:** Chalcone, dithiocarbamate derivative, sol-gel, mercury, adsorption

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**TERBITAN DITIOKARBAMAT BAGI KALKON YANG DIGABUNGAN  
DENGAN SOL-GEL UNTUK PENYINGKIRAN DAN PEMEKATAN ION  
RAKSA(II) ION DALAM LARUTAN AKUEUS.**

**ABSTRAK**

Kajian ini menunjukkan penggunaan terbitan ditiokarbamat bagi kalkon sebagai ligan untuk penyingkiran dan pra-pemekatan ion raksa ( $Hg^{2+}$ ) dalam air. Kalkon merupakan sebatian semulajadi yang boleh diperolehi daripada buah-buahan, sayur-sayuran, tumbuhan dan rempah. Di bahagian pertama kajian ini, kalkon telah diubah suai secara kimia untuk menghasilkan terbitan ditiokarbamat, 3-okso-1,3-difenilpropil-2-(naftalena-2-ilamino) etilkarbamoditioat (ODPPNE). Seterusnya, sol-gel yang bergabung dengan kalkon (SG-C) dan sol-gel yang bergabung dengan ODPPNE (SG-ODPPNE) disintesis sebagai penjerap untuk  $Hg^{2+}$ . Hasil kajian ini menunjukkan bahawa dengan kehadiran kumpulan berfungsi ditiokarbamat, SG-ODPPNE menunjukkan kepilihan yang tinggi terhadap penjerapan  $Hg^{2+}$  berbanding dengan ion logam yang lain. Kesan daripada parameter seperti saiz penjerap, jumlah penjerap, masa, kepekatan  $Hg^{2+}$  dan pH larutan bagi penjerapan  $Hg^{2+}$  oleh SG-ODPPNE telah dikaji. Data penjerapan yang diperolehi adalah patuh kepada isoterma Langmuir dan muatan jerapan ekalapis yang diperolehi ialah 13.5 mg/g. Dalam kajian kinetik jerapan, data eksperimen adalah padan dengan model tertib pseudo kedua. Menurut kepada model resapan intrazarah, proses penjerapan  $Hg^{2+}$  oleh SG-ODPPNE melibatkan resapan tipisan, resapan intrazarah dan peringkat keseimbangan. Untuk bahagian kedua kajian ini, nanopartikel bermagnet telah disalutkan dengan gel silika yang digabungkan dengan ODPPNE (ODPPNE@MNP). ODPPNE@MNP telah digunakan sebagai fasa pepejal dalam kaedah pengekstrakan fasa pepejal bermagnet secara penyebaran ( $D-\mu$ SPE) untuk pemekatan dan penentuan  $Hg^{2+}$  dalam sampel air. Dibawah keadaan optimum, kaedah ini berjaya mencapai had

pengesanan kaedah yang rendah ( 4.0 ng/L) , julat linear yang luas (50.0-5000.0 ng/L), faktor pra-pemekatan yang tinggi (100), pekali regresi yang baik (0.9985) dan keterulangan yang memuaskan (4.5-6.5%) . Kaedah ini juga telah berjaya digunakan dalam penentuan  $Hg^{2+}$  dalam air minuman, air paip dan air permukaan dengan pemisahan keupayaan yang baik (90.1-99.0%). Sisihan piawai relatif bagi analisis intraday dan interday adalah 0.7-8.8% dan 1.1-7.7% masing-masing. Kesimpulannya, ODPPNE berasaskan sebatian semulajadi merupakan ligan yang berkesan dan terpilih dalam penentuan  $Hg^{2+}$  dan penyingkiran  $Hg^{2+}$  dalam air.

**Kata kunci:** Kalkone, terbitan ditiokarbamat, sol-gel, raksa, penjerapan

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## TABLE OF CONTENTS

Abstract .....	iii
Abstrak .....	v
Acknowledgements .....	vii
Table of Contents .....	viii
List of Figures .....	xii
List of Tables.....	xviii
List of Symbols and Abbreviations.....	xix
List of Appendices .....	xxii
<b>CHAPTER 1: INTRODUCTION.....</b>	<b>1</b>
1.1 Background of study.....	1
1.2 Objective of study.....	9
1.3 Research scope.....	9
<b>CHAPTER 2: LITERATURE REVIEW.....</b>	<b>10</b>
2.1 Conventional treatment methods of Hg <sup>2+</sup> removal in water.....	10
2.1.1 Coagulation and flocculation.....	10
2.1.2 Co-precipitation.....	11
2.1.3 Electrocoagulation.....	12
2.1.4 Membrane filtration.....	13
2.1.5 Adsorption.....	14
2.2 Removal of aqueous metal ion by using sol-gel based adsorbent .....	15
2.2.1 Sol-gel and silica gel .....	15
2.2.2 Modification of silica gel .....	17
2.2.2.1 Surface modification of silica gel through grafting method .....	17

2.2.2.2	Surface modification of silica gel through co-condensation method.....	19
2.2.2.3	Modification of silica gel by using Periodic mesoporous organosilica .....	20
2.2.2.4	Immobilization of metal capturing ligand onto the surface of silica gel.....	21
2.2.2.5	Metal capturing ligand incorporated silicagel.....	25
2.3	Sulphur containing ligand modified silica gel for the removal of aqueous Hg <sup>2+</sup> ..	27
2.4	Natural product based ligand.....	31
2.4.1	Metal capturing ability of natural products .....	31
2.4.2	Chalcone.....	33
2.5	Pre-concentration of trace heavy metal from aqueous sample .....	34
2.5.1	Solid phase extraction and solid phase micro-extraction as the pre-concentration method .....	34
2.5.2	D- $\mu$ SPE.....	35
2.5.3	D- $\mu$ SPE as pre-concentration method for heavy metal ions in water .....	36
2.5.4	MNP as adsorbent phase in D- $\mu$ SPE.....	37
2.5.5	Silica coated MNP (Fe <sub>3</sub> O <sub>4</sub> -SiO <sub>2</sub> ).....	38
2.5.6	Ligand modified Fe <sub>3</sub> O <sub>4</sub> -SiO <sub>2</sub> and its application in the pre-concentration of Hg <sup>2+</sup> in water sample .....	38
2.5.7	Ligand incorporated Fe <sub>3</sub> O <sub>4</sub> -SiO <sub>2</sub> in pre-concentration of Hg <sup>2+</sup> from water sample.....	41

## **CHAPTER 3: MATERIALS AND METHODS ..... 42**

3.1 Materials ..... 42

3.2 Instrumental analysis ..... 42

3.3	Preparation of ODPPNE .....	43
3.4	Preparation of Chalcone and ODPPNE incorporated silica gels .....	44
3.5	Metal ion adsorption by SG-C and SG-ODPPNE .....	44
3.5.1	Determination of the selectivity of SG-C and SG-ODPPNE .....	44
3.5.2	Batch adsorption of aqueous Hg <sup>2+</sup> by SG-ODPPNE.....	45
3.5.3	Hg <sup>2+</sup> removal by SG-ODPPNE adsorbent in real water samples.....	45
3.6	Pre-concentration and determination of Hg <sup>2+</sup> in water.....	46
3.6.1	Synthesis of magnetic nanoparticle (MNP).....	46
3.6.2	Synthesis of ODPPNE-silica coated magnetic nanoparticle (ODPPNE@MNP) .....	46
3.6.3	Pre-concentration of Hg <sup>2+</sup> using ODPPNE@MNP as solid phase for dispersive micro solid phase extraction (D- $\mu$ SPE).....	46
3.6.4	Pre-concentration of Hg <sup>2+</sup> in real water samples.....	47
<b>CHAPTER 4: RESULT AND DISCUSSION.....</b>		<b>49</b>
4.1	Characterization of SG-C, SG-ODPPNE and ODPPNE@MNP.....	49
4.1.1	FTIR analysis .....	49
4.1.2	Elemental analysis.....	54
4.1.3	SEM analysis.....	55
4.1.4	TGA and DTA analysis .....	58
4.1.5	Leaching Test .....	61
4.2	Selectivity of SG-C, SG-ODPPNE, SiO <sub>2</sub> @MNP, and ODPPNE@MNP in the removal of heavy metals.....	62
4.3	Hg <sup>2+</sup> removal in aqueous by SG-ODPPNE.....	64
4.3.1	Effect of adsorbent size .....	64
4.3.2	Effect of pH of aqueous solution.....	65

4.3.3	Effect of contact time .....	67
4.3.4	Effect of Hg <sup>2+</sup> initial concentration .....	68
4.3.5	Effect of SG-ODPPNE dosage .....	69
4.3.6	Application of SG-ODPPNE in the removal of Hg <sup>2+</sup> in real water samples .....	70
4.4	Pre-concentration of Hg <sup>2+</sup> in aqueous sample by ODPPNE@MNP .....	72
4.4.1	Amount of ODPPNE@MNP .....	73
4.4.2	Adsorption time .....	74
4.4.3	pH of aqueous solution .....	74
4.4.4	Concentration of Hg <sup>2+</sup> in aqueous solution .....	76
4.4.5	Desorption reagent for Hg <sup>2+</sup> .....	77
4.4.6	Desorption time .....	79
4.4.7	Reusability of ODPPNE@MNP in D- $\mu$ SPE process .....	80
4.4.8	Application of ODPPNE@MNP as solid adsorbent in the pre-concentration of Hg <sup>2+</sup> in real water sample .....	81
4.5	Adsorption isotherm .....	85
4.6	Kinetic study .....	90
4.6.1	Pseudo-first order and Pseudo-second order Model .....	90
4.6.2	Intra-particle diffusion and Boyd model .....	95
<b>CHAPTER 5: CONCLUSIONS AND FUTURE WORKS .....</b>		<b>99</b>
5.1	Conclusion .....	99
5.2	Future work .....	100
<b>References .....</b>		<b>101</b>
<b>List of Publications and paper presented .....</b>		<b>126</b>
<b>Appendices .....</b>		<b>128</b>

## LIST OF FIGURES

<b>Figure</b>	<b>Description</b>	<b>Page</b>
<b>Figure 1.1</b>	Mercury species exist in environment system	3
<b>Figure 1.2</b>	(a) Chalcone and (b) ODPPNE	7
<b>Figure 2.1</b>	The mechanism for the formation sol-gel through hydrolysis and condensation of silicon alkoxides (Brinker and Scherer, 2013)	16
<b>Figure 2.2</b>	Surface functionalized silica gel through grafting methods	17
<b>Figure 2.3</b>	(a) APTES and (b) amine functionalized silica based adsorbent	18
<b>Figure 2.4</b>	(a) MPTS and (b) mercapto-functionalized silica gel	18
<b>Figure 2.5</b>	(a) Diethylphosphatoethyltriethoxysilane and (b) phosphorus acid- functionalized silica gel	19
<b>Figure 2.6</b>	Formation pathways of functionalized silica gel through co-condensation method	20
<b>Figure 2.7</b>	Formation pathways of periodic mesoporous organosilicas (PMO)	21
<b>Figure 2.8</b>	Bisilylated crown ether	21
<b>Figure 2.9</b>	(a) Chloro functionalized silica gel, (b) tris(2-aminoethyl) amine and (c) tris(2-aminoethyl) amine modified silica gel	22
<b>Figure 2.10</b>	(a) <i>N</i> -(2-hydroxyethyl) salicylaldimine and (b) <i>N</i> -(2-hydroxyethyl) salicylaldimine functionalized mesoporous silica gel	22
<b>Figure 2.11</b>	(a) 1 <i>H</i> -pyrrole-2-carbaldehyde and (b) 1-(Pyrrol-2-yl)imine modified silica gel	23

<b>Figure 2.12</b>	(a) 2, 2'-(propane-1,3-diylbis(oxy))dibenzaldehyde and (b) Bisaldehyde modified silica gel	23
<b>Figure 2.13</b>	(a) 5-sulfosalicylic acid and (b) 5-sulfosalicylic acid / PAMAM modified silica gel	24
<b>Figure 2.14</b>	(a) Dibutyl (3-chloro-2-hydroxypropyl) phosphate and (b) phosphoryl modified mesoporous silica gel	24
<b>Figure 2.15</b>	Formation pathways of metal capturing incorporated silica gel	25
<b>Figure 2.16</b>	A variety of ligand used to incorporated into silica gel	26
<b>Figure 2.17</b>	(a) 1-furoyl thiourea, (b)1-furoyl thiourea functionalized SBA-15 (co-condensation route) and (c) 1-furoyl thiourea functionalized SBA-15 (grafting method)	28
<b>Figure 2.18</b>	1,3,5-trithiane doped in silica matrix	28
<b>Figure 2.19</b>	Common structure of dithiocarbamate compound	29
<b>Figure 2.20</b>	(a) CS <sub>2</sub> modified diethylenetriamine functionalized silica gel, (b) CS <sub>2</sub> modified tetraethylenepentamine-salicaldehyde functionalized silica gel, (c) CS <sub>2</sub> modified diethylenetriamine functionalized silica gel and (d) CS <sub>2</sub> modified tetraethylenepentamine-salicaldehyde functionalized silica gel	29
<b>Figure 2.21</b>	Silica coated magnetite particles derivatized with dithiocarbamate group	30
<b>Figure 2.22</b>	(a) Siloxydithiocarbamate compound and (b) dithiocarbamate modified silica gel coated magnetite particle	30
<b>Figure 2.23</b>	(a) Curcumin, (b) Rutin, (c) Quercetin and (d) Morin	32
<b>Figure 2.24</b>	Synthesis pathway of ODPPNE	33
<b>Figure 2.25</b>	A variety of metal capturing ligand used to modify Fe <sub>3</sub> O <sub>4</sub> -SiO <sub>2</sub>	40

<b>Figure 2.26</b>	ODPPNE incorporated silica coated magnetic nanoparticle (ODPPNE@MNP)	41
<b>Figure 4.1</b>	IR spectrum of (a) Chalcone and (b) ODPPNE	50
<b>Figure 4.2</b>	IR spectrum of (a) SG, (b) SG-C and (c) SG-ODPPNE and (d) isolated SG-ODPPNE after Hg <sup>2+</sup> adsorption	52
<b>Figure 4.3</b>	IR spectrum of (a) MNP (Fe <sub>3</sub> O <sub>4</sub> ), (b) SiO <sub>2</sub> @MNP, (c) ODPPNE@MNP and (d) isolated ODPPNE@MNP after Hg <sup>2+</sup> adsorption	53
<b>Figure 4.4</b>	SEM images of (a) SG, (b) SG-C and (c) SG-ODPPNE	56
<b>Figure 4.5</b>	SEM images of (a) MNP, (b) SiO <sub>2</sub> @MNP and (c) ODPPNE@MNP	57
<b>Figure 4.6</b>	(a) TGA and (b) DTA profile of SG, SG-C and SG-ODPPNE	59
<b>Figure 4.7</b>	(a) TGA and (b) DTA profile of MNP, SiO <sub>2</sub> @MNP and ODPPNE@MNP	60
<b>Figure 4.8</b>	The comparison of UV spectra for free ODPPNE, SG-ODPPNE and ODPPNE@MNP in water with different pH	61
<b>Figure 4.9</b>	The removal percentage of Cr <sup>3+</sup> , Ni <sup>2+</sup> , Cu <sup>2+</sup> , Zn <sup>2+</sup> , Cd <sup>2+</sup> , Hg <sup>2+</sup> and Pb <sup>2+</sup> by SG-ODPPNE, SG-C and SG in aqueous sample. (Amount of adsorbent = 50 mg, [Metal ion] = 1 mg/L, volume of aqueous solution = 10 mL, pH of aqueous solution = 7.5 and contact time = 24 h)	63
<b>Figure 4.10</b>	The removal percentage of Cr <sup>3+</sup> , Ni <sup>2+</sup> , Cu <sup>2+</sup> , Zn <sup>2+</sup> , Cd <sup>2+</sup> , Hg <sup>2+</sup> and Pb <sup>2+</sup> by ODPPNE@MNP and SiO <sub>2</sub> @MNP in aqueous sample. (Amount of adsorbents = 15 mg, [Metal ion] = 1 mg/L, volume of aqueous solution = 25 mL, pH of aqueous solution = 8 and contact time = 30 min )	63

<b>Figure 4.11</b>	Effect of 0.06 mm and 2.00 mm SG-ODPPNE on removal percentage of $\text{Hg}^{2+}$ in aqueous sample. (Amount of SG-ODPPNE = 50 mg, $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of $\text{Hg}^{2+}$ solution = 10 mL, pH of $\text{Hg}^{2+}$ solution = 7.5 and contact time = 24 h)	64
<b>Figure 4.12</b>	Effect of pH on the removal percentage of $\text{Hg}^{2+}$ in aqueous sample by SG-ODPPNE. (Amount of SG-ODPPNE = 50 mg, $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of $\text{Hg}^{2+}$ solution = 10 mL and contact time = 24 h)	66
<b>Figure 4.13</b>	(a) The structure of neutral, protonated and deprotonated ODPPNE, and (b) The variation of fraction of neutral, protonated and deprotonated ODPPNE in the pH range of 6 to 8	66
<b>Figure 4.14</b>	Effect of contact time on the removal percentage of $\text{Hg}^{2+}$ in aqueous sample by SG-ODPPNE. (Amount of SG-ODPPNE = 50 mg, $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of $\text{Hg}^{2+}$ solution = 10 mL and pH of $\text{Hg}^{2+}$ solution = 8)	67
<b>Figure 4.15</b>	Effect of $\text{Hg}^{2+}$ concentration on removal percentage of $\text{Hg}^{2+}$ in aqueous sample. (Amount of SG-ODPPNE = 50 mg, volume of $\text{Hg}^{2+}$ solution = 10 mL, pH of $\text{Hg}^{2+}$ solution = 8 and contact time = 6 h)	68
<b>Figure 4.16</b>	Effect of SG-ODPPNE amount on removal percentage of $\text{Hg}^{2+}$ in aqueous sample. ( $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of $\text{Hg}^{2+}$ solution = 10 mL, pH of $\text{Hg}^{2+}$ solution = 8 and contact time = 6 h)	69
<b>Figure 4.17</b>	Removal percentage of $\text{Hg}^{2+}$ by SG-ODPPNE in real water samples. (Amount of SG-ODPPNE = 50 mg, spiked $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of water samples = 10 mL, pH of water samples = 8 and contact time = 6 h)	70
<b>Figure 4.18</b>	D- $\mu$ SPE process	72



- Figure 4.19** Effect of the amount of ODPPNE@MNP on removal percentage of  $\text{Hg}^{2+}$  in water. ( $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of  $\text{Hg}^{2+}$  solution = 25 mL, pH of aqueous solution = 8 and adsorption time = 30 min) 73
- Figure 4.20** Effect of adsorption time on removal percentage of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg,  $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , pH of aqueous solution = 8 and volume of  $\text{Hg}^{2+}$  solution = 25 mL) 74
- Figure 4.21** Effect of pH on removal percentage of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg,  $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of aqueous solution = 25 mL and adsorption time = 10 min) 75
- Figure 4.22** Effect of  $\text{Hg}^{2+}$  concentration on removal percentage of  $\text{Hg}^{2+}$  in aqueous sample. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min and pH of aqueous solution = 7) 76
- Figure 4.23** Effect of the type of eluent used and its concentration on recovery efficiency of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, desorption time = 30 min and volume of acid = 25 mL) 78
- Figure 4.24** Effect of the volume of HCl on recovery efficiency of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, desorption time = 30 min and  $[\text{HCl}] = 1.5 \text{ M}$ ) 78
- Figure 4.25** Effect of the desorption time on recovery efficiency of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, volume of HCl = 0.25 mL and  $[\text{HCl}] = 1.5 \text{ M}$ ) 79

<b>Figure 4.26</b>	Reusability of ODPPNE@MNP. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, volume of HCl = 0.25 mL, [HCl] = 1.5 M, and desorption time = 10 min)	80
<b>Figure 4.27</b>	Linearized adsorption isotherm Langmuir Model for Hg <sup>2+</sup> adsorption on (a) SG-ODPPNE and (b) ODPPNE@MNP	86
<b>Figure 4.28</b>	Linearized adsorption isotherm Freundlich Model for Hg <sup>2+</sup> adsorption on (a) SG-ODPPNE and (b) ODPPNE@MNP	88
<b>Figure 4.29</b>	Pseudo-first order model for the adsorption of Hg <sup>2+</sup> on (a) SG-ODPPNE and (b) ODPPNE@MNP	91
<b>Figure 4.30</b>	Pseudo-second order model for the adsorption of Hg <sup>2+</sup> on (a) SG-ODPPNE and (b) ODPPNE@MNP	93
<b>Figure 4.31</b>	The intra-particle diffusion model for the adsorption of Hg <sup>2+</sup> on (a) SG-ODPPNE and (b) ODPPNE@MNP	96
<b>Figure 4.32</b>	Boyd plot for the adsorption of Hg <sup>2+</sup> on (a) SG-ODPPNE and (b) ODPPNE@MNP	98

## LIST OF TABLES

<b>Table</b>	<b>Description</b>	<b>Page</b>
<b>Table 1.1</b>	Heavy metal pollution status of some rivers and lakes in Malaysia and other country	2
<b>Table 4.1</b>	Elemental composition of SG, SG-C and SG-ODPPNE	54
<b>Table 4.2</b>	Elemental composition of MNP, SiO <sub>2</sub> @MNP and ODPPNE@MNP	55
<b>Table 4.3</b>	Comparison of the adsorption capacity and selectivity of SG-ODPPNE with other reported dithiocarbamate-based absorbents	71
<b>Table 4.4</b>	Intra and inter day analysis result for real water samples	83
<b>Table 4.5</b>	Comparison with previous reported analytical methods for pre-concentration or determination of Hg <sup>2+</sup> in aqueous sample	84
<b>Table 4.6</b>	Adsorption isotherm parameter of (a) Langmuir and (b) Freundlich model	89
<b>Table 4.7</b>	Kinetic study parameter of (a) Pseudo-first order and (b) Pseudo-second order	94

## LIST OF SYMBOLS AND ABBREVIATIONS

%E	: Recovery efficiency
%R	: Removal percentage
AAS	: Atomic absorption spectroscopy
AC	: Activated carbon
Ag-NP	: Silver-nanoparticle
APTES	: 3-aminopropyltrimethoxysilane
ATR/FTIR	: Attenuated total reflection/ Fourier-transform Infrared
$B_f$	: Freundlich constant
$B_L$	: Langmuir constant
$B_t$	: Mathematical function for fraction of $Hg^{2+}$ adsorbed at different time
$C_e$	: Equilibrium concentration
CF-CVAAS	: Continuous-Flow Cold Vapor Atomic Absorption Spectrometry
$C_{id}$	: Constant related to the thickness of the boundary layer
CNT	: Carbon nanotube
$C_o$	: Initial concentration
CPTS	: 3-chloropropyltriethoxysilane
$C_r$	: Extracted concentration
CV-AAS	: Cold Vapor Atomic Absorption Spectrometry
CV-ETAAS	: Electrothermal Atomic Absorption Spectrometer
DMA	: Direct mercury analyser
D-SPE	: Dispersive solid phase extraction
DTA	: Differential thermal analysis

DWQS	: Drinking Water Quality Standard
D- $\mu$ SPE	: Dispersive micro-solid phase extraction
EC	: Electrocoagulation
$F$	: Fraction of $\text{Hg}^{2+}$ adsorbed at different time
$\text{Fe}_3\text{O}_4\text{-SiO}_2$	: Silica gel coated iron oxide magnetic nanoparticle
FI-MSPME	: Flow injection magnetic solid phase micro-extraction
GO	: Graphene oxide
ICP-OES	: Inductively Coupled Plasma Optical Emission Spectrometry
$k_1$	: Pseudo-first order rate of reaction
$k_2$	: Pseudo-second order rate constant
$k_{id}$	: Intra-particle diffusion rate constant
LOD	: Limit of detection
LOQ	: Limit of quantitation
MA	: Mercury analyser
MCLG	: Maximum contaminant level goal
MDL	: Method of detection limit
MNP	: Magnetic nanoparticle
MOHM	: Ministry of Health Malaysia
MPTS	: Methacryloxypropyltriethoxysilane
MWCNT	: Multiwalled carbon nanotube
$n$	: Adsorption intensity constant
NWQS	: National Water Quality Standards
ODPPNE	: 3-oxo-1,3-diphenylpropyl-2-(naphthalen-2-ylamino) ethylcarbamidithioate
ODPPNE@MNP	: ODPPNE-silica coated magnetic nanoparticle

PEUF	: Polymer enhanced ultrafiltration
PMO	: Periodic mesoporous organosilica
$Q_e$	: Adsorption capacity at equilibrium
$Q_{e,cal}$	: Calculated adsorption capacity at equilibrium
$Q_{e,exp}$	: Experimental adsorption capacity at equilibrium
$Q_m$	: Maximum adsorption capacity
$Q_t$	: Amount of adsorbed sorbate at time $t$
R <sup>'''</sup>	: Organic functionalities
$R_L$	: Dimensionless constant
SG	: Blank sol-gel
SG-C	: Chalcone incorporated sol-gel
SG-ODPPNE	: 3-oxo-1,3-diphenylpropyl-2-(naphthalen-2-ylamino) ethylcarbamidithioate incorporated sol-gel
SiO <sub>2</sub>	: Porous silica frameworks
SiO <sub>2</sub> @MNP	: Silica coated magnetic particle
SPE	: Solid phase extraction
SPME	: Solid phase micro-extraction
SWCNT	: Single walled carbon nanotube
TGA	: Thermogravimetric analysis
UNICEF	: United Nations Children's Fund
USEPA	: United States Environmental Protection Agency
$V_0$	: Initial volumes of aqueous solution
$V_f$	: Volume of desorption agent
WEPA	: Water Environment Partnership in Asia
WHO	: World Health Organization
$\chi^2$	: Chi-square values

## LIST OF APPENDICES

<b>Appendix</b>	<b>Description</b>	<b>Page</b>
<b>Appendix A</b>	$^1\text{H}$ -NMR spectra of ODPPNE	128
<b>Appendix B</b>	$^{13}\text{C}$ -NMR spectra of ODPPNE	129
<b>Appendix C</b>	Raw data	130

University of Malaya

## CHAPTER 1: INTRODUCTION

### 1.1 Background Study

Clean drinking water is a basic human need. Unfortunately, 748 million people around the world still facing the lack access to the improved drinking-water (WHO and UNICEF, 2014). This problem is particularly acute in the developing countries (WHO, 2017). There are numbers of threats to drinking water which include chemicals, animal wastes, pollutants and human wastes which have been frequently contaminated the sources of drinking water (USEPA, 2004). Among various pollutants, metal contamination in the aquatic environment has attracted global attention owing to its toxicity and persistence in the environment (Islam et al., 2015). Small amounts of heavy metal are commonly found in our environment and diet. Some of these metals are necessary for diet; for example, living organism required various amounts of heavy metal such as iron, cobalt, copper, manganese, molybdenum and zinc (Singh et al., 2011) for metabolism process (Abbaspour et al., 2014; Bost et al., 2016; Fenech, 2001; Mendel, 2013; Roohani et al., 2013; Seo and Park, 2008). However, due to the bioaccumulation and biomagnifications in the food chain, metals and metalloids from natural and anthropogenic sources are continuously posing the serious threat to human and ecological health (Rahman et al., 2012). Most of the metals are entering to the natural water system through the anthropogenic activities such as mining, disposal of untreated and partially treated effluents which containing toxic metals, metal chelates from different industries, indiscriminate use of heavy metal-containing fertilizer and pesticides in agricultural fields (Reza and Singh, 2010). Table 1.1 shows the heavy metal pollution status in several surface water sources in Malaysia and other countries. The amount of some heavy metal such as aluminum (Al), arsenic (As), boron (B), cadmium (Cd), chromium (Cr), iron (Fe), lead (Pb), manganese (Mn), mercury (Hg) and selenium (Se) have been found at the level which is higher than the quality standard regulated by National Water Quality Standards



for Malaysia (NWQS), Drinking Water Quality Standard for Malaysia (DWQS) and World Health Organization (WHO) Guidelines for Drinking-water Quality.

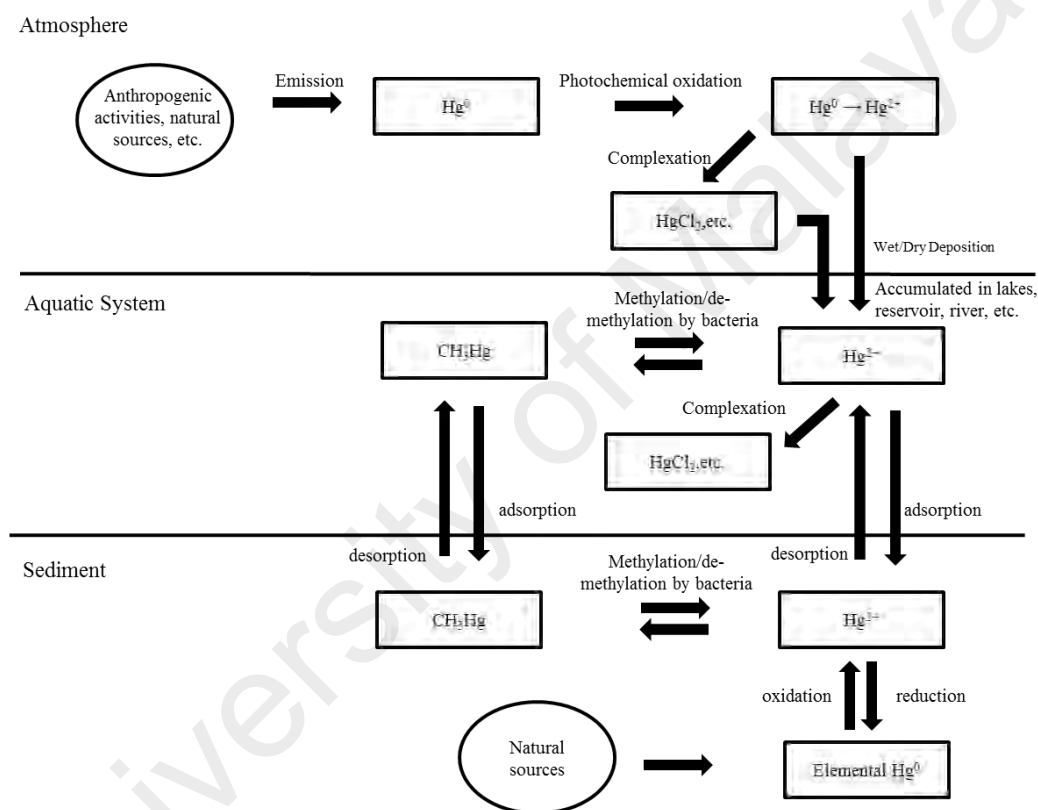
**Table 1.1:** Heavy metal pollution status of some rivers and lakes in Malaysia and other countries

Heavy metal that exceeded the water quality standard	Location
Hg <sup>a, b, c, 1</sup>	Langat River Basin, Selangor
Fe and Mn <sup>a, b, c, 2</sup>	Well, river and tap water, Sungai Buloh village, Selangor.
Al and Fe <sup>a, b, c, 3</sup>	Selangor River, Selangor
As <sup>a, b, c, 1</sup>	Klang River Basin, Kuala Lumpur
Fe, Pb and Se <sup>a, b, c, 4</sup>	Curtin Lake, Miri Sarawak
As, Cd, Cr and Pb <sup>c, 5</sup>	Dhalai Beel , Bangladesh
As ,Cd, Cr and Pb <sup>c, 5</sup>	Bangshi River, Bangladesh
As and B <sup>c, 6</sup>	Chasicó Lake, Argentina
Al, Cd and Pb <sup>c, 7</sup>	Ismailia Canal, Nile River, Egypt
Pb <sup>c, 8</sup>	Siling Reservoir Watershed in Zhejiang Province, China
As and Pb <sup>c, 9</sup>	Shadow Lake of Yangtze River region, China
Hg <sup>c, 10</sup>	River in Artisanal gold mining site, Asutifi District, Ghana
As and Hg <sup>c, 11</sup>	Can Tho/Hau Giang provinces, Mekong Delta, Vietnam

<sup>a</sup>NWQS (WEPA, 2006), <sup>b</sup>DWQS (MOHM, 2010), <sup>c</sup>WHO Guidelines for Drinking-water Quality (WHO, 2011)

<sup>1</sup>Poon et al., 2016, <sup>2</sup>Ambu et al., 2014, <sup>3</sup>Daniela and Kawasaki, 2016, <sup>4</sup>Prasanna et al., 2012, <sup>5</sup>Rahman et al., 2014, <sup>6</sup>Avigliano et al., 2015, <sup>7</sup>Goher et al., 2014, <sup>8</sup>Naveedullah et al., 2014, <sup>9</sup>Liu and Li, 2011, <sup>10</sup>Adjei-Kyereme et al., 2015, <sup>11</sup>Wilbers et al., 2014

Among various heavy metals, one of the serious threats to human health is associated with the exposure to mercury (Hg) and this metal is required to be removed to very low levels during water treatment. Hg has been found to bioaccumulate in the living organism to a level that produced adverse effects (Hennebery et al., 2011). In the environment, mercury can exist and circulate in several chemical forms which include elemental mercury ( $\text{Hg}^0$ ), mercury ions ( $\text{Hg}^+$  and  $\text{Hg}^{2+}$ ) and organomercury ( $\text{CH}_3\text{Hg}^+$ ) as shown in Figure 1.1.



**Figure 1.1:** Mercury species exist in environment system.

Elemental  $\text{Hg}^0$  is the predominant form of mercury in the atmosphere (Lamborg et al., 2002) with natural and anthropogenic activities as the major sources (Strode et al., 2007). The atmospheric half-life of  $\text{Hg}^0$  vapour is within 0.5 to 1 year. Due to the long half-life,  $\text{Hg}^0$  can spread globally in the atmosphere (Selin, 2009; Weiss-Penzias et al., 2016). For the human, the poisoning of  $\text{Hg}^0$  vapour is mainly through inhalation (Lambertson, 2005). In Prestea, Ghana, 46.7% of small-scale gold miners inhaled high

level of  $\text{Hg}^0$  vapour that released from gold mining activities were experienced high  $\text{Hg}^0$  concentration in their urine (Mensah et al., 2016). The chronic exposure of  $\text{Hg}^0$  vapour can damage the central nervous system and kidneys (Lambertson, 2005). On the other hand, the absorption of  $\text{Hg}^0$  through ingestion and the dermal process has been found to be poor and limited (Park and Zheng, 2012).

Inorganic mercury in the form of mercuric (II) ion ( $\text{Hg}^{2+}$ ) is the most abundant mercury species in the aquatic environment (Bridges and Zalups, 2010). Conversion of elemental  $\text{Hg}^0$  to gaseous inorganic mercury  $\text{Hg}^{2+}$  or particle bound  $\text{Hg}^{2+}$  compounds can be occurred through photochemical oxidation of  $\text{Hg}^0$  in the atmosphere (Selin, 2009; Weiss-Penzias et al., 2016).  $\text{Hg}^{2+}$  species with shorter half-life and water-soluble behaviour is then deposited in the aquatic system (Stein et al., 1996; Zhang et al., 2012). Thus, the  $\text{Hg}^{2+}$  was predominantly found in freshwater and sea water system (Karthiga et al., 2016). Mercurous ( $\text{Hg}^+$ ) and mercuric ( $\text{Hg}^{2+}$ ) complexes can be found in the aquatic system resulted from the complexation between deposited  $\text{Hg}^+$  or  $\text{Hg}^{2+}$  with anions in water such as chloride and hydroxide ions (Lambertson, 2005). On the other hand, the atmospheric  $\text{Hg}^{2+}$  tends to form complex also with the other ions such as chloride ion in the atmosphere (Stein et al., 1996). The main  $\text{Hg}^{2+}$  intake route for the human is by  $\text{Hg}^{2+}$  contaminated food or drink (Bridges and Zalups, 2010). The study by Monteiro et al. (2013) also showed that, inorganic mercury has the potential to undergo bioaccumulation through the food chain in the aquatic system. The toxicity of  $\text{Hg}^{2+}$  complexes is largely depending on their solubility in water. Hence, the low water-soluble forms of  $\text{Hg}^+$  complexes are less poisonous than water soluble  $\text{Hg}^{2+}$  complexes (Langford and Ferner, 1999). The corrosive feature of inorganic mercury enhances the gastrointestinal permeability and absorption. Oral exposure to mercury salt causes the syndrome like burning chest pain, darkened discoloration of the oral mucous membrane and severe

gastrointestinal symptoms and follow by signs of mercurial stomatitis and impaired kidney function (Park and Cheng, 2012).

Organic mercury such as methyl mercury ( $\text{CH}_3\text{Hg}^+$ ) is the most toxic mercury form as compared to  $\text{Hg}^0$ ,  $\text{Hg}^+$  and  $\text{Hg}^{2+}$  (Hong et al., 2012). Methyl mercury is formed through methylation of  $\text{Hg}^{2+}$  in the aquatic system by microorganism such as sulfate and iron reducing bacteria (Gilmour et al., 2013). The hazardous methylmercury is taken up by the aquatic organism and initiates the bioaccumulation of mercury in the food chain. Methyl mercury intake by human body can happen through the contaminated aquatic organism such as fish which are consumed and as food. (Hong et al., 2012). Methyl mercury with high lipid-soluble properties can permeate into the blood and reach the brain and placental barrier which ended up at central nervous system (Lambertson, 2005).

This study was focused on the removal and pre-concentration of  $\text{Hg}^{2+}$ . World Health Organization (2005) reported that almost all mercury in drinking water present in the form of  $\text{Hg}^{2+}$ . The Hg mostly presents in the air as  $\text{Hg}^0$  vapour while the organic mercury such as methyl mercury is mainly accumulating in biota. Moreover, methyl mercury is not produced until the methylation of inorganic mercury (Hong et al., 2012) in water. Due to the hazardous effect of mercury, the maximum allowable concentration of mercury in drinking water is kept under 0.001 mg/L by Drinking Water Quality Standard of Malaysia (DWQS) (MOHM, 2010), 0.002 mg/L by the United States Environmental Protection Agency (USEPA) (USEPA, 2009) and 0.001 mg/L by World Health Organization (WHO) (WHO, 2011).

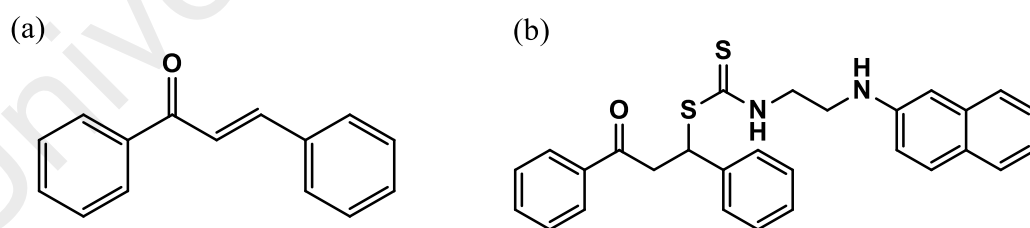
Conventional water treatment methods for mercury ion ( $\text{Hg}^{2+}$ ) removal that have been developed are such as coagulation and flocculation (Henneberry et al., 2011), chemical precipitation (Lewis, 2010; Sumesh et al., 2011), electrochemical methods (Wang et al., 2011), membrane filtration (Bessbousse et al., 2010; Song et al., 2012) and adsorption process (Dong et al., 2016). Among these methods, adsorption process is

receiving high attention because of its high efficiency, technical flexibility and cost-effectiveness (Dong et al., 2016). A variety of adsorbents for heavy metal removal had been studied and discussed by many researchers. These adsorbents are such as activated carbon, bioadsorbent, agricultural wastes and clay material (Abu-Eishah, 2008; Ghorbani et al., 2011; Kavand et al., 2014; Khoramzadeh et al., 2013; Monier and Abdel-Latif, 2012; Najafi et al., 2012). On the other hand, these materials have its own limitation such as low loading capacities, relatively small metal ion binding constant and less selectivity (Najafi et al., 2012). Recently, the used of porous silica frameworks ( $\text{SiO}_2$ ) or so-called sol-gel as adsorbent in the removal of toxic substances such as heavy metal have become a popular method due to the simplicity in preparation, low cost, large surface areas, excellent thermal and mechanical stability, rapid adsorption kinetics, and excellent anti-swelling properties (Niu et al., 2015; Zhao et al., 2012). In addition, the sol-gel is readily modified by a variety of functionalities ligand for selective removal of the target metal ion such as aqueous  $\text{Hg}^{2+}$  (Esmaeili Bidhendi et al., 2014; Khor et al., 2017)

A wide range of sol-gel based adsorbents has been developed for the adsorption of heavy metals and the sol-gel with incorporated metal capturing ligand has been reported as one of the effective adsorbents (Zhao et al., 2012). This material has become an attractive adsorbent due to its simplicity in preparation (Zaitoun et al., 2014). Thus far, various ligands such as *N*-(dipropylcarbamothioyl) thiophene-2-carboxamide, polyamidoamine dendrimers, trioctylmethylammonium 1-phenyl-3-methyl-4-benzoyl-5-onate, 2-aminothiazole, 1,4,10,13-tetraoxa-7,16-diazacyclooctadecane-7,16-bis(malonate), and dithizone have been synthesized for the removal and also the determination of metals ions (Mehmood et al., 2013; Sun et al., 2014; Turanov et al., 2016; Tzvetkova and Nickolov, 2012; Yost et al., 2000; Zhang et al., 2014). These ligands are often synthesized through a series of organic reactions, which is not environmental friendly. On the other hand, numerous studies also have shown the ability of natural

products such as rutin (Ikeda et al., 2015) and curcumin (Picciano and Vaden, 2013) to form complexes with metal ions.

The first part of this study demonstrated the application of a natural product called chalcone as a ligand for the removal of  $\text{Hg}^{2+}$  in water. Chalcone contains two aromatic rings linked by a three-carbon  $\alpha, \beta$ -unsaturated carbonyl system (Figure 1.2a). Chalcone-type of natural products can be obtained from fruits (e.g., citruses, apples), vegetables (e.g., tomatoes, shallots, bean sprouts, and potatoes), various plants and spices (Orlikova et al., 2011; Patil et al., 2009). Chalcone was selected because of its low-toxicity, eco-friendly, and possible chemical modification (Ghouila et al., 2012; Hsieh et al., 2012). In this study, the chemical modification was also carried out on chalcone to increase its selectivity towards the removal of  $\text{Hg}^{2+}$ . Among various functional groups, dithiocarbamate functionalized ligands have been found to be selective towards the interaction with  $\text{Hg}^{2+}$  (Figueira et al., 2011; Tavares et al., 2013). Therefore, in this study, chalcone was modified into dithiocarbamate derivative, 3-oxo-1,3-diphenylpropyl-2-(naphthalen-2-ylamino) ethylcarbamoate (ODPPNE) (Figure 1.2b). The ODPPNE was then incorporated on the sol-gel to generate the effective adsorbent in removal aqueous  $\text{Hg}^{2+}$ .



**Figure 1.2:** (a) Chalcone and (b) ODPPNE.

The concentration of total dissolved mercury in natural water samples could be varying from  $\mu\text{g/L}$  to  $\text{ng/L}$  (Zhang et al., 2014). However, the detection limits for inorganic mercury for common instruments such as Atomic Absorption Spectrometry (AAS) are at the  $\mu\text{g/L}$  level (WHO, 2005). Therefore, an appropriate pre-concentration

method is required before  $\text{Hg}^{2+}$  determination. The application of solid phase extraction method that employing modified magnetic particles as adsorbents in analytical chemistry has increased significantly in recent years (Wierucka and Biziuk, 2014; Ríos and Zougagh, 2016). When magnetic particle-based adsorbents are used for the extraction, super paramagnetic properties of these materials allow it to be separated from water by an external magnetic field. As a result, the duration of sample preparation can significantly shorten and simplified. A wide range of magnetic adsorbents have been developed for selective determination of  $\text{Hg}^{2+}$  (e.g. Adlnasab et al., 2014; Abolhasani et al., 2015; Alonso et al., 2016; Cui et al., 2015; Es'haghi et al., 2016; López-Garcia et al., 2015; Sobhi et al., 2017; Zhang et al., 2014). Most of these magnetic adsorbents were produced through a series of reactions. These reactions are such as synthesis of iron oxide ( $\text{Fe}_3\text{O}_4$ ) magnetic nanoparticle, coating of  $\text{Fe}_3\text{O}_4$  with silica layer, functionalization of silica coated  $\text{Fe}_3\text{O}_4$  and bonding of selected ligand onto the functionalized silica coated  $\text{Fe}_3\text{O}_4$  (Alonso et al., 2016; Cui et al., 2015; Sobhi et al., 2017). Some of this reactions involved high temperature reflux and also time consuming. Hence, the second part of this study demonstrated the coating of sol-gel doped with ODPPNE ligand onto  $\text{Fe}_3\text{O}_4$  to produce an adsorbent ( $\text{ODPPNE@MNP}$ ) for pre-concentration of  $\text{Hg}^{2+}$ . This method simplifies the preparation of adsorbent by incorporating the ligand during the coating of  $\text{Fe}_3\text{O}_4$  with silica layer. The performance of  $\text{ODPPNE@MNP}$  as solid phase for  $\text{Hg}^{2+}$  pre-concentration and determination was evaluated through a series of experiment.

## 1.2 Objective of Study

The objectives of this study were:

- a) to prepare and characterize the ODPPNE incorporated sol-gel (SG-ODPPNE) and the magnetic nanoparticle coated with ODPPNE incorporated sol-gel (ODPPNE@MNP).
- b) to evaluate the  $\text{Hg}^{2+}$  adsorption performance of the adsorbents
- c) to investigate the capability of selected adsorbent (ODPPNE@MNP) for pre-concentration of  $\text{Hg}^{2+}$ .
- d) to develop a  $\text{Hg}^{2+}$  pre-concentration method for analysis water sample by using ODPPNE@MNP as solid phase in magnetic dispersive micro-solid phase extraction technique (D- $\mu$ SPE).

## 1.3 Research scope

Generally, this research study can be divided into two parts. First part of the study was consisted of the synthesis of SG-ODPPNE as adsorbent for the removal of  $\text{Hg}^{2+}$  in water sample. In the second part of the study, ODPPNE incorporated silica gel which showed the greatest selectivity towards the adsorption of  $\text{Hg}^{2+}$  was used as the coating material for iron oxide magnetic nanoparticle (MNP) to produce ODPPNE@MNP. The ODPPNE@MNP was used as an adsorbent for dispersive micro-solid phase extraction technique (D- $\mu$ SPE) to pre-concentrate  $\text{Hg}^{2+}$  in water sample.



## CHAPTER 2: LITERATURE REVIEW

### 2.1 Conventional treatment methods for $\text{Hg}^{2+}$ removal in water

Generally, the conventional treatment methods which have been used for  $\text{Hg}^{2+}$  removal are include coagulation-flocculation, co-precipitation, electrochemical treatment, membrane filtration and adsorption (Dong et al., 2016; Henneberry et al., 2011; Huang et al., 2016; Nanseu-Njiki et al., 2009; Santhosh et al., 2013).

#### 2.1.1 Coagulation and Flocculation

The coagulation-flocculation process is a common technique used for the removal of suspended solids in water during water and wastewater treatment (Lanciné et al., 2008). During coagulation, coagulants such as ferric chloride and alum are added to the water. The cation species such as  $\text{Al}^{3+}$  and  $\text{Fe}^{3+}$  are neutralized the negatively charged suspended solids. The suspended solids are then allowed to agglomerate into larger settable flocs during flocculation (Amuda and Amoo, 2007; Folens et al., 2017; Lanciné et al., 2008). The flocs are then precipitated as sludge. Positively charged heavy metals are known to form the strong complexes with organic based suspended solids (Muresan et al., 2011). Haitzer et al. (2002) reported that the  $\text{Hg}^{2+}$  bind favourably to organic matter that containing the sulphur atom. Hence, the certain fraction of  $\text{Hg}^{2+}$  can be removed from the water when the suspended solids are removed through coagulation-flocculation. For Hg removal, Henneberry et al. (2011) reported the efficiency of three different coagulants namely ferric sulfate ( $\text{FeSO}_4$ ), ferric chloride ( $\text{FeCl}_2$ ) and poly aluminium chloride (PAC) in the removal of inorganic mercury ( $\text{Hg}^+$  and  $\text{Hg}^{2+}$ ) in surface water by using coagulation-flocculation process. They found that 96, 97, and 84% of inorganic mercury were removed when  $\text{FeSO}_4$ ,  $\text{FeCl}_2$ , and PAC were used as the coagulant. Although the coagulation-flocculation method was widely used it's generally facing some limitation. This method required high operation cost due to chemical consumption (Kurniawan et al., 2006) and the further treatment of the sludge that generated during the process (Teh

et al., 2016). Furthermore, the usage of the conventional coagulant such as alum was limited by its dosage due to the high dosage of alum-based coagulant released and increased the amount of toxic aluminium species in water (Teh et al., 2016).

### **2.1.2 Co-precipitation**

The co-precipitation method was performed by the addition of the co-precipitation reagent such as sodium hydroxide and iron sulphide into the metal contaminated water. The metal ions are then reacted with the added reagent to form metal hydroxide or metal sulphide as insoluble precipitates (Santhosh et al., 2013). Besides that, heavy metal in water also can be removed as the insoluble metal-ligand precipitate by the addition of synthetic ligand into the water (Blue et al., 2008). The insoluble precipitates can be separated from aqueous solution by filtration or sedimentation. For  $\text{Hg}^{2+}$  removal through the co-precipitation method, a previous study reported the application of hydrogen sulphide and alkali metal sulphide salts as co-precipitation reagents (Ebadian, 2001). This study reported that 99.9% of  $\text{Hg}^{2+}$  was removed from water. In another study, Blue et al. (2008) applied a synthetic ligand called dipotassium salt of 1,3-benzendiamidoethanethiol ( $\text{K}_2\text{BDET}$ ) to treat  $\text{Hg}^{2+}$  contaminated ground water. The  $\text{Hg}^{2+}$  was found to bind with the  $\text{BDET}^{2-}$  and subsequently, formed the insoluble  $\text{Hg-BDET}$  complex as the precipitate. They found that 99.9% of  $\text{Hg}^{2+}$  was removed. Although this method showed high efficiency in  $\text{Hg}^{2+}$  removal, it also has its own weaknesses. For example, the co-precipitation process tends to produce the large amount of low-density sludge, which is difficult to remove from water (Fu and Wang, 2011). In addition, the metal sulphide based precipitate tends to form the colloidal system, which may cause difficulties in the separation process (Fu and Wang, 2011). Moreover, the evolution of toxic  $\text{H}_2\text{S}$  fumes may occur under acidic condition if the sulphur-type of co-precipitation reagents was used (Fu and Wang, 2011).

### 2.1.3 Electrocoagulation

Electrocoagulation (EC) is a technique that applies the electrochemical method for the treatment of polluted water (Ferniza-García et al., 2017; Hakizimana et al., 2017). In EC process, the electric current is applied to water through an electrode (anode) which commonly consisted of iron or aluminum material. The electrochemical dissolution of anode electrode generates the coagulants species such as  $\text{Fe}^{3+}$  or  $\text{Al}^{3+}$ , which have the capability coagulate the soluble or suspended particles to form the settleable floc (Ferniza-García et al., 2017). On the other hand, the reduction of water at cathode will release the hydroxide ion ( $\text{OH}^-$ ) and hydrogen gas ( $\text{H}_2$ ) (Bazrafshan et al., 2012). The  $\text{OH}^-$  reacts with  $\text{Al}^{3+}$  to form aluminum hydroxide ( $\text{Al}(\text{OH})_3$ ) as floc. The  $\text{Al}(\text{OH})_3$  floc with high surface area, acts as a trap for the contaminant such as metal ions in water (Nouri et al., 2010; Nanseu-Njiki et al., 2009). Meanwhile, the released  $\text{H}_2$  gases enhanced the removal of flocculated particles from water (Bazrafshan et al., 2012). According to Nanseu-Njiki et al. (2009),  $\text{Hg}^{2+}$  also can be removed by EC from the water. In this study, the electrode consisted of iron or aluminum was used as the anode. The metal ion released from anode was found to react with  $\text{OH}^-$  to form hydroxide species of  $\text{Hg}^{2+}$ . The reported result showed that 99.9 to 100% of aqueous  $\text{Hg}^{2+}$  were removed. The main concern of this method was the large initial capital investment due to long term operation and costly electricity supply which may restrict its applicability (Arbabi and Golshani, 2016; Fu and Wang, 2011).

#### 2.1.4 Membrane Filtration

Membrane technology such as ultrafiltration (UF), nanofiltration (NF), and reverse osmosis (RO) is one of the popular methods for water purification (Bessbousse et al., 2010). During the membrane filtration process, the water is passing through the permeable membrane with pore size varying from 0.5 to 20 nm. This membrane can retain macromolecule and suspended solid (Barakat et al., 2011). The low-molecular weight solutes and metal ions, which soluble in water are readily to pass through the membranes. Hence, removal of metal ions through membrane filtration always associated with the addition of metal chelating polymers to the water. Incorporation of the metal chelating ligand into the membrane is also another method that has been introduced for metal ions removal. Among various membrane filtration process, polymer enhanced ultrafiltration (PEUF) process is one of the techniques which have been applied in the removal of  $\text{Hg}^{2+}$  in water. In PEUF process, the water-soluble polymer such as polyvinyl alcohol (PVA), polyethylenimine (PEI), polyvinylamine (PVAm) and poly (acrylic acid) (PAA) (Huang et al., 2016; Jana et al., 2011) was added to the water to bind with  $\text{Hg}^{2+}$ . The water sample was then filtered through UF membrane where the  $\text{Hg}^{2+}$ -polymer complexes were rejected by the membrane (Huang et al., 2016). Jana et al. (2011) applied the combination of PVA and chitosan coated ceramic ultrafiltration membrane in UF process. The result shows that almost 100% of  $\text{Hg}^{2+}$  and  $\text{As}^{3+}$  were removed. Huang et al., (2015) reported that the combination of PVAm and pristine UF membrane managed to remove 99% of  $\text{Hg}^{2+}$  in water. Although, PEUF can be a good alternative for metal ions removal, however, membrane fouling by the water-soluble polymer is the main concern in this method. To resolve the fouling problem, the increase of pressure and periodical cleaning have to be carried out and consequently, the maintenance cost increases (Kabay and Bryjak., 2013).

### 2.1.5 Adsorption

Among various treatment methods, removal of heavy metal through adsorption process is receiving high attention because of its high efficiency, technical flexibility and cost-effectiveness (Dong et al., 2016). A wide range of silica-based and carbon-based adsorbents have been developed for the metal ions removal. The carbonaceous materials such as activated carbon (AC), graphene oxide (GO) and carbon nanotube (CNT) have been frequently reported as the effective adsorbents for the removal of the heavy metal ion in water (Arcibar-Orozco et al., 2015; Mubarak et al., 2014; Ren et al., 2013). In general, the carbonaceous materials are not selective materials. In order to enhance the selectivity in the adsorption of the specific metal ion such as  $\text{Hg}^{2+}$ , these carbonaceous materials were often modified with metal capturing groups. For example, Zhu et al. (2009) reported the application of AC that functionalized with the amine group in the removal of  $\text{Hg}^{2+}$ . According to the result obtained by Zhu et al. (2009), the removal efficiency of  $\text{Hg}^{2+}$  by the modified AC was much higher than when the unmodified AC. In another study, polypyrrole was intercalating into GO, and the maximum adsorption capacity of this adsorbent to the  $\text{Hg}^{2+}$  was 980 mg/g (Chandra and Kim, 2011). Pillay et al. (2013) demonstrated the application of sulphur containing MWCNT (S-MWCNT) and AC (S-AC) in the removal of  $\text{Hg}^{2+}$ . They reported that the maximum adsorption capacity was 72.8  $\mu\text{g/g}$  for S-MWCNT and 44.7  $\mu\text{g/g}$  for S-AC. The carbonaceous materials also suffer from a few drawbacks such as the high commercial cost and poor dispersal ability in water (Saka, 2012; Shawky et al., 2012). For example, low dispersal ability of GO in water causing the surface area of GO to decrease drastically in water (Hashim et al., 2016). Hence, the hybridized GO are often produced to overcome the concern on the dispersal ability (Hashim et al., 2016). Moreover, the synthesis processes hybridized carbonaceous materials was tedious and harsh reaction condition are often required.

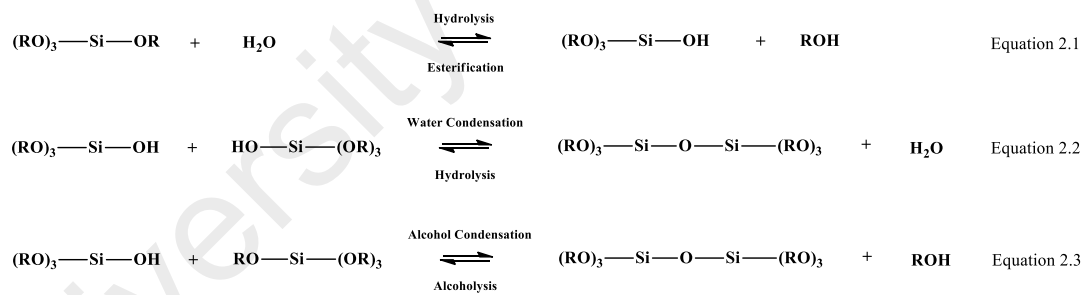
## **2.2 Removal of aqueous metal ion by using sol-gel based adsorbent**

### **2.2.1 Sol-gel and silica gel**

A wide range of silica-based adsorbents has been developed for the removal of heavy metals in aqueous solution. The porous silica or metal frameworks ( $\text{SiO}_2$ ) or so-called sol-gel have become a popular material for metal ions removal due to its simplicity in preparation, low cost, large surface areas, excellent thermal and mechanical stability, rapid adsorption kinetics, excellent anti-swelling properties and good dispersal ability in water (Niu et al., 2015; Zhao et al., 2012). A “sol” is a colloidal suspension of the dispersed solid particle in a dispersion medium or liquid. In this system, the dispersed solid is stable and does not precipitate through gravitational force. The condensation process of the dispersion medium leads to the formation of the cluster, and the bonding between the clusters leads to the formation of a single giant network called gel (Brinker and Scherer, 2013).

There are several routes in producing sol-gel. These processes are such as hydrolysis and condensation of metal or metalloid alkoxide precursor, Pechini’s method, pyrolysis method, organic-hybrids method and non-hydrolytic reaction (Danks et al., 2016; Kumar et al., 2015; Sciancalepore et al., 2017; Wang et al., 2014; Wu et al., 2016). Among these methods, hydrolysis and condensation of various metal or metalloid alkoxide are the most widely used method for the preparation of sol-gel (Dimitriev et al., 2008; Brinker and Scherer, 2013). In hydrolysis and condensation method, various chemicals such as silicates, borate, aluminate and transition metal alkoxide have been used as the precursor (Brinker and Scherer, 2013). Silicon alkoxide such as tetraethoxysilane ( $\text{Si}(\text{OC}_2\text{H}_5)_4$ , TEOS) and tetramethoxysilane ( $\text{Si}(\text{OCH}_3)_4$ , TMOS) are the most common and thoroughly studied materials in sol-gel preparation (Brinker and Scherer, 2013). Sol-gel that produced from silicon alkoxides is also known as silica gel

The preparation of silica gel through hydrolysis and condensation of silicon alkoxide (Figure 2.1) begins with the hydrolysis of alkoxy silane ( $\text{Si}(\text{OR})_4$ ) group under the acidic or basic condition to form the silanol group ( $\text{Si}-\text{OH}$ ) (Equation 2.1). This process continues with the formation of siloxane group ( $\text{Si}-\text{O}-\text{Si}$ ) which constitute the entire silica networks by condensation between  $\text{Si}-\text{OH}$  group (Equation 2.2) or between  $\text{Si}-\text{OH}$  and  $\text{Si}(\text{OR})_4$  group (Equation 2.3) (Hench and West, 1990). Poly-condensation between  $\text{Si}-\text{OH}$  or  $\text{Si}-\text{OH}$  with  $\text{Si}(\text{OR})_4$  form the cluster and the collision between cluster finally forms large aggregate called gel (Brinker and Scherer, 2013). The aging process takes place after gelation process where the poly-condensation process continued to complete the formation of the gel. During the aging process, the gel shrinks due to the expulsion of liquid from the pores (Hench and West, 1990). Finally, the entrapped liquid in the pore network is removed by evaporation to form a xerogel. The gels also can be dried under supercritical conditions to produce aerogels (Danks et al., 2016).



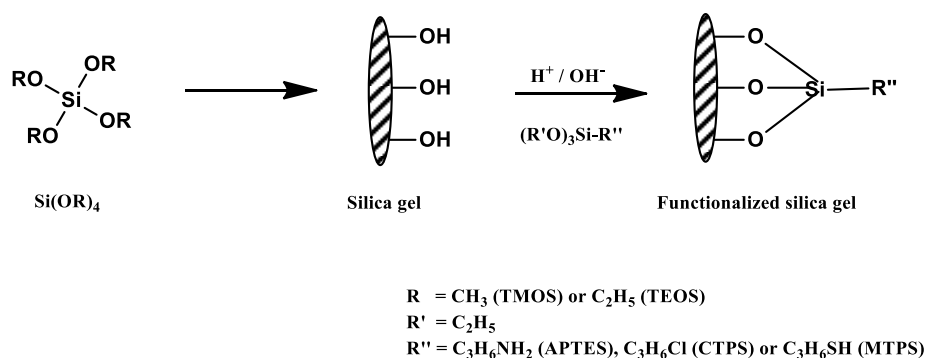
**Figure 2.1:** The mechanism for the formation sol-gel through hydrolysis and condensation of silicon alkoxides (Brinker and Scherer, 2013).

## 2.2.2 Modification of silica gel

Silica gel is a functional material with an impressive range of applications in controlled release process of drug delivery, protective coatings, adsorption, chromatography, separation, biotechnology, energy conservation, cultural heritage restoration, environmental remediation, and many other fields of contemporary technology (Ciriminna et al., 2013). In order to enhance the properties and effectiveness of silica gel in metal ions adsorption, this material is often modified through various surface functionalization process. The silica gel with the OH groups at the surface are often functionalized by grafting method, co-condensation method and the bridged organosilane as precursors (Hoffmann et al., 2006). To further improve the performance of the adsorbent in adsorption of metal ion, various metal capturing ligands also have been immobilized onto the functionalized silica gel or incorporated into the silica gel matrix.

### 2.2.2.1 Surface modification of silica gel through grafting method

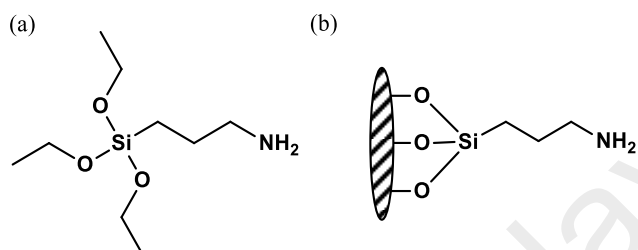
The functionalization of mesoporous silica can be carried out by covalently immobilizing the organosilane or so-called silane coupling reagents onto the silica surface through grafting method (Yokoi et al., 2004). This process is achieved by reacting organosilanes such as 3-aminopropyltrimethoxysilane (APTES), 3-chloropropyltriethoxysilane (CPTS) and methacryloxypropyltriethoxysilane (MPTS) with the free silanol group of silica gel (Jal et al., 2004; Rahman and Padavettan, 2012) as shown in Figure 2.2.



**Figure 2.2:** Surface functionalized silica gel through grafting methods.

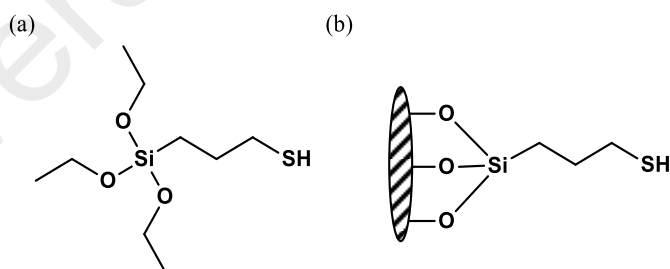


Heidari et al. (2009) functionalized the nano-MCM-41 mesoporous silica using APTES (Figure 2.3a) to generate the amine functionalized silica-based adsorbent (Figure 2.3b) (nano NH<sub>2</sub>-MCM 41) for the removal of Ni<sup>2+</sup>, Cd<sup>2+</sup>, and Pb<sup>2+</sup> from ternary aqueous solution. The removal efficiency of this material was 92, 93 and 97% for Ni<sup>2+</sup>, Cd<sup>2+</sup>, and Pb<sup>2+</sup>, respectively, by using 5.0 g/L of nano NH<sub>2</sub>-MCM 41.



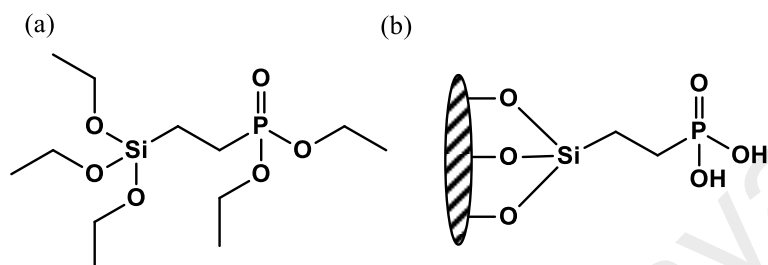
**Figure 2.3:** (a) APTES and (b) amine functionalized silica based adsorbent.

Fan et al. (2016) grafted the MPTS (Figure 2.4a) onto the surface of silica gel surface to study the adsorption ability of this mercapto-functionalized silica gel (Figure 2.4b) towards Sb<sup>3+</sup>. This adsorbent showed high adsorption affinity toward Sb<sup>3+</sup>, and it was suggested as an efficient adsorbent for the removal of Sb<sup>3+</sup> from aqueous solution.



**Figure 2.4:** (a) MPTS and (b) mercapto-functionalized silica gel.

Diethylphosphatoethyltriethoxysilane (Figure 2.4a) was also grafted onto the silica gel to produce phosphorus acid-functionalized silica gel (Figure 2.4b) to produce an adsorbent for the adsorption of  $U^{6+}$  from aqueous solution. The maximum adsorption capacity of this material was found to be 76.9 mg/g (Zhou et al., 2016).

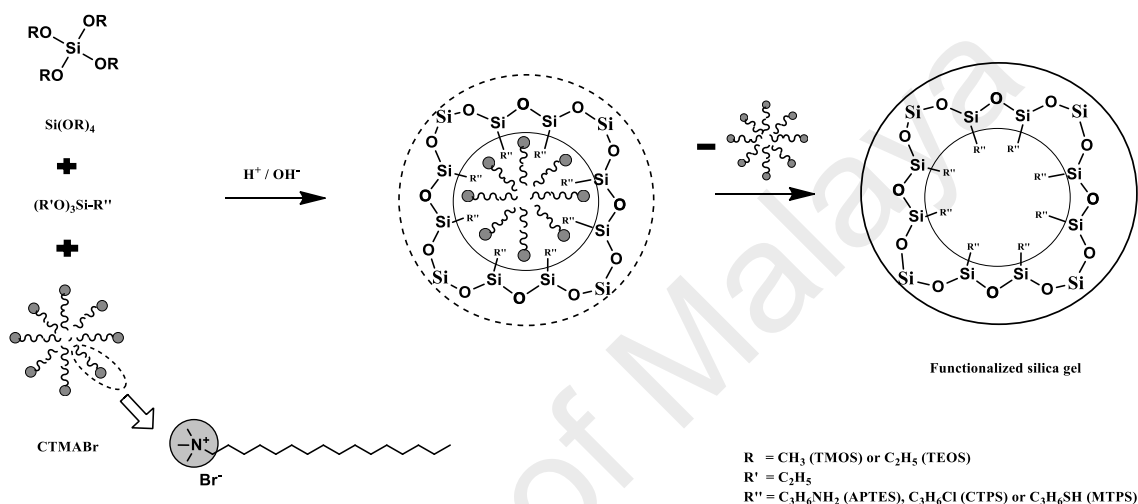


**Figure 2.5:** (a) Diethylphosphatoethyltriethoxysilane and (b) phosphorus acid-functionalized silica gel.

#### 2.2.2.2 Surface modification of silica gel through co-condensation method

Co-condensation process (Figure 2.6) is another method for the functionalization of silica gel. In this method, the organic functionalities are covalently bonded onto the silica gel through one-pot synthesis. For the synthesis, the organosilanes that are containing specific functional group is mixed with the aqueous cationic surfactant and  $Si(OR)_4$  during condensation process under basic condition (Trewyn et al., 2007). The cationic surfactant such as cetyltrimethylammonium bromide (CTMABr-C<sub>19</sub>H<sub>42</sub>NBr), tetradecyltrimethylammonium bromide (TTMABr-C<sub>17</sub>H<sub>38</sub>NBr) and trimethyloctadecylammonium bromide (DTMABr-C<sub>21</sub>H<sub>46</sub>NBr) act as structure directing agent, which is responsible to generate the porosity of silica gel matrix (Costa et al., 2014; Soto et al., 2016). Da'na and Sayari (2011) synthesized amine-functionalized mesoporous silica gel by mixing TEOS, APTES, and Pluronic P123 surfactant. This adsorbent was found to be highly selective and effective in removing of  $Cu^{2+}$ . On the other hand, Machida et al. (2012) investigated the ability of amino (NH<sub>2</sub>), and mercapto (SH) functionalized mesoporous silica (HMS) for the adsorption of  $Cd^{2+}$  and  $Pb^{2+}$ . These

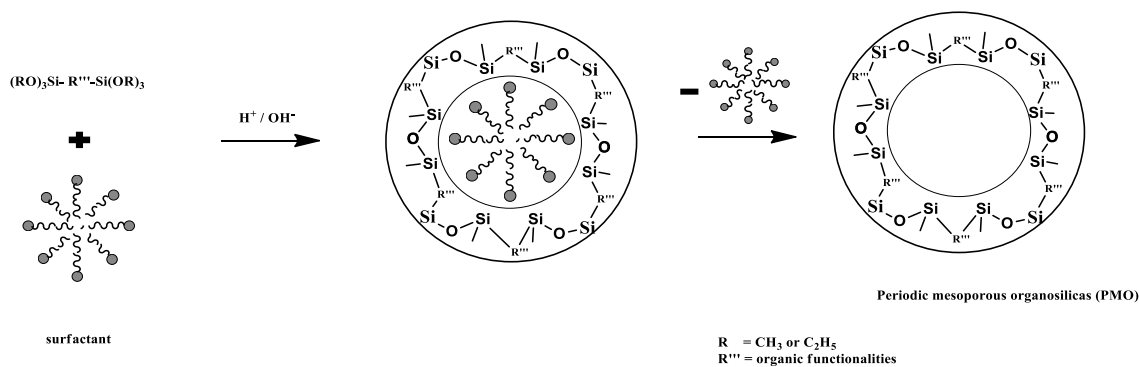
materials were synthesized through the co-condensation method by using TEOS, Dodecylamine (DDA) surfactant, APTES (for NH<sub>2</sub>-HMS) and MPTS (for SH-HMS) (Machida et al., 2012). The result showed that NH<sub>2</sub>-HMS adsorbed the highest amount of Cd<sup>2+</sup> and Pb<sup>2+</sup> with maximum adsorption capacity ( $Q_m$ ) equal to 0.25 and 0.45 mmol/g respectively.



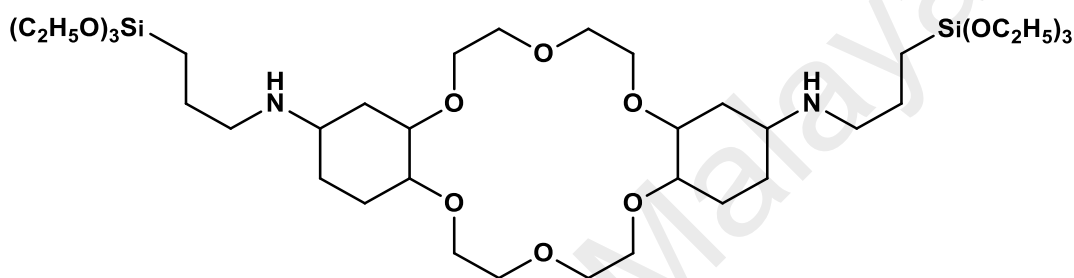
**Figure 2.6:** Formation pathways of functionalized silica gel through co-condensation method.

### 2.2.2.3 Modification of silica gel by using Periodic mesoporous organosilica

Grafting and co-condensation method are related to the surface modification of silica gel. On the other hand, functionalization of silica gel also can be carried out by using bridged organosilane precursors. Periodic mesoporous organosilica (PMO) are produced using bridged bi-silane,  $(\text{RO})_3\text{Si-R}'''\text{-Si(OR)}_3$ .  $(\text{RO})_3\text{Si-R}'''\text{-Si(OR)}_3$  containing organic functionalities (R''') such as ethane, ethene, 2,5-thiophene, and 1,4-benzene (Dag et al., 2001) which connecting two silane groups. The R''' group is entrapped in the three-dimensional silica gel matrix (Figure 2.7). For example, Leng et al. (2013) used the bisilylated crown ether (Figure 2.8) alongside with TMOS to synthesize a PMO for the adsorption of Sr<sup>2+</sup>. As shown in the result obtained by Leng et al. (2013), the PMO incorporated silica adsorbent was selective towards the adsorption of Sr<sup>2+</sup> in the presence of the various interfering ions.



**Figure 2.7:** Formation pathways of periodic mesoporous organosilicas (PMO).



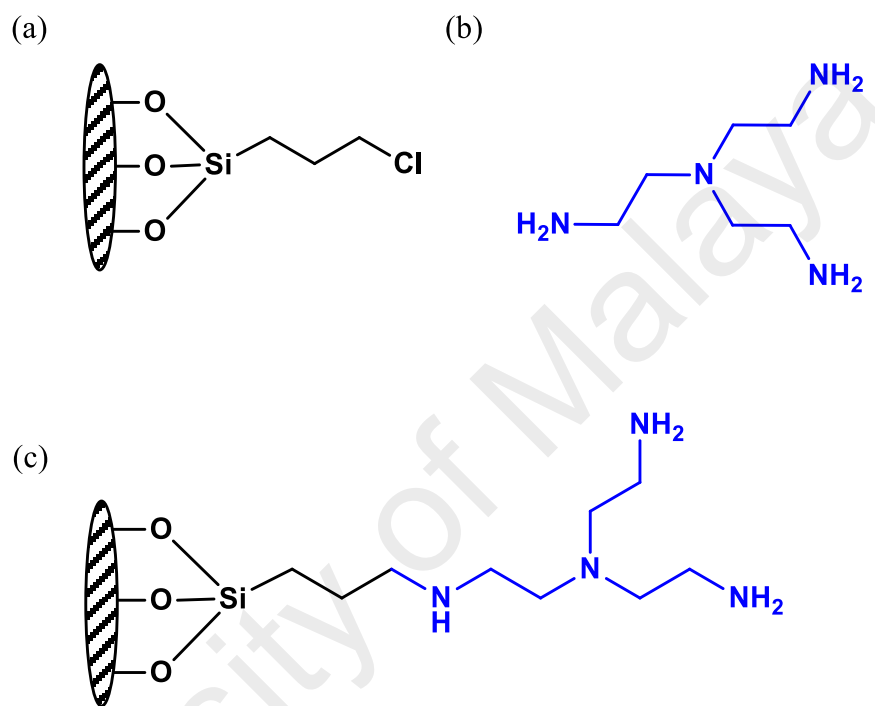
**Figure 2.8:** Bisilylated crown ether.

#### 2.2.2.4 Immobilization of metal capturing ligand onto the surface of silica gel

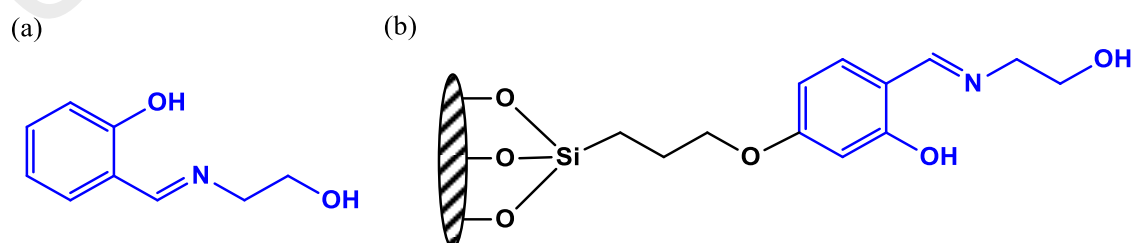
Despite the direct functionalization of silica gel, various metal capturing ligands also have been immobilized onto silica gel. These metal capturing ligands tend to enhance the metal ions adsorption ability and selectivity of the functionalized silica gel. The ligands that exhibit strong affinity towards specific metal ion are widely available. For example, sulphur-containing ligands such as dithiocarbamate derivatives are often found to be the selective ligands toward the complexation with  $Hg^{2+}$ . Hence, these ligands can be immobilized onto the silica gel to produce selective adsorbents for  $Hg^{2+}$ .

Throughout the history, various selective adsorbents have been produced for the adsorption of specific metal ions. For example, in a study reported by Huang et al. (2008), the silica gel was first functionalized with chloro group (Figure 2.9a). Then, the tris(2-aminoethyl) amine ligand (Figure 2.9b) was immobilized onto this chloro-functionalized silica gel. The tris(2-aminoethyl) amine modified silica gel (Figure 2.9c) was applied as

the adsorbent for  $\text{Cr}^{3+}$ ,  $\text{Cd}^{2+}$ , and  $\text{Pb}^{2+}$ . The reported maximum adsorption capacities were 32.7, 36.4 and 64.6 mg/g for  $\text{Cr}^{3+}$ ,  $\text{Cd}^{2+}$ , and  $\text{Pb}^{2+}$ . In another study, a Schiff base, *N*-(2-hydroxyethyl) salicylaldimine (Figure 2.10a), was used as a ligand to modify the chloro functionalized SBA-15 mesoporous silica (Tadjarodi et al., 2015). This material (Figure 2.10b) removed 96% of  $\text{La}^{3+}$  in water (Tadjarodi et al., 2015).

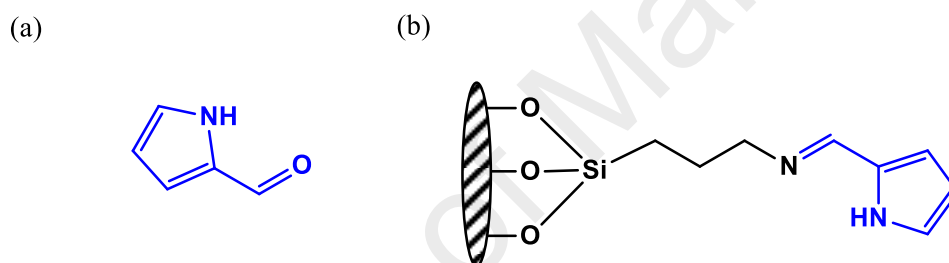


**Figure 2.9:** (a) Chloro functionalized silica gel, (b) tris(2-aminoethyl) amine and (c) tris(2-aminoethyl) amine modified silica gel.

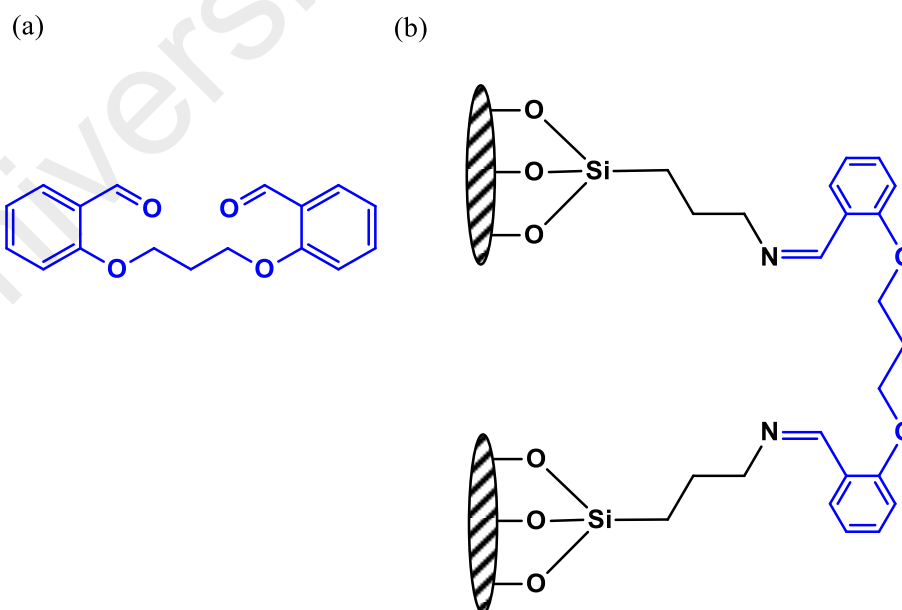


**Figure 2.10:** (a) *N*-(2-hydroxyethyl) salicylaldimine and (b) *N*-(2-hydroxyethyl) salicylaldimine-functionalized mesoporous silica gel.

Radi et al. (2014) immobilized a ligand called 1*H*-pyrrole-2-carbaldehyde (Figure 2.11a) onto an amine-functionalized silica gel to form a new adsorbent (Figure 2.11b). This adsorbent was found to be selective towards the adsorption of Cu<sup>2+</sup>, Zn<sup>2+</sup>, and Cd<sup>2+</sup> from aqueous solution. The reported maximum adsorption capacity was 27.9, 24.2 and 20.3 mg/g for Cu<sup>2+</sup>, Zn<sup>2+</sup>, and Cd<sup>2+</sup>. Banaei et al. (2015) reported the immobilization of bisaldehyde ligand, 2,2'-(propane-1,3-diylbis(oxy))dibenzaldehyde (Figure 2.12a) onto the silica-coated magnetite particle to generate the bisaldehyde functionalized magnetic silica gel (Figure 2.12b). This material selectively removed more than 95% Ag<sup>+</sup> from aqueous samples.

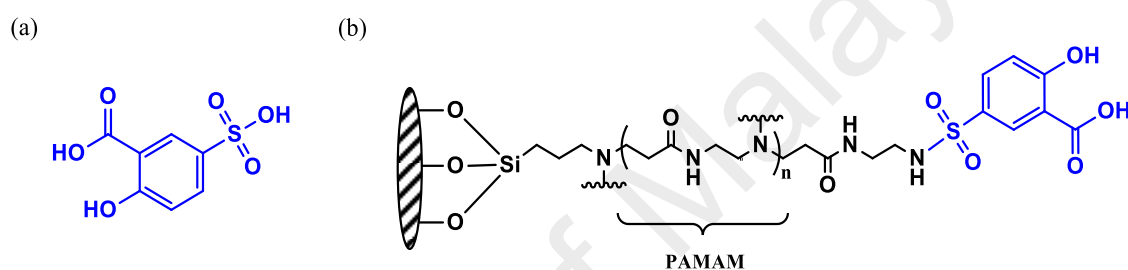


**Figure 2.11:** (a) 1*H*-pyrrole-2-carbaldehyde and (b) 1-(Pyrrol-2-yl)imine modified silica gel.

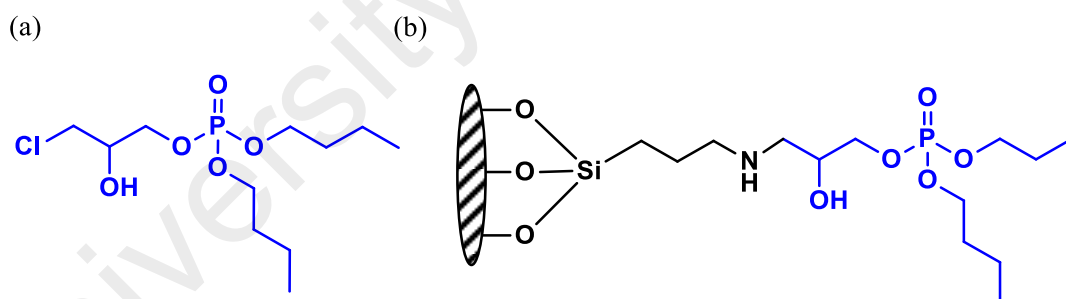


**Figure 2.12:** (a) 2, 2'-(propane-1,3-diylbis(oxy))dibenzaldehyde and (b) bisaldehyde modified silica gel.

In another study, 5-sulfosalicylic acid (Figure 2.13a) was bonded to dendrimer-like poly-amidoamine (PAMAM) modified silica gel (Wu et al., 2016). The immobilized 5-sulfosalicylic acid silica gel (Figure 2.13b) was used to adsorb  $Pb^{2+}$  in the water sample. Wu et al. (2016) revealed that almost 100% of  $Pb^{2+}$  was successfully removed from the water. Guo et al. (2017) immobilized the dibutyl (3-chloro-2-hydroxypropyl) phosphate (Figure 2.14a) onto the surface of mesoporous silica gel (Figure 2.14b). This material was used to remove  $U^{6+}$  in water. The result showed that this material was able to remove almost 100% of  $U^{6+}$ .



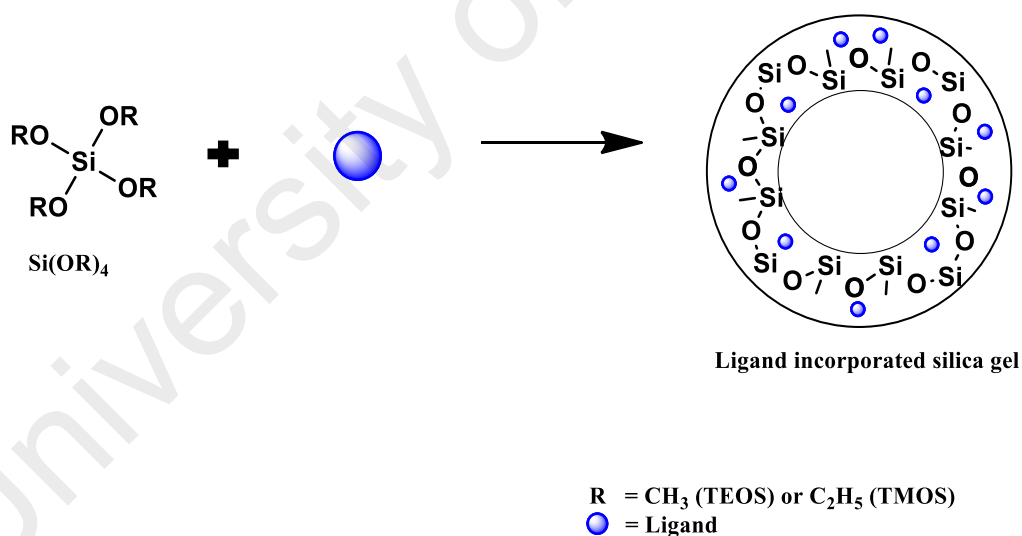
**Figure 2.13:** (a) 5-sulfosalicylic acid and (b) 5-sulfosalicylic acid / PAMAM modified silica gel.



**Figure 2.14:** (a) Dibutyl (3-chloro-2-hydroxypropyl) phosphate and (b) phosphoryl modified mesoporous silica gel.

### 2.2.2.5 Metal capturing ligand incorporated silica gel

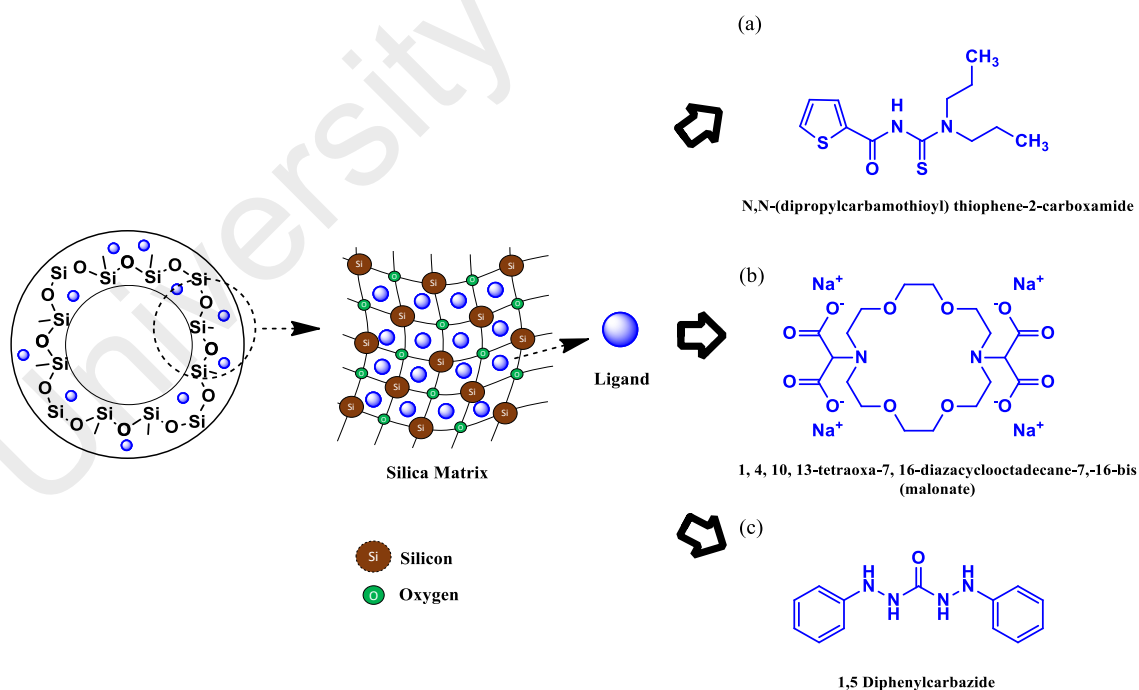
The modification of silica gel by immobilization of ligand involved multi-step reaction. Also, the functionalization of silica gel through grafting, co-condensation, and PMO methods often involved the use of various chemicals, which included silane coupling agent, structure directing reagent, solvents, and ligands. This may increase the chemical usage and the time of synthesis. Hence, to overcome such disadvantages, the approach to incorporate the metal capturing ligand into silica gel matrix during its preparation has been developed (Figure 2.15). In this approach, the ligand is entrapped into the silica gel matrix instead of covalently bonding it to the silica gel. Furthermore, the incorporated ligand or so-called doped-ligand was found to retained its chemical properties (Yost et al., 2000) and the synthesized route was relatively simple compared with the immobilization method.



**Figure 2.15:** Formation pathways of metal capturing incorporated silica gel.



For example, by just using TEOS as a precursor, Mehmood et al. (2013) incorporated a ligand called *N,N*-(dipropylcarbamothioyl) thiophene-2-carboxamide (Figure 2.16a) into the silica gel matrix. This adsorbent managed to remove 95% of  $\text{Cu}^{2+}$  from  $\text{Cu}^{2+}$  solution with the concentration of 1 mg/L. The crown ether type of ligand, 1, 4, 10, 13-tetraoxa-7, 16-diazacyclooctadecane-7,-16-bis (malonate) (Figure 2.16b) was incorporated into the silica gel matrix. The selected ligand is selective toward the complexation with  $\text{Sr}^{2+}$  (Yost et al., 2000). The crown ether incorporated silica gel has been found to retain its chemical property where it was selective in the removal of  $\text{Sr}^{2+}$  in aqueous solution (Yost et al., 2000). Besides that, an organic ligand, 1,5-diphenylcarbazide (DPC) (Figure 2.16c) was doped into the silica gel matrix by Khan et al. (2006). The DPC tends to coordinate with  $\text{Hg}^{2+}$  to form the complex. This ligand has been found to be a promising material for  $\text{Hg}^{2+}$  extraction from the aqueous sample. Khan et al. (2006) reported that about 90% of  $\text{Hg}^{2+}$  was removed from water by the DPC incorporated silica gel.

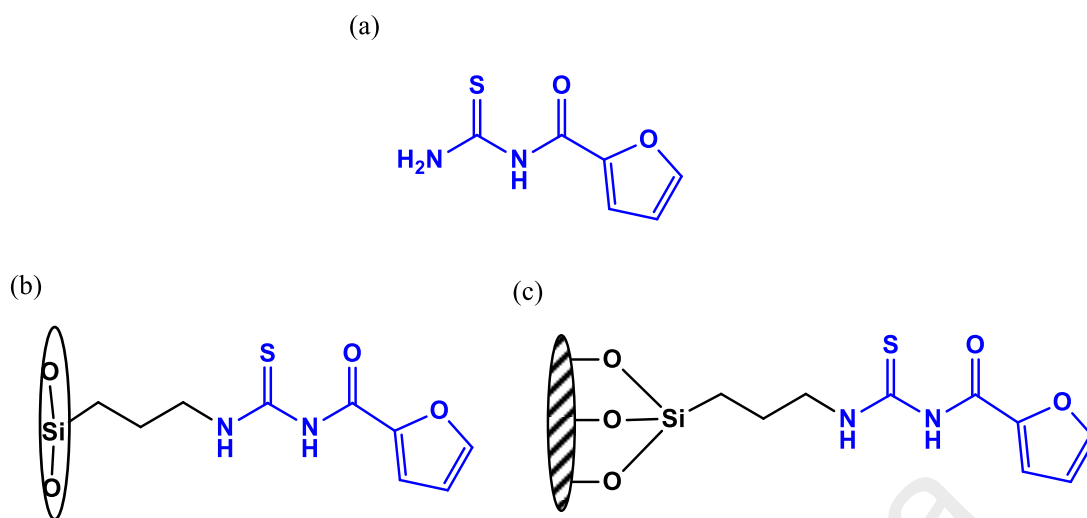


**Figure 2.16:** A variety of ligand used to incorporate into silica gel.

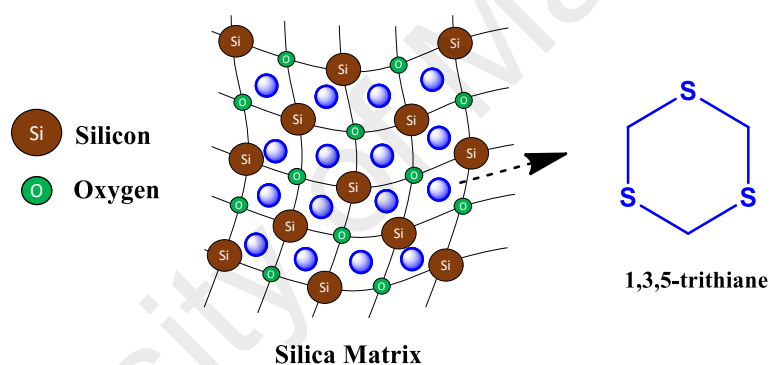
### 2.3 Sulphur containing ligand modified silica gel for the removal of aqueous $\text{Hg}^{2+}$

Sulphur containing compounds have frequently been used as the ligand to capture  $\text{Hg}^{2+}$  in aqueous solution (Qu et al., 2013).  $\text{Hg}^{2+}$  is a soft acid, and it tends to bind to the sulphur atom, which acts as the soft base through complexation (Wajima and Sugawara, 2011). Silica gel that modified with functional group that containing sulphur atom has also shown great chemical activity to remove  $\text{Hg}^{2+}$  in aqueous solution (Aguado et al., 2005; Antochshuk et al., 2003; Cestari and Airoidi, 1997; Evangelista et al., 2007; Johari et al., 2014; Prado et al., 2004; Puanggam and Unob, 2008).

The sulphur containing ligands are often grafted or incorporated on silica gel. For example, 1-furoyl thiourea (Figure 2.17a) was covalently anchored onto chloro-functionalized silica gel through co-condensation (Figure 2.17b) and grafting methods (Figure 2.17c) by Mureseanu et al. (2010) for the preparation of adsorbents for  $\text{Hg}^{2+}$ . The maximum adsorption capacity of the adsorbents that prepared through co-condensation and grafting methods were 56.2 and 122.4 mg Hg/g, respectively. Esmaeili Bidhendi et al. (2014) synthesized another ligand named 1,3,5-trithiane (Figure 2.18) and incorporated it into mesoporous silica gel matrix. This 1,3,5-trithiane doped silica gel showed a good capability in  $\text{Hg}^{2+}$  removal with the maximum adsorption capacity of 10 mg/g.



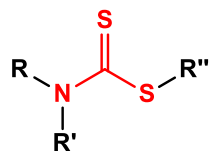
**Figure 2.17:** (a) 1-furoyl thiourea, (b) 1-furoyl thiourea functionalized SBA-15 (co-condensation route) and (c) 1-furoyl thiourea functionalized SBA-15 (grafting method).



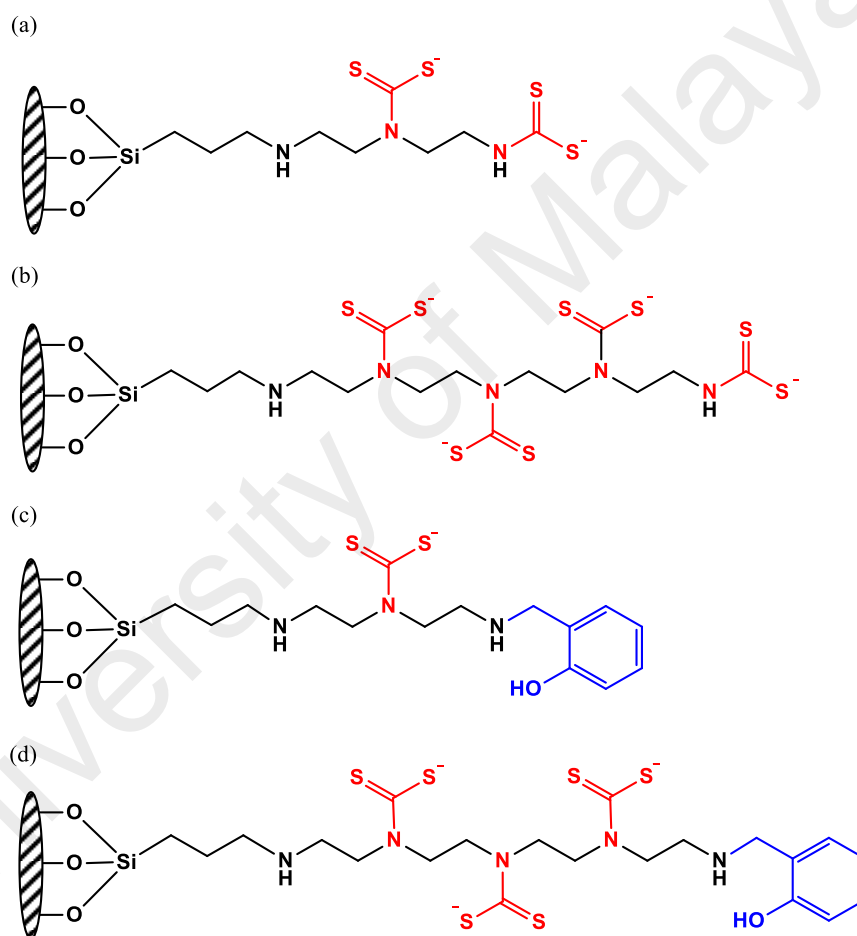
**Figure 2.18:** 1,3,5-trithiane doped in silica matrix.

Among the various sulphur containing ligands, the capability of dithiocarbamate (Figure 2.19) and its derivatives to complex with  $\text{Hg}^{2+}$  has been widely reported (Denizli et al., 2000; Figueira et al., 2011; Girginova et al., 2010; He et al., 2015; He et al., 2016; Say et al., 2008; Venkatesan et al., 2002). Silica gel that containing dithiocarbamate group (Si-DiTC) can be synthesized directly by modifying the functionalized silica gel with  $\text{CS}_2$  (Venkatesan et al., 2002). For example, He et al. (2015) and He et al. (2016) functionalized the silica gel with diethylenetriamine, tetraethylenepentamine, diethylenetriamine-salicylaldehyde and tetraethylenepentamine-salicylaldehyde (Figure 2.20) to prepare amine groups functionalized silica gel. The amine groups functionalized

silica gel was then modified with CS<sub>2</sub> to produce Si-DiTC. With the presence of various metal ions, these synthetic adsorbents showed high maximum adsorption capacity ranging from 169.7 to 225.8 mg/g for Hg<sup>2+</sup>.

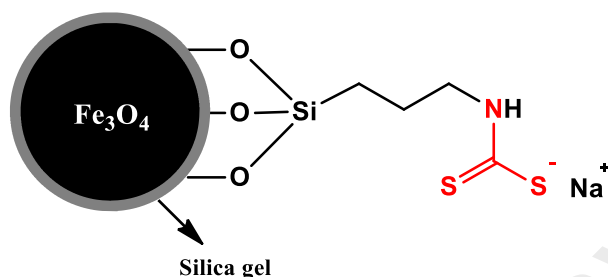


**Figure 2.19:** Common structure of dithiocarbamate compound.



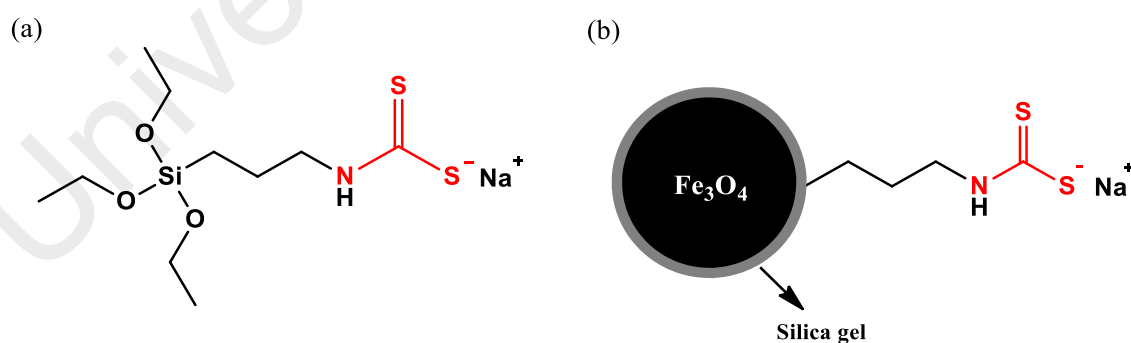
**Figure 2.20:** (a) CS<sub>2</sub> modified diethylenetriamine functionalized silica gel, (b) CS<sub>2</sub> modified tetraethylenepentamine-salicylaldehyde functionalized silica gel, (c) CS<sub>2</sub> modified diethylenetriamine functionalized silica gel and (d) CS<sub>2</sub> modified tetraethylenepentamine-salicylaldehyde functionalized silica gel.

On the other hand, the silica coated magnetite particles derivatized with dithiocarbamate groups (Figure 2.21) was synthesized by Girginova et al. (2010) by grafting the CS<sub>2</sub> on amine functionalized silica gel, and the high efficiency of Hg<sup>2+</sup> uptake (74%) was recorded by this material.



**Figure 2.21:** Silica coated magnetite particles derivatized with dithiocarbamate group.

Instead of grafting CS<sub>2</sub> to the functionalized silica gel, the Si-DiTC also can be obtained by converting the silane coupling agent such as APTES to dithiocarbamate derivative before the silica gel preparation (Tavares et al., 2013). The siloxydithiocarbamate (Figure 2.22a) compound was used as precursor material alongside with TEOS to coat the surface of magnetite particles (Figure 2.22b). This material successfully removed 99.8% of Hg<sup>2+</sup> in the aqueous sample.



**Figure 2.22:** (a) Siloxydithiocarbamate compound, and (b) dithiocarbamate modified silica gel coated magnetite particle.

The reaction between CS<sub>2</sub> and amine group on silica surface are generally conducted under harsh conditions where the strong alkaline condition may cause the degradation of silica gel (Bai et al., 2011). In addition, to attach the dithiocarbamate group onto the silica gel, silica gel need to be functionalized with small molecular weight amine derivatives such as diethylenetriamine and tetraethylenepentamine (He et al., 2015; He et al., 2016) and this reduce the number of dithiocarbamate group on Si-DiTC (Bai et al., 2011).

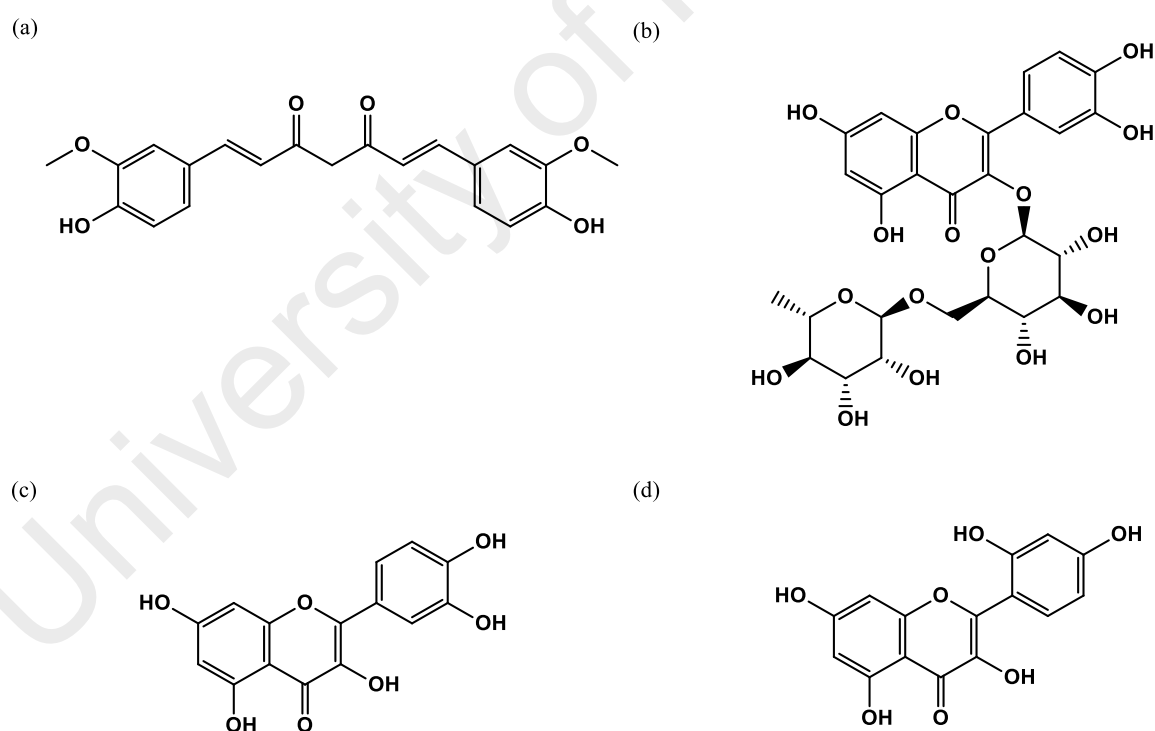
## **2.4 Natural product based ligand**

### **2.4.1 Metal capturing ability of natural products**

So far, most of the doped or immobilized ligands onto the silica gel are mostly synthetic chemicals. Synthesis of ligands is not economic and not environmentally friendly since it involved multi-step reaction and required various chemicals. Therefore, it is worth to study the potential of natural products as metal capturing ligands. Natural products are organic compounds, which can be extracted from microbes, plants, and animals. These compounds have remarkable structural diversity and biological characteristics (Ding et al., 2016; Wang et al., 2016). Some natural products are containing various functional groups such as carbonyl, hydroxyl, amines, and ketone group as electron donating group. Consequently, these natural compounds also have the potential to complex with metal ions. The metal capturing ability of some natural products such as curcumin, quercetin, rutin, and morin also has been proven.

Curcumin (Figure 2.23a) is a hydrophobic polyphenol with the chemical structure called bis-R-unsaturated-diketone, which can be extracted from ginger (Arnand et al., 2007; Karri et al., 2015). The ability of curcumin and its derivatives to form complexes with several metals was reported by Wanninger et al. (2015). Picciano and Vaden (2013)

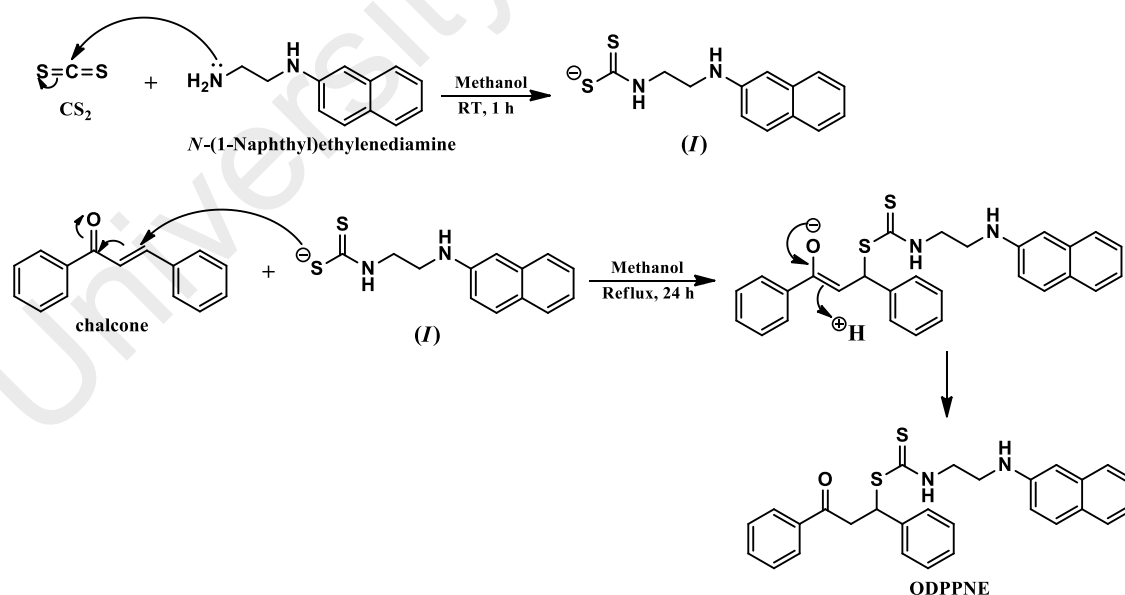
further proved the binding ability of curcumin toward  $\text{Cu}^{2+}$ . Rutin (Figure 2.23b) is a naturally occurring flavonoid, which consists of ketone and hydroxyl group. Due to the rich of functional group, natural rutin has been shown to have the capability to form the complexes with  $\text{Cr}^{3+}$ ,  $\text{Zn}^{2+}$ , and  $\text{Sn}^{2+}$  (Ikeda et al., 2015; Panhwar and Memon, 2014; Zhai et al., 2014). Quercetin (Figure 2.23c) is another flavonoid that can be obtained from various plants. It tends to form complexes with  $\text{Al}^{3+}$  and  $\text{Tb}^{3+}$  (Dolatabadi et al., 2014; Furia et al., 2014). In addition, another natural product called morin (Figure 2.23d) was found to form a complex with  $\text{Zn}^{2+}$  (Sendrayaperumal et al., 2014). So far, most of these natural product based ligands are belong to a class of chemical named flavonoid. This study investigated the potential of another class of natural product named chalcone as metal capturing ligand.



**Figure 2.23:** (a) Curcumin, (b) Rutin, (c) Quercetin and (d) Morin.

## 2.4.2 Chalcone

Chalcone (Figure 1.2a) is a type of natural product that containing two aromatic rings linked by a three carbons  $\alpha$ ,  $\beta$ -unsaturated carbonyl system. Chalcone-type of natural products can be obtained easily from fruits (e.g., citruses, apples), vegetables (e.g., tomatoes, shallots, bean sprouts, and potatoes), and spices (Orlikova et al., 2011; Patil et al., 2010). Chalcone and its derivative showed the remarkable biological activities such as anti-cancer, anti-inflammatory, anti-HIV, etc. (Singh et al., 2014) but the adsorption ability of chalcone for various metal ions has not been reported elsewhere. In this study, the chalcone was modified into dithiocarbamate derivative, ODPPE, through reaction pathway shown in Figure 2.24. As mentioned previously, dithiocarbamate has the chelating ability towards  $\text{Hg}^{2+}$  (Heard, 2005; Kanchi et al., 2014). The synthesized ODPPE was doped into the silica gel for the preparation of adsorbent for the removal of  $\text{Hg}^{2+}$  in water. ODPPE was also incorporated onto the silica gel coated magnetic particles for the preparation of solid phase to pre-concentrate  $\text{Hg}^{2+}$  in water.



**Figure 2.24:** Synthesis pathway of ODPPE.



## **2.5 Pre-concentration of trace heavy metal from aqueous sample.**

Direct determination of trace pollutants such as heavy metal ions in water may require complicated sample preparation procedure due to the limitation of instruments (Wen and Zhu, 2014). For example, the concentration of Hg in natural water samples could vary from pg/L to ng/L (Zhang et al., 2014) while the detection limit for instruments which can be used to quantify Hg such as ICP and AAS are at the  $\mu\text{g/L}$  level (WHO, 2005). In addition, the matrix effect appears in the water sample may interfere with the analysis. Therefore, an appropriate pre-concentration method for trace metal analysis is required.

### **2.5.1 Solid phase extraction and solid phase micro-extraction as the pre-concentration method**

Conventional solid phase extraction methods (SPE) have become the standard technique to pre-concentrate trace element in the aqueous sample due to its simplicity, less chemical consumption, rapid, and high enrichment factor (Hu et al., 2015; Pytlakowsk, 2016; Yilmaz and Soylak, 2014). In SPE process, the analytes are transferred from the water sample to the solid adsorbent phase (Hu et al., 2015). The analytes that retained on the adsorbent can be recovered by elution with specific solvent or reagent. The adsorbent phase employed in conventional SPE can consist of different materials such as polymer beads, silica gel, modified silica gel, activated carbon (Habila et al., 2014), molecularly imprinted polymer (Nestora et al., 2016) and metal-organic framework (Xie et al., 2015). These SPE adsorbents are contained in the cartridges, syringe barrels or disk (Wells et al., 2003).

In order to enhance the efficiency of conventional SPE, the manipulated SPE technique called solid phase micro-extraction (SPME) was developed. In SPME, the conventional adsorbents were replaced by the nano-size adsorbent in according to their high surface-area-to-volume ratio, simple derivatization procedure, and unique thermal,

mechanical or electronic properties (Zhang et al., 2013). Among the nano-size adsorbents, carbonaceous materials such as single wall carbon nanotube (SWMNT) (Asghari et al., 2016; Gutierrez et al., 2017), multiwall carbon nanotube (MWCNT) (Yilmaz and Soylak, 2014; Zhou et al., 2014), graphene oxide (GO) (Pourjavid et al., 2014; Yang et al., 2012) were widely used as adsorbent in SPME. However, the application of these nanoparticles in SPME can be disrupted by several conditions. The nanoparticles may aggregate to cause the reduction of surface area of adsorbent, produced the back-pressure in extraction instrument and clogging SPME device resulted in the failure of extraction process (Pytlakowski, 2016). Also, SPME method also suffers other drawbacks such as large secondary wastes, time-consuming, and complex equipment may be needed (Asgharinezhad et al., 2014). Therefore, to overcome the problems mentioned above, Anastassiades et al. (2003) have introduced an easy and rapid method called dispersive-solid phase extraction (D-SPE).

### **2.5.2 D- $\mu$ SPE**

In D-SPE, a small amount of adsorbent is directly added to the water sample. The nano-size adsorbents are dispersed in water using various agitation methods (Khezeli and Daneshfar, 2017). The dispersed adsorbent adsorbs the target analytes such as heavy metal ions in the water. Then, centrifugation or filtration is often applied to isolate the dispersed adsorbent. The analytes retained on the isolated adsorbent can be recovered through desorption process using suitable solvent or reagent (Xian et al., 2017). This approach enables the adsorbent to interact equally with all samples and greater capacity per amount of adsorbent can be achieved (Abdolmohammad-Zadeh and Talleb, 2012). Recently, dispersive micro-solid phase extraction method (D- $\mu$ SPE) has been developed as the miniaturized extraction technique when nanoparticles with unique size and physical/chemical properties were used as the adsorbent (Pytlakowski, 2016; Khezeli and Daneshfar, 2017).

### 2.5.3 D- $\mu$ SPE as pre-concentration method for heavy metal ions in water

The application of D- $\mu$ SPE as the pre-concentration process of trace metal ion in aqueous solution has been widely reported. The conventional adsorbents used in D- $\mu$ SPE can consist of the nanoparticle materials such as carbon nanotube (CNT) (Krawczyk and Jeszka-Skowron, 2016), graphene (Kocot and Sitko, 2014), graphene oxide (GO) nanosheet (Ghazaghi et al., 2016). Application of these materials in D- $\mu$ SPE usually required the addition of metal capturing ligand to enhance the selectivity. For example, Feist (2016) incorporated a chelating reagent named 1,10-phenanthroline to the oxidized MWCNT. This adsorbent was to pre-concentrate  $\text{Cd}^{2+}$  and  $\text{Pb}^{2+}$ . In another method, ammonium pyrrolidine dithiocarbamate (APDC) was applied as the metal capturing ligand for  $\text{Cd}^{2+}$  and  $\text{Pb}^{2+}$  in the D- $\mu$ SPE process (Kocot et al., 2013). In this method, the obtained  $\text{Cd}^{2+}$ -APDC and  $\text{Pb}^{2+}$ -ADDC complex was then adsorbed by the dispersed MWCNT to form the sediments which was isolated from the water sample (Kocot et al., 2013). Another modification process was reported by Bahadir et al. (2015) where an anionic exchanger tricaprilmethylammonium chloride (Aliquat 336) was loaded onto the MWCNT in order to extract  $\text{Cr}^{6+}$  in drinking water through D- $\mu$ SPE. Pytlakowski (2016) reported that another D- $\mu$ SPE process where  $\text{Cr}^{3+}$ ,  $\text{Co}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Pb}^{2+}$  and  $\text{Zn}^{2+}$  in water samples was pre-concentrated using an azo dye named 2-(5-bromo-2-pyridylazo)-5-diethylaminophenol (5-Br-PADAP), as a complexing reagent and the GO nanoparticles as an adsorbent. Zawisza et al. (2016) reported the application of ethylenediamine modified GO (EDA-GO) as a solid phase for the pre-concentration  $\text{Fe}^{3+}$ ,  $\text{Co}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Pb}^{2+}$ , and  $\text{Zn}^{2+}$  in the real water sample. This material was synthesized through the suspension of GO in ethylenediamine and refluxed with *N,N*-dicyclohexylcarbodiimide (Zawisza et al., 2016).

Instead of the carbonaceous nanoparticle, other nanomaterials such as halloysite nanotube (Krawczyk et al., 2016), silica-nanoparticle (Shirkhanloo et al., 2016), and silver-nanoparticle (Krawczyk and Stanisiz, 2015) also have been employed as the adsorbent phase in D- $\mu$ SPE. Krawczyk et al. (2016) reported the application of dendrimer modified halloysite nanotubes as an adsorbent for ultrasound-assisted D- $\mu$ SPE for the pre-concentration of Cd<sup>2+</sup> and Pb<sup>2+</sup> in the water sample. For selective extraction of Ni<sup>2+</sup> in the water sample, Jalali and Aliakbar, (2015) modified the mercapto functionalized MCM-41 mesoporous silica with 4-nitrophenol and the resulting material was employed as the adsorbent phase in the D- $\mu$ SPE system. The combination of silver-nanoparticle (Ag-NP) as solid adsorbent and D- $\mu$ SPE for determination of Hg<sup>2+</sup> in water sample was reported by Krawczyk and Stanisiz (2015).

In spite of the popularity gain by the application of D- $\mu$ SPE technique in the pre-concentration process, however, the laborious and time-consuming procedure such as centrifugation and filtration is always required in retrieving adsorbents after extraction (Wierucka and Biziuk, 2014). Hence, the application of magnetic nanoparticle (MNP) as the adsorbent phase for D- $\mu$ SPE has drawn attention by many researchers (Giakisikli and Anthemidis, 2013). With magnetic property, MNP can be retrieved from the water by using external magnetic field without any instrumentation.

#### **2.5.4 MNP as adsorbent phase in D- $\mu$ SPE**

Magnetic nanoparticle (MNP) has the special characteristic such as large surface area, easy to isolate by applying the external magnetic force and simplicity in preparation. When MNP are used adsorbents, their superparamagnetic properties allow it to be separated from water by an external magnetic field. As a result, the duration of sample preparation can be significantly shortened. Iron oxide (Fe<sub>3</sub>O<sub>4</sub>) is the most common MNP (Lee et al., 2015). Pure Fe<sub>3</sub>O<sub>4</sub> is an inorganic nanoparticle which tends to form large

aggregates which may alter its surface area.  $\text{Fe}_3\text{O}_4$  is also not selective to any compounds, and this may lead to its unsuitability to be used as the adsorbent phase for D- $\mu$ SPE. Thus, coating and modification of the surface of  $\text{Fe}_3\text{O}_4$  with appropriate method and materials are necessary to overcome this limitation. The coating material for  $\text{Fe}_3\text{O}_4$  can consist of carbon (Baig et al., 2014), chitosan (Jiang et al., 2015), polymers (Muliwa et al., 2016), silica gel (Kunzmann et al., 2011; Lien and Wu, 2008), silver-nanoparticle (López-García et al., 2015) and surfactants (Asgharinezhad and Ebrahimzadeh, 2016).

#### **2.5.5 Silica coated iron oxide magnetic nanoparticle ( $\text{Fe}_3\text{O}_4\text{-SiO}_2$ )**

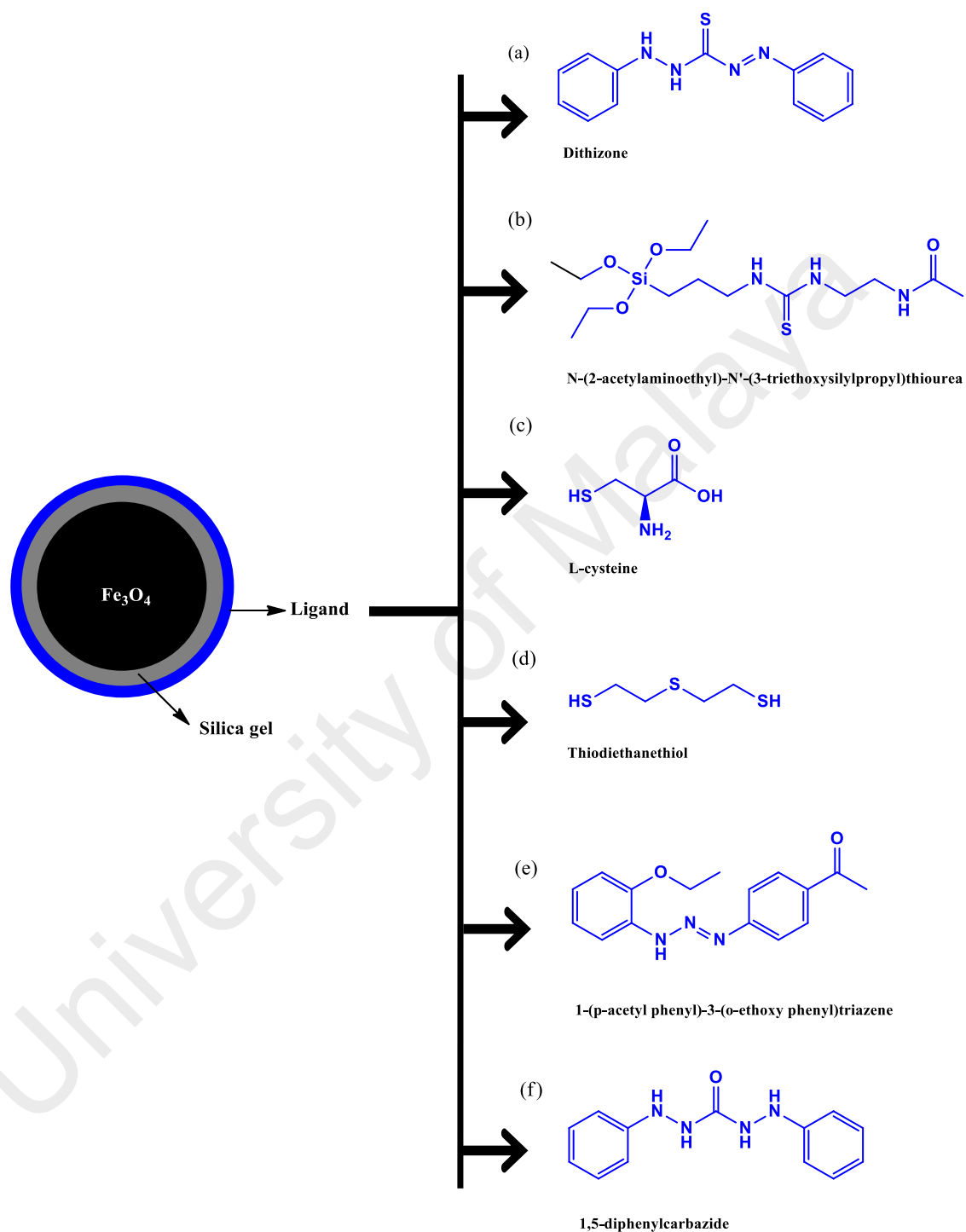
Silica gel is the most common used material that has been used to modified iron oxide due to its chemical stability, low-cost, simple preparation step, versatile and modifiable properties (Bumb et al., 2008; Kunzmann et al., 2011; Lien and Wu, 2008). Moreover, the silica gel can be modified with various chemicals to improve its property for metal ions adsorption (Khor et al., 2017). Hence, the silica gel coated iron oxide magnetic nanoparticle ( $\text{Fe}_3\text{O}_4\text{-SiO}_2$ ) that modified with various metal capturing ligand have been frequently applied as adsorbent phase for D- $\mu$ SPE (Adlnasab et al., 2014; Abolhasani et al., 2015; Alonso et al., 2016; Cui et al., 2015; Es'haghi et al., 2016; Sobhi et al., 2017; Zhang et al., 2014).

#### **2.5.6 Ligand modified $\text{Fe}_3\text{O}_4\text{-SiO}_2$ and its application in the pre-concentration of $\text{Hg}^{2+}$ in water sample**

Various ligands have been used to modify the  $\text{Fe}_3\text{O}_4\text{-SiO}_2$  to produce adsorbent phase that selective towards the adsorption of  $\text{Hg}^{2+}$  in water. By using the ligand modified  $\text{Fe}_3\text{O}_4\text{-SiO}_2$  as the adsorbent in the extraction process, various analytical methods has been developed for the determination of traces  $\text{Hg}^{2+}$  in the water sample. For example, as reported in many literatures (Mudasir et al., 2016; Zhang et al., 2014), dithizone (Figure 2.25a) was one of the effective adsorbents for  $\text{Hg}^{2+}$ . Adlnasab et al. (2014) modified the

chloro-functionalized  $\text{Fe}_3\text{O}_4\text{-SiO}_2$  with dithizone, and this material was successfully applied for the determination of trace  $\text{Hg}^{2+}$  in the environmental sample by using D- $\mu$ SPE technique coupling with Continuous-Flow Cold Vapor Atomic Absorption Spectrometry method (CF-CVAAS). The limit of detection (LOD) achieved by this method was 50 ng/L. Cui et al. (2015) introduced a selective magnetic adsorbent for  $\text{Hg}^{2+}$  in environmental samples. They grafted the *N*-(2-acetylaminoethyl)-*N'*-(3-triethoxysilylpropyl)thiourea (AMPTs) (Figure 2.25b) onto the  $\text{Fe}_3\text{O}_4\text{-SiO}_2$ . The  $\text{Hg}^{2+}$  extracted by  $\text{Fe}_3\text{O}_4\text{-SiO}_2\text{-AMPTs}$  was examined using mercury analyser and the detection limit obtained was 17 ng/L (Cui et al., 2015). To improve the analytical performance of MNP, the silica was also modified with L-cysteine (Figure 2.25c) (Xiang et al., 2013). This thiol modified  $\text{Fe}_3\text{O}_4\text{-SiO}_2$  was employed as the effective adsorbent for  $\text{Hg}^{2+}$  and the reported method of the detection limit of 60 ng/L (Xiang et al., 2013). In Beiraghi et al. (2014), a sulphur-rich ligand named thiodiethanethiol (Figure 2.25d) was used as the modifier to generate the adsorbent for separation and pre-concentration of various heavy metals which include  $\text{Hg}^{2+}$  in an environmental sample. The extracted  $\text{Hg}^{2+}$  was determined using CV-AAS and the LOD recorded by this proposed method was 4.0 ng/L. In another study, an effective and selective adsorbent for  $\text{Hg}^{2+}$  was synthesized through a series of reaction which includes the functionalization of  $\text{Fe}_3\text{O}_4\text{-SiO}_2$  with APTS and modification of this amine functionalized  $\text{Fe}_3\text{O}_4\text{-SiO}_2$  with a synthetic ligand named 1-(*p*-acetyl phenyl)-3-(*o*-ethoxy phenyl)triazene (Figure 2.25e) (Rofouei et al., 2012). The  $\text{Hg}^{2+}$  extracted by this adsorbent via D- $\mu$ SPE was analysed by Inductively Coupled Plasma Optical Emission Spectrometry (ICP-OES) and the LOD achieved by this proposed method was 40 ng/L (Rofouei et al., 2012). 1,5-diphenylcarbazide (DPC) (Figure 2.25f) with its favourable coordination capacity and selectively toward  $\text{Hg}^{2+}$  was chosen as the doping material for the preparation of functionalized magnetic particle (Zhai et al., 2010).  $\text{Fe}_3\text{O}_4\text{-SiO}_2\text{-DPC}$  was used as an adsorbent in D- $\mu$ SPE for the

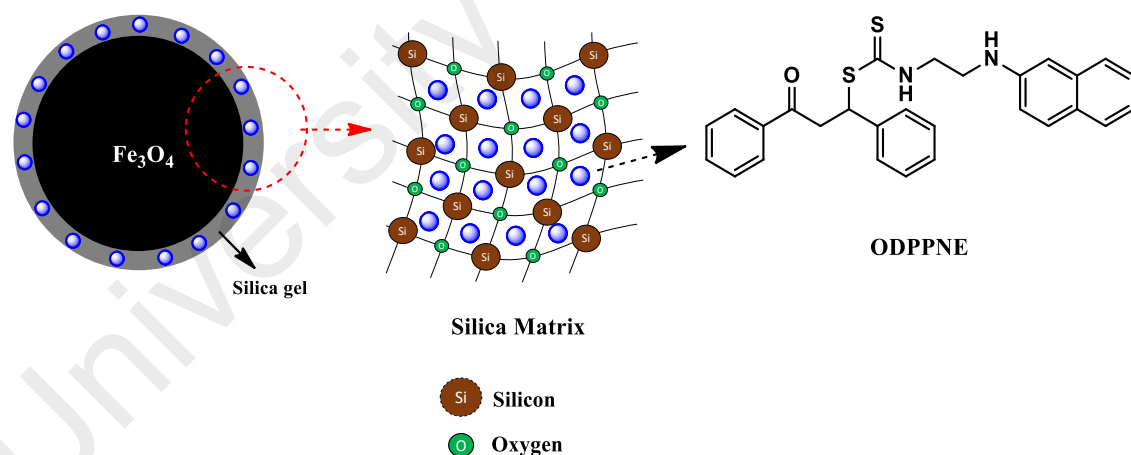
determination of  $\text{Hg}^{2+}$  in aqueous solution. In this study,  $\text{Hg}^{2+}$  was analysed using CV-AAS, and the reported LOD was 160.0 ng/L. (Zhai et al., 2010).



**Figure 2.25:** A variety of metal capturing ligand used to modify  $\text{Fe}_3\text{O}_4\text{-SiO}_2$ .

### 2.5.7 Ligand incorporated Fe<sub>3</sub>O<sub>4</sub>-SiO<sub>2</sub> in pre-concentration of Hg<sup>2+</sup> from water sample

Generally, the reactions involved in the preparation of adsorbents with magnetic property are such as (i) synthesis of Fe<sub>3</sub>O<sub>4</sub>, (ii) coating of Fe<sub>3</sub>O<sub>4</sub> with silica layer, (iii) functionalization Fe<sub>3</sub>O<sub>4</sub>-SiO<sub>2</sub> and (iv) bonding of selected ligand onto the functionalized Fe<sub>3</sub>O<sub>4</sub>-SiO<sub>2</sub> which may also involve several steps (Alonso et al., 2016; Cui et al., 2015; Sobhi et al., 2017). Some of these reactions involved higher temperature reflux and also time-consuming. Hence, this study demonstrated a simple preparation route for the preparation of ligand modified Fe<sub>3</sub>O<sub>4</sub>-SiO<sub>2</sub>. This study demonstrated the coating of silica gel doped with metal capturing ligand onto Fe<sub>3</sub>O<sub>4</sub> to produce an adsorbent for pre-concentration of Hg<sup>2+</sup>. This method simplifies the preparation of adsorbent by incorporating the ligand during the coating of Fe<sub>3</sub>O<sub>4</sub> with silica layer which was performed in single step (Figure 2.26).



**Figure 2.26:** ODPPE incorporated silica coated magnetic nanoparticle (ODPPE@MNP).



## CHAPTER 3: MATERIALS AND METHODS

### 3.1 Materials and Chemicals

*N*-(1-Naphthyl)ethylenediamine hydrochloride (98.5%) was purchased from BDH (England). Chalcone (97%) and tetraethoxysilane (99.999%) (TEOS) were obtained from Sigma (USA). Carbon disulfide ( $\geq 99.90\%$ ) ( $\text{CS}_2$ ), mercury (II) nitrate ( $\text{Hg}(\text{NO}_3)_2$ ), iron (II) chloride tetrahydrate ( $\geq 98.0\%$ ) ( $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$ ), iron (III) chloride hexahydrate (99.0-102.0%) ( $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ ), ammonia hydroxide solution (25%) ( $\text{NH}_4\text{OH}$ ), concentrated hydrochloric acid (37%) ( $\text{HCl}$ ), concentrated sulphuric acid (98%) ( $\text{H}_2\text{SO}_4$ ), concentrated phosphoric acid (85%) ( $\text{H}_3\text{PO}_4$ ), ethanol ( $\geq 99.9\%$ ) ( $\text{EtOH}$ ), methanol ( $\geq 99.8\%$ ) ( $\text{MeOH}$ ), isopropanol ( $\geq 99.8\%$ ) ( $\text{iPrOH}$ ) and dichloromethane ( $\geq 99.9\%$ ) ( $\text{DCM}$ ) were obtained from Merck (Germany). The standard solutions of  $\text{Cr}^{3+}$ ,  $\text{Cd}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Pb}^{2+}$ , and  $\text{Zn}^{2+}$  with the concentration of 1000 mg/L were obtained from Merck (Germany). Ultra-pure deionized water was produced by Elga (UK) water purification system.

### 3.2 Instrumental Analysis

FTIR spectra were recorded using Perkin Elmer Spectrum 400 ATR/FTIR spectrophotometer. NMR spectrum was recorded by using Nuclear Magnetic Resonance spectroscopy FT-NMR ECA 400. Hitachi Energy Dispersive X-ray spectroscopy (EDX) and Field Emission Scanning Electron Microscopy (FESEM) SU8200 was used for elemental analysis and SEM imaging. The thermogravimetric analysis (TGA) and differential thermal analysis (DTA) were carried out using Perkin Elmer Simultaneous Thermal Analyzer STA-6000. The concentration of  $\text{Hg}^{2+}$  ion was monitored using NIC Mercury Analyser RA-3 whereas the concentration of other metal ions was determined using Agilent Inductively Coupled Plasma Mass Spectrometry ICPMS 7500 Single Turbo

System. UV-Visible spectra were recorded using Thermo Fisher Scientific GENESYS 10S UV-Vis Spectrophotometer.

### 3.3 Preparation of ODPPNE

ODPPNE was synthesized by reacting *N*-(1-Naphthyl)ethylenediamine hydrochloride, chalcone and CS<sub>2</sub> in methanol as described by Behalo and Aly (2010). Briefly, 1 mmol of *N*-(1-Naphthyl)ethylenediamine hydrochloride and CS<sub>2</sub> (9 mmol) were first dissolved in 30 mL methanol. The mixture was stirred for 60 min at room temperature. Then, 1 mmol of chalcone was then added, and the mixture was refluxed for 24 h. The obtained product in solid form was washed with dichloromethane to remove the unreacted chalcone followed by acidified water to separate *N*-(1-Naphthyl)ethylenediamine hydrochloride residue from the pure product. The NMR spectra of ODPPNE are presented in Appendix A (<sup>1</sup>H-NMR) and Appendix B (<sup>13</sup>C-NMR).

Yield: 78%; Melting point. 171-173°C. (IR, cm<sup>-1</sup>) 3388 (N-H), 1675 (C=O), 1596-1510 (N-C=S), 1080-979 (S-C=S), 820 (C=S). <sup>1</sup>H-NMR DMSO-d<sub>6</sub>, δ ppm = 3.12 (t, 2H, CH<sub>2</sub>N), 3.49 (t, 2H, CH<sub>2</sub>N), 3.80 (dd, 1H, CH<sub>2</sub>CO), 4.02 (dd, 1H, CH<sub>2</sub>CO), 5.36 (t, 1H, CHS), 6.57 (d, 1H, Ar), 7.10 (t, 1H, Ar), 7.22 (t, 2H, Ar), 7.35-7.53 (m, 8H, Ar), 7.63 (t, 1H, Ar), 8.02 (d, 2H, Ar), 8.10 (d, 1H, Ar), 8.28 (d, 1H, Ar), 8.32 (brs, 2H, NH). <sup>13</sup>C-NMR DMSO-d<sub>6</sub>, δ ppm = 37.96, 40.90, 41.10, 44.95, 103.36, 123.11, 124.20, 124.29, 124.40, 125.18, 126.32, 127.91, 128.31, 128.51, 128.67, 129.19, 132.41, 133.66, 137.29, 142.72, 145.77, 198.70.

### **3.4 Preparation of Chalcone and ODPPNE incorporated sol-gel**

Chalcone and ODPPNE incorporated sol-gel (SG-C and SG-ODPPNE) were prepared as reported by previous studies (Ali et al., 2012; Saad et al., 2006; Turanov et al., 2016; Yost et al., 2000). Briefly, a mixture of TEOS, ethanol, and water in the molar ratio of 1:4:16 was first acidified with concentrated hydrochloric acid to form a sol solution (Buckley and Greenblatt, 1994). Then, the pre-dissolved chalcone and ODPPNE was added to the sol solution, and the molar ratio of TEOS to chalcone and ODPPNE was kept at 30:1 (Esmaili Bidhendi et al., 2014; Tadayon et al., 2012; Yost et al., 2000). The resulting solution was stirred vigorously for 2 h in a capped vial to allow the gelation to occur. The synthesized sol-gel was dried in the oven for 24 h at 60 °C. The gel was then ground to the size of 0.06 and 2.00 mm in diameter. For conditioning, the sol-gel was soaked in deionized water for 24 h and then dried at 60 °C for 24 h.

### **3.5 Metal ion adsorption by SG-C and SG-ODPPNE**

#### **3.5.1 Determination of the selectivity of SG-C and SG-ODPPNE**

The selectivity of SG-C and SG-ODPPNE towards the adsorption of metal ions was evaluated by adding 50 mg of the prepared adsorbents to 10 mL of aqueous solution containing 1 mg/L of Cr<sup>3+</sup>, Ni<sup>2+</sup>, Cu<sup>2+</sup>, Zn<sup>2+</sup>, Cd<sup>2+</sup>, Hg<sup>2+</sup> and Pb<sup>2+</sup> in a plastic vial. The mixture was shaken using an orbital shaker at 150 rpm for 24 h. The remaining concentration of the metal ions in the solution was analysed using ICP-MS.

### 3.5.2 Batch adsorption of aqueous $\text{Hg}^{2+}$ by SG-ODPPNE

In this study, 50 mg of SG-ODPPNE was first added to the 10 mL of 1 mg/L  $\text{Hg}^{2+}$  solution in a plastic vial. The mixture was then shaken with an orbital shaker at the defined time interval, and the remaining  $\text{Hg}^{2+}$  in solution was analysed using portable NIC Mercury Analyser model RA-3 (Tokyo, Japan). Several operation conditions which can influence the adsorption process such as pH of the solution (pH 6-9), the initial concentration of  $\text{Hg}^{2+}$  (1-100 mg/L), contact time (5-360 min), dosage (0.01-0.10 g) and size of SG-ODPPNE (0.06 mm and 2.00 mm) were evaluated. Removal percentage (%R) of  $\text{Hg}^{2+}$  in aqueous solution by SG-ODPPNE and the adsorption capacity  $Q_e$  (mg/g) of SG-ODPPNE at equilibrium were determined using the following equations (Equation 3.1 and Equation 3.2):

$$\%R = \frac{C_o - C_e}{C_o} \times 100\% \quad \text{Equation 3.1}$$

$$Q_e = \frac{C_o - C_e}{m} \times V \quad \text{Equation 3.2}$$

where  $C_o$  (mg/L) represents the initial concentration of  $\text{Hg}^{2+}$ ,  $C_e$  (mg/L) is the concentration of  $\text{Hg}^{2+}$  at equilibrium,  $m$  (g) is the amount of adsorbent and  $V$  (L) is the volume of aqueous solution.

### 3.5.3 $\text{Hg}^{2+}$ removal by SG-ODPPNE adsorbent in real water samples

The ability of SG-ODPPNE to remove  $\text{Hg}^{2+}$  in real environment water samples was also investigated. In this study, lake water (from Tasik Varsity, University of Malaya, Kuala Lumpur, Malaysia), drinking water, and deionized water were spiked with 1 mg/L of  $\text{Hg}^{2+}$ . Then, 50 mg of SG-ODPPNE was added to each 10 mL of this spiked real water sample in the plastic vial. The mixture was shaken using an orbital shaker for 6 h, and the concentration of the remaining  $\text{Hg}^{2+}$  was determined with Mercury Analyser.

### **3.6 Pre-concentration and determination of $\text{Hg}^{2+}$ in water**

#### **3.6.1 Synthesis of magnetic nanoparticle (MNP)**

MNP was synthesized as reported by Karaagac et al. (2010). Briefly,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  and  $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$  was first dissolved in 50 mL of deionized water with the molar ratio  $\text{Fe}^{3+}:\text{Fe}^{2+}$  of 3:2. Then, 50 mL of 25% ammonium hydroxide was added, and the mixture was stirred for 30 min. The MNP was precipitated using the external magnetic field. The synthesized MNP was washed with deionized water and dried using freeze dryer.

#### **3.6.2 Synthesis of ODPPNE-silica coated magnetic nanoparticle (ODPPNE@MNP)**

0.1 g of ODPPNE was first dissolved in 20 mL of methanol. Then, 0.3 g of MNP was dispersed in the mixture of isopropanol (50 mL) and deionized water (4 mL). The ODPPNE solution was then added into the dispersed MNP followed by the addition of 2 mL of TEOS and 5 mL of 25% ammonium hydroxide solution. The mixture solution was stirred for 24 h. The obtained ODPPNE@MNP was precipitated using an external magnet field. ODPPNE@MNP was washed with deionized water and ethanol. Then, the ODPPNE@MNP was dried under vacuum. Besides ODPPNE@MNP, the silica coated MNP ( $\text{SiO}_2$ @MNP) was obtained through same procedure but without the addition of ODPPNE.

#### **3.6.3 Pre-concentration of $\text{Hg}^{2+}$ using ODPPNE@MNP as solid phase for dispersive micro solid phase extraction (D- $\mu$ SPE)**

The pre-concentration and determination of  $\text{Hg}^{2+}$  in water were carried out using ODPPNE@MNP as the solid phase for the D- $\mu$ SPE method. In this experiment, the operation parameters of D- $\mu$ SPE such as pH of the solution (pH 5-9), the initial concentration of  $\text{Hg}^{2+}$  (0.5-100 mg/L), adsorption time (5-30 min), selectivity, dosage of ODPPNE@MNP (5-30 mg), type of desorption reagent (HCl,  $\text{H}_2\text{SO}_4$  and  $\text{H}_3\text{PO}_4$ ), the

volume of desorption reagent (0.25-25 mL), and desorption time (1-10 min) were optimized to obtain the optimal condition for  $\text{Hg}^{2+}$  analysis. These parameters were found to influence the performance of heavy metals pre-concentration process (Abolhasani et al., 2015; Adlnasab et al., 2014; Sobhi et al., 2017). This experiment was started by the addition of ODPPNE@MNP to the 25 mL of 1 mg/L  $\text{Hg}^{2+}$  solution. The mixture was then sonicated using an ultrasonic agitator for the defined time interval. After sonication, the ODPPNE@MNP was isolated by using a magnet, and the solution was decanted. The isolated ODPPNE@MNP was rinsed with deionized water for three times before  $\text{Hg}^{2+}$  desorption process. For the  $\text{Hg}^{2+}$  desorption process, the isolated ODPPNE@MNP was dispersed in HCl solution. The amount of  $\text{Hg}^{2+}$  in HCl was analysed using Mercury Analyser. Recovery efficiency (%E) of  $\text{Hg}^{2+}$  in aqueous solution by ODPPNE@MNP was determined using the following equation:

$$\%E = \frac{C_r}{C_o} \times 100\% \quad \text{Equation 3.3}$$

where  $C_o$  (mg/L) represents the initial concentration of  $\text{Hg}^{2+}$ ,  $C_r$  (mg/L) is the concentration of extracted  $\text{Hg}^{2+}$ .

#### 3.6.4 Pre-concentration of $\text{Hg}^{2+}$ in real water samples

The developed D- $\mu$ SPE method was applied in the real water samples analysis to verify its applicability. In this study, 25 mL of the selected drinking, tap and surface water (lake water) sample were spiked with known concentration of  $\text{Hg}^{2+}$  varying from 0.05  $\mu\text{g/L}$  to 2  $\mu\text{g/L}$  and the pH of this water sample was adjusted to pH 7. 15 mg of ODPPNE@MNP was dispersed in the water sample by the aid of ultra-sonication for 10 min. After the sonication process, the ODPPNE@MNP was isolated from the water sample by using magnet. The isolated ODPPNE@MNP was washed with the deionized water three times to eliminate the unabsorbed  $\text{Hg}^{2+}$  before the desorption process. For the  $\text{Hg}^{2+}$  desorption

process, isolated ODPPNE@MNP was dispersed in 0.25 mL of 1.5 M HCl for 5 min. The HCl solution was separated from ODPPNE@MNP and the amount of desorbed  $\text{Hg}^{2+}$  in HCl was analysed.

University of Malaya

## CHAPTER 4: RESULTS AND DISCUSSIONS

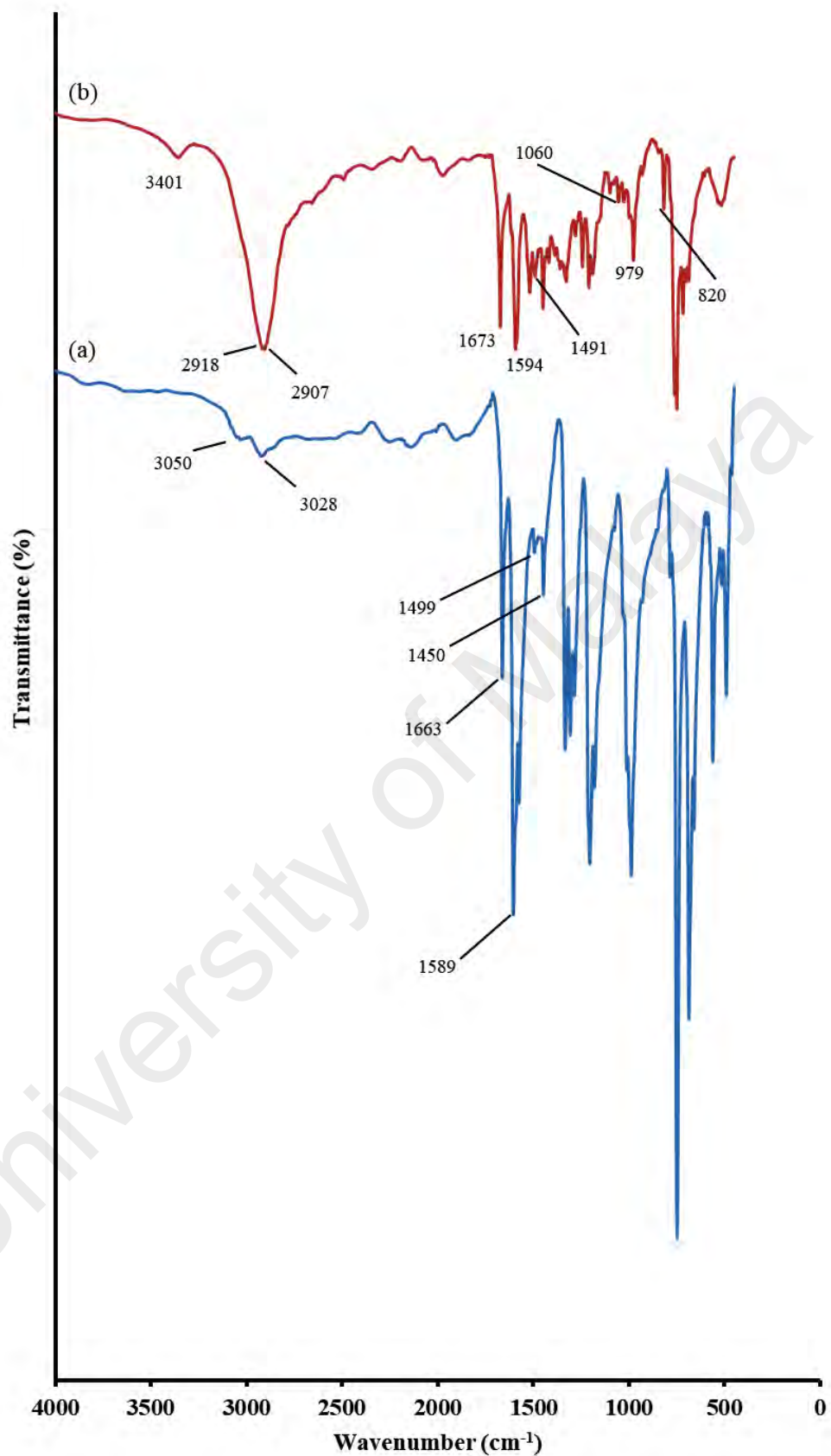
### 4.1 Characterization of SG-C, SG-ODPPNE and ODPPNE@MNP

#### 4.1.1 FTIR Analysis

In this study, the three-component one-pot reaction was used to produce ODPPNE as metal capturing ligand. The three components that involved were CS<sub>2</sub>, *N*-(1-Naphthyl)ethylenediamine hydrochloride and chalcone. During the reaction, CS<sub>2</sub> was first reacted with *N*-(1-Naphthyl)ethylenediamine hydrochloride to produce (2-(naphthalen-2-ylamino)ethyl)carbamodithioate (*I*). Then, (2-(naphthalen-2-ylamino)ethyl)carbamodithioate was then reacted with chalcone to produce ODPPNE (Figure 2.24). For chalcone, the main characteristic peaks in FTIR were found to appear in the region of 1589-1400 cm<sup>-1</sup> (Figure 4.1a). These peaks were attributed to aliphatic and aromatic C=C stretching of chalcone (Prasadarao and Mohan, 2012). Besides that, the C-H stretching bands of the =C-H group of chalcone were observed at 3050-3028 cm<sup>-1</sup> (Aksöz and Ertan, 2012). The characteristic peak of C=O for chalcone appeared at 1663 cm<sup>-1</sup>. For ODPPNE, the peak at 3401 cm<sup>-1</sup> was attributed to N-H stretching (Figure 4.1b) and the peak at 2918 and 2907 was corresponded to the sp<sup>3</sup> C-H stretch (Behalo and Aly, 2010). The presence of S-C=S group was characterized by the peaks at 1060 and 940 cm<sup>-1</sup> (Onwudiwe and Ajibade, 2011). The peak at 820 cm<sup>-1</sup> confirmed the presence of C=S (Tiwari et al., 2015). The peaks at 1580 -1450 cm<sup>-1</sup> represents the C-N stretching in N-C=S group of ODPPNE (Onwudiwe and Ajibade, 2011).

IR spectra for SG (blank silica gel, Figure 4.2a), SG-C (Figure 4.2b) and, SG-ODPPNE (Figure 4.2c) showed a strong peak around 1080 cm<sup>-1</sup> corresponded to asymmetric stretching of Si-O-Si (Bari et al., 2009). SG-ODPPNE showed the characteristic peaks of free ODPPNE suggesting ODPPNE was incorporated into the sol-gel matrix (Figure 4.2c). These characteristic peaks appeared at 3372, 2920, 2912, 1673,

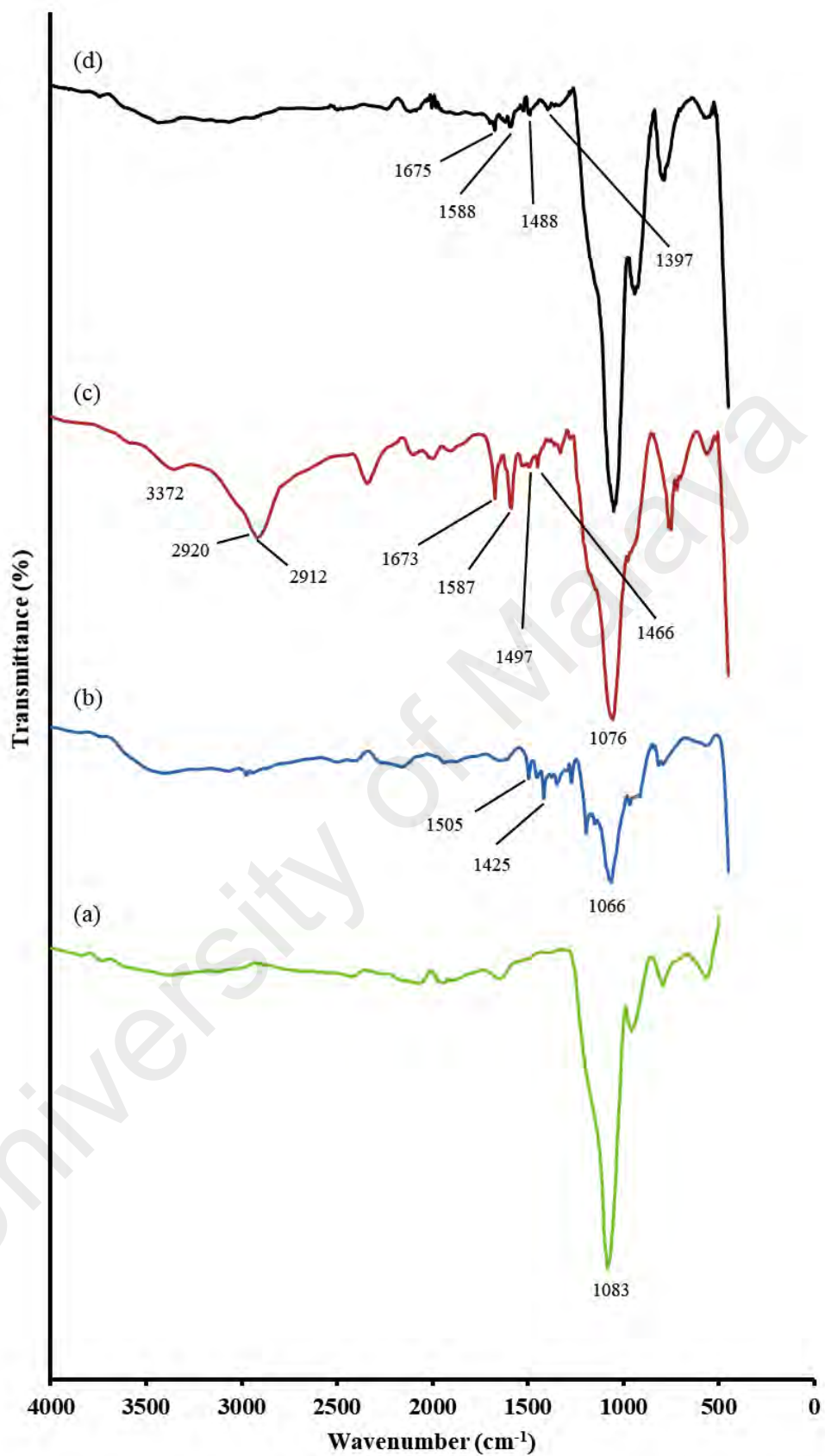




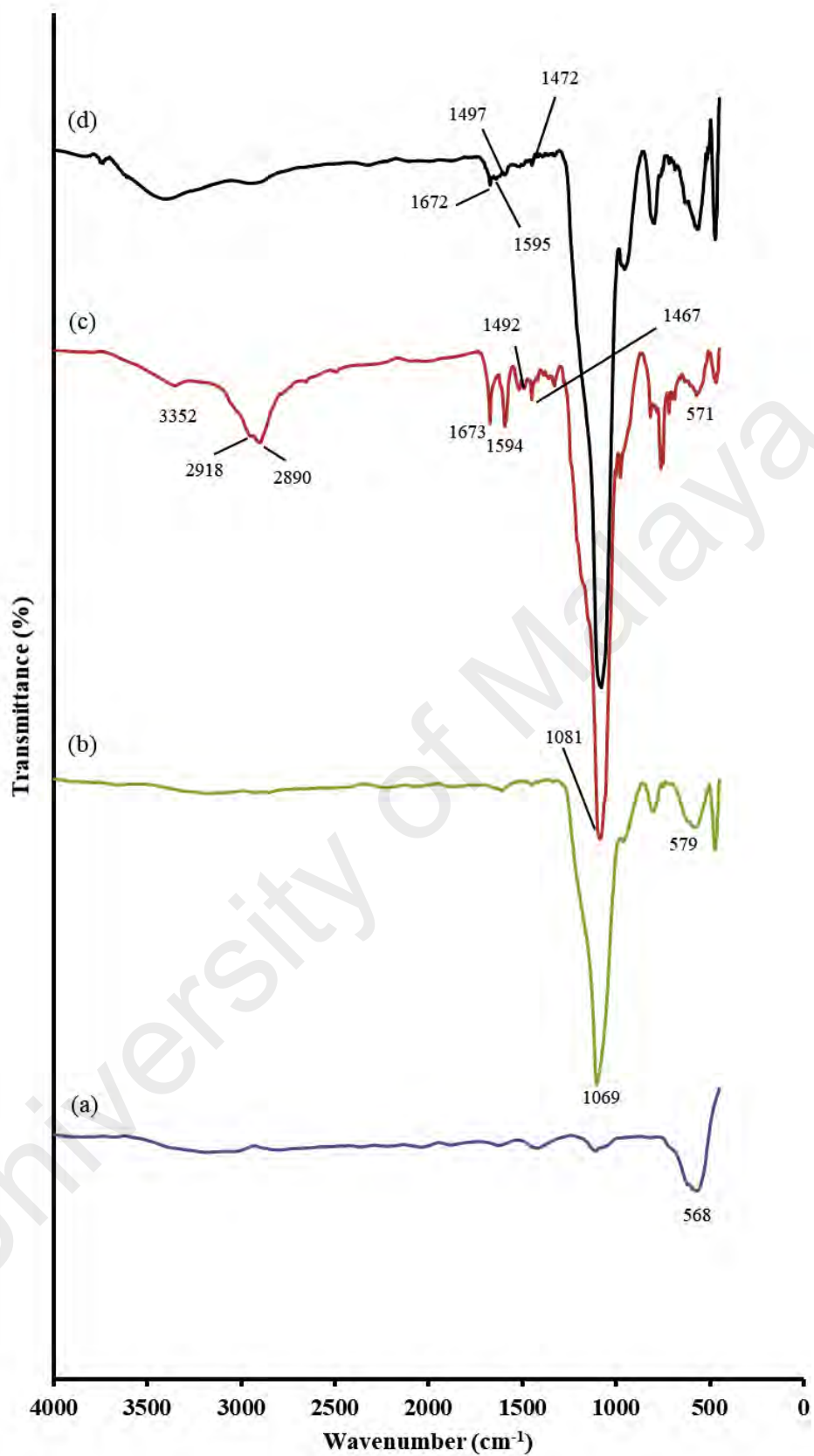
**Figure 4.1:** IR spectrum of (a) Chalcone and (b) ODPPNE.

1587 and 1497  $\text{cm}^{-1}$ . On the other hand, the peaks that appeared around 1500-1400  $\text{cm}^{-1}$  for SG-C indicates the presence of chalcone in the sol-gel matrix (Figure 4.2b). To understand the mechanism of the interaction between  $\text{Hg}^{2+}$  and the ODPPNE that containing in the sol-gel matrix, SG-ODPPNE was isolated from the solution after  $\text{Hg}^{2+}$  adsorption process. The SG-ODPPNE was then characterized using FTIR. The result showed that the characteristic peak of N-C=S group of ODPPNE was shifted from 1497-1466  $\text{cm}^{-1}$  (Figure 4.2c) to 1488-1397  $\text{cm}^{-1}$  (Figure 4.2d). This downward shift showed the involvement of N-C=S group in the complexation between ODPPNE with  $\text{Hg}^{2+}$ .

In order to prove the presence of ODPPNE on the ODPPNE@MNP, the IR spectrum of MNP ( $\text{Fe}_3\text{O}_4$ ),  $\text{SiO}_2$ @MNP and ODPPNE@MNP (Figure 4.3) were recorded. For MNP (Figure 4.3a), the presence of a strong band at around 568  $\text{cm}^{-1}$  was attributed to Fe-O stretching vibration (Karaagac and Kockar, 2016; Li et al., 2015). This peak was also observed in the IR spectrum of  $\text{SiO}_2$ @MNP (Figure 4.3b) and ODPPNE@MNP (Figure 4.3c). For  $\text{SiO}_2$ @MNP and ODPPNE@MNP, the appearances of strong absorption peak around 1080  $\text{cm}^{-1}$  indicated the presence of Si-O bonding (Bari et al., 2009). This observation indicated that silica gel was successfully coated on MNP. On the other hand, the characteristic peak of free ODPPNE ligand at 3352, 2918, 2890, 1673, 1594, 1492 and 1467  $\text{cm}^{-1}$  was found to appear in the IR spectrum of ODPPNE@MNP. Hence, this is a strong evidence that ODPPNE was incorporated into the silica gel matrix which is coated on MNP. To prove the adsorption of  $\text{Hg}^{2+}$  by ODPPNE@MNP, ODPPNE@MNP was isolated from the  $\text{Hg}^{2+}$  solution after adsorption process. The characteristic peaks of ODPPNE which indicates the N-C=S group was found to be shifted from 1492-1467  $\text{cm}^{-1}$  to 1497-1472  $\text{cm}^{-1}$  (Figure 4.3d). This result further proves the interaction between ODPPNE and  $\text{Hg}^{2+}$  in the silica gel matrix.



**Figure 4.2:** IR spectrum of (a) SG, (b) SG-C and (c) SG-ODPPNE and (d) isolated SG-ODPPNE after  $\text{Hg}^{2+}$  adsorption.



**Figure 4.3:** IR spectrum of (a) MNP (Fe<sub>3</sub>O<sub>4</sub>), (b) SiO<sub>2</sub>@MNP, (c) ODPNE@MNP and (d) isolated ODPNE@MNP after Hg<sup>2+</sup> adsorption.

#### 4.1.2 Elemental Analysis

SG-ODPPNE, SG-C, and SG were analysed using EDX to confirm the presence of ODPPNE and chalcone in the sol-gel matrix. The result in Table 4.1 indicated that the nitrogen and sulphur were detected in SG-ODPPNE as compared to SG and SG-C. This result further indicates the presence of ODPPNE in the silica gel matrix. For SG-C, the percentage of carbon was detected at the level of 9.73% showing the presence of chalcone in SG-C. To further confirm the adsorption of  $\text{Hg}^{2+}$  by the SG-ODPPNE, after adsorption of  $\text{Hg}^{2+}$ , SG-ODPPNE, SG-C and SG were isolated and analysed using EDX. The result showed that  $\text{Hg}^{2+}$  was detected in both SG-C and SG-ODPPNE only. Therefore, it can be concluded that both SG-C and SG-ODPPNE have the ability to adsorb  $\text{Hg}^{2+}$ .

**Table 4.1:** Elemental composition of SG, SG-C and SG-ODPPNE.

Element	Composition of element (%)				
	SG	SG-C*	SG-C**	SG-ODPPNE*	SG-ODPPNE**
Silica (Si)	29.62	39.06	29.14	49.32	26.94
Oxygen (O)	70.38	51.21	47.60	34.64	34.20
Carbon (C)	-	9.73	22.82	11.70	28.51
Nitrogen (N)	-	-	-	4.22	7.73
Sulphur (S)	-	-	-	0.12	1.71
$\text{Hg}^{2+}$	-	-	0.44	-	0.91

\* Determined before adsorption process

\*\*Determined after adsorption process

#Not detected

In order to verify the presence of ODPPNE in ODPPNE@MNP, MNP,  $\text{SiO}_2$ @MNP, and ODPPNE@MNP were also analysed using EDX. The presence of nitrogen and sulphur in ODPPNE@MNP indicated that ODPPNE was successfully incorporated on  $\text{SiO}_2$ @MNP (Figure 4.2). To further confirm the adsorption of  $\text{Hg}^{2+}$  by  $\text{SiO}_2$ @MNP and ODPPNE@MNP, both adsorbents were isolated from the  $\text{Hg}^{2+}$  solution after adsorption process, and the isolated adsorbents were then subjected to EDX analysis.

According to the result obtained (Table 4.2),  $\text{Hg}^{2+}$  was only detected on the isolated ODPPNE@MNP. This observation further indicates the role of ODPPNE in the adsorption of  $\text{Hg}^{2+}$ .

**Table 4.2:** Elemental composition of MNP,  $\text{SiO}_2$ @MNP and ODPPNE@MNP.

Element	Composition of element (%)				
	MNP	$\text{SiO}_2$ @MNP*	$\text{SiO}_2$ @MNP**	ODPPNE @MNP*	ODPPNE @MNP**
Iron (Fe)	74.63	23.85	17.18	15.58	9.73
Oxygen (O)	25.37	43.25	52.79	45.55	37.49
Silica (Si)	-	32.90	30.03	19.07	12.98
Carbon (C)	-	-	-	12.65	11.11
Nitrogen (N)	-	-	-	5.93	1.83
Sulphur (S)	-	-	-	1.22	1.53
$\text{Hg}^{2+}$	-	-	#ND	-	25.34

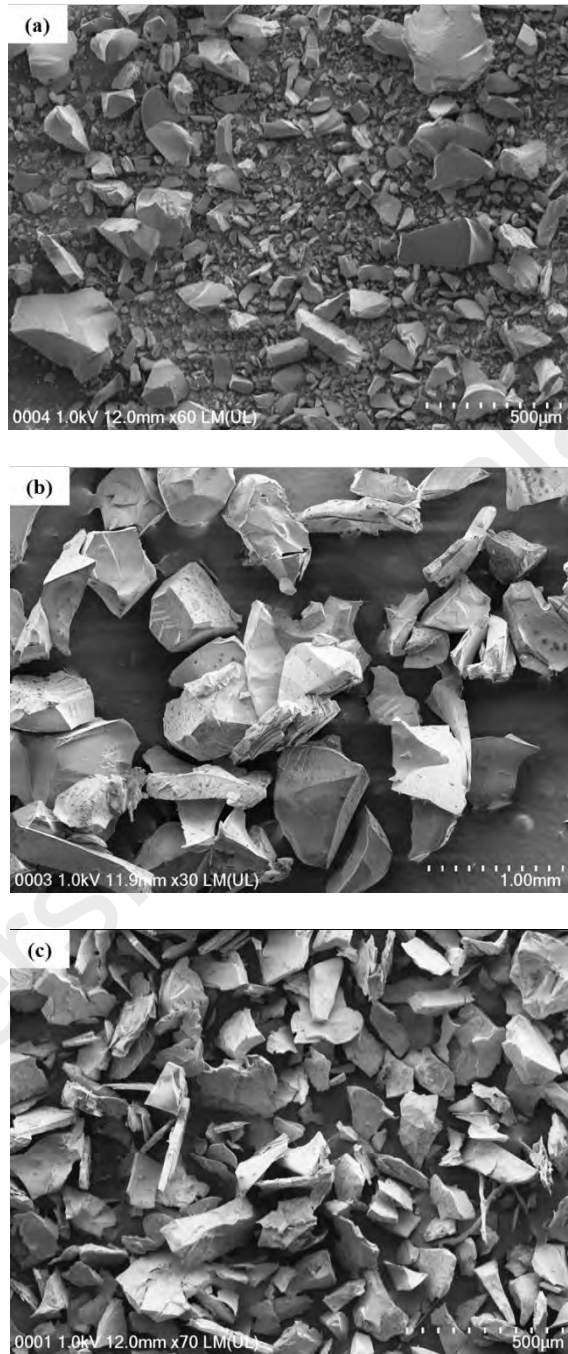
\* Determined before adsorption process

\*\*Determined after adsorption process

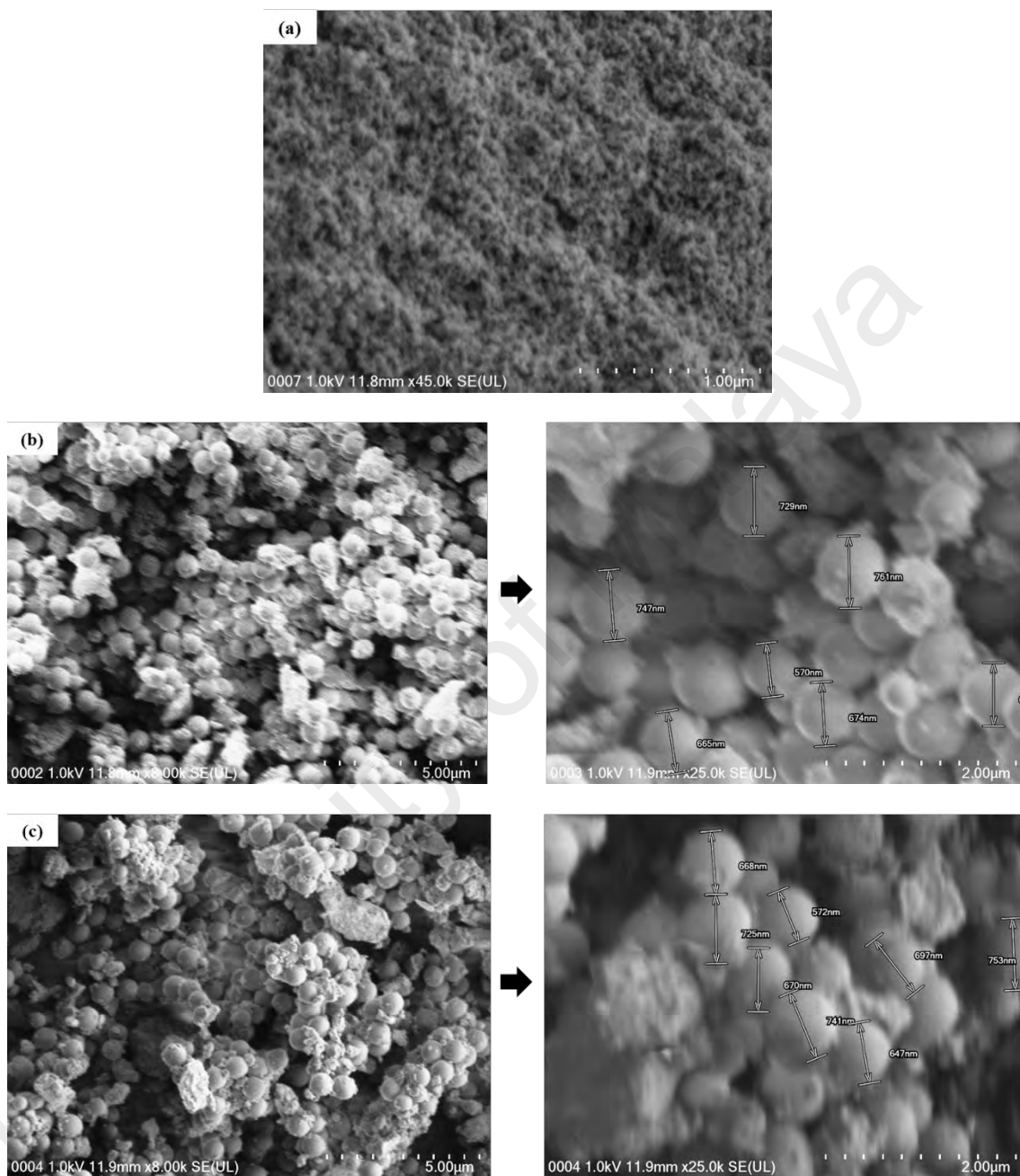
#Not detected

#### 4.1.3 SEM analysis

Scanning electron microscopy was performed to observe the morphology of SG, SG-C, SG-ODPPNE, MNP,  $\text{SiO}_2$ @MNP, and ODPPNE@MNP. The SEM image of SG (Figure 4.4a), SG-C (Figure 4.4b) and SG-ODPPNE (Figure 4.4c) showed that the morphology of these three materials was almost similar. For MNP, the agglomeration of this nano-size material was observed in the SEM image (Figure 4.5a). Both  $\text{SiO}_2$ @MNP (Figure 4.5b) and ODPPNE@MNP (Figure 4.5c) exhibited the spherical shape with the diameter ranging from around 600 – 700 nm. There are no significant differences in morphology between  $\text{SiO}_2$ @MNP and ODPPNE@MNP.



**Figure 4.4:** SEM images of (a) SG, (b) SG-C and (c) SG-ODPPNE.



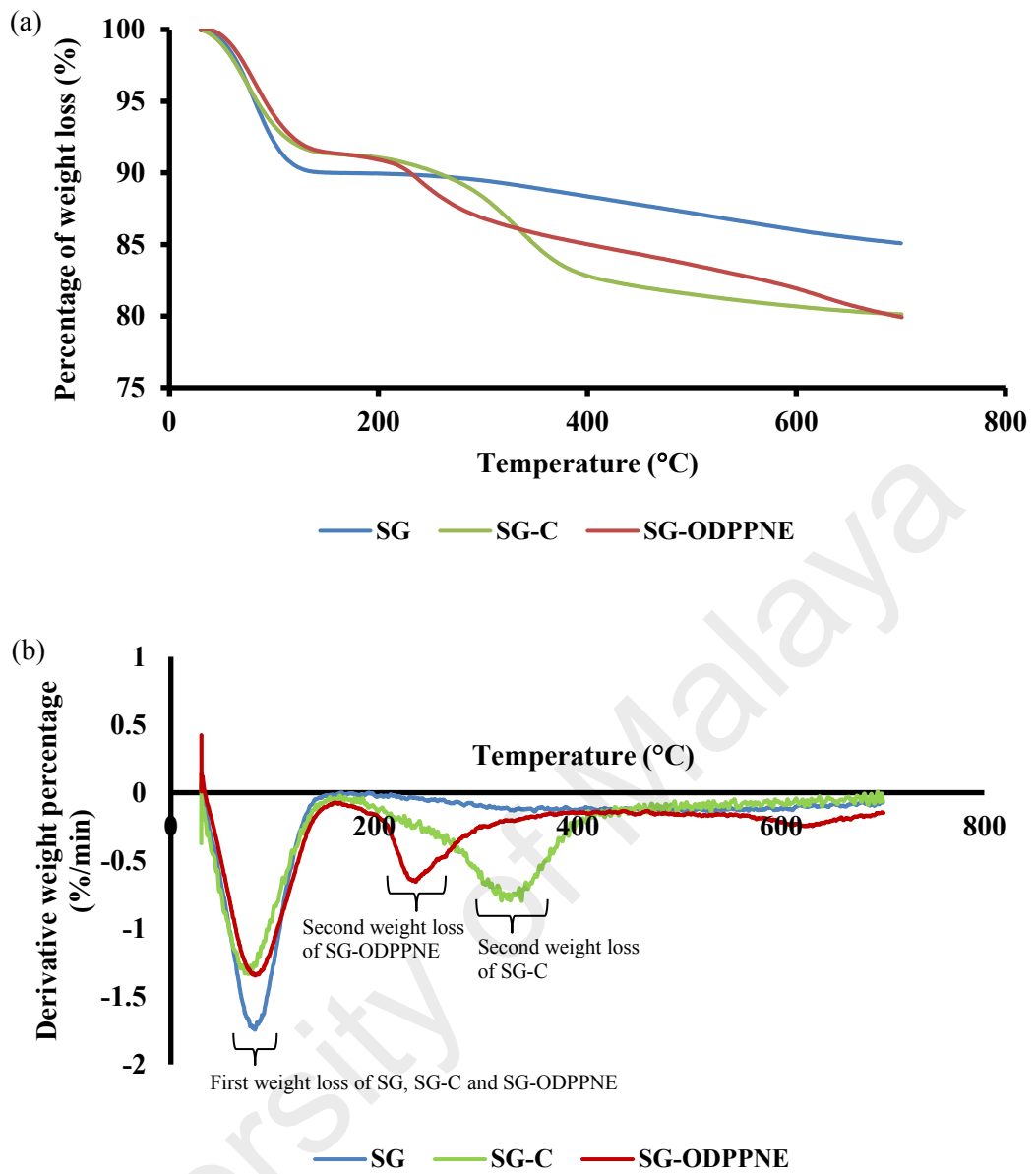
**Figure 4.5:** SEM images of (a) MNP, (b) SiO<sub>2</sub>@MNP and (c) ODPPNE@MNP.



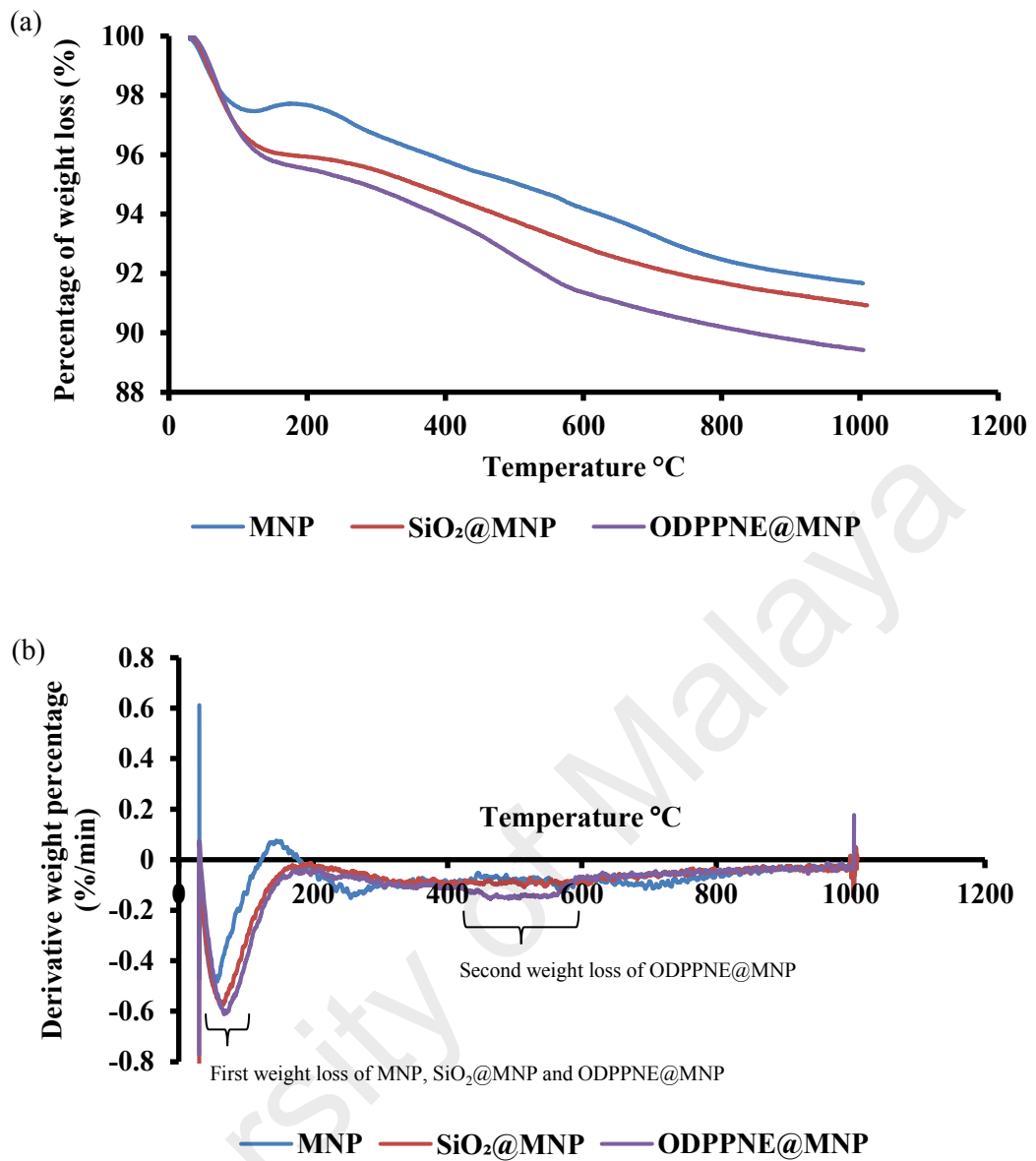
#### 4.1.4 TGA and DTA Analysis

TGA and DTA analysis were performed to further characterize the synthesized adsorbents. The TGA (Figure 4.6a) and DTA (Figure 4.6b) profiles showed that SG-ODPPNE, SG-C, and SG exhibit the first weight loss at around 150 °C corresponded to the removal of physically adsorbed water. SG-ODPPNE and SG-C experienced the second weight loss that occurred at 160 – 400 °C. The maximum weight loss for SG-ODPPNE and SG-C was found to occur at 241 and 344 °C, respectively. These weight losses indicate the decomposition of ODPPNE and chalcone that containing in the silica gel matrix. Based on the weight loss data, the loading of chalcone and ODPPNE in SG-C and SG-ODPPNE was 50 and 90 mg/g, respectively.

The TGA and DTA profile of MNP, SiO<sub>2</sub>@MNP, and ODPPNE@MNP are presented in Figure 4.7. All synthesized materials showed a sharp weight loss at the temperature around 100 °C which corresponded to the loss of absorbed water. The ODPPNE@MNP experienced a second weight loss at around 400 to 600 °C, which corresponded to the decomposition of ODPPNE that incorporated in the silica gel matrix of ODPPNE@MNP. Based on the weight loss of ODPPNE, the concentration of ODPPNE in ODPPNE@MNP was 26 mg/g.



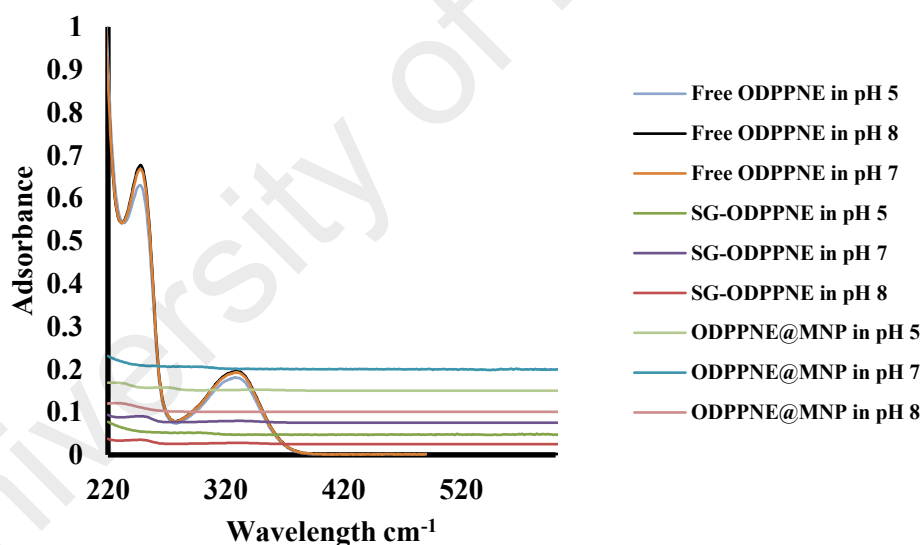
**Figure 4.6:** (a) TGA and (b) DTA profile of SG, SG-C and SG-ODPPNE.



**Figure 4.7:** (a) TGA and (b) DTA profile of MNP, SiO<sub>2</sub>@MNP and ODPPNE@MNP.

#### 4.1.5 Leaching Test

To investigate the stability of embedded ODPPNE in the silica gel matrix, the SG-ODPPNE and ODPPNE@MNP were shaken in water at different pHs for 24 h. The water was then analysed using a UV-Visible spectrometer to detect the ODPPNE. The UV-Visible spectrum of free ODPPNE at pH 5, 7 and 8 showed two  $\lambda_{\max}$  at 248 and 322 nm (Figure 4.8). The result indicated ODPPNE was not detected in water and therefore it was concluded that ODPPNE was not leached into the water during the adsorption process. Also, to ensure the stability of the adsorbed  $\text{Hg}^{2+}$  on SG-ODPPNE and ODPPNE@MNP, the isolated adsorbent was exposed to water with different pHs for 24 h. Then, the presence of  $\text{Hg}^{2+}$  was determined using Mercury Analyser. The results showed that the  $\text{Hg}^{2+}$  was not detected in all cases.

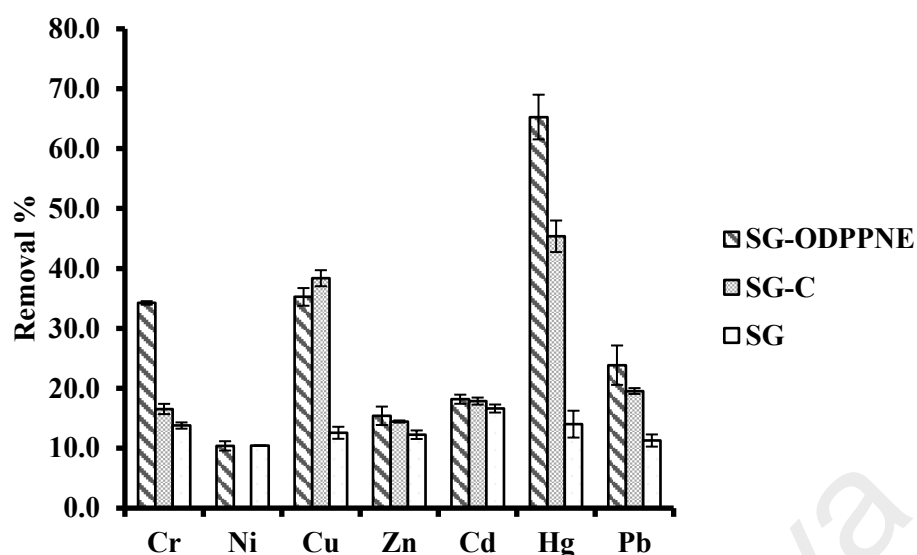


**Figure 4.8:** The comparison of UV spectra for free ODPPNE, SG-ODPPNE and ODPPNE@MNP in water with different pH. (The overlapped UV spectra of SG-ODPPNE and ODPPNE@MNP was separated by cumulatively adding 0.025 to the UV spectra in a sequence order SG-ODPPNE (pH 8, 5 and 7) and ODPPNE@MNP (pH 8, 5 and 7).)

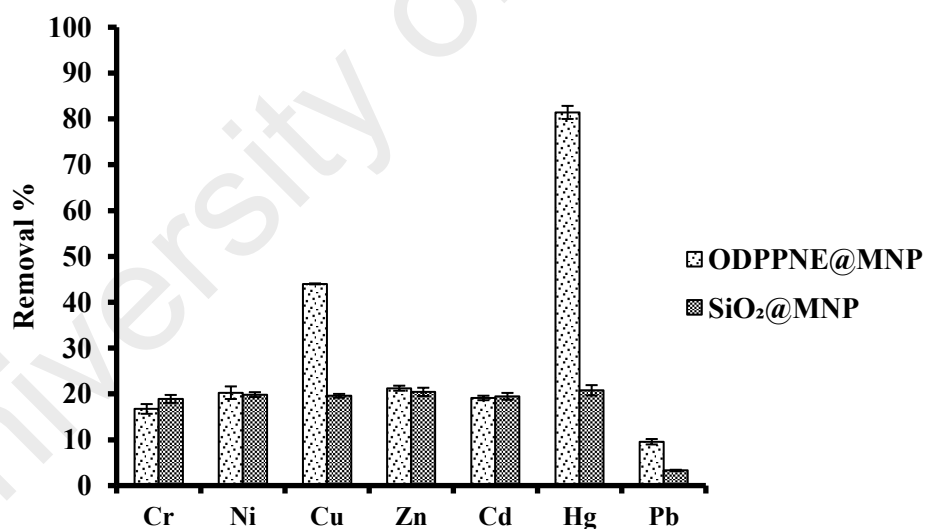
#### 4.2 Selectivity of SG-C, SG-ODPPNE, SiO<sub>2</sub>@MNP, and ODPPNE@MNP in the removal of heavy metals

The ability of SG-C, SG-ODPPNE, and SG to remove metals ion was evaluated using a solution containing 1 mg/L of Cr<sup>3+</sup>, Ni<sup>2+</sup>, Cu<sup>2+</sup>, Zn<sup>2+</sup>, Cd<sup>2+</sup>, Pb<sup>2+</sup> and Hg<sup>2+</sup> (Figure 4.9). The removal percentage of the selected metal ions by SG was ranged from 10.4 to 16.6%. When SG-C was used as an adsorbent, removal percentage of Cu<sup>2+</sup> and Hg<sup>2+</sup> were clearly increased to 38.4 and 45.4%, respectively. The removal of Hg<sup>2+</sup> was increased to 65.3% when SG-ODPPNE was used as an adsorbent. Also, the removal percentage of Cr<sup>3+</sup> and Pb<sup>2+</sup> was also found to increase to 34.2, and 23.9%, respectively.

The adsorption performance of SiO<sub>2</sub>@MNP and ODPPNE@MNP toward Hg<sup>2+</sup> in the presence of various metal ions such as Cr<sup>3+</sup>, Ni<sup>2+</sup>, Cu<sup>2+</sup>, Zn<sup>2+</sup>, Cd<sup>2+</sup>, and Pb<sup>2+</sup> was also investigated. As shown in Figure 4.10, the SiO<sub>2</sub>@MNP showed no selectivity and low removal percentages (3.3-20.8%) towards all selected metal ions. For ODPPNE@MNP, 81.4% of Hg<sup>2+</sup> was successfully removed as compared to the other metal ions where the removal efficiency was ranged from, 9.6 to 44.0%. In general, it can be concluded that the metal ions adsorption efficiency of the silica gel particularly for Cr<sup>3+</sup>, Cu<sup>2+</sup>, Hg<sup>2+</sup>, and Pb<sup>2+</sup> could be enhanced by incorporating the chalcone. The selectivity of silica gel as well as the silica gel coated MNP in the adsorption of Hg<sup>2+</sup>, could be further enhanced by incorporating the ODPPNE with dithiocarbamate moiety as metal capturing ligand.



**Figure 4.9:** The removal percentage of  $\text{Cr}^{3+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Zn}^{2+}$ ,  $\text{Cd}^{2+}$ ,  $\text{Hg}^{2+}$  and  $\text{Pb}^{2+}$  by SG-ODPPNE, SG-C and SG in aqueous sample. (Amount of adsorbent = 50 mg, [Metal ion] = 1 mg/L, volume of aqueous solution = 10 mL, pH of aqueous solution = 7.5 and contact time = 24 h).



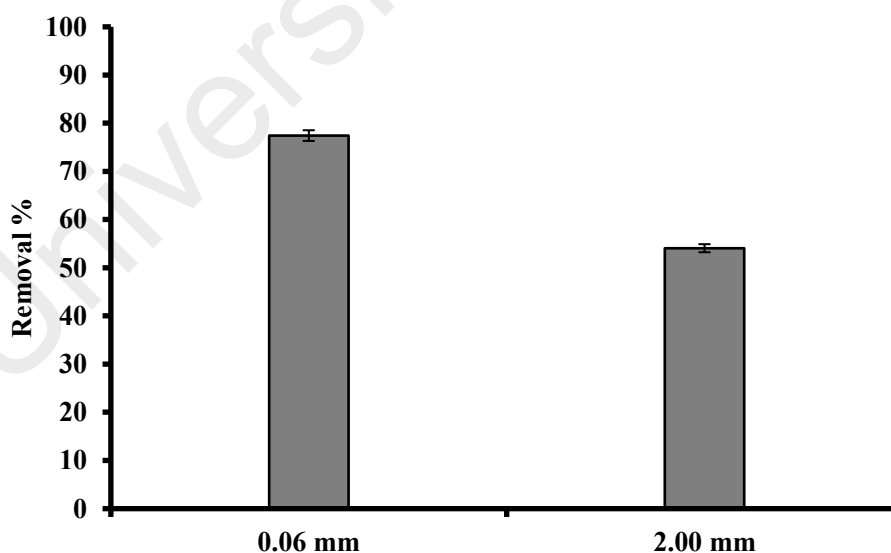
**Figure 4.10:** The removal percentage of  $\text{Cr}^{3+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Zn}^{2+}$ ,  $\text{Cd}^{2+}$ ,  $\text{Hg}^{2+}$  and  $\text{Pb}^{2+}$  by ODPNE@MNP and SiO<sub>2</sub>@MNP in aqueous sample. (Amount of adsorbents = 15 mg, [Metal ion] = 1 mg/L, volume of aqueous solution = 25 mL, pH of aqueous solution = 8 and contact time = 30 min).

### 4.3 Hg<sup>2+</sup> removal in aqueous by SG-ODPPNE

Effect of several important parameters toward the removal of aqueous Hg<sup>2+</sup> by SG-ODPPNE was studied in detail in order to obtain the optimum condition for removal Hg<sup>2+</sup> in water. By using the obtained conditions, the isotherm and kinetics of the adsorption of Hg<sup>2+</sup> by SG-ODPPNE were then determined. The performance of the developed method in the real water treatment was also evaluated.

#### 4.3.1 Effect of adsorbent size

To study the effect of the size of SG-ODPPNE on the removal of Hg<sup>2+</sup>, SG-ODPPNE was ground into the size of 0.06 and 2 mm. 54.1% of Hg<sup>2+</sup> was removed by SG-ODPPNE with the size of 2 mm whereas SG-ODPPNE with the size of 0.06 mm managed to improve the Hg<sup>2+</sup> removal efficiency to 77.4% (Figure 4.11). This result indicated that SG-ODPPNE with the larger surface area (smaller particle size) (Rahman and Padavettan, 2012) provides more binding sites to adsorb Hg<sup>2+</sup>. Therefore, adsorbent with the size of 0.06 mm was selected for further study.

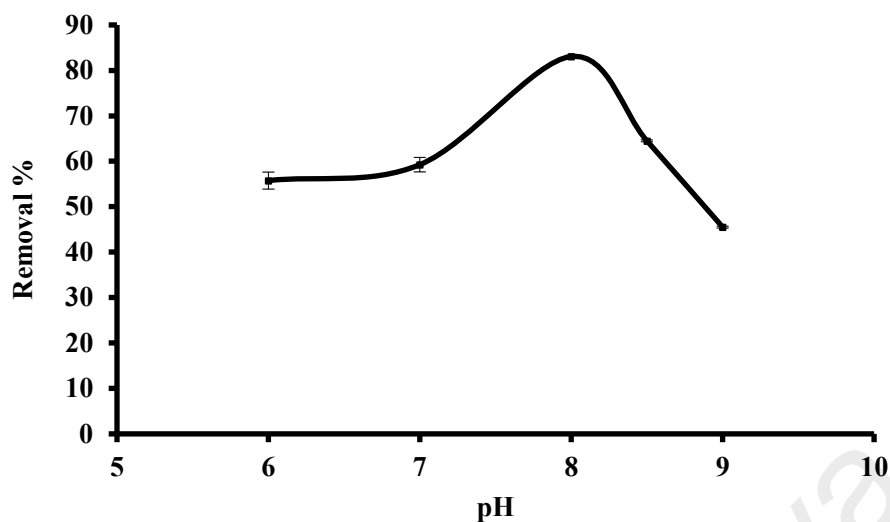


**Figure 4.11:** Effect of 0.06 mm and 2.00 mm SG-ODPPNE on removal percentage of Hg<sup>2+</sup> in aqueous sample. (Amount of SG-ODPPNE = 50 mg, [Hg<sup>2+</sup>] = 1 mg/L, volume of Hg<sup>2+</sup> solution = 10 mL, pH of Hg<sup>2+</sup> solution = 7.5 and contact time = 24 h).

### 4.3.2 Effect of pH of aqueous solution

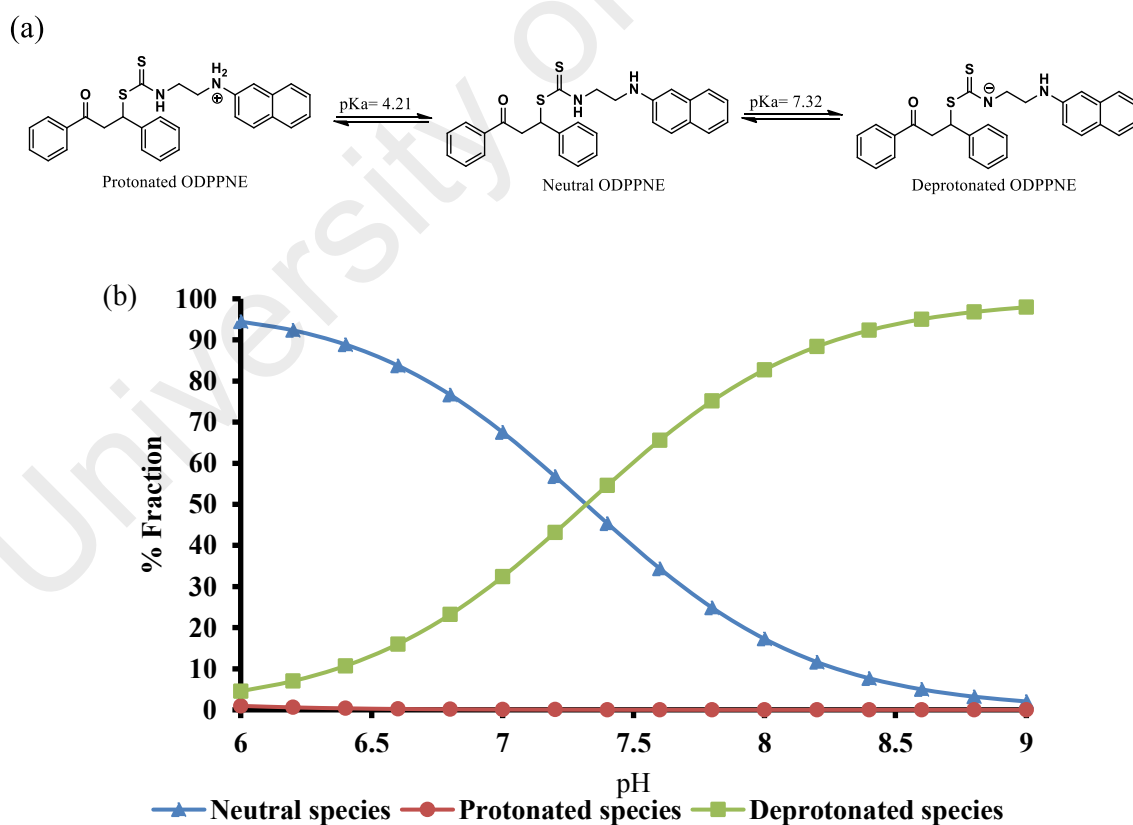
In this study, the effect of pH on the efficiency of  $\text{Hg}^{2+}$  removal was determined by varying the pH of the  $\text{Hg}^{2+}$  solution from 6 to 9 (Figure 4.12). The removal efficiency of  $\text{Hg}^{2+}$  was found to increase when the pH was increased from 6 to 8. The efficiency of  $\text{Hg}^{2+}$  removal was found to reduce when the pH was exceeded 8. This result indicated that the adsorption process in aqueous solution is a pH-dependent process. Due to the presence of secondary amine groups, ODPPNE can present in the form of neutral, deprotonated and protonated species (Figure 4.13a). In this study, the pKa of ODPPNE was calculated using MarvinSketch software (Version 17.2.6). The calculated pKa of ODPPNE was 4.21 and 7.32. Based on the calculated pKa, ODPPNE appeared dominantly in neutral and deprotonated forms at the selected pH range (Figure 4.13b). Therefore, the lower efficiency of SG-ODPPNE in  $\text{Hg}^{2+}$  removal at acidic condition was mainly due to the presence of the higher fraction of neutral ODPPNE (Figure 4.13a) which has the lower capability to complex with  $\text{Hg}^{2+}$ . When the pH increases, the higher amount of ODPPNE appeared in the deprotonated form. Deprotonated ODPPNE could interact favorably with  $\text{Hg}^{2+}$  due to the presence of negative charge. At pH 9, the decreased in the adsorption efficiency might due to the formation of  $\text{Hg}(\text{OH})_2$  which is neutral and less likely to complex with ODPPNE as compared to  $\text{Hg}^{2+}$  (Shen et al., 2014).





**Figure 4.12:** Effect of pH on the removal efficiency of  $\text{Hg}^{2+}$  in aqueous sample by SG-ODPPNE.

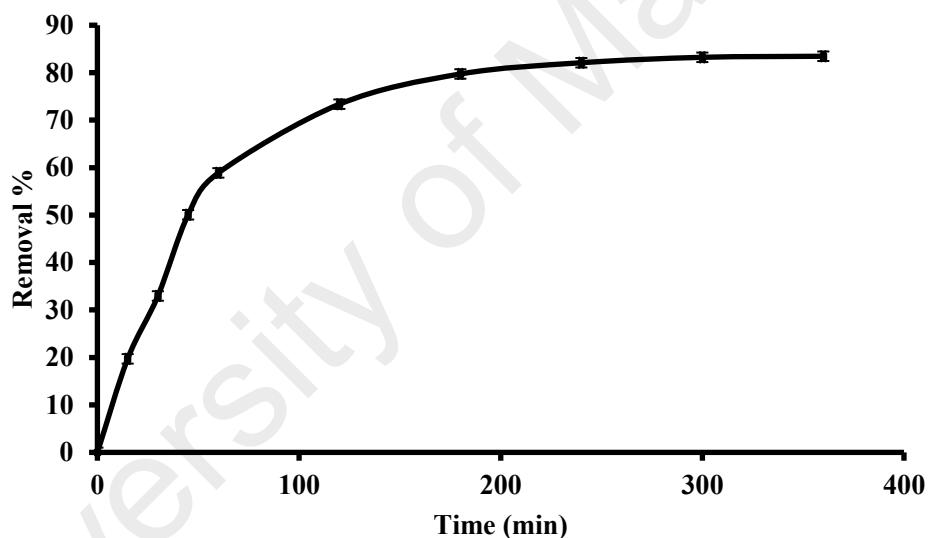
(Amount of SG-ODPPNE = 50 mg,  $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of  $\text{Hg}^{2+}$  solution = 10 mL and contact time = 24 h).



**Figure 4.13:** (a) The structure of neutral, protonated and deprotonated ODPPNE, and (b) The variation of fraction of neutral, protonated and deprotonated ODPPNE in the pH range of 6 to 8.

### 4.3.3 Effect of contact time

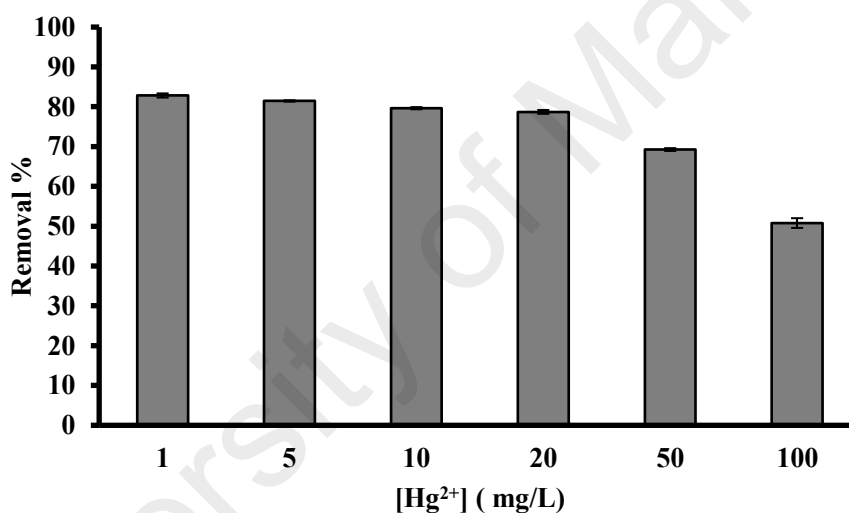
The contact time for the adsorption process is important for the determination of the kinetic of  $\text{Hg}^{2+}$  removal. In this experiment, the removal of  $\text{Hg}^{2+}$  by SG-ODPPNE was evaluated from 5 to 360 min. The result showed that the percentage removal of  $\text{Hg}^{2+}$  increased rapidly to 58.9% for the first 60 min (Figure 4.14). After 60 min, the percentage removal of  $\text{Hg}^{2+}$  was found to increase slowly to 82.1% at 240 min. No significant enhancement in  $\text{Hg}^{2+}$  removal was observed after 240 min. This may due to the available site of adsorbent for adsorption of  $\text{Hg}^{2+}$  decrease with time and finally saturated after 240 min (Zewail and Yousef, 2015).



**Figure 4.14:** Effect of contact time on the removal percentage of  $\text{Hg}^{2+}$  in aqueous sample by SG-ODPPNE. (Amount of SG-ODPPNE = 50 mg,  $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of  $\text{Hg}^{2+}$  solution = 10 mL and pH of  $\text{Hg}^{2+}$  solution = 8).

#### 4.3.4 Effect of $\text{Hg}^{2+}$ initial concentration

The effect of initial  $\text{Hg}^{2+}$  concentration was studied by varying the initial concentration of  $\text{Hg}^{2+}$  from 1 to 100 mg/L. The result showed that the removal percentage decreased with increasing initial concentration of the  $\text{Hg}^{2+}$  solution (Figure 4.15). This could be explained by the fact that the amount of  $\text{Hg}^{2+}$  increases with increasing concentration of the  $\text{Hg}^{2+}$  solution. However, the number of adsorption sites remained constant and subsequently higher amount of  $\text{Hg}^{2+}$  was not absorbed and remained in the solution when the higher concentration of the  $\text{Hg}^{2+}$  solution was used.

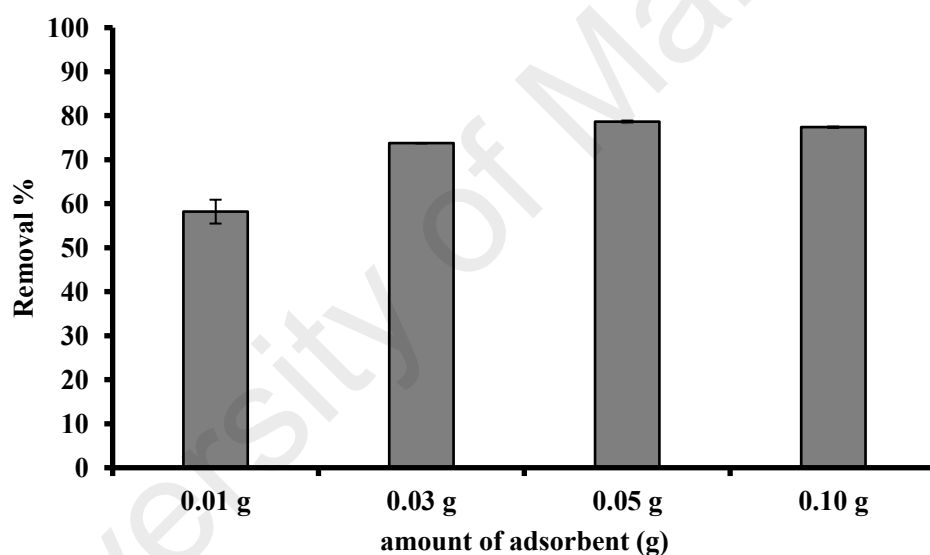


**Figure 4.15:** Effect of  $\text{Hg}^{2+}$  concentration on removal percentage of  $\text{Hg}^{2+}$  in aqueous sample.

(Amount of SG-ODPPNE = 50 mg, volume of  $\text{Hg}^{2+}$  solution = 10 mL, pH of  $\text{Hg}^{2+}$  solution = 8 and contact time = 6 h).

#### 4.3.5 Effect of SG-ODPPNE dosage

The dosage of SG-ODPPNE is an important parameter to obtain quantitative  $\text{Hg}^{2+}$  removal. The removal of  $\text{Hg}^{2+}$  was found to increase from 58.2 to 78.7% when the amount of SG-ODPPNE increased from 10 to 50 mg (Figure 4.16). No significant improvement on  $\text{Hg}^{2+}$  removal was observed when 100 mg of SG-ODPPNE was used. The increased of the removal percentage of  $\text{Hg}^{2+}$  with increasing dosage was due to the presence of higher amount of adsorption site which is accessible for  $\text{Hg}^{2+}$ . At the higher amount of SG-ODPPNE, the saturation of  $\text{Hg}^{2+}$  removal percentage was due to the overlapping of adsorption site that reduced the effective surface area (Mandal et al., 2013).

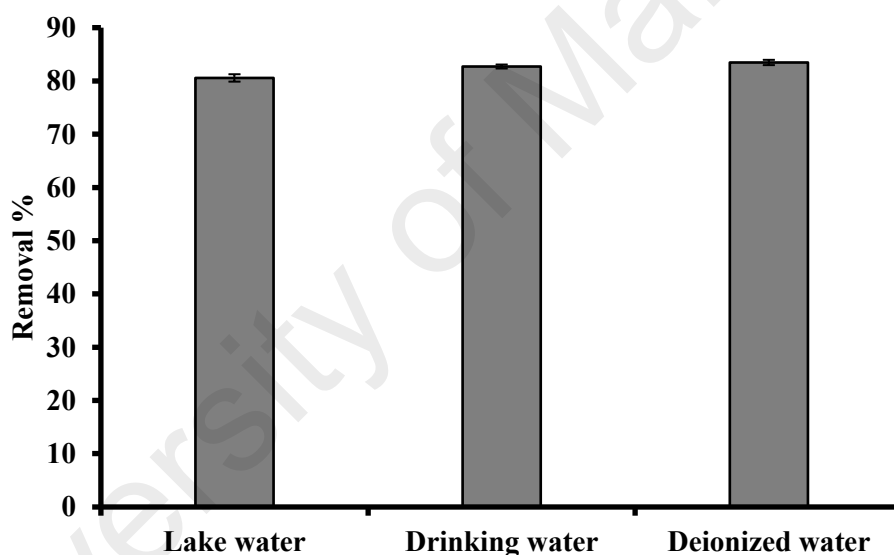


**Figure 4.16:** Effect of SG-ODPPNE amount on removal percentage of  $\text{Hg}^{2+}$  in aqueous sample.

( $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of  $\text{Hg}^{2+}$  solution = 10 mL, pH of  $\text{Hg}^{2+}$  solution = 8 and contact time = 6 h).

#### 4.3.6 Application of SG-ODPPNE in the removal of $\text{Hg}^{2+}$ in real water samples

Adsorption experiment was carried out in drinking water and lake water to evaluate the performance of SG-ODPPNE in the removal of  $\text{Hg}^{2+}$  in real water samples. These two water samples have different water matrices. The selected water samples were found to be free from  $\text{Hg}^{2+}$ . Therefore, the selected water samples were spiked with  $\text{Hg}^{2+}$  at the level of 1 mg/L. As compared to the deionized water, no significant reduction in the  $\text{Hg}^{2+}$  removal efficiency was observed when the adsorption was performed in the selected water samples. This result indicated that the selected water matrices were not significantly influenced the adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE (Figure 4.17).



**Figure 4.17:** Removal percentage of  $\text{Hg}^{2+}$  by SG-ODPPNE in real water samples. (Amount of SG-ODPPNE = 50 mg, spiked  $[\text{Hg}^{2+}] = 1$  mg/L, volume of water samples = 10 mL, pH of water samples = 8 and contact time = 6 h).

The adsorption capacity of SG-ODPPNE on  $\text{Hg}^{2+}$  was compared with previously reported dithiocarbamate-based adsorbents (Table 4.3). These adsorbents were prepared by anchoring the 3-aminopropyltriethoxysilane onto the surface of silica gel (Mahmoud, 1999; Venkatesan et al., 2002), mesoporous silica gel (Venkatesan et al., 2003), and magnetite coated siliceous hybrid shells (Tavares et al., 2013) followed by the addition

of CS<sub>2</sub> to yield dithiocarbamate functional group. The adsorption capacity of SG-ODPPNE was found to be lower than the dithiocarbamate anchored silica gel and mesoporous silica gel. This might due to the ODPPNE that located in the sol-gel matrix and less accessible by Hg<sup>2+</sup>. For dithiocarbamate anchored silica gel and mesoporous silica gel with higher adsorption capacity, the dithiocarbamate is located at the surface of adsorbents and more accessible by Hg<sup>2+</sup>. In term of selectivity, the performance of SG-ODPPNE was found to be comparable with dithiocarbamate anchored silica gel (Mahmoud, 1999).

**Table 4.3:** Comparison of the adsorption capacity and selectivity of SG-ODPPNE with other reported dithiocarbamate-based absorbents.

Adsorbent	Maximum Adsorption Capacity (mg/g)	Selectivity [Metal ion (normalized $Q_e$ )]
Dithiocarbamate anchored silica gel <sup>1</sup>	#NR	Hg <sup>2+</sup> ( <b>1</b> ), Mg <sup>2+</sup> (0.02), Ca <sup>2+</sup> (0.06), Cr <sup>3+</sup> (0.12), Mn <sup>2+</sup> (0.12), Co <sup>2+</sup> (0.09), Cu <sup>2+</sup> (0.32), Zn <sup>2+</sup> (0.10), Cd <sup>2+</sup> (0.16), Ba <sup>2+</sup> (0.30), Pb <sup>2+</sup> (0.45)
Dithiocarbamate anchored silica gel <sup>2</sup>	~61	#NR
Dithiocarbamate grafted on mesoporous silica <sup>3</sup>	40	#NR
Magnetite coated with siliceous hybrid shells <sup>4</sup>	20	#NR
Chalcone based dithiocarbamate derivative incorporated sol-gel <sup>5</sup>	13.5	Hg <sup>2+</sup> ( <b>1</b> ), Cr <sup>3+</sup> (0.52), Ni <sup>2+</sup> (0.16), Cu <sup>2+</sup> (0.54), Zn <sup>2+</sup> (0.24), Cd <sup>2+</sup> (0.28), and Pb <sup>2+</sup> (0.37)

#NR: Not reported

<sup>1</sup>Mahmoud, 1999, <sup>2</sup>Venkatesan et al., 2002, <sup>3</sup>Venkatesan et al., 2003, <sup>4</sup>Tavares et al., 2013 and <sup>5</sup>This work.

#### 4.4 Pre-concentration of $\text{Hg}^{2+}$ in aqueous sample by ODPPNE@MNP

So far, most of the ligand incorporated silica gels are frequently used as adsorbents for the metal ions removal. In this study, SG-ODPPNE was coated onto the magnetic particles for the preparation of adsorbent (ODPPNE@MNP) for the pre-concentration of  $\text{Hg}^{2+}$ . This study demonstrated the application of ligand incorporated silica gel in trace  $\text{Hg}^{2+}$  analysis. The selected method for pre-concentration was D- $\mu$ SPE (Figure 4.18). In D- $\mu$ SPE, ODPPNE@MNP as the solid adsorbent was dispersed in water through sonication to allow the adsorption of  $\text{Hg}^{2+}$ . After adsorption, ODPPNE@MNP was separated from water using an external magnet. In this case, the magnetic property was added to the ODPPNE@MNP to ease the separation of adsorbent after the pre-concentration process. Then the water sample was decanted leaving the ODPPNE@MNP in the vials. The  $\text{Hg}^{2+}$  that adsorbed by ODPPNE@MNP was desorbed using desorption reagent, and the  $\text{Hg}^{2+}$  was analysed using mercury analyser. In this study, the operating parameters (such as the amount of adsorbent, adsorption time, pH and concentration of  $\text{Hg}^{2+}$ ) of D- $\mu$ SPE were optimized to develop an efficient pre-concentration technique.

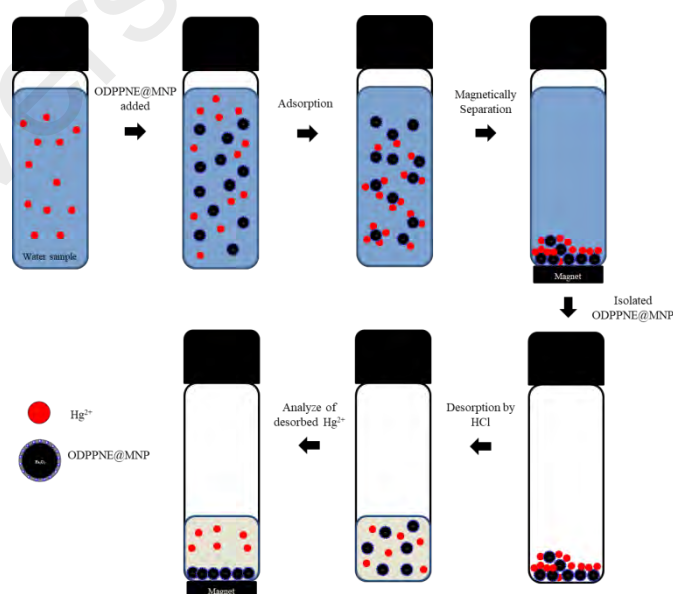
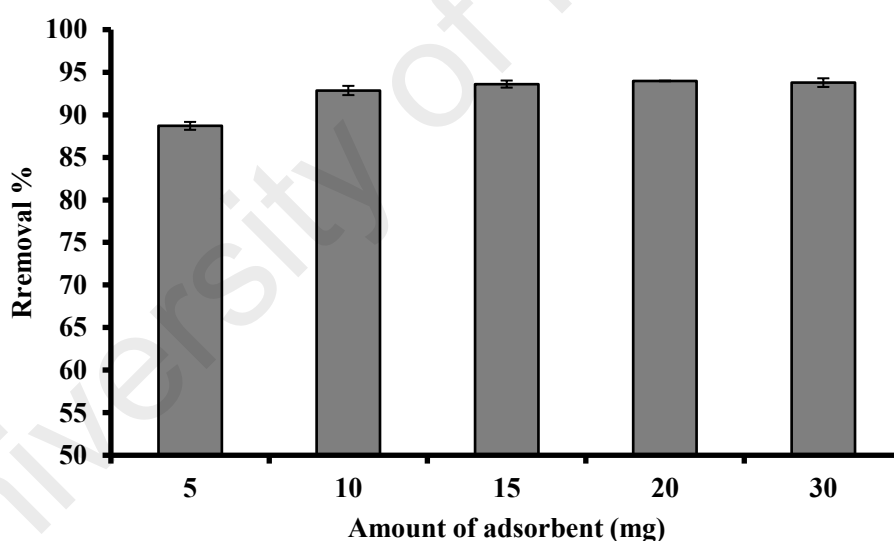


Figure 4.18: D- $\mu$ SPE process.

#### 4.4.1 Amount of ODPPNE@MNP

The adsorption process was carried out by varying the amount of ODPPNE@MNP from 5 to 30 mg to determine the optimum amount of ODPPNE@MNP required to achieve the optimum adsorption of  $\text{Hg}^{2+}$ . The percent removal of  $\text{Hg}^{2+}$  was found to increase from 88.7 to 93.6% when the amount of ODPPNE@MNP was increased from 5 to 15 mg. This result was mainly due to the increased of metal adsorption site when the amount of ODPPNE@MNP was increased. However, there was no significant increase in the percent removal of  $\text{Hg}^{2+}$  when the amount of ODPPNE@MNP was increased to 20, and 30 mg (Figure 4.19). This result indicates that 15 mg of ODPPNE@MNP was sufficient to achieve the highest  $\text{Hg}^{2+}$  removal efficiency. Thus, the dosage of ODPPNE@MNP used for subsequent adsorption process was 15 mg.



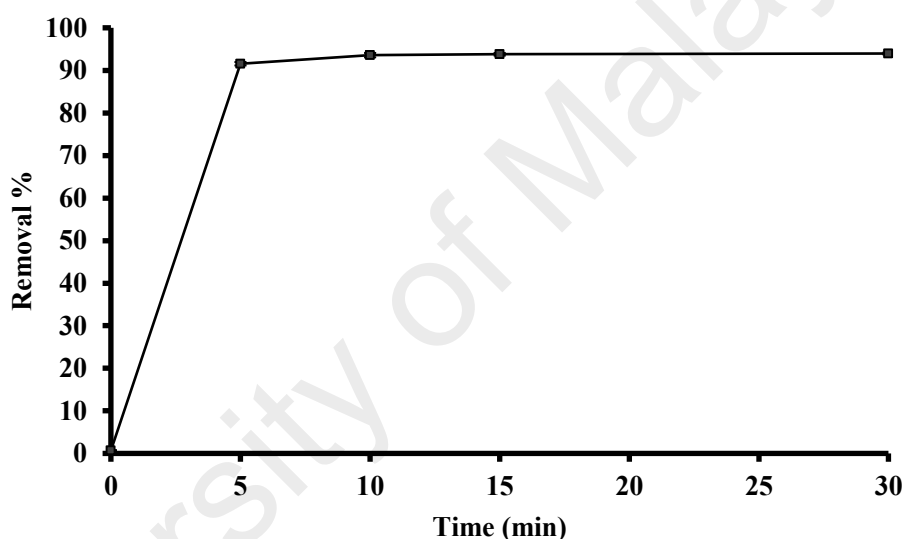
**Figure 4.19:** Effect of the amount of ODPPNE@MNP on removal percentage of  $\text{Hg}^{2+}$  in water.

( $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of  $\text{Hg}^{2+}$  solution = 25 mL, pH of aqueous solution = 8 and adsorption time = 30 min).



#### 4.4.2 Adsorption time

In D- $\mu$ SPE, ODPPNE@MNP was dispersed in the water with the aid of sonication. Hence, the sonication time was investigated to ensure the ODPPNE@MNP was completely and evenly dispersed in the  $\text{Hg}^{2+}$  solution to acquire the optimal removal efficiency. According to the result obtained (Figure. 4.20), the removal efficiency achieved increased significantly to 91.6% for the first 5 min of sonication. At 10 min, the obtained percent removal was 93.6%, and it remained constant after 10 min of sonication time. Therefore, the adsorption time for D- $\mu$ SPE was fixed to 10 min in this study.



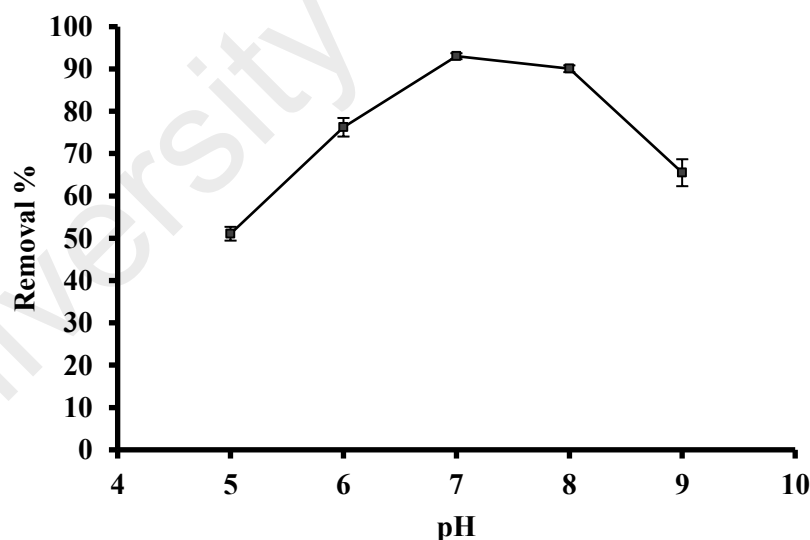
**Figure 4.20:** Effect of adsorption time on removal percentage of  $\text{Hg}^{2+}$  in aqueous solution.

(Amount of ODPPNE@MNP = 15 mg,  $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , pH of aqueous solution = 8 and volume of  $\text{Hg}^{2+}$  solution = 25 mL.

#### 4.4.3 pH of aqueous solution

The effect of pH on the performance of ODPPNE@MNP for  $\text{Hg}^{2+}$  adsorption was studied by varying the pH of the solution from 5 to 9. The result (Figure 4.21) showed that the adsorption of  $\text{Hg}^{2+}$  by ODPPNE@MNP was found to increase from 51.1 to around 90% when the pH of the solution was increased from 5 to 8. This result is in agreement with SG-ODPPNE which also achieved its highest adsorption efficiency at pH 8. As shown in

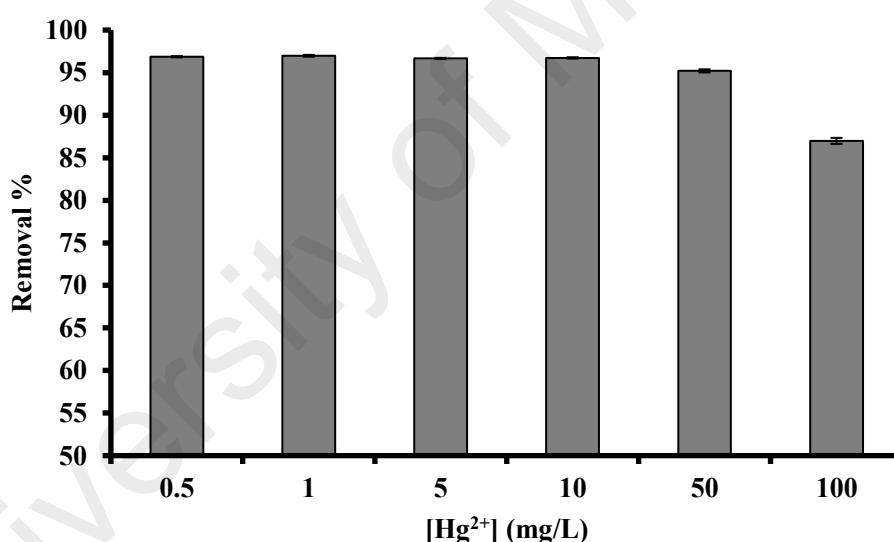
Section 4.3.2, the calculated pKa of ODPPNE was 4.21 and 7.32. Therefore, ODPPNE also appeared dominantly in neutral and deprotonated forms at this selected pH range. The lower efficiency of ODPPNE@MNP in  $\text{Hg}^{2+}$  removal at acidic condition was mainly due to the presence of the higher fraction of neutral ODPPNE which has the lower capability to complex with  $\text{Hg}^{2+}$ . When the pH increases to 8, the higher amount of ODPPNE appeared in the deprotonated form. Deprotonated ODPPNE could interact favorably with  $\text{Hg}^{2+}$  due to the presence of negative charge. When the pH of the aqueous solution was high, the formation of  $\text{Hg}(\text{OH})_2$  which is neutral and less favorable (Shen et al., 2014) to interact with ODPPNE as compared with  $\text{Hg}^{2+}$ . Since ODPPNE@MNP showed slightly higher efficiency in adsorbing  $\text{Hg}^{2+}$  at pH 7, this pH condition was selected for the following experiment.



**Figure 4.21:** Effect of pH on removal percentage of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg,  $[\text{Hg}^{2+}] = 1 \text{ mg/L}$ , volume of aqueous solution = 25 mL and adsorption time = 10 min).

#### 4.4.4 Concentration of $\text{Hg}^{2+}$ in aqueous solution

The effect of initial concentration of  $\text{Hg}^{2+}$  in the aqueous sample on the adsorption performance of ODPPNE@MNP was studied by varying the initial concentration of  $\text{Hg}^{2+}$  from 0.5 to 100 mg/L. The result (Figure 4.22) indicated that the adsorption efficiency of  $\text{Hg}^{2+}$  by ODPPNE@MNP was excellent when the concentration of  $\text{Hg}^{2+}$  was increased from 0.5 to 10 mg/L, and 97% of  $\text{Hg}^{2+}$  was removed. However, the efficiency of ODPPNE@MNP was found to reduce when the concentration of  $\text{Hg}^{2+}$  was further increased to 50 and 100 mg/L. This observation was due to the increasing amount of  $\text{Hg}^{2+}$  when the concentration was increased, but the available active site at ODPPNE@MNP remained unchanged and saturated with  $\text{Hg}^{2+}$  (Denizli et al., 2000).

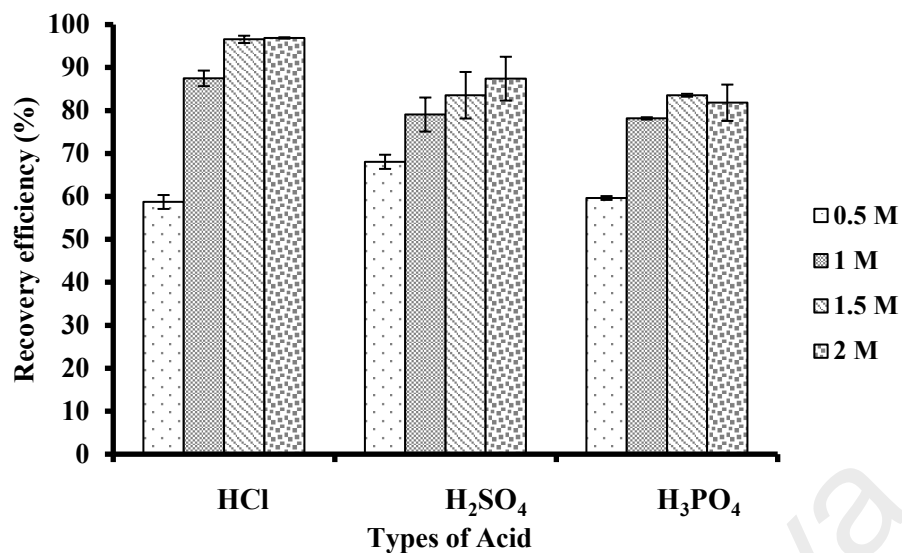


**Figure 4.22:** Effect of  $\text{Hg}^{2+}$  concentration on removal percentage of  $\text{Hg}^{2+}$  in aqueous sample.

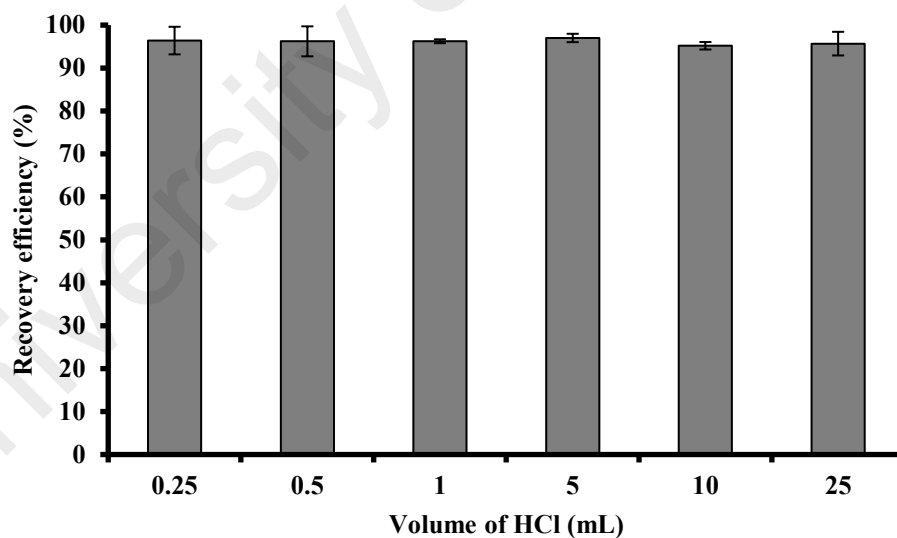
(Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min and pH of aqueous solution = 7).

#### 4.4.5 Desorption reagent for $\text{Hg}^{2+}$

In order to determine the most suitable desorption reagent to desorb the adsorbed  $\text{Hg}^{2+}$  from ODPPNE@MNP, several types of acids which included hydrochloric acid (HCl), sulphuric acid ( $\text{H}_2\text{SO}_4$ ) and phosphoric acid ( $\text{H}_3\text{PO}_4$ ) with different concentration were used in the desorption process. Acid was selected because it can dissolve metal ions. Desorption process was also carry out using sonication. According to Figure 4.23, the highest percentage recovery of  $\text{Hg}^{2+}$  was achieved using HCl as desorption reagent as compared to  $\text{H}_2\text{SO}_4$  and  $\text{H}_3\text{PO}_4$ . This result might be due to the favorable reaction between  $\text{Hg}^{2+}$  with HCl to form chloro complexes of  $\text{Hg}^{2+}$  (Bhattacharyya et al., 2013). The effect of concentration of acid on the desorption of  $\text{Hg}^{2+}$  was evaluated in this experiment. Figure 4.23 showed that the percent recovery of  $\text{Hg}^{2+}$  was increased with increasing concentration of acid ranging from 0.5 to 1.5 M. No significant changes in the percent recovery when the concentration of acid was further increased to 2.0 M. Therefore, HCl with the concentration of 1.5 M was selected as desorption reagent in the D- $\mu$ SPE. The recovery process was performed under by varying the volume of HCl from 0.25 to 25 mL to determine the effect of volume of 1.5 M HCl toward the  $\text{Hg}^{2+}$  recovery efficiency. The result showed that the recovery efficiency of  $\text{Hg}^{2+}$  was unaffected by the volume of HCl (Figure 4.24). Therefore, 0.25 mL of 1.5 M HCl was selected as desorption reagent to reduce the chemical consumption of the developed D- $\mu$ SPE.



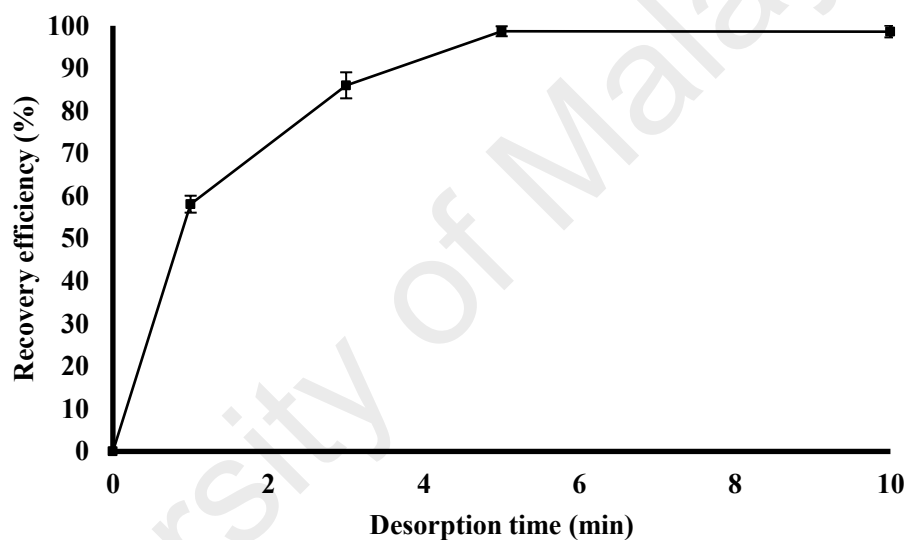
**Figure 4.23:** Effect of the type of eluent used and its concentration on recovery efficiency of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, desorption time = 30 min and volume of acid = 25 mL).



**Figure 4.24:** Effect of the volume of HCl on recovery efficiency of  $\text{Hg}^{2+}$  in aqueous solution. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, desorption time = 30 min and [HCl] = 1.5 M).

#### 4.4.6 Desorption Time

Desorption time was studied in detail to obtain a fast and efficient D- $\mu$ SPE technique for  $\text{Hg}^{2+}$  analysis. In this study, the desorption processes were carried out with the aid of sonication to enhance desorption process. The recovery of  $\text{Hg}^{2+}$  was examined within 1 to 10 min of sonication. The result showed that (Figure 4.25), the percent recovery of  $\text{Hg}^{2+}$  was increased significantly to 98.7% within first 5 min. The recovery of  $\text{Hg}^{2+}$  was remained unchanged after 5 min of sonication. Therefore, desorption process by sonication was performed at 5 min for the following experiment.

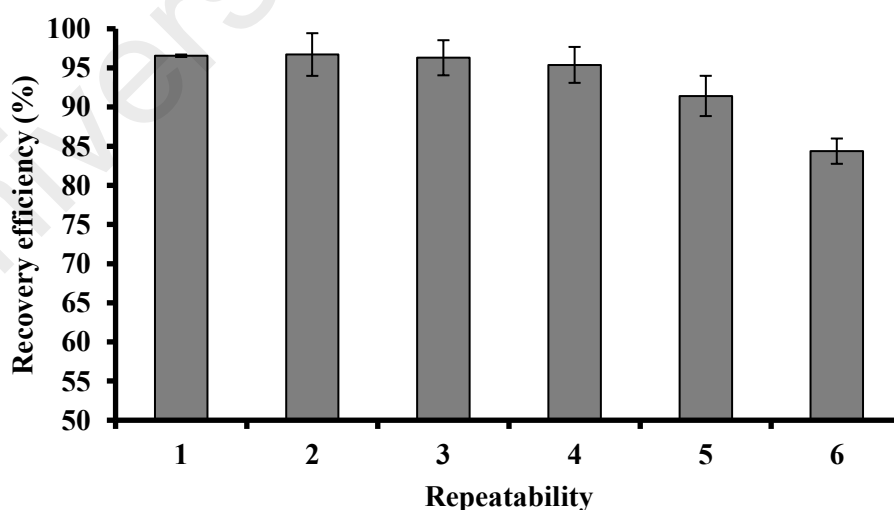


**Figure 4.25:** Effect of the desorption time recovery efficiency of  $\text{Hg}^{2+}$  in aqueous solution.

(Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, volume of HCl = 0.25 mL and  $[\text{HCl}] = 1.5 \text{ M}$ ).

#### 4.4.7 Reusability of ODPPNE@MNP in D- $\mu$ SPE process

Reusability is an important feature for the adsorbents in the green chemical analysis. Reusable adsorbents can reduce the chemical consumption during its production. In this experiment, the used ODPPNE@MNP was washed with 1.5 M of HCl and deionized water for three times before the following pre-concentration process was performed to ensure the ODPPNE@MNP was completely free from  $\text{Hg}^{2+}$ . Each pre-concentration process was performed under identical conditions as the first process, and the percent recovery of  $\text{Hg}^{2+}$  was monitored. As shown in Figure 4.26, the percent recovery remained constant ( $> 95\%$ ) within the first four pre-concentration. However, the percent recovery of  $\text{Hg}^{2+}$  was found to decrease to 91.4% and 84.4% for the fifth and sixth time of the pre-concentration process. The degradation in the  $\text{Hg}^{2+}$  pre-concentration efficiency might occur due to the dissolution of the silica gel coating by acid which causes the ODPPNE to leak from ODPPNE@MNP and consequently reduced the efficiency of ODPPNE@MNP in the pre-concentration process. As a conclusion, the ODPPNE@MNP can be reused up to four times of pre-concentration.



**Figure 4.26:** Reusability of ODPPNE@MNP. (Amount of ODPPNE@MNP = 15 mg, volume of aqueous solution = 25 mL, adsorption time = 10 min, pH of aqueous solution = 7, volume of HCl = 0.25 mL, [HCl] = 1.5 M, and desorption time = 10 min).

#### 4.4.8 Application of ODPPNE@MNP as solid adsorbent in the pre-concentration of Hg<sup>2+</sup> in real water sample

According to the Section 4.4.1-4.4.7, the optimized condition for the pre-concentration of Hg<sup>2+</sup> was 15 mg of ODPPNE@MNP, adsorption time of 10 min, pH 7, 1.5 M of HCl as desorption reagent, and 5 min of desorption time. The pre-concentration factor for the optimized method was calculated using Equation 4.1:

$$\text{Pre - concentration Factor} = \frac{V_0}{V_f} \quad \text{Equation 4.1}$$

where  $V_0$  and  $V_f$  are the initial volumes of the water sample and volume of desorption agent. In this experiment, Hg<sup>2+</sup> in 25 mL of water sample was adsorbed by ODPPNE@MNP, and 0.25 mL of 1.5 M HCl was used to desorb the adsorbed Hg<sup>2+</sup>. Therefore, the pre-concentration factor for Hg<sup>2+</sup> in this study was 100.

The analytical performance and validation of the optimized pre-concentration method were evaluated using linearity, the method of detection limit (MDL) or limit of detection (LOD), limit of quantitation (LOQ), inter-day and intra-day precision. The optimized method showed good regression coefficient ( $R^2$ ) of 0.9985 for the linear range of 50 to 5000 ng/L. The MDL and LOQ were determined through seven replicates of deionized water spiked with Hg<sup>2+</sup> at the concentration that equal to signal to noise ratio of five (Ripp, 1996). MDL and LOQ were determined using the following equations (Equation 4.2 and Equation 3):

$$MDL = s \times (t - value) \quad \text{Equation 4.2}$$

$$LOQ = s \times 10 \quad \text{Equation 4.3}$$

where  $s$  is the standard deviation of the concentration of Hg<sup>2+</sup> obtained from the seven replicates and  $t$ -value is the  $t$ -student value based on six degrees of freedom which is



equal to 3.143. The obtained MDL and LOQ for the optimized method were 4.0 and 12.9 ng/L, respectively. These values were far below the maximum contaminant level goal (MCLG) of inorganic mercury, which is 2 µg/L (U.S. EPA, 2009). The intra-day and inter-day reproducibility of the proposed method was expressed in relative standard deviation (%RSD) by analysing five replicates of 0.05 µg/L Hg<sup>2+</sup>. %RSD obtained for intra-day and inter-day analyses were 6.9 and 3.7%, respectively.

For validation, drinking water, tap water, and surface water that spiked with Hg<sup>2+</sup> at the concentration of 50, 500 and, 2000 ng/L were analysed using the optimized method. The intraday and interday precision of the optimized method are presented in Table 4.4. The obtained recovery for Hg<sup>2+</sup> was ranged from 90.1 to 99.0 % with relative standard deviation of 0.7 - 8.8 and 1.1 - 7.7% for the intra-day and inter-day precision. These results showed that the matrices of the selected water samples have no significant effect on the performance of the developed method. A typical comparison with other methods reported by previous studies is presented in Table 4.5. The analytical characteristics such as MDL or LOD, LOQ, and linearity range obtained from the optimized method are more sensitive than other previous methods. Therefore, it can be concluded that the proposed method was an effective and robust method for the pre-concentration of Hg<sup>2+</sup> in water.

**Table 4.4:** Intra and inter day analysis result for real water samples.

Sample	Spiked [Hg <sup>2+</sup> ] (ng/L)	Intra-day (n=5)		Inter-day (n=5)	
		Recovery efficiency (%)	RSD (%)	Recovery efficiency (%)	RSD (%)
Drinking water	50	96.2	8.8	95.1	1.1
	500	97.5	1.9	96.9	2.3
	2000	98.1	8.7	98.1	4.0
Tap Water	50	99.0	0.7	92.3	4.7
	500	98.2	6.6	98.1	5.9
	2000	90.1	3.1	96.6	7.7
Surface Water	50	90.7	6.5	91.4	5.2
	500	90.8	3.6	90.3	3.4
	2000	91.8	5.2	91.2	1.2

**Table 4.5:** Comparison with previous reported analytical methods for pre-concentration or determination of Hg<sup>2+</sup> in aqueous sample.

Adsorbent	Analytical Method	Detection Limit (ng/L)	LOQ (ng/L)	Linearity (µg/L)
Fe <sub>3</sub> O <sub>4</sub> magnetic nanoparticles functionalized with dithizone <sup>1</sup>	D-µSPE/CV-AAS	50*	200	0.2-100
Fe <sub>3</sub> O <sub>4</sub> nanoparticles covered with a shell of silica and modified with the N-(2-acetylaminoethyl)-N-(3-triethoxysilylpropyl)thiourea <sup>2</sup>	D-µSPE /DMA	17*	#NR	#NR
Thiol-modified magnetic silica sorbent <sup>3</sup>	D-µSPE /CV-AAS	60*	#NR	0.2-5
Thiodiethanethiol grafted tetraethyl orthosilicate modified nanoparticles <sup>4</sup>	D-µSPE /CV-AAS	4*	#NR	0.01-750
Fe <sub>3</sub> O <sub>4</sub> magnetite nanoparticles modified with 1-(p-acetyl phenyl)-3-(o-ethoxy phenyl) triazene <sup>5</sup>	D-µSPE /ICP-OES	40*	130	0.2-200
Magnetic nanoparticles functionalized with 1,5-bis(di-2-pyridil)methylene thiocarbohydrazide <sup>6</sup>	FI-MSPME/CV-ETAAS	7.4*	#NR	0.099-10/10-50
Rattle-type Fe <sub>3</sub> O <sub>4</sub> @SnO <sub>2</sub> core-shell nanoparticles <sup>7</sup>	D-µSPE /CV-AAS	28*	#NR	0.1-40
ODPPNE@MNP <sup>8</sup>	D-µSPE /MA	4.0**	12.9	0.05-5.0

\*LOD, \*\*MDL, #NR: Not reported

<sup>1</sup>Adlnasab et al., 2014, <sup>2</sup>Cui et al., 2015, <sup>3</sup>Xiang et al., 2013, <sup>4</sup>Beiraghi et al., 2014, <sup>5</sup>Rofouei et al., 2012, <sup>6</sup>Alonso et al., 2016, <sup>7</sup>Mehdinia et al., 2017 and <sup>8</sup>This work.

#### 4.5 Adsorption isotherm

Adsorption isotherm describes the phenomenon that is governing the retention, release, and mobility of a substance from the aqueous to a solid-phase at a constant temperature and pH (Foo and Hameed, 2010). In this study, the adsorption isotherm was determined to understand the mechanism of adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE and MNP@ODPPNE. The obtained adsorption data were fitted to Langmuir and Freundlich models to obtain the best model that described the adsorption  $\text{Hg}^{2+}$  process by both SG-ODPPNE and MNP@ODPPNE (Abas et al., 2013). Langmuir model assumes the adsorption occurs at monolayer or so-called unilayer adsorption (Sadeek et al., 2015). According to this model, sorbates are adsorbed by equivalent active site with identical energy. These active sites were located on the surface of adsorbent and consequently formed a saturated monolayer. The Langmuir model can be expressed by Equation 4.4 (Foo and Hameed, 2010):

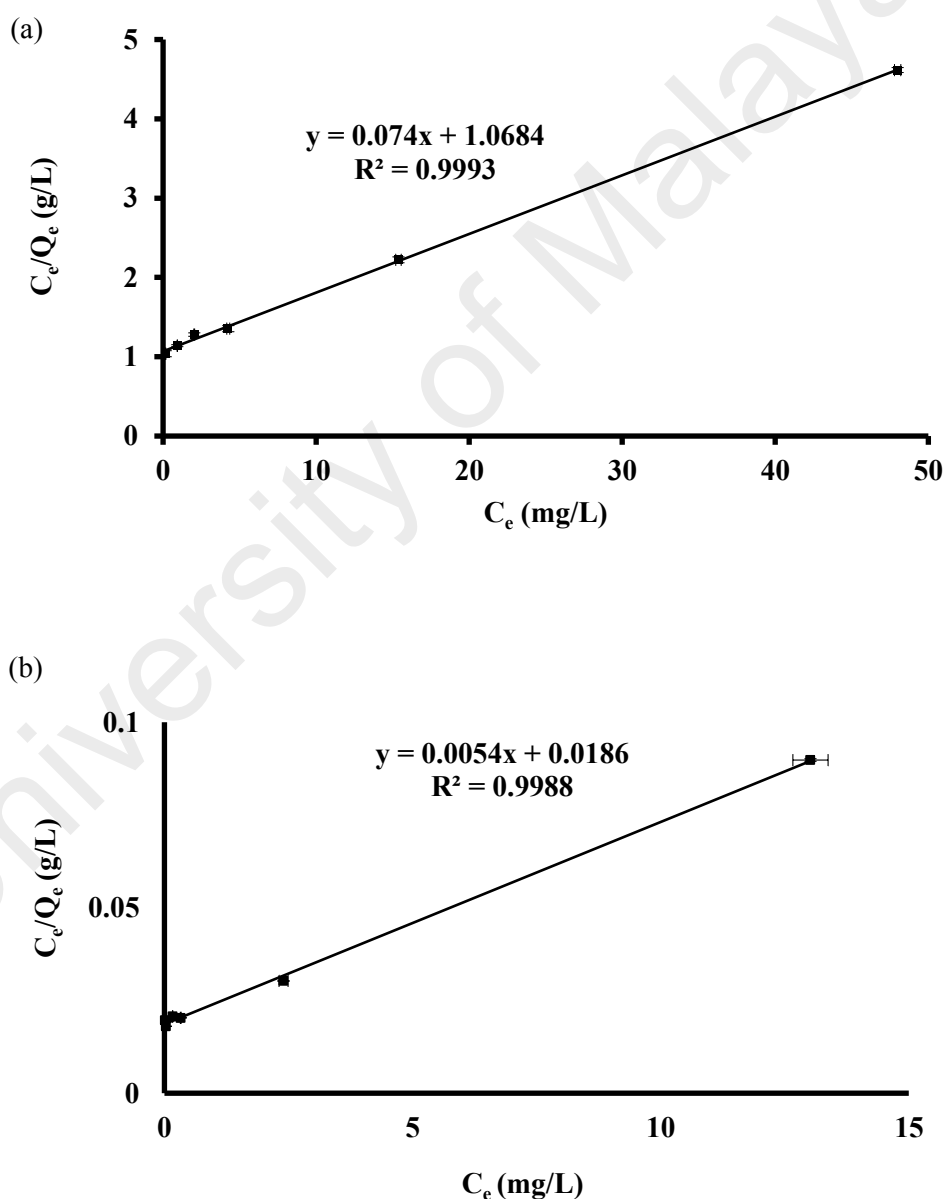
$$\frac{C_e}{Q_e} = \frac{1}{Q_m B_L} + \frac{C_e}{Q_m} \quad \text{Equation 4.4}$$

where  $C_e$  is referring to the concentration of sorbate which is  $\text{Hg}^{2+}$  at equilibrium,  $Q_e$  and  $Q_m$  represent the adsorption capacity of adsorbent at equilibrium and maximum adsorption capacity (mg/g), and  $B_L$  is the Langmuir constant (L/mg) related to the energy of adsorption. By plotting the curve of  $C_e/Q_e$  versus  $C_e$ ,  $Q_m$  and  $B_L$  can be determined from slope and intercept of the graph. The dimensionless constant or separation factor  $R_L$  can be determined to show the favorability of adsorption.  $R_L$  can be calculated using the following Equation 4.5 (Ramos-Ramírez et al., 2009):

$$R_L = \frac{1}{1 + (B_L \times C_o)} \quad \text{Equation 4.5}$$

where  $C_o$  represents the initial concentration of  $\text{Hg}^{2+}$  as adsorbate. The adsorption process

is described as favorable if  $0 < R_L < 1$ , unfavorable if  $R_L > 1$  and linear when  $R_L = 0$  (Ramos-Ramírez et al., 2009). For SG-ODPPNE, the  $C_e/Q_e$  versus  $C_e$  plot (Figure 4.27a) was linear with the correlation coefficients ( $R^2$ ) of 0.9993. The  $Q_m$  obtained from the curve was 13.5 mg/g, and the  $R_L$  value was in the range of 0.1428 to 0.9434. The results obtained from the  $R_L$  value indicates the adsorption of  $Hg^{2+}$  is a favorable process. The  $C_e/Q_e$  versus  $C_e$  plot (Figure 4.27b) for ODPPNE@MNP was also linear with the  $R^2$  value of 0.9988. The  $Q_m$  obtained for ODPPNE@MNP was 185.2 mg/g.



**Figure 4.27:** Linearized adsorption isotherm Langmuir Model for  $Hg^{2+}$  adsorption on (a) SG-ODPPNE and (b) ODPPNE@MNP.

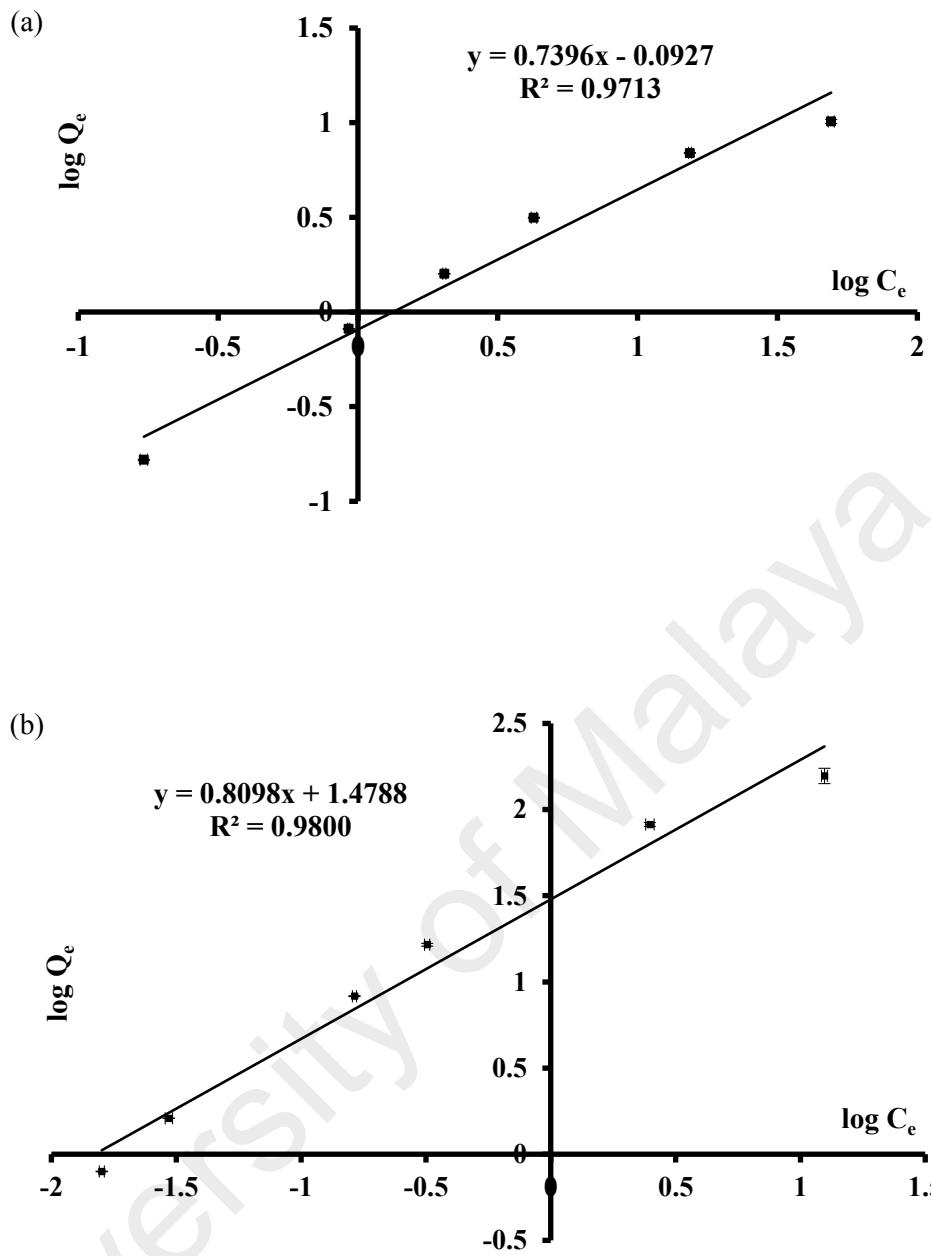
ODPPNE@MNP also showed favorable adsorption process towards  $\text{Hg}^{2+}$  with the  $R_L$  value ranging from 0.0333 to 0.8732. The  $Q_m$  value obtained for ODPPNE@MNP was 13.7 times higher than SG-ODPPNE. ODPPNE@MNP with smaller particle (~600 nm) with the larger surface area could adsorb higher amount of  $\text{Hg}^{2+}$  as compared to SG-ODPPNE with the size of 0.06 mm.

Freundlich isotherm is an empirical equation that describes the adsorption process on the heterogeneous surface with the non-uniform active site, which also refers to multilayer adsorption process (Sadeek et al., 2015; Yan et al., 2015). The Freundlich model can be described by Equation 4.6 (Mushtaq et al., 2016):

$$\log Q_e = \log B_f + \frac{1}{n} \log C_e \quad \text{Equation 4.6}$$

where  $B_f$  represents the Freundlich constant that related to adsorption capacity, and  $n$  is the adsorption intensity constant. The  $R^2$  values obtained from  $\log Q_e$  versus  $\log C_e$  curve (Figure 4.28) for SG-ODPPNE and MNP@ODPPNE were 0.9713 and 0.9800, respectively.

The best-fitted model for this adsorption process was determined by the  $R^2$  and Chi-square values ( $\chi^2$ ) obtained from Figure 4.27 and Figure 4.28 (Mandal et al., 2013). The result showed that the  $R^2$  value of Langmuir model was significantly higher than Freundlich model for both SG-ODPPNE and MNP@ODPPNE (Table 4.6). In addition, the  $\chi^2$  of Langmuir model for SG-ODPPNE and MNP@ODPPNE adsorption was found to be lower than Freundlich model. This observation suggested that the adsorption process of  $\text{Hg}^{2+}$  on SG-ODPPNE and ODPPNE@MNP follows Langmuir isotherm model which indicates the unilayer adsorption. In addition, this result also indicated that ODPPNE trapped in the silica gel matrix are equivalent active site with identical energy for  $\text{Hg}^{2+}$  adsorption.



**Figure 4.28:** Linearized adsorption isotherm Freundlich Model for  $Hg^{2+}$  adsorption on (a) SG-ODPPNE and (b) ODPPNE@MNP.

**Table 4.6:** Adsorption isotherm parameter of (a) Langmuir and (b) Freundlich model.

(a)		
Parameter	Langmuir model	
	SG-ODPPNE	ODPPNE@MNP
$Q_m$ (mg/g)	13.5135	185.1852
$B_L$ (L/mg)	0.06926	0.2903
$R_L$	0.14-0.94	0.033-0.87
$R^2$	0.9993	0.9988
$\chi^2$	0.0139	0.1891

(b)		
Parameter	Freundlich model	
	SG-ODPPNE	ODPPNE@MNP
$B_F$ (L/mg)	0.8078	30.1162
$1/n$	0.7396	0.8098
$n$	1.3521	1.2349
$R^2$	0.9713	0.9800
$\chi^2$	1.6830	33.9432



## 4.6 Kinetics study

Adsorption kinetics study was carried out to further determine the mechanism of the adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE and MNP@ODPPNE. This study was performed by fitting the obtained data to several kinetic models (Wu et al., 2014). In this study, the data were fitted into pseudo-first order, pseudo-second order and intra particle diffusion models.

### 4.6.1 Pseudo-first order and Pseudo-second order Model

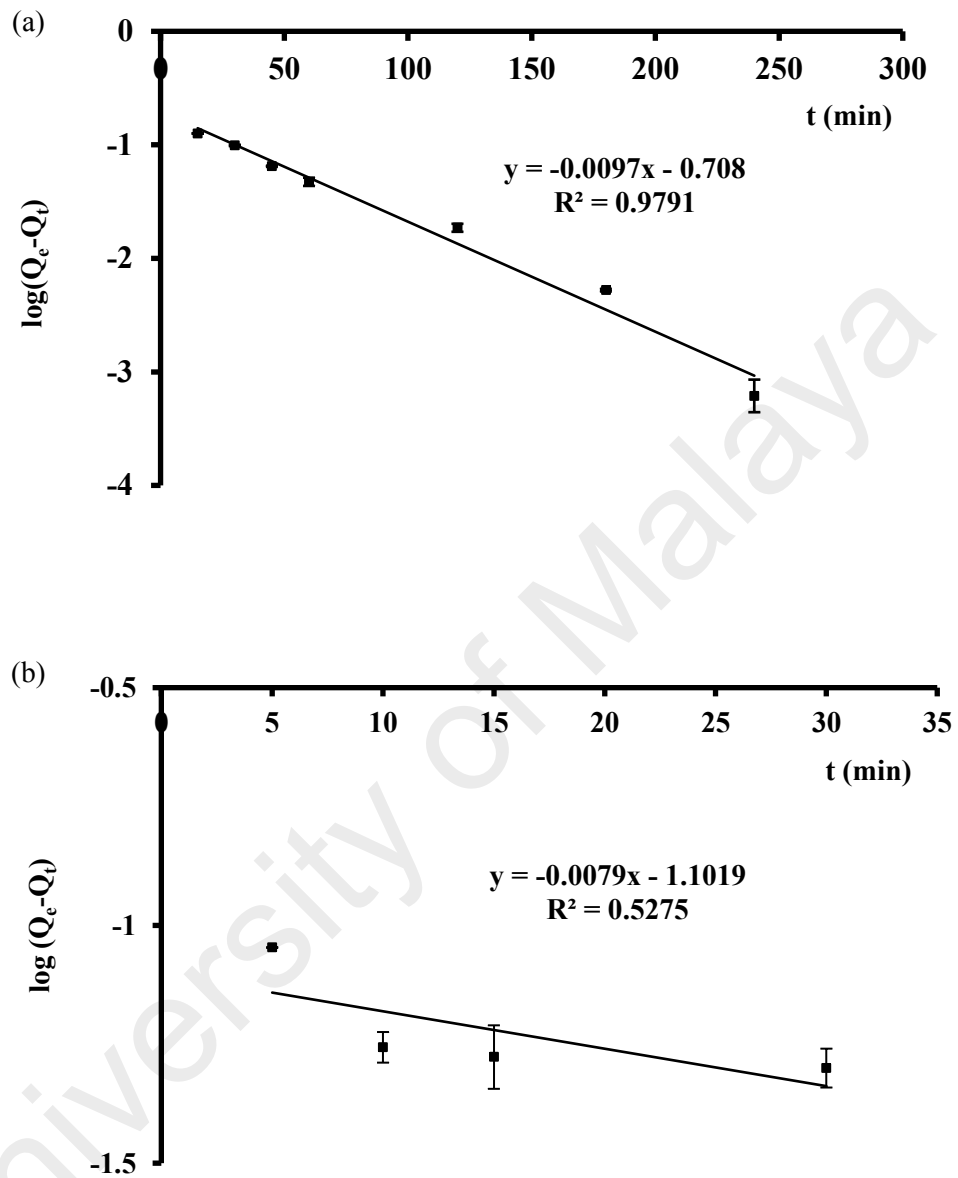
In the past four decades, Pseudo-first order model has been widely used to study the kinetics of the adsorption of pollutants from aqueous solution by various adsorbents such as peat, organobentonite, chitosan, etc. (Cheung et al., 2007; Ho, 2006; Yan et al., 2015). This model describes the adsorption process in the absent of sorbate-sorbate interaction (Kumar, 2006). In this study the sorbate is referring to  $\text{Hg}^{2+}$ . The linearized equation of pseudo-first order is presented as follows (Equation 4.7) (Ho, 2006):

$$\log(Q_e - Q_t) = \log Q_e - \frac{k_1}{2.303} t \quad \text{Equation 4.7}$$

where  $Q_t$  (mg/g) is the amount of adsorbed adsorbate at time  $t$  and  $k_1$  represents the pseudo-first order rate constant.

The data from adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE were found to be well fitted at the early stages of the adsorption process (Figure 4.29a) due to the absent of sorbate-sorbate interaction on SG-ODPPNE (Kumar, 2006). However, the linear slope was deviated after 60 min of adsorption time and suggested that pseudo-first order model was inapplicable to describe the entire adsorption process due to the sorbate-sorbate interaction that occurred after 60 min (Ho and MacKay, 1998). On the other hand, the data obtained from adsorption of  $\text{Hg}^{2+}$  by ODPPNE@MNP was not fitted well to this

model where the poor value of  $R^2$  (0.5275) was obtained (Figure 4.29b). This result further indicates the presence of strong sorbate-sorbate interaction.



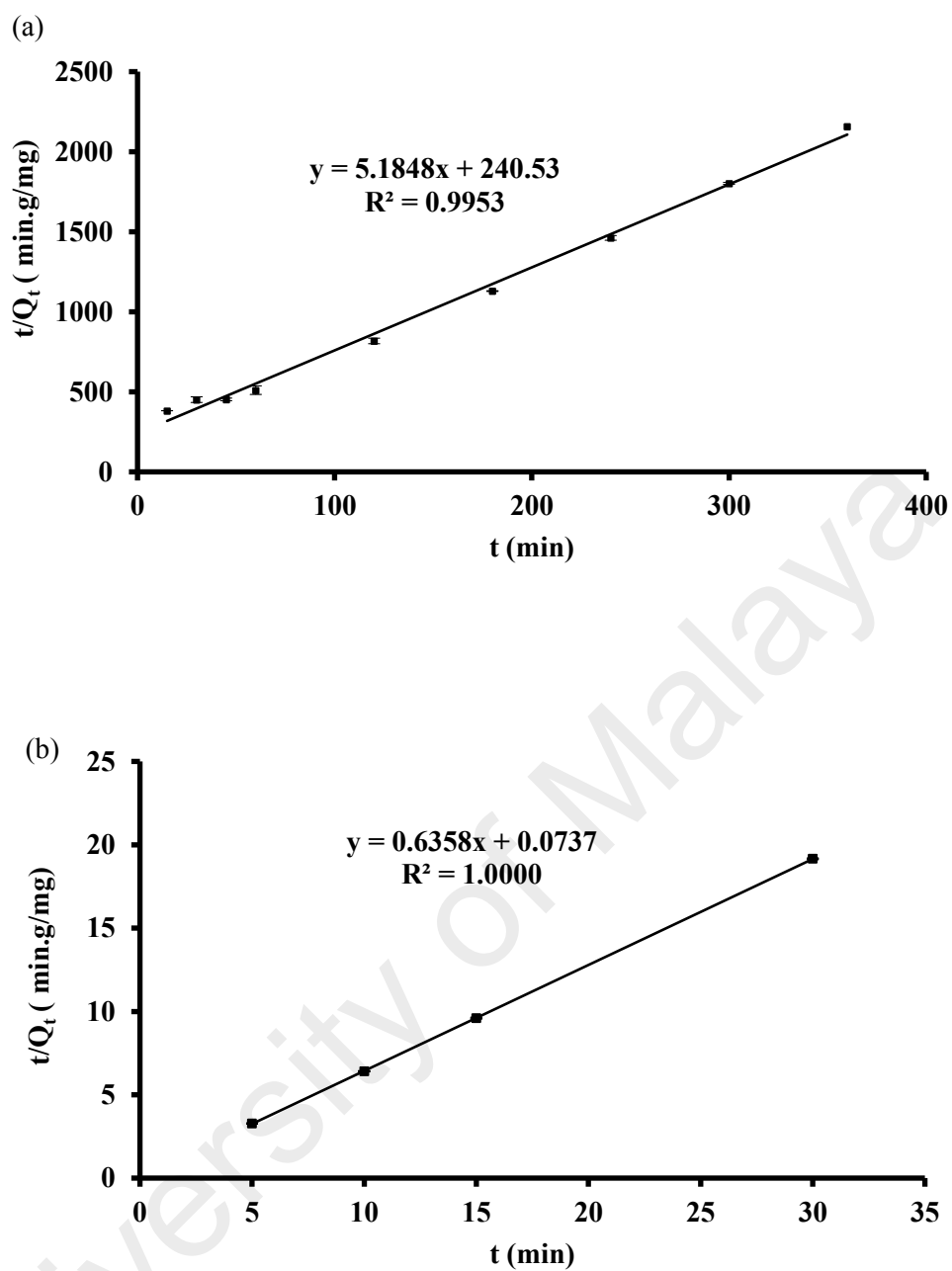
**Figure 4.29:** Pseudo-first order model for the adsorption of  $Hg^{2+}$  on (a) SG-ODPPNE and (b) ODPPNE@MNP.

To further evaluate the kinetics of adsorption process, the experiment data were fitted into pseudo-second order model. Pseudo-second order model describes the chemisorption between sorbate and adsorbent, which involved sharing or transfer of valence electron (Ho, 2006). The pseudo-second order equation is described by equation 4.8:

$$\frac{t}{Q_t} = \frac{t}{Q_e} + \frac{1}{k_2 Q_e^2} \quad \text{Equation 4.8}$$

where  $Q_t$  (mg/g) is the amount of adsorbed adsorbate at time  $t$  and  $k_2$  is the pseudo-second order rate constant which can be determined from the intercept of graph  $t/Q_t$  versus  $t$ .

According to Table 4.7 and Figure 4.30, the  $R^2$  values (0.9953 and 1) obtained from pseudo-second order plot of SG-ODPPNE and ODPPNE@MNP was found to be higher than that of pseudo-first order. This result suggested that the pseudo-second order model was the better model to describe the kinetics of the sorption process in this study. Therefore, it can be concluded that the adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE and ODPPNE@MNP was a chemisorption process which involved complexation reaction between ODPPNE and  $\text{Hg}^{2+}$ .



**Figure 4.30:** Pseudo-second order model for the adsorption of  $Hg^{2+}$  on (a) SG-ODPPNE and (b) ODPPNE@MNP.

**Table 4.7:** Kinetic study parameter of (a) Pseudo-first order and (b) Pseudo-second order.

(a)		
Parameter	Pseudo-first order model	
	SG-ODPPNE	ODPPNE@MNP
$Q_{e,cal}$ (mg/g)	0.1653	1.6163
$Q_{e,exp}$ (mg/g)	0.1959	0.0791
$k_1$ (min <sup>-1</sup> )	0.0244	0.0182
$R^2$	0.9791	0.5275

(b)		
Parameter	Pseudo-second order model	
	SG-ODPPNE	ODPPNE@MNP
$Q_{e,cal}$ (mg/g)	0.1653	1.6163
$Q_{e,exp}$ (mg/g)	0.1929	1.5728
$k_2$ (min.g)/mg	0.1118	5.4850
$R^2$	0.9953	1.0000

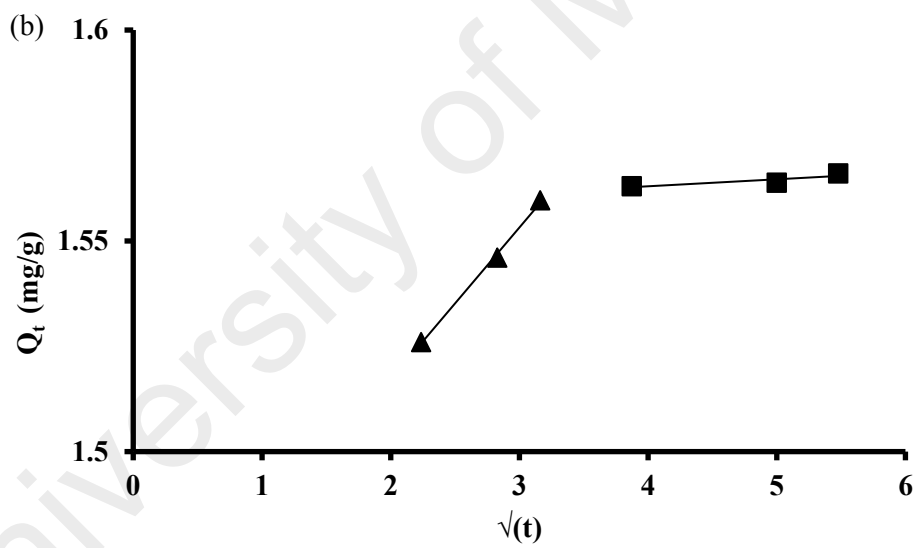
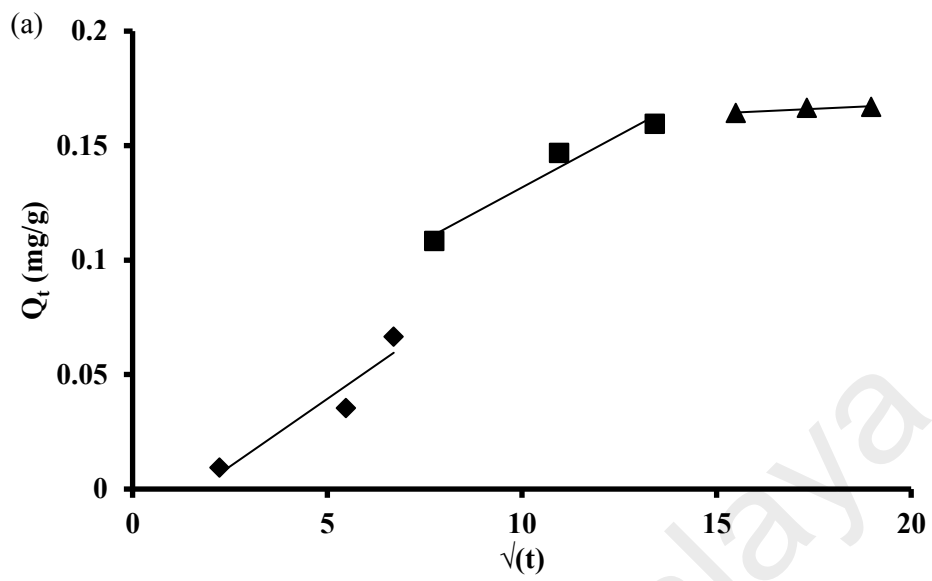
#### 4.6.2 Intra-particle diffusion and Boyd model

In general, solid-liquid adsorption process involves three stages (Wen et al., 2015). The first stage is the film diffusion of sorbate through the bulk phase to the surface of the adsorbent. The second step involves the gradual adsorption or intra-particle diffusion of sorbate. The final stage is related to the equilibrium stage. In this study, the Weber and Morris intra-particle diffusion model was used to predict the rate of determining step of the adsorption process (Wen et al., 2015). This model can be described by Equation 4.9:

$$Q_t = k_{id}\sqrt{t} + C_{id} \quad \text{Equation 4.9}$$

where  $k_{id}$  is the intra-particle diffusion rate constant, and  $C_{id}$  is a constant related to the thickness of the boundary layer. If the graph of  $Q_t$  versus  $\sqrt{t}$  is linear and pass through the origin, it indicates the intra-particle diffusion step is the only rate-determining step for entire adsorption process. Otherwise, multi-linear slope indicates that transportation stage and equilibrium stage may also control the adsorption process (Cheung et al., 2007).

According to Figure 4.31a, three linear portions were observed for  $Q_t$  versus  $\sqrt{t}$  curve of SG-ODPPNE. The first slope represents the mechanism where  $\text{Hg}^{2+}$  was transported from aqueous solution to the external surface of the adsorbent. The second slope denotes the gradual adsorption of  $\text{Hg}^{2+}$  onto SG-ODPPNE. The final part of the linear slope represents the equilibrium stage. At this final stage, diffusion rate was slow down due to the low concentration of  $\text{Hg}^{2+}$ . For the adsorption of  $\text{Hg}^{2+}$  by ODPPNE@MNP, the intra-particle diffusion curve (Figure 4.31b) showed two linear portions only. This observation also has been reported by other studies (Mahmoud, 2015; Nethaji et al., 2013). The first slope in this graph was corresponded to the external mass transport of  $\text{Hg}^{2+}$  to external surface of ODPPNE@MNP. The second portion of the slope represented the gradual adsorption of  $\text{Hg}^{2+}$  onto ODPPNE@MNP via intra-particle diffusion.



**Figure 4.31:** The intra-particle diffusion model for the adsorption of  $Hg^{2+}$  on (a) SG-ODPPNE and (b) ODPPNE@MNP.

The multi-linear slope obtained from this kinetic study indicated that the entire adsorption process of  $\text{Hg}^{2+}$  onto SG-ODPPNE and ODPPNE@MNP was controlled by two or more mechanisms involved. However, there was only one rate-determining step that exists in the particular time range as described by Cheung et al. (2007). Since the equilibrium stages are fast and it can consider as not the determining step (Karthikeyan et al., 2010). Therefore, the kinetic data were further analysed with Boyd model to distinguished either film diffusion or intra-particle diffusion stages was the main rate-determining step of this adsorption process, (Gusain et al., 2014). The Boyd model can be described by the Equation 4.10 (Kumar et al., 2005):

$$F = 1 - \left(\frac{6}{\pi^2}\right) \exp[-Bt] \quad \text{Equation 4.10}$$

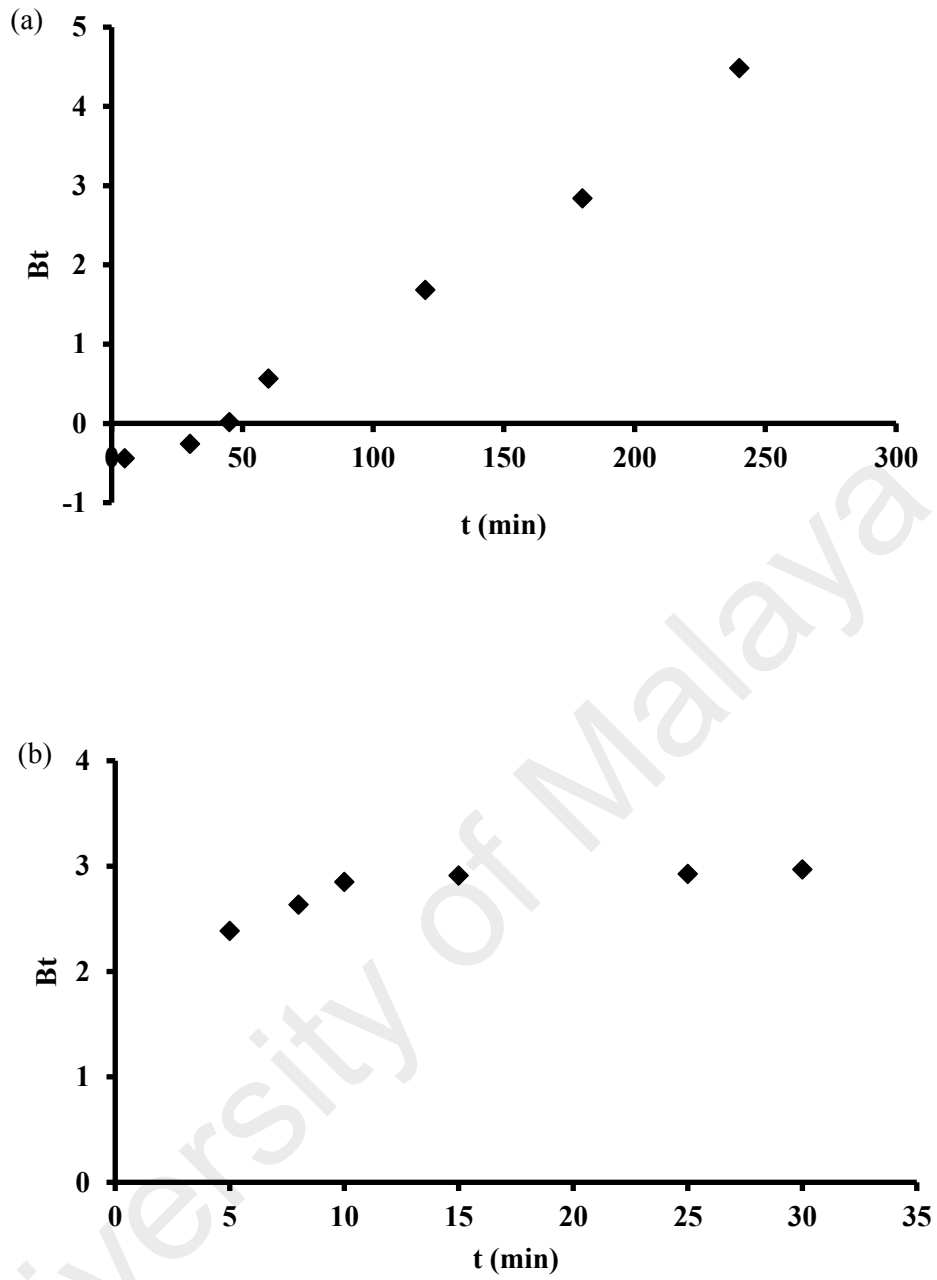
$$F = \frac{Q_t}{Q_e} \quad \text{Equation 4.11}$$

where  $F$  is the fraction of  $\text{Hg}^{2+}$  adsorbed at different time  $t$  and  $Bt$  is a mathematical function of  $F$ . By substituting Equation 4.10 into Equation 4.11, the kinetic expression can be written as:

$$Bt = -0.4977 - \ln(1 - F) \quad \text{Equation 4.12}$$

Therefore, the  $Bt$  value was calculated from Equation 4.12, and the Boyd plot was obtained by plotting the graph  $Bt$  against  $t$ . If the slope of this graph is a straight line that passes through the origin, the intraparticle diffusion stages were the rate-determining step otherwise the reaction was governed by film diffusion stage (Mohan and Singh, 2002). According to Boyd plot presented in Figure 4.32, the slope obtained was not pass through the origin for both SG-ODPPNE and ODPPNE@MNP. This result indicated that film diffusion stage was the rate-determining step in both adsorption processes.





**Figure 4.32:** Boyd plot for the adsorption of  $Hg^{2+}$  on (a) SG-ODPPNE and (b) ODPPNE@MNP.

## CHAPTER 5: CONCLUSIONS AND FUTURE WORK

### 5.1 Conclusions

In this study, the chalcone was chemically modified to obtain dithiocarbamate derivative (ODPPNE). The synthesized ODPPNE was incorporated into the sol-gel matrix to form SG-ODPPNE as the adsorbent. The result showed that the efficiency and selectivity of  $\text{Hg}^{2+}$  removal were largely enhanced by modifying the chalcone into dithiocarbamate derivative. The adsorption of  $\text{Hg}^{2+}$  was studied in batch mode under different experimental conditions. The result showed that the efficiency of the  $\text{Hg}^{2+}$  adsorption process depends on the size of adsorbent, pH of the solution, contact time, the concentration of  $\text{Hg}^{2+}$  and the SG-ODPPNE dosage. By applying the optimized condition, 80% of  $\text{Hg}^{2+}$  was successfully removed from aqueous solution by using SG-ODPPNE as the adsorbent. The removal efficiency of  $\text{Hg}^{2+}$  by SG-ODPPNE was not significantly influenced by the matrices effect of the real water samples.

ODPPNE incorporated silica gel was also coated on the surface of the magnetic nanoparticle (MNP) to demonstrate the application of this hybrid material, ODPPNE@MNP, in the pre-concentration of  $\text{Hg}^{2+}$  in water. By using this method of preparation, the synthesise route of ligand modified adsorbent was simplified, and the chemical usage was minimized. The ODPPNE@MNP was used as the adsorbent for the pre-concentration process to determine the trace amount of  $\text{Hg}^{2+}$  in the water sample. Under optimize condition, an effective method was developed by employing ODPPNE@MNP as the solid adsorbent for aqueous  $\text{Hg}^{2+}$  in D- $\mu$ SPE process. This D- $\mu$ SPE method with low method detection limit (4 ng/L), wide linearity (50-5000 ng/L), high pre-concentration factor (100) and good repeatability (4.5-6.5 %) was successfully demonstrated. The applicability of the developed method in the analysis of  $\text{Hg}^{2+}$  was evaluated by using three real water samples (drinking water, tap water, and surface water). The determination of  $\text{Hg}^{2+}$  in drinking water, tap water and surface water by the

developed method achieved the recovery efficiency of 90.1 to 99.0 % with the intraday and interday relative standard deviation of 0.7-8.8 % and 1.1-7.7 %, respectively.

The adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE and ODPPNE@MNP was found to obey the Langmuir model which suggested the presence of monolayer adsorption. The kinetics study showed that the adsorption of  $\text{Hg}^{2+}$  by SG-ODPPNE and ODPPNE@MNP was found to follow the pseudo-second-order model which implies the presence of chemisorption process. The mechanisms involved in adsorption process were film diffusion, intra-particle diffusion, and equilibrium stage. It was also found that the intra-particle diffusion step was not the only rate-determining step in this adsorption process. The kinetic data were further analysed by Boyd model to distinguish either film diffusion, or intra-particle diffusion was governing the overall adsorption reaction. The Boyd plot indicated that overall adsorption process of  $\text{Hg}^{2+}$  by SG-ODPPNE and ODPPNE@MNP was governed by the film diffusion stage.

## 5.2 Future works

In future, several research works, which are the extension of the current study, can be carried out. First, the natural product with metal capturing ability such as curcumin, quercetin, rutin, and morin can be incorporated into silica gel matrix to generate the effective adsorbent for metal ions. Secondly, some of these natural products with similar structure with chalcone such as curcumin can be further modified into dithiocarbamate derivative to produce the selective and effective adsorbent for  $\text{Hg}^{2+}$  removal and pre-concentration of trace  $\text{Hg}^{2+}$  in the water sample.

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## LIST OF PUBLICATIONS AND PAPERS PRESENTED

### 1. Publication

Khor, S. W., Lee, Y. K., Abas, M. R. B., & Tay, K. S. (2017). Application of chalcone-based dithiocarbamate derivative incorporated sol–gel for the removal of Hg (II) ion from water. *Journal of Sol-Gel Science and Technology*, 82(3), 834-845.

### 2. Poster presented

Khor Soo Wei, Mhd Radzi Bin Abas, Tay Kheng Soo, Chalcone Derived Ligand Incorporated Sol-gel for Mercury (II) Ion Removal in Water. Poster Presentation at UM#111-Chemistry Symposium. 3<sup>rd</sup> March 2016, Department of Chemistry, Faculty of Science, University of Malaya.

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